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COMPUTATIONS OF SOOT AND NO_X EMISSIONS FROM GAS TURBINE COMBUSTORS

FINAL REPORT

by

S. K. Srivatsa

Garrett Turbine Engine Company
P.O. Box 5217
Phoenix, Arizona 85010



Prepared for

National Aeronautics and Space Administration
NASA-Lewis Research Center
Cleveland, Ohio 44135

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FOREWORD

This document is the final report for work performed by the Garrett Turbine Engine Company under Contract NAS3-22542. This program, under the sponsorship of the National Aeronautics and Space Administration (NASA) Lewis Research Center accomplished the technical effort involved in the computations of emissions using a 3-D combustor computer program.

The assistance and guidance rendered by Dr. C. J. Marek, who was the NASA Project Manager for the program, is acknowledged.

John C. Clark

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CHAPTER I

INTRODUCTION

A. Background

Significant advances have been made in combustor analytical modeling over the past five years. The use of advanced numerics and kinetics has given the combustion engineer the ability to predict internal combustor flow field characteristics. These advanced tools, while still in their incipient stages, offer the potential of reducing the design and development time required for gas turbine combustors. At the same time, the analytical models increase the understanding of the phenomena affecting combustor performance and provide the basis for designing better combustors. The optimization of the design process will require a judicious blend of the emerging analytical tools (correlated and updated with test data) with the established empirical techniques.

Starting in 1970, Garrett has demonstrated a company commitment to develop combustor analytical design tools and utilize them in the everyday design and development process. In addition to extensive company-sponsored efforts, a significant contribution to this highly successful effort has been the USARTL Combustor Design Criteria Validation Program (Contract DAAJ02-75-C-0044).¹ Among the models developed under the above-mentioned USARTL program was the 3-D Combustor Performance Model, which is the basis for the present program. The present program entailed extending the capability of the model to predict pollutant emissions of nitrogen oxides and smoke.

B. Objectives

The objective of the program was to utilize and extend an existing three-dimensional(3-D) combustor performance computer program:¹

- o To predict pollutant emissions of smoke and NO_x;
- o To include the influence of soot, CO₂, and H₂O on radiation heat transfer; and
- o To extend the two-step hydrocarbon oxidation mechanism to a more detailed four-step scheme.

The program consisted of four tasks:

- o Task I - Formulation of the Method
- o Task II - Computer Coding
- o Task III - Computation of Test Cases
- o Task IV - Reporting and Documentation.

In Task I, a method was formulated to predict the emissions of soot and NO_x and to extend the radiation and hydrocarbon oxidation models.

In Task II, the method was incorporated into the 3-D combustor program in order to compute the emissions of NO_x and soot and the radiant transfer to the combustor walls.

In Task III, the resulting program was exercised for idle, cruise, and takeoff conditions of a JT8D combustor.

In Task IV, reports were submitted to NASA during and at the end of the program.

C. Summary

This report is the Final Report of the computations of emissions program, and presents the work carried out by Garrett under the program. Chapter II of the report includes a brief description of the original 3-D combustor performance computer program, provided for completeness. Chapters III and IV describe the soot emissions model and the influence of soot on radiation heat transfer. The NO_x emissions model and the hydrocarbon oxidation mechanism are described in Chapters V and VI, respectively. Chapter VII includes a description of the results of the computations. Chapter VIII contains concluding remarks. Chapters IX and X, respectively, contain a list of nomenclature and list of references, as cited in this report. Finally, Appendices A, B, C, and D contain, respectively, a description of the 3-D program, the program input, a list of FORTRAN variables and a listing of the new 3-D combustor performance program.

CHAPTER II

DESCRIPTION OF THE 3-D COMBUSTOR PERFORMANCE PROGRAM

The 3-D Combustor Performance Model Computer Program that forms the basis of the present work, is briefly described. For complete details, refer to Report No. USARTL-TR-55C.¹

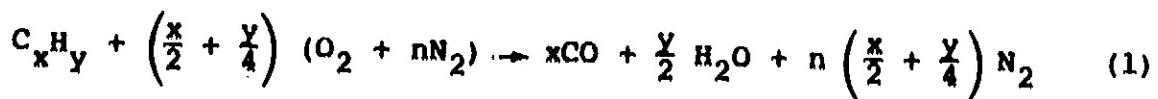
The 3-D program is general and is capable of predicting recirculating turbulent flow in gas-turbine combustion chambers. Reacting or nonreacting, swirling or nonswirling, diffusion and/or premixed flames, and gaseous and/or liquid fuel combustion can be handled by the program. The program computes the following variables in the region of interest:

- o Axial, radial, and swirl velocity components;
- o Pressure;
- o Enthalpy (temperature); in conjunction with the equation of state, the temperature determines the density variations in the flow field;
- o Turbulent kinetic energy and its dissipation rate;
- o Mass fractions of total fuel (mixture fraction), unburned fuel, oxygen, carbon monoxide, CO_2 and H_2O .
- o Three radiation flux vectors;
- o Spray trajectory, droplet size distribution, and evaporation rates.

The program employs the following physical models to solve the variables mentioned above:

- Turbulence - Two-equation ($k-\epsilon$) turbulence model to obtain turbulent kinetic energy and its dissipation rate.

- Chemistry - Two-step chemical reaction scheme:



- Chemical Reaction Rate - Fuel and CO consumption rates are assumed to be governed by either the time-averaged Arrhenius model or the turbulent eddy break-up model.
- Radiation - A six-flux model of radiation.

The transport equations for all dependent variables ϕ are written in the following general form:

$$\text{div} (\vec{\rho} \vec{u} \phi - \frac{\mu_t}{\sigma_\phi} \text{grad } \phi) = S_\phi \quad (3)$$

where ρ denotes the mixture density, \vec{u} the velocity vector, μ_t the effective or turbulent viscosity, σ_ϕ the effective Prandtl/Schmidt number, S_ϕ the sources of ϕ ; i.e., S_ϕ includes the creation/destruction of ϕ plus other quantities that do not fall under the convective and diffusive terms. Table E-1 in Appendix E includes a list of the dependent variables ϕ and their source terms.

An iterative, general finite-difference solution procedure suitable for 3-D elliptic flows in complex geometries is used to solve the above system of coupled, nonlinear partial-differential equations. The solution procedure involves discretizing the differential equations by integration over elementary finite-difference control volumes surrounding grid nodes that are nonuniformly spaced over the flow field.

CHAPTER III

SOOT EMISSIONS

In this chapter, soot formation and oxidation in combustion chambers are discussed. A general background on soot emissions is provided first. Details of the soot formation and oxidation mechanisms reported in the literature are discussed next. Quasi-global expressions for soot formation and oxidation are described. A description of the influence of turbulence on soot formation and oxidation is included. The approach adopted in the present work is described next. This approach considers the influence of turbulent fluctuations on soot formation and oxidation rates.

A. Background

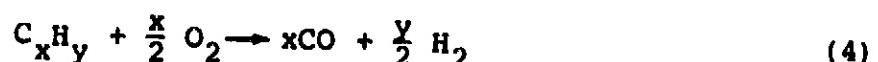
The particulate emission of primary concern in the combustion of hydrocarbon fuels is soot, which is evident in the form of exhaust smoke. The emission of smoke from gas turbine engines is responsible for the following problems:

- o Higher liner temperatures due to increased radiative heat transfer
- o Impingement of carbon on metal surfaces, resulting in erosion and reduced equipment lifetimes
- o Distortion of fuel spray distribution due to carbon deposits, leading to hot spots
- o Visible pollution and associated health hazards
- o Tactical problems in military applications.

Recently, attention is being directed toward the combustion of alternate fuels derived from coal liquids and shale oil. Since the use of these fuels results in significant increases in smoke production, a better understanding of the physical and chemical processes governing soot production is needed.

The processes governing the formation and subsequent oxidation of soot are of a particularly complex nature; and, as such, quantitative models of soot production have yet to be developed. Soot is not an equilibrium product of combustion; and, therefore, its formation is influenced as much by the physical processes of atomization, evaporation, and fuel/air mixing as by reaction kinetics. Soot is generally produced anywhere within the combustor where fuel/air mixing is inadequate, resulting in oxygen-deficient, high-temperature zones.

For the pressures and temperatures normally prevalent in gas turbine combustors, equilibrium calculations indicate that solid carbon appears when there is insufficient oxygen to oxidize the hydrocarbon to CO and H₂ according to the relation:



That is, the carbon-oxygen mass ratio for incipient soot formation is 12:16; or, alternatively, the atomic C-O ratio is unity. However, since soot formation is essentially a nonequilibrium phenomenon, experimentally, soot is observed at C-O ratios (a) much less than unity at low temperatures (<2000°K); and (b) greater than unity at higher temperatures.²

Smoke levels are primarily dependent on the following:

- Air/fuel mixing
- Temperature

- o Equivalence ratio
- o Residence time of air/fuel mixture
- o Pressure
- o Fuel composition.

These factors influence both the formation and subsequent oxidation of soot and are dependent on engine operating conditions, details of the combustor internal flow field, fuel droplet characteristics, etc.

B. Mechanism of Soot Formation

Detailed discussions of the many mechanisms proposed to explain the chemical and physical processes governing soot formation are available in reviews by Haynes and Wagner,³ Street and Thomas,⁴ Palmer and Culliss,⁵ Gaydon and Wolfhard,⁶ Homann,⁷ and Bittner and Howard.⁸ Based on the information available, the process of soot formation can be considered to occur in three distinct stages:

- o Soot-particle nucleation
- o Agglomeration and surface growth
- o Coagulation.

The first stage of soot-particle nucleation is the most difficult to describe, and there is considerable controversy regarding this. The two most viable hypotheses advanced to date are based on ionic and radical polymerizations.

The theory of ionic polymerizations contends that positive ions serve as the nuclei for carbon formation in flames.^{9,10} Based on this theory, Howard¹¹ showed that the chain structure of carbon particles and the uniform size of the spherical chain units can be explained. Experiments by Howard and coworkers¹² have demonstrated this theory to be feasible.

The theory of radical polymerizations considers that fuel pyrolysis gives rise to elementary unsaturated hydrocarbon molecules (e.g., acetylene), which polymerize via radical chain mechanisms.¹³ Thus, soot formation is mainly due to gas-phase reactions and is not directly due to liquid pyrolysis. This mechanism has also been proposed by Porter¹⁴ as the "Acetylene Mechanism of Soot Formation." Mass spectrometric measurements of species such as C₂H₂, C₄H₂, C₆H₂, C₈H₂, etc. obtained in flames¹³ and shock-tube investigations¹⁵ tend to support the radical polymerization theory. However, since a continuation of such a chain-reaction sequence cannot lead directly to carbon particles,¹³ chain-branched and ring-closure, followed by agglomeration and dehydrogenation,^{5,16} must take place at some point prior to soot formation.

In the second stage of soot formation (agglomeration and surface growth), spherical units of carbon particles (about 250 \AA in size) are formed by agglomeration and surface growth of the nuclei formed in the first stage.

Finally, in the third stage, the coagulation of the spherical carbon particles leads to the characteristic chain-like structure of soot. Dehydrogenation continues through both the second and third stages.

Jensen¹⁷ proposed a model that treats the various steps of soot formation in some detail. The model agreed qualitatively with experimental observations in a methane flame. However, due to the complexities associated with the detailed reaction mechanism, and uncertainties in the rate constants, the Jensen model is not suitable for gas-turbine combustor analysis.

Since quantitative description of the soot formation mechanism applicable to general conditions are not available, quasi-global models as described later in this chapter are required for the computation of soot emissions.

C. Mechanism of Soot Oxidation

Analytical and empirical literature on soot oxidation is extensive. However, because of the complexities involved, considerable controversy exists concerning the mechanism of soot oxidation, and many basic questions have yet to be answered. Consideration of soot oxidation processes is important, since soot concentration in the exhaust gases is determined by both the relative rates of soot formation and oxidation in the flame zone and the surface oxidation rate in hot post-flame gases. In this Chapter, a limited review of the soot oxidation models and a rationale for selecting the model used in the present work is presented.

Many studies have been reported on the derivation of mass-transfer (oxidation) rates for single-carbon particles in a hot-oxidizing ambient environment. Recently, studies on the theory of burning carbon particles were made by Avedesian and Davidson,¹⁹ Ubhayakar and Williams,²⁰ and Libby and Blake.²¹ These studies involved simplifying assumptions with regard to the fluid-mechanical and chemical aspects of the problem. Amundson and coworkers^{22,23,24} presented a model for the diffusion and chemical reaction in the boundary layer surrounding a burning spherical carbon particle in a quiescent gas. The model accounted for radiation and for the homogeneous combustion of CO in the gas phase and the heterogeneous surface reactions of carbon with oxygen and CO₂. The model predicted the distribution of the product concentrations around the particle.

High-temperature soot oxidation rates were measured by Lee, et al.,²⁵ in the tail of propane diffusion flames. The soot oxidation rate (R_{ox}) per unit particle surface area was determined as a function of temperature and partial pressure of oxygen, as follows:

$$R_{ox} = 1.09 \times 10^5 P_{O_2} T^{-1/2} \exp(-19725/T) \text{ kg/m}^2\text{s} \quad (5)$$

The measurements were conducted in the temperature range of 1310° to 1670°K. Tesner and Tsibulevsky²⁶ also measured flame-soot oxidation rates over the temperature range of 1400° to 2000°K and found good agreement with the above expression. Feugier²⁷ measured soot concentrations in fuel-rich ethane-oxygen flames and deduced a kinetic expression for the oxidation of soot particles similar to the one by Lee, et al.²⁵

Based on the measurements of the surface oxidation rates of pyrolytic graphite and the similarity of small soot particles to pyrolytic graphite at the microscopic level, Radcliffe and Appleton²⁸ proposed that the soot oxidation rate should exhibit a local maximum (for a fixed O_2 partial pressure and increasing temperature) at temperatures from 2000° to 2500°K for O_2 partial pressure in the range of 0.05 to 1.0 atmosphere. Additionally, the soot oxidation rate should exhibit a first-order dependence on the O_2 partial pressure for $P_{O_2} \leq 0.01$ atmosphere and, at higher pressures, should asymptotically approach a zero-order dependence. The semi-empirical formula for soot oxidation rate proposed by Nagle and Strickland-Constable²⁹ (discussed later in this chapter) confirms this behavior. The model of Lee, et al., can be derived from that of Nagle and Strickland-Constable for fuel-lean conditions. Therefore, the more general model of Nagle and Strickland-Constable has been adopted in the present work.

D. Quasi-global Models of Soot Formation and Oxidation

Since the elementary steps in the formation and oxidation of soot are not totally understood, the present program uses quasi-global models that characterize soot production occurring via a few overall steps. Such models have been successful in predicting soot production.³² In this section, some of the quasi-global models reported in the literature are described.

The quasi-global models do not predict the size of soot particles. With the current state-of-the-art, it is not possible to predict the size of formation of the soot particles in any practical flow situation. Therefore, it is assumed that particles are produced at a known size. It may also be assumed that particles are produced in accordance with a specified size distribution (e.g., Gaussian).

Tesner, et al.,³³ proposed a soot production model which grouped the complex processes of pyrolysis, nuclei formation, and soot formation into three rate-limited subglobal steps that include (a) a pyrolysis rate first order in hydrocarbon concentration, (b) a chain branching and chain termination rate for soot nuclei formation rate, and (c) a soot formation rate.

Pyrolysis:

$$n_o = a_o C_{fu} \exp (-E/RT) \text{ (part./m}^3\text{.s)} \quad (6)$$

Nuclei Formation:

$$R_{n,f} = n_o + (f-g)n - g_o Nn \text{ (part./m}^3\text{.s)} \quad (7)$$

Soot Formation:

$$R_{S,f} = m_p (a - bN) n \text{ (kg/m}^3\text{.s)} \quad (8)$$

where a_0 , E , f , g , g_0 , a , and b are constants for a given fuel; n_0 is the rate of spontaneous formation of nuclei; n is the nucleus concentration; N is concentration of soot particles; m_p is the mass of a soot particle; and $R_{n,f}$ and $R_{s,f}$ are the nuclei and soot formation rates, respectively.

Khan and Greeves³⁴ proposed a single-step global expression as a function of the partial pressure of unburned hydrocarbons (P_{HC}), the unburned equivalence ratio (ϕ_u), and the temperature (T):

$$R_{s,f} = 0.468 P_{HC} \phi_u^3 \exp(-40,000/RT) \text{ gm/cm}^3\text{s} \quad (9)$$

This model is overly sensitive to the equivalence ratio and, therefore, is not considered in the present work. In addition, in both the above models, soot oxidation rates are not considered.

Edelman, et al.,³² consider both soot formation (R_f) and soot oxidation (R_{ox}) and express the net soot formation rate as:

$$\frac{dC_s}{dt} = R_f - A_t R_{ox} \quad (10)$$

where A_t equals total surface area available for oxidation. This model is more general and, therefore, it has been adopted in the present work with appropriate modifications to account for turbulence effects as described next in Section E. The formation step is expressed by a modified Arrhenius type of relation:

$$R_f = AT^\alpha C_{HC}^a C_{O_2}^b \exp(-E/RT) \text{ gm/cm}^3\text{s} \quad (11)$$

where C_{O_2} , C_{HC} equal the concentration of unburned oxygen and hydrocarbon (gm/cm^3) and where A , α , a , b , E are model constants.

For the oxidation step, Edelman, et al.,³² adopt the semi-empirical formula of Nagle and Strickland-Constable²⁹ for pyrolytic graphite oxidation; this formula is nonlinear and non-Arrhenius in P_{O_2} and T:

$$A_t R_{OX} = 12 \left[\left(\frac{K_A P_{O_2}}{1 + K_Z P_{O_2}} \right) \psi + K_B P_{O_2} (1 - \psi) \right] A_t \text{ gm/s} \quad (12)$$

where:

$$\psi = [1 + K_T / (K_B P_{O_2})]^{-1} \quad (13)$$

$$K_A = 20 \exp(-30,000/RT) \text{ gm/cm}^2 \cdot \text{s atm} \quad (14)$$

$$K_B = 4.46 \times 10^{-3} \exp(-15,200/RT) \text{ gm/cm}^2 \cdot \text{s. atm.} \quad (15)$$

$$K_T = 1.51 \times 10^5 \exp(-97,000/RT) \text{ gm/cm}^2 \cdot \text{s} \quad (16)$$

$$K_Z = 21.3 \exp(4100/RT) \text{ atm}^{-1} \quad (17)$$

Shock-tube measurement¹⁸ of soot oxidation rates qualitatively confirms the features of the above formula. With these expressions for soot formation and oxidation and assuming a single-soot particle size of 250Å, Edelman, et al.³² obtained close agreement of the predicted soot concentration (mg/l) with the experimental data in a jet-stirred reactor. Thus, these expressions assume perfect mixing. In a gas-turbine combustor, however, regions of unmixed species will exist, and turbulence will also influence the soot production rates. As such, modifications to these expressions are required before they can be used for a general 3-D turbulent flow.

E. Influence of Turbulence on Soot Formation and Oxidation

Magnussen, et al.,^{35,36} have proposed a model that accounts for the influence of turbulent fluctuations on soot production rates.

In turbulent flows, chemical reaction occurs when reactants at a sufficiently high temperature are mixed at the molecular level. The molecular mixing process is analogous to the dissipation (ϵ) of turbulent kinetic energy k and is associated with the smallest scales of turbulence. Dissipation is concentrated in highly strained regions of the fluid occupied by fine structures with characteristic dimensions of the same magnitude as the Kolmogorov microscale. The reactants are molecularly mixed in these fine structures, where reaction occurs. Magnusson, et al., proposed the following expressions for the mass fraction contained in the fine structures:

$$\gamma^* = 9.7 \cdot (R_t)^{-3/4} \quad (18)$$

where R_t is the turbulence Reynolds number, and the rate of transfer of mass per unit mass between the fine structures and the surrounding fluid is:

$$\dot{m} = 23.6 \cdot (R_t)^{-1/4} \frac{\epsilon}{k} \quad (19)$$

The rate of reaction is proportional to $\dot{m}X$ where X is the fraction of small-structure eddies that are sufficiently heated to react. It is assumed that X is proportional to the ratio of local reacted fuel concentration and total fuel concentration. Thus, the rate of reaction is:

$$R_{fu} = 23.6 (R_t)^{-1/4} \frac{\epsilon}{k} X C_{min} \text{ (kg/m}^3 \text{ s)} \quad (20)$$

where

$$X = \frac{C_{pr}/(1+i)}{C_{pr}/(1+i) + C_{fu}} \quad (21)$$

C_{\min} is the smaller of C_{fu} and (C_{O_2}/i) and i is the stoichiometric oxygen requirement. The temperature T^* of the reacting fine structures is T above the local time-mean temperature T :

$$T^* = T + \Delta T = T + \frac{\Delta H}{\rho C_p} \frac{C_{\min}}{C_p} \quad (22)$$

where

ΔH_R = the heat of reaction

C_p = the specific heat

and the surrounding temperature T^0 is

$$T^0 = T - \Delta T \frac{\gamma^* X}{1 - \gamma^* X} \quad (23)$$

Using Equations (6) and (8), the mean rates of nuclei and soot formation are then expressed as:

$$\begin{aligned} R_{n,f} &= n_{O,T^*} \gamma^* X \frac{\rho/\rho^*}{\rho/\rho^*} + n_{O,T^0} (1 - \gamma^* X) \frac{\rho/\rho^0}{\rho/\rho^0} \\ &+ (f - g)_n - g_O n^* N^* \gamma^* X \frac{\rho/\rho^*}{\rho/\rho^*} \\ &- g_O n^0 N^0 (1 - \gamma^* X) \frac{\rho/\rho^0}{\rho/\rho^0} \end{aligned} \quad (24)$$

and

$$\begin{aligned} R_{s,f} &= m_p (a - b N^*) n^* \gamma^* X \frac{\rho/\rho^*}{\rho/\rho^*} + m_p (a - b N^0) n^0 \\ &(1 - \gamma^* X) \frac{\rho/\rho^0}{\rho/\rho^0} \end{aligned}$$

Finally, the mean rates of nuclei and soot oxidation are expressed as:

$$R_{n,c} = R_{fu} n/C_{fu} \text{ (part/m}^3 \text{ s)} \quad (26)$$

$$R_{s,c} = R_{fu} C_s/C_{fu} \text{ (kg/m}^3 \text{ s)} \quad (27)$$

Magnussen, et al., used this model to compute the soot concentrations in a turbulent C₂H₂ diffusion flame. By adjusting the particle diameter (entered as m_p, the particle mass in Equation (8), and the constant a₀ in Equation (6), good agreement with experimental measurements was obtained.

F. Present Approach

The model adopted for computing soot emissions in the present program is described in the following paragraphs.

The computation of soot emissions involves the solution of two additional transport equations for the concentrations of (a) nuclei and (b) soot. These two equations are of the same general form as Equation (3) solved by the 3-D Combustor Program. To complete the equation specifications, the source terms and the Schmidt numbers for these two variables are as follows:

The source term in the nuclei concentration equation is expressed as

$$R_{n,f} = R_{n,c} \quad (28)$$

where R_{n,f} is given by the smaller of the two values from Equations (7) and (24); R_{n,c} is given by Equation (26). Thus, these expressions amount to the use of the turbulent reaction rates, subject to the limitation that they cannot be greater than the rates under well-stirred reactor conditions.

The source term in the soot concentration equation is similarly expressed as

$$R_{s,f} = R_{s,c} \quad (29)$$

where $R_{s,f}$ is given by the smaller of the two values from Equations (11) and (25); $R_{s,c}$ is given by the smaller of the two values from Equations (12) and (27).

The turbulent Schmidt numbers σ_s and σ_n for soot and nuclei concentrations are assumed the same as for gaseous fuel (i.e., 0.9).

In the computations carried out in the present work, a distribution of two particle sizes was considered: a small size of 0.025 microns as resulting from nucleation and a large size of one micron as resulting from fuel droplet pyrolysis and char formation. The relative rates of formation of these two sizes of particles was assumed to be 90-10 percent. The consideration of two particle sizes leads to the solution of a transport equation of the same general form as Equation (1) for the concentration of the particles in each size. The extension to other sizes is straightforward but involves extra computational effort, since an additional equation must be solved for each additional size considered. In view of the several assumptions inherent in the analysis of soot production, the consideration of other size groups is not necessary at this stage.

The calculation of soot formation is bypassed if the temperature is less than a value below which the formation rates are negligible. It is also bypassed if the local carbon-to-oxygen ratio is less than the incipient soot formation limit. Both of these limits of temperature and carbon-to-oxygen ratio are inputs to the calculation procedure and can be varied at will.

A lack of data exists for computing particle coagulation. Attempts to model particle growth in flames^{38,39} have had little success. No definite conclusions could be reached with these models. A lack of understanding of the phenomena and the absence of data reduces coagulation computations to mere speculation. Therefore, this phenomenon is not addressed in the present work.

CHAPTER IV

RADIATION HEAT TRANSFER

A. Background

The contributors to radiation in combustors fueled by hydrocarbons are soot, CO_2 , H_2O (vapor), inorganic particles, CO, unburned fuel (C_xH_y), NO_x , and SO_2 . Only the influence of soot, CO_2 , and H_2O (vapor) are considered in the present work. Although CO and unburned C_xH_y contribute to emission and attenuation of radiation within flames, these contributions are localized and of secondary importance when total heat-transfer rates are considered. The contributions of NO_x and SO_2 can be neglected because of their low concentrations.

The determination of the influence of soot on radiant heat transfer reduces to two factors: (a) soot distribution in the flame and (b) the radiative properties of gas-soot mixtures. The first was discussed in the preceding chapter. Radiative properties of gas-soot mixtures are discussed in this chapter.

The radiation properties of the principal radiating species including soot, CO_2 , and H_2O , are significantly nongrey. Consequently, the calculation of the radiation properties is a time-consuming task. However, spectral calculations are unnecessary since approximate calculations (by means of curve fits) are more convenient and provide good accuracy.⁴⁰

An approximate curve-fit procedure for the calculation of radiation properties is employed in the present work.

B. Radiation Properties of Soot, CO₂, and H₂O Mixtures

The absorptivity (α) of the gas-soot mixture includes the soot absorptivity, the absorptivity due to the absorption bands of CO₂ and H₂O, and corrections for the overlapping of bands.

Utilizing the spectral data,⁴¹ the gas absorptivity is calculated by taking a summation over the absorption bands of CO₂ and H₂O. In the approximate calculation method adopted here, a simpler approach is used. The gas absorptivity α_g is written as⁴²

$$\alpha_g = \epsilon_g (T/T_s)^{(0.6-0.2\zeta)} \quad (30)$$

where $\zeta = P_w/(P_w + P_c)$ (31)

ϵ_g = gas emissivity at a temperature T and path length
 LT_s/T

T, T_s = gas and blackbody source temperatures, respectively

P_c, P_w = partial pressures of CO₂ and H₂O

ϵ_g is given by

$$\epsilon_g = \epsilon_c + \epsilon_w - \Delta\epsilon_{cw} \quad (32)$$

where ϵ_c , ϵ_w = emissivities of CO₂ and H₂O

$\Delta\epsilon_{cw}$ = overlap correction factor

ϵ_g can be computed using a temperature adjusted version of Leckner's⁴³ approximate overlap correction $\Delta\epsilon_{cw}$, and approximating

ϵ_c and ϵ_w by curve fits of P_c , P_w , P_L , and T to spectral calculations. In the range of interest in gas-turbine combustors, such calculations agree to within 5 percent of the spectral calculations and the experimental results.

The temperature adjusted version of Leckner's⁴³ overlap correction $\Delta\epsilon_{cw}$, which accounts for the 2.7 and 15 μm overlapped regions for mixtures of CO_2 and H_2O , is⁴⁰

$$\Delta\epsilon_{cw} = \frac{\zeta}{(10.7 + 101\zeta)} - \frac{10.4}{111.7}$$

$$\{\log_{10}[101.3(p_c + p_w)L]\}^{2.76} F(T)$$

for $(p_c + p_w)L \geq 0.1 \text{ atm-m}$

$$= 0 \text{ for } (p_c + p_w)L < 0.1 \text{ atm-m}$$

where ζ is defined by Equation (31) and $F(T)$ is given by:

$$F(T) = -1.0204 \times 10^{-6}T^2 + 2.2449$$

$$10^{-3}T - 0.23469 \quad (T \text{ in degrees K})$$

The coefficients involved in the curve fits of ϵ_c and ϵ_w to P_c , P_w , P_L and T are given in Reference 40 and are not reproduced here.

The absorptivity (α) of the gas-soot mixture is given by

$$\alpha = \alpha_s + \alpha_g - \alpha_s \alpha_g \quad (33)$$

With α_g obtained above, it remains to determine α_s , the soot absorptivity. This is obtained by the method of Felske and Tien.⁴⁴ This method assumes that the complex refractive index of soot is independent of wavelength and that the soot particle diameter is small compared to the wavelength of radiation, so that scattering is negligible. The spectrally integrated absorptivity α_s can then be written in a closed-form expression to determine α_s .

By using the radiative property calculations of the type described above, Sarofim⁴⁵ indicated that radiation calculations can be made with fair confidence, and that the major source of uncertainty in such calculations is soot concentration, rather than gas-radiation properties.

C. Present Approach

The six-flux radiation model incorporated into the 3-D Combustor Performance Computer Program was used in computing radiation heat transfer in the present work.

This model is based on the Schuster-Hamaker approximation.⁴⁶ It should be noted that, as pointed out by Siddall,⁴⁷ other flux model approximations such as Milne-Eddington and Schuster-Schwarzschild can be represented by the same form of flux equations with constants being different.

The differential equations describing the variations of the fluxes along six directions can be reduced to the following three second-order ordinary differential equations:

$$\frac{d}{dx} \left(\frac{1}{a+S} \frac{dR^x}{dx} \right) = a(R^x - E) + \frac{S}{3} (2R^x - R^r - R^z) \quad (34)$$

$$\frac{1}{r} \frac{d}{dr} \left(\frac{r}{a+S+1} \frac{dR^r}{dr} \right) = a(R^r - E) + \frac{S}{3} (2R^r - R^x - R^z) \quad (35)$$

$$\frac{1}{r} \frac{d}{d\theta} \left(\frac{1}{a+S} \frac{dR^z}{d\theta} \right) = a(R^z - E) + \frac{S}{3} (2R^z - R^x - R^r) \quad (36)$$

Where the composite-fluxes R^x , R^r and R^z are defined as

$$R^x = \frac{1}{2} (I_{x+} + I_{x-}) \quad (37)$$

$$R^r = \frac{1}{2} (I_{r+} + I_{r-}) \quad (38)$$

$$R^z = \frac{1}{2} (I_{\theta+} + I_{\theta-}) \quad (39)$$

where I_{x+} , I_{r+} , and $I_{\theta+}$ are the fluxes along the positive directions of axial, radial, and circumferential directions, respectively; I_{x-} , I_{r-} , and $I_{\theta-}$ are the corresponding fluxes along the negative directions.

a = Absorption coefficient, defined as radiation absorbed per unit length

s = Scattering coefficient, defined as radiation scattered per unit length

E = Black body emissive power = σT^4

σ = The Stefan-Boltzman constant

The absorption coefficient a is related to the absorptivity α of the gas-soot mixture and the path length L by:

$$a = -\frac{1}{L} \ln (1-\alpha)$$

In the original version of the 3-D combustor program,¹ the radiation properties were assigned constant values. For the present work, the absorption coefficient was computed locally as a function of gas and soot concentrations by the approximate procedure described above.

The scattering due to soot particles, which are generally of diameters below one micron, is negligible. In the present work, a uniform value of 0.01 m^{-1} was assumed for the scattering coefficient.

CHAPTER V

NITROGEN-OXIDE EMISSIONS

A. Background

Nitrogen oxides (NO_x) are formed during any combustion process involving air within the normal range of adiabatic flame temperatures and comprise nitric oxide (NO), nitrogen dioxide (NO_2), and small amounts of nitrous oxide (N_2O). For turbopropulsion engines, the NO_x emissions consist mostly of NO, particularly at high power conditions, where maximum NO_x concentrations are encountered. However, the contribution of NO to total NO_x emissions decreases at low power points. The NO_x is conventionally expressed in mass units of NO_2 , to which the NO would eventually react in the atmosphere.

The major influences contributing to the formation of NO_x are (a) high flame temperature, (b) the availability of oxygen as provided by excess air, and (c) sufficient residence time for the reactions to take place. Formation of NO is preceded by the generation of N and O atoms. Nitrogen (N) atoms are formed by the dissociation of nitrogen (N_2) in the air at high temperatures, and can also be a product of hydrocarbon reactions if the fuel contains nitrogen. Oxygen (O) atoms are formed primarily from oxygen (O_2) dissociation. Thus, NO forms both in the reaction zone and in the post-reaction, high-temperature gases. A super-equilibrium of O, N, and OH concentrations (i.e., concentrations exceeding equilibrium levels) in the reaction zone leads to NO formation in this zone (often termed as 'prompt NO'). Nitric oxide formation is controlled by rate-limited reactions, and its calculation is dependent on a knowledge of other radical concentrations.

The conservation equations for the radical and NO_x concentrations form a set of coupled 'stiff' nonlinear differential equations and their solution requires special integration procedures. One such procedure, which has been developed by Pratt and Wormeck,⁴⁸ is described next. This procedure has been incorporated into the 3-D combustor program and has been used to compute the NO_x emissions in the present work.

B. The Chemical Kinetics Program

The conservation equations for the species involved in NO_x production form a set of 'stiff' equations. Pratt and Wormeck⁴⁸ have developed a numerically efficient computer program (CREK) for the solution of such a set of equations. The CREK procedure is briefly described in the following paragraphs.

The species and energy conservation equations for a node, P, are expressed in the following standard finite-difference form:

$$A_P \phi_P = A_E \phi_E + A_W \phi_W + A_N \phi_N + A_S \phi_S + A_H \phi_H + A_L \phi_L + S_\phi \quad (40)$$

where A is the finite-difference coefficient containing the convective and diffusive fluxes; ϕ is the dependent variable (species concentration, enthalpy); S_ϕ is the source of ϕ ; subscripts E, W, N, S, H, and L refer to the six neighboring nodes of P.

The CREK program is used to solve the above finite-difference equation. The solution is simultaneous for all the species concentrations and temperature at a given node P; and proceeds node-by-node until all of the nodes in the flow field are covered. The solution procedure involves the derivation of a set of Newton-Raphson correction equations for the species concentrations and temperature. These equations are solved iteratively by pivoted Gaussian elimination.

The program requires as input the following information:

- (1) Previous solution or estimate of ϕ_p and temperature at node P;
- (2) Pressure at node P;
- (3) Finite-difference coefficients $A_p A_E, A_W, A_N, A_S, A_H$, and A_L , as calculated in the 3-D combustor program;
- (4) $\phi_p^* = (A_E \phi_E + A_W \phi_W + A_N \phi_N + A_S \phi_S + A_H \phi_H + A_L \phi_L) / A_p$
- (5) Enthalpy source coefficients Q, where, enthalpy source = $-(Q_0 + Q_1 T + Q_2 T^2 + Q_3 T^3 + Q_4 T^4)$.

The outputs from the program are

- (1) Mole numbers of all chemical species;
- (2) Temperature at node P;
- (3) Density at node P.

Further details of the CREK procedure are contained in Reference 48.

C. Present Approach

The number of species considered in the present program is 14: $C_x H_y$, $C_x H_{y-2}$, CO, CO_2 , H, H_2 , O, O_2 , OH, H_2O , N, N_2 , NO, NO_2 . Here, $C_x H_{y-2}$ denotes the intermediate hydrocarbon as explained in Chapter VI. Each of these species concentrations is governed by a transport equation of the same general form as Equation (3). To complete the equation specifications, the source terms and the

Schmidt numbers for these variables have to be determined. The turbulent Schmidt numbers, σ_ϕ , for all the species are assumed to be 0.9. The computation of the source terms, S_ϕ , is based on the reaction mechanism given in Table I. The calculation involved for each reaction is illustrated below with reference to the reaction $A+B \rightleftharpoons C+D$.

The laminar Arrhenius rate

$$R_L = \rho^2 M_A M_B A T^b \exp(-E/RT) \quad (41)$$

where M_A and M_B are the mass fractions of A and B.

The turbulent eddy-break-up rate for species A is

$$R_T = C_R \rho M_{MIN} \epsilon / k \quad (42)$$

where C_R is a constant, ρ is the density, and where M_{MIN} is the smaller of M_A and M_B/i , i being the mass of B required per unit mass of A in this reaction. The rate of production/consumption of A is

$$R = \text{smaller of } R_L \text{ and } R_T$$

The backward rate is treated similarly. All of the reactions listed in Table I and the global reactions discussed in Chapter VI are treated in this way, and the sources due to chemical reaction in the conservation equations for the species are obtained by summing the rates due to all of these reactions. The resulting species equations are solved by the computer program CREK described above. This determines the concentrations of all of the species. Modifications have been made to the CREK program in the present work in order to treat the global reactions and the eddy-break-up rates for the reaction steps.

TABLE I. NO_x REACTION MECHANISM.

$$K_f = 10^x T^b \exp(-E/RT)$$

Reaction					x	b	E/R (°K)	
1. H	H	M	=	H ₂	M	12.300	-1.000	0.0
2. O	O	M	=	O ₂	M	11.000	-1.000	0.0
3. H	OH	M	=	H ₂ O	M	13.850	-1.000	0.0
4. H	O ₂		=	OH	O	11.350	0.0	8400.000
5. O	H ₂		=	OH	H	10.240	0.0	4730.000
6. H	H ₂ O		=	OH	H ₂	10.920	0.0	10050.000
7. O	H ₂ O		=	OH	OH	10.760	0.0	9000.000
8. N ₂	O		=	NO	N	9.000	0.0	25000.000
9. N	O ₂		=	NO	O	5.000	1.000	2000.000
10. N	OH		=	NO	H	9.000	0.0	0.0
11. N ₂	O ₂		=	N	NO ₂	11.431	-1.000	60600.000
12. NO	NO		=	N	NO ₂	7.000	0.0	0.0
13. NO	O ₂		=	NO ₂	O	9.000	0.0	22900.000
14. H	NO ₂		=	NO	OH	10.477	0.0	0.0

NOTE: Values are in SI units.

Reverse rate constant obtained from forward rate constant equilibrium constant.

The consideration of a detailed mechanism as shown in Table I is computationally time consuming when considering a three-dimensional problem. The chemical kinetics solution involves a point-by-point procedure, proceeding from one grid node at a time to the next until all nodes are covered. At any stage, the species concentrations at the nodes that are yet to be solved also influence the concentrations at the node currently being solved. Therefore, the concentrations at the nodes not yet solved, have to be estimated or are known from the previous iteration. Due to this explicit (as opposed to implicit) nature of the coupling between values at neighboring nodes, the solution has to be repeated several times in order to achieve convergence with attendant large computer times.

In order to reduce computer times, the partial equilibrium assumption has been used in some work reported in the literature. This involves the assumption that the following four bimolecular reactions are equilibrated:



This assumption reduces the number of kinetic equations to be solved. The equilibration of these reactions in several premixed combustion systems is supported by the studies of References 49-51. Their equilibration in a CH₄-Air diffusion flame was demonstrated by Mitchell, et al.²⁵ They showed that these reactions are in equilibrium over a range of equivalence ratios from little less than unity up to approximately 2.5 for a flame at atmospheric pressure with the reactants initially at about 300°K. The equilibration of these reactions at different conditions, more closely resembling those in gas-turbine combustors, has not been demonstrated. Thus,

the partial equilibrium assumption may not be valid in all regions of a gas-turbine combustor; hence, it has not been used in the present work. The present approach, although more time-consuming, is general and does not involve any simplifications regarding the chemistry.

There have been reports of fast integrators for stiff kinetic equations in recent literature, e.g., Reference 57. The use of these instead of CREK (which was used in the present work because of its availability in a well-tested form while other schemes were still in their development and testing phases) will reduce computer times and will make fine grid 3-D computations possible without undue computational costs. The framework for the kinetics calculations has been provided here and the substitution of CREK for another procedure should be a straightforward task. The use of fast integrators will also enable the treatment of a more detailed reaction mechanism for NO_x . Thus, steps involving species such as HCN (on fuel-rich side) can be included if reliable kinetic data is available.

CHAPTER VI

THE FOUR-STEP HYDROCARBON OXIDATION MECHANISM

A. Background

A successful modeling of combustion systems depends on an adequate description of the reaction mechanism. For hydrocarbon oxidation, a large number of species participating simultaneously in numerous elementary kinetic steps is required to specify the reaction mechanism. This results in "stiff" differential equations requiring special time-consuming integration methods. For a complex 3-D problem, the computing costs would be prohibitive. Besides the large number of species equations to be solved, the elementary steps and their rate constants are not well known except for the simplest of hydrocarbons e.g., CH₄. To get around this problem, the gas turbine combustion modeling effort has frequently been simplified by using a global approach that reduces chemistry to the specification of an overall global oxidation scheme, which can predict quantities of interest: fuel consumption and heat release rates.

The oxidation of hydrocarbon fuel can be described by the following basic steps:

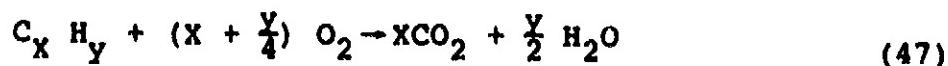
- (a) Transformation of the hydrocarbon fuel into intermediate hydrocarbons and hydrogen with little release of energy;
- (b) Oxidation of intermediates to CO and H₂;
- (c) Oxidation of CO to CO₂;
- (d) Oxidation of H₂ to H₂O.

Steps (b) through (d) are exothermic and are responsible for the release of energy and associated temperature rise. A global reaction scheme, which is designed to correctly model the oxidation process, must include a description of these steps.

B. Hydrocarbon Reaction Mechanisms

One Step Scheme

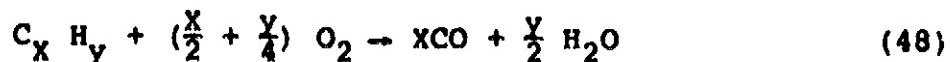
The simplest global mechanism is the one-step scheme:



The advantage of this mechanism is its simplicity; it involves the solution of the conservation equations for unburned fuel and the mixture fraction. The heat release and the concentrations of the other species are then obtained from linear functions of the amount of fuel consumed. This mechanism, however, fails to predict the important characteristics of hydrocarbon oxidation, i.e., the formation of intermediates and CO, which influence the process considerably. As a result, this mechanism is inadequate for obtaining quantitative predictions.

Two-Step Scheme

A slightly more complex scheme is the two-step mechanism:

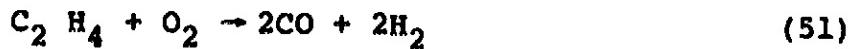
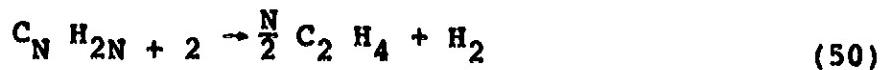


This involves the solution of one additional equation: that for the concentration of CO. Here again, the formation of intermediates is ignored and so this mechanism cannot predict the time delay

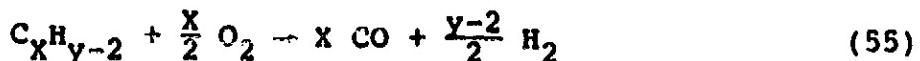
between the initial disappearance of fuel into intermediates and a significant rise in temperature.

Four-Step Scheme

The simplest mechanism which accounts for the essential features of the hydrocarbon oxidation is the following four-step scheme proposed by Hautman, et al.⁵³



This scheme is valid only for aliphatic hydrocarbons of the type $C_N H_{2N+2}$. To accommodate a general hydrocarbon $C_x H_y$, the first two steps have been modified in the present work:



This scheme involves the solution of two additional equations: for the concentrations of $C_x H_{y-2}$ and H_2 .

The rate expressions for the four-step scheme developed primarily from propane oxidation results⁵³ are

$$\frac{d[C_x H_y]}{dt} = -10^x \exp(-E/RT) [C_x H_y]^a [O_2]^b [C_x H_{y-2}]^c \text{ mole/cc-s} \quad (56)$$

$$\frac{d[C_{x,y-2}]}{dt} = -10^x \exp(-E/RT) [C_{x,y-2}]^a [O_2]^b [C_{x,y}]^c \text{ mole/cc-s} \quad (57)$$

$$\frac{d[CO]}{dt} = \{-10^x \exp(-E/RT) [CO]^a [O_2]^b [H_2O]^c\} \times S \text{ mole/cc-s} \quad (58)$$

$$\frac{d[H_2]}{dt} = -10^x \exp(-E/RT) [H_2]^a [O_2]^b [C_{x,y-2}]^c \text{ mole/cc-s} \quad (59)$$

where [CO], etc. are the species concentrations in gm-moles/cc. The parameters⁵³ for (56) are $x = 17.32 \pm 0.88$, $E = 49,600 \pm 2400$, $a = 0.50 \pm 0.02$, $b = 1.07 \pm 0.05$, and $c = 0.40 \pm 0.03$;

for (57), $x = 14.70 \pm 2.00$, $E = 50,000 \pm 5000$, $a = 0.90 \pm 0.08$, $b = 1.18 \pm 0.10$, and $c = -0.37 \pm 0.04$;

for (59), $x = 13.52 \pm 2.2$, $E = 41,000 \pm 6400$, $a = 0.85 \pm 0.16$, $b = 1.42 \pm 0.11$, and $c = -0.56 \pm 0.20$;

and for (58), $x = 14.6 \pm 0.25$, $E = 40,000 \pm 1200$, $a = 1.0$, $b = 0.25$, and $c = 0.50$;

$S = 7.93 \exp(-2.48\phi)$, where ϕ is the initial equivalence ratio and S cannot take values greater than 1.

The rate expressions were found to predict within reasonable accuracy flow reactor and shock tube results on propane oxidation, which encompass an equivalence ratio range 0.12 to 2.0, a temperature range 960 to 1540K, and a pressure range 1 to 9 atm. With modification to the parameters, experimental flow reactor results on the oxidation of butane, 2- and 3-methylpentane, and n-octane are also predicted.⁵³

The tolerance bands on the various parameters reflect the sensitivity of the predictions to these parameters and the modifications necessary to the values of these parameters in order to

obtain predictions in agreement with experimental measurements for different conditions. In the present work, it was found that the tolerance band on most of the parameters is rather wide and that for any given flow, changing a parameter from its lower to its upper limit can alter the predictions significantly. For the results reported in Chapter VII, the median values of all the parameters were used. Further comparison with more experimental measurements is necessary in order to narrow the tolerance bands and obtain more certain values.

C. Present Approach

The four-step mechanism described above has been incorporated into the 3-D Combustor Performance Program. This involved the solution of two additional differential equations of the same general form as Equation (3), for the concentrations of C_xH_{y-2} and H_2 . The source terms in these equations were obtained from the mechanism given by Equation (50-55). The rate expressions given by Equations (56-59) were modified by the eddy-break-up rate to account for the influence of turbulence. The procedure used was the same as that for the fuel equation¹. The effective Schmidt numbers for these two species were assumed to be the same as for other species, i.e., 0.9.

Other modifications to the 3-D program to incorporate the four-step scheme were:

- o The source terms for C_xH_y and CO were modified to be in accordance with the four-step scheme: C_xH_y consumed in Step (1); CO produced in Step (2) and consumed in Step (3).
- o Mixture molecular weight, density, enthalpy (and hence temperature) calculation sequences were modified to include the two new species: C_xH_{y-2} and H_2 .

- o Computations of O_2 , CO_2 , H_2O concentrations from element conservation were modified to include the two new species: C_xH_{y-2} and H_2 .

The four-step scheme was proved to be far superior to the two-step scheme in computations of a plug flow reactor (see Chapter VII, Results).

CHAPTER VII

RESULTS AND DISCUSSION

In this section, the results of the computations performed in the present program are described. The results of the validation of the four-step hydrocarbon oxidation scheme are presented followed by computations of the emissions from a JT8D combustor.

A. Four-Step Hydrocarbon Oxidation Scheme Results

Measurements in a plug flow reactor were conducted by Hautman, et al.,⁵³ for lean, stoichiometric, and rich propane flames. These measurements were used to test the validity of the four-step scheme. Computations were performed for these three cases with both the two-step and four-step schemes. Sixty axial grid points were used in these computations. Reduction of the axial spacing by a factor of two, showed negligible changes, thus demonstrating the grid-independency of the results.

Comparison of the results with the measurements are shown in Figures 1, 2, and 3 for the lean, stoichiometric and rich cases, respectively. From these figures, it is clear that the four-step scheme is far superior to the two-step scheme in predicting the salient features of hydrocarbon combustion.

Figure 1 (a, b, and c) shows the two-step and four-step hydrocarbon oxidation scheme predictions and the corresponding measurements for the lean C₃H₈ flame. The four-step predictions of CO₂, C₃H₈, and temperature agree very closely with the measurements. The four-step CO and H₂ predictions are slightly higher than the measurements, but the discrepancy is not large. Since in the predictions all the intermediates are lumped into C₂H₄, the total measured intermediates are shown in Figure 1c for a more meaningful comparison; here, again, the agreement is good. On the other hand,

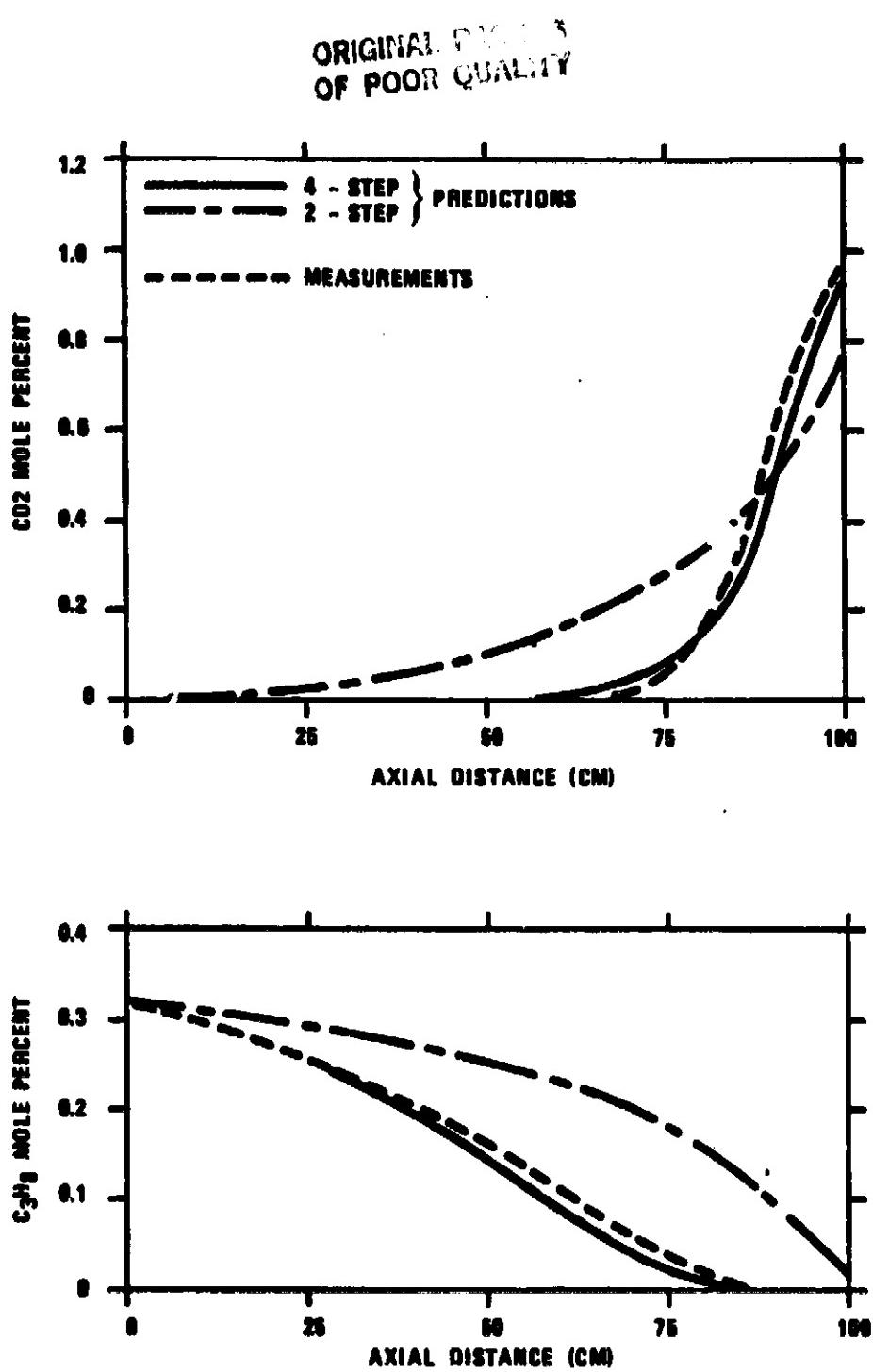


Figure 1a. Lean C₃H₈ Flame ($\phi = 0.12$).

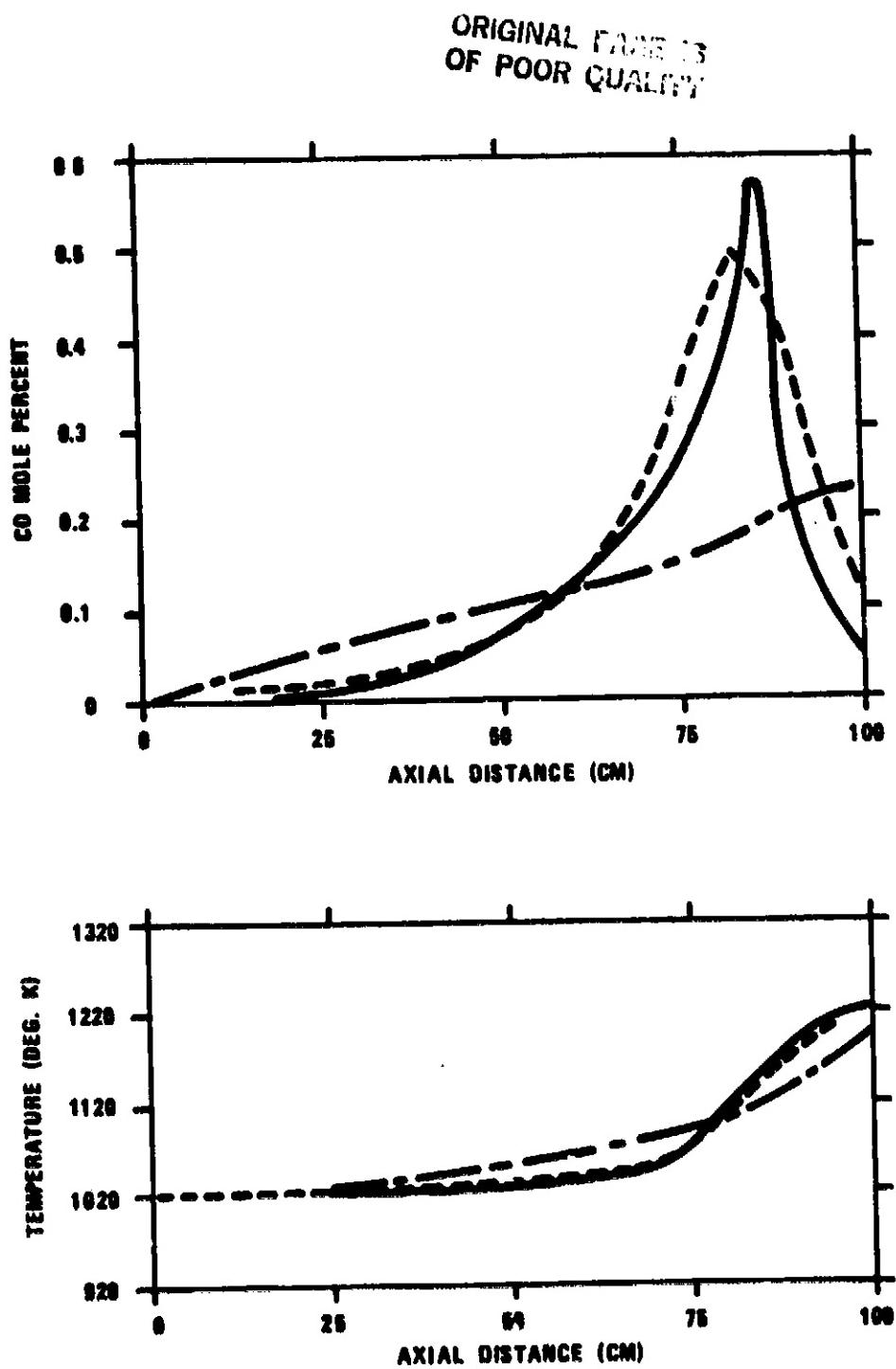


Figure 1b. Lean C_3H_8 Flame ($\phi = 0.12$).

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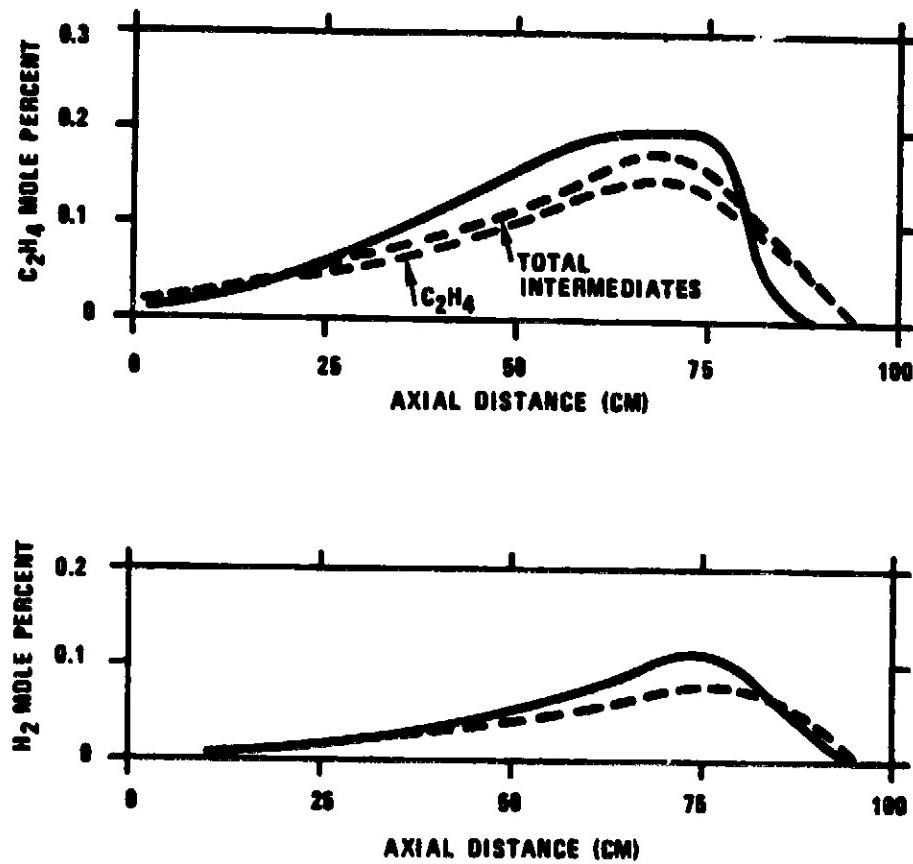


Figure 1c. Lean C₃H₈ Flame ($\phi = 0.12$).

ORIGINAL DRAWING
OF PORTION

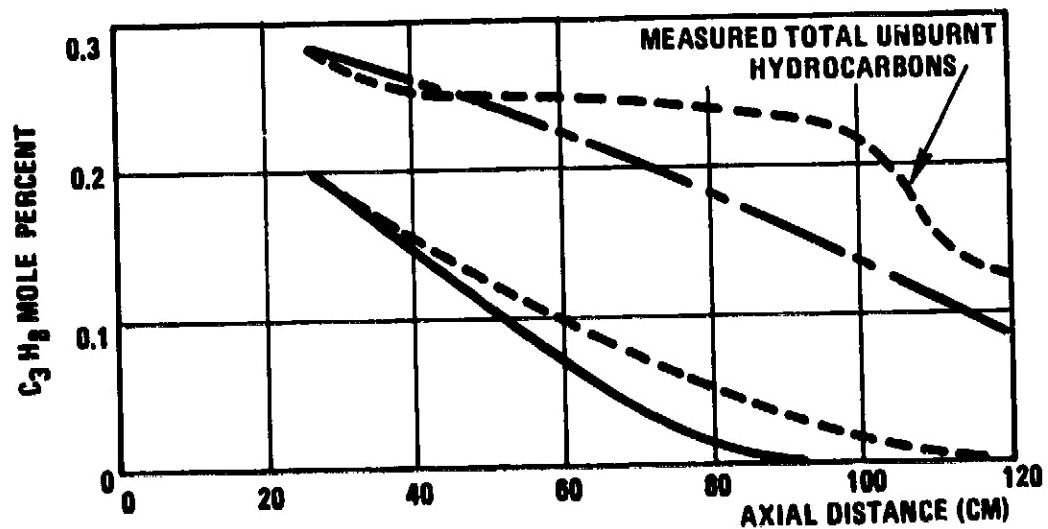
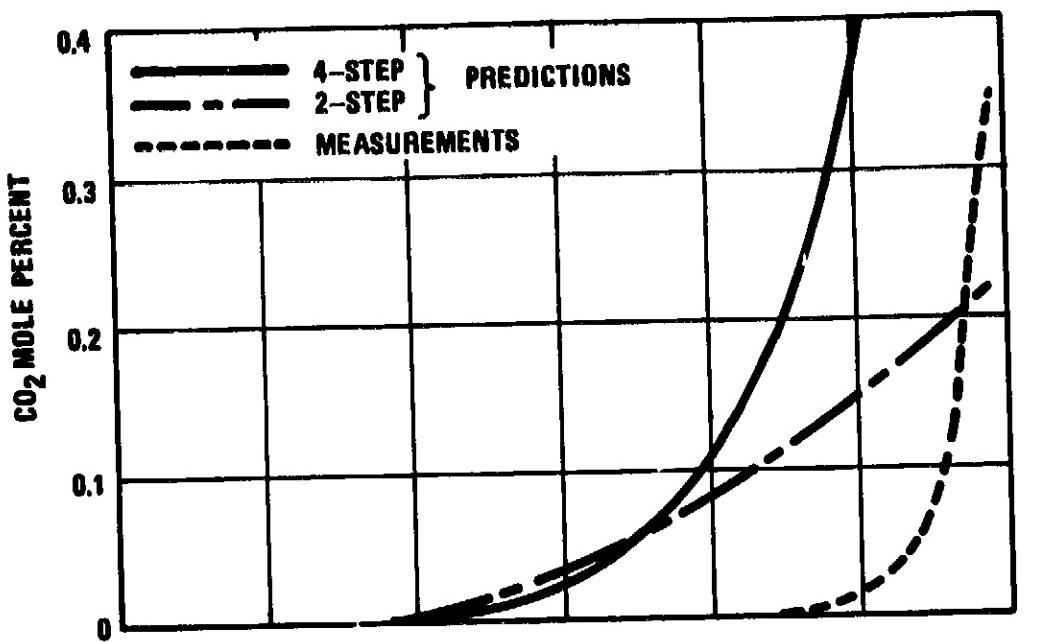


Figure 2a. Stoichiometric C₃H₈ Flame ($\phi=0.98$).

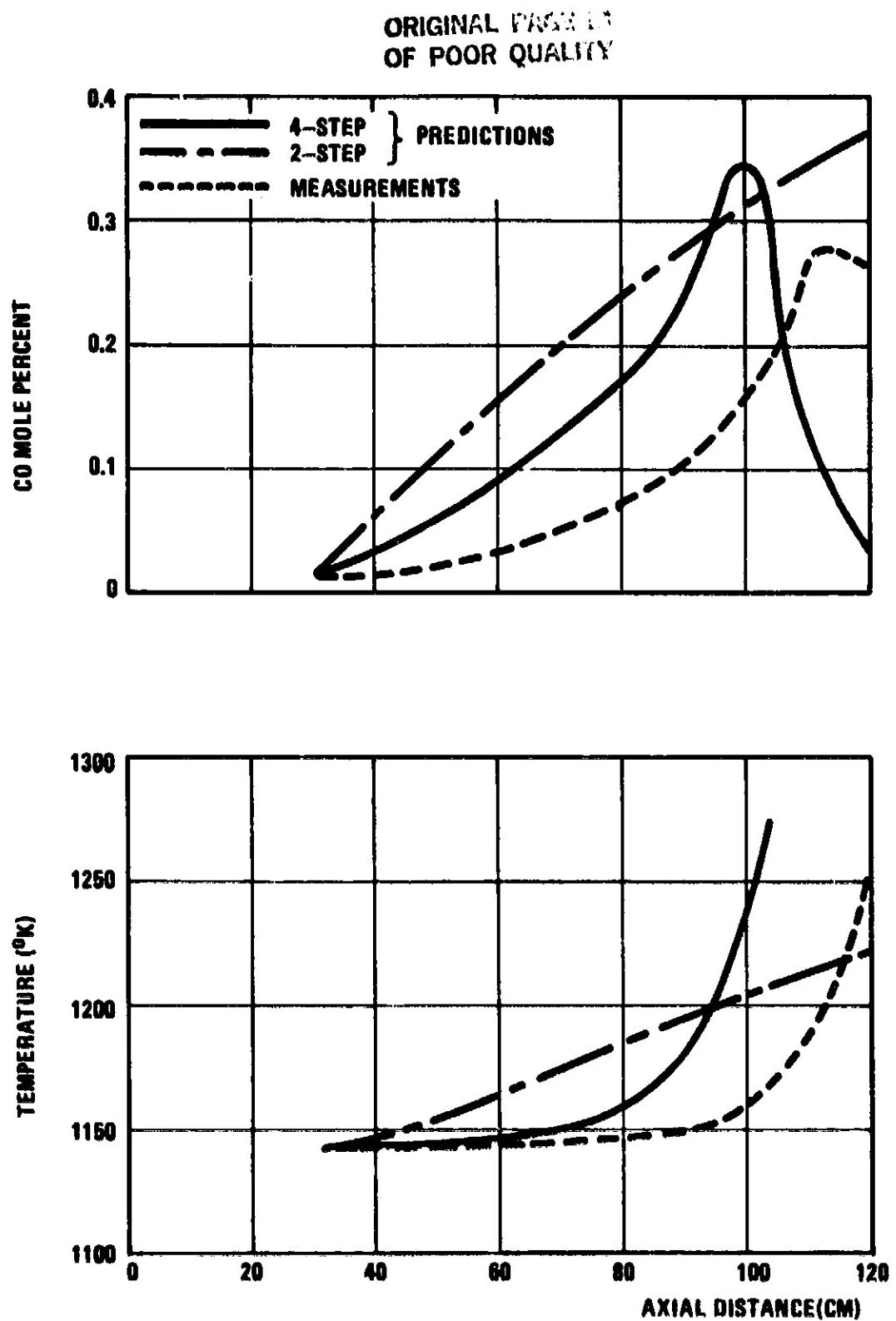


Figure 2b. Stoichiometric C_3H_8 Flame ($\phi=0.98$).

ORIGINAL VIEW
OF FLAME

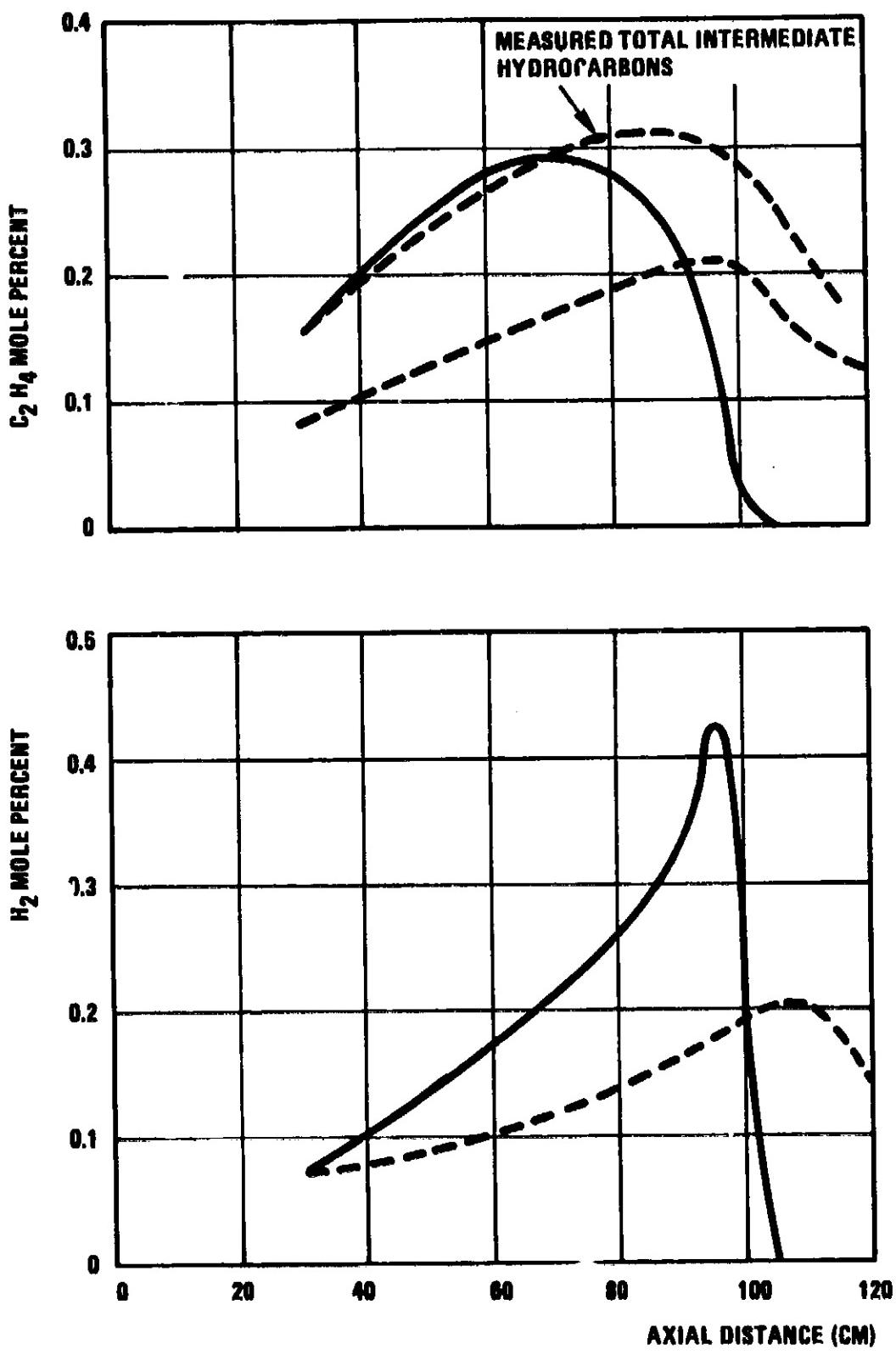


Figure 2c. Stoichiometric C₃H₈ Flame ($\phi=0.98$).

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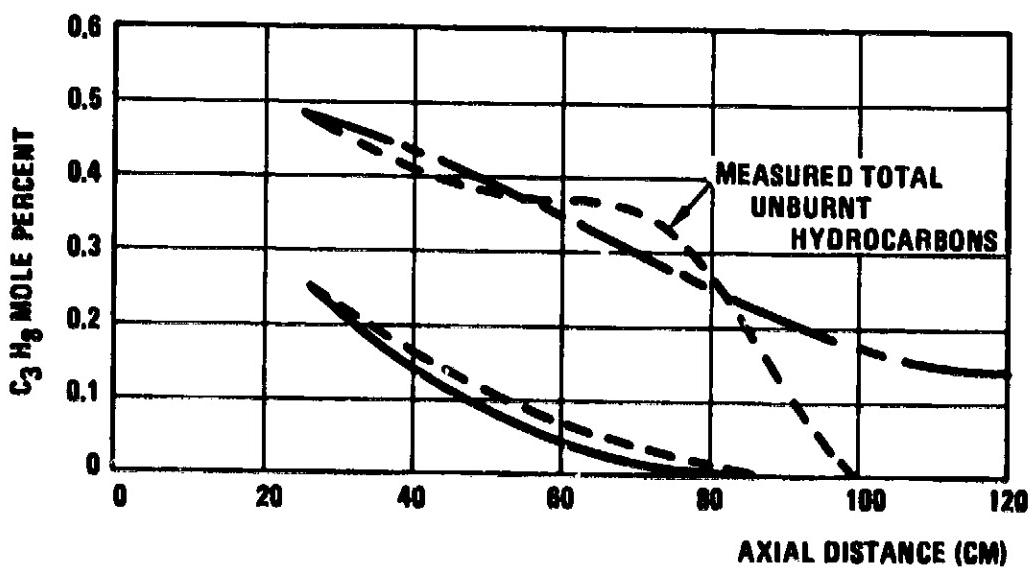
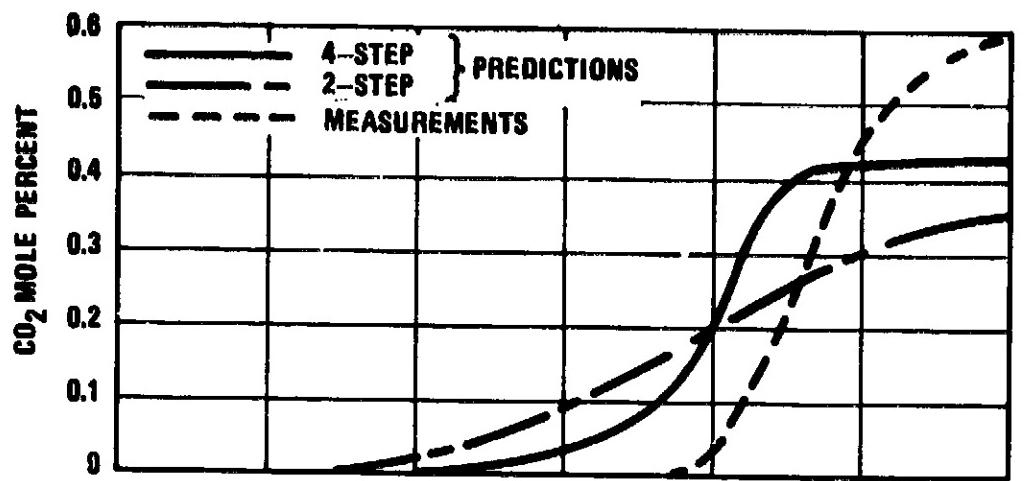


Figure 3a. Rich C₃H₈ Flame ($\phi=1.59$).

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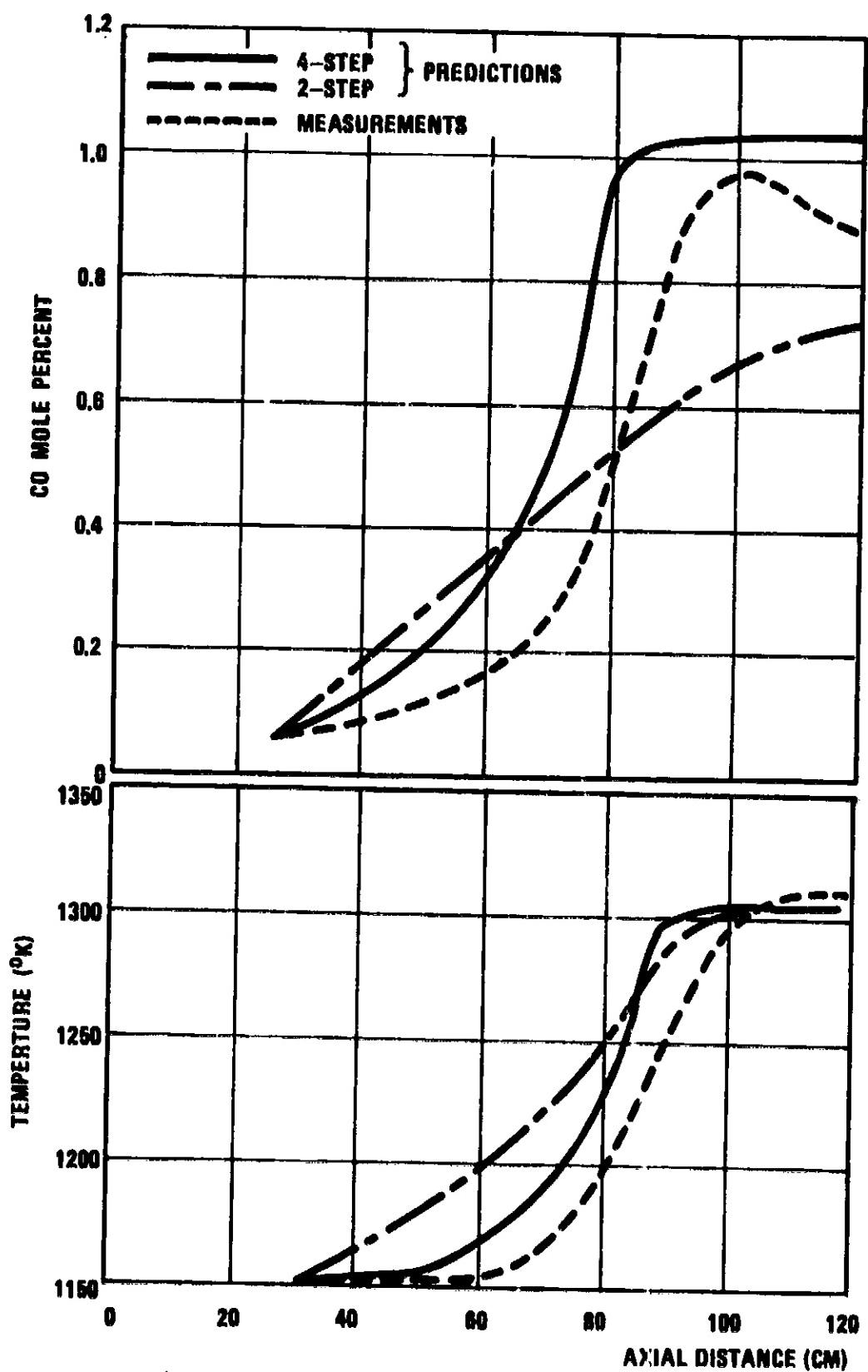


Figure 3b. Rich C_3H_8 Flame ($\phi=1.59$).

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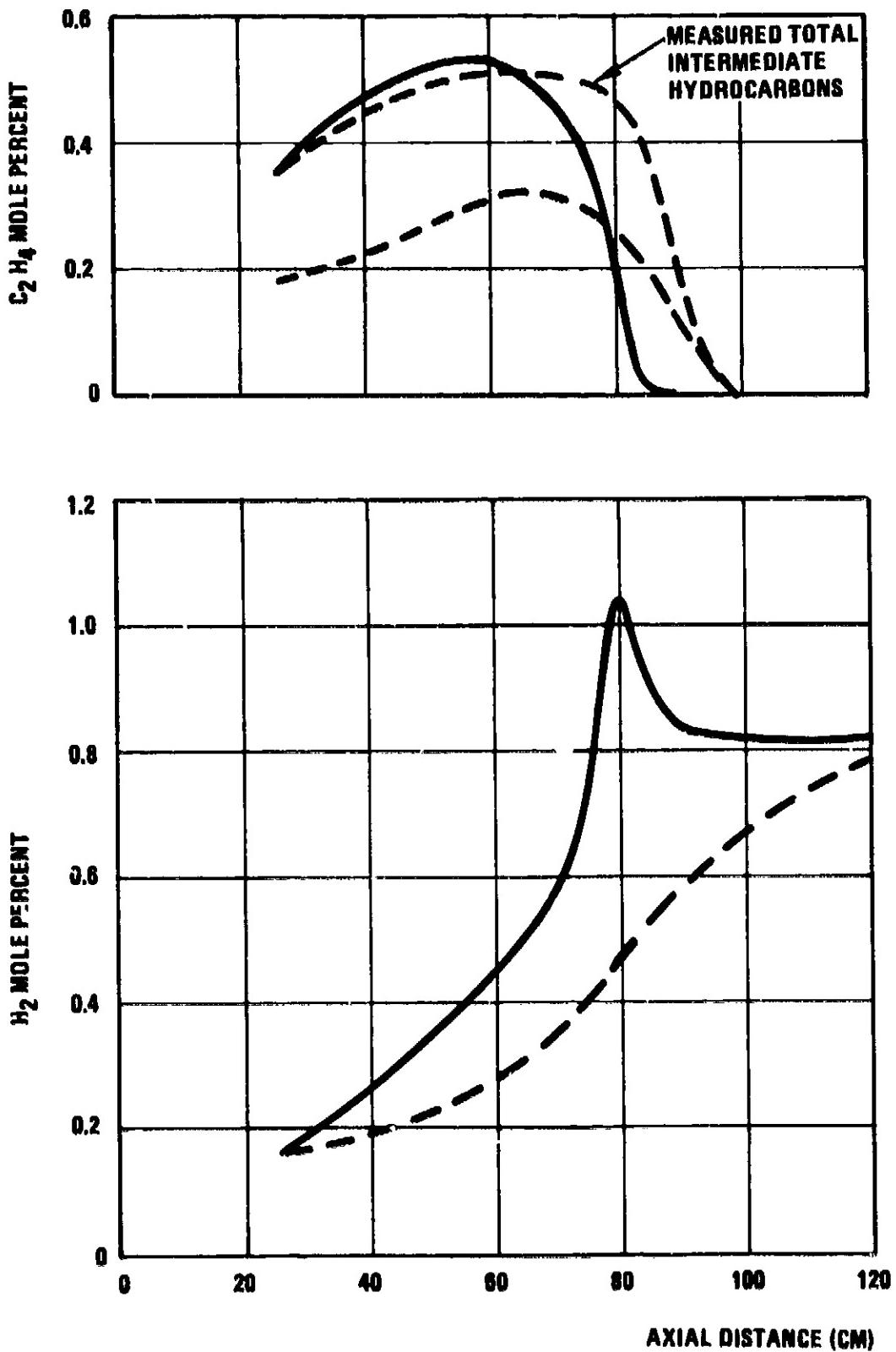


Figure 3c. Rich C_3H_8 Flame ($\phi=1.59$).

the two-step predictions show considerable discrepancy for all the species and for the temperature.

Figure 2 (a, b, and c) shows the measurements and predictions for the stoichiometric case. Here the four-step predictions are not as good as for the lean case; however, compared to the two-step predictions, the four-step results are in much closer agreement with the measurements. A major discrepancy is the predicted (four-step) H_2 concentration, which is considerably higher than the measured values.

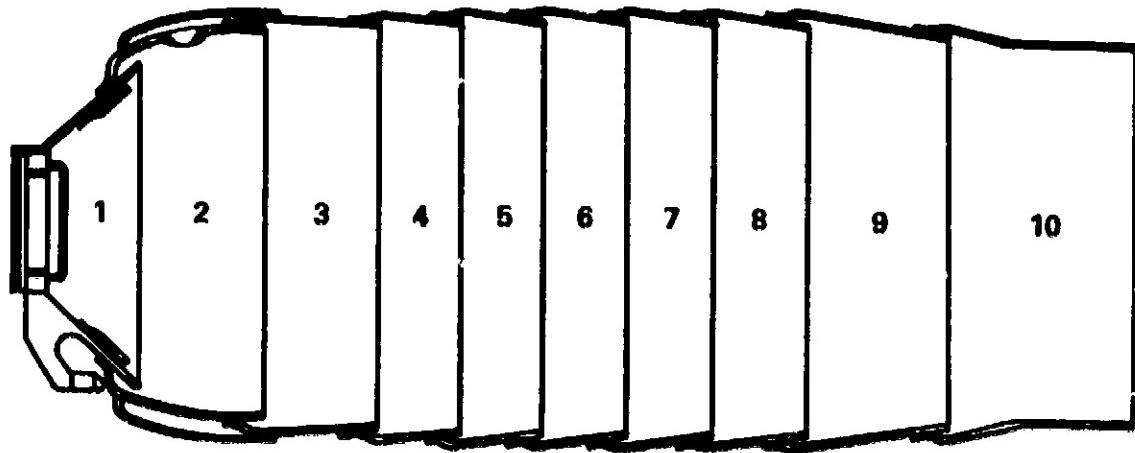
Figure 3 (a, b, and c) shows the measurements and predictions for the fuel-rich case. Here, again, the four-step predictions, although not in very close agreement with the measurements, are far superior to the two-step predictions. The four-step fuel concentration and temperature profiles are in good agreement with the measurements; CO , CO_2 , and C_2H_4 are in fair agreement. Again, the H_2 concentration is overpredicted as in the stoichiometric case.

As shown by these results, a problem not resolved with the four-step scheme is the discrepancy between predicted and measured H_2 and H_2O concentrations, especially at stoichiometric and fuel rich conditions. The H_2 oxidation rate is predicted to occur more slowly, and results in an excess of H_2 and under-prediction of H_2O , as compared to the measurements. A similar observation was also made by Hautman, et al.⁵³

B. JT8D Combustor Computations

The 3-D Combustor Performance Program was set up and run for a JT8D-17 combustor as shown in Figure 4. This combustor uses a single pressure atomizing injector on the centerline of the can. Air is admitted around the injector through a 45-degree swirler. The operating points for the computations represent idle, cruise, and take-off and are given below:

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FUEL INJECTOR AND PRIMARY SWIRLER EQUIVALENT
METERING AREA 7.61 PERCENT

Equivalent Metering Area

Louver Cooling Air		Combustion Air	
Panel	%	Panel	%
1	1.53	2	7.93
2	5.62	3	1.92
3	7.56	5	8.00
4	5.69	8	15.85
5	4.24	9	18.09
6	3.41		
7	3.42		
8	3.43		
9	2.78		
10	1.81		

Figure 4. JT8D-17 Combustor.

Condition	Airflow lbs/sec	Pressure psia	Temperature °F	Fuel/Air Ratio
Idle	4.06	39.6	260	0.0074
Cruise	7.87	103.0	657	0.0138
Take-Off	16.45	256.0	825	0.0182

The steps adopted in the solution procedure for the JT8D combustor are outlined below:

- (1) The 3-D combustor program was used to solve for the variables: velocity, pressure, turbulence energy and dissipation, enthalpy (temperature), mixture fraction, mass fractions of unburned fuel, $C_x H_{y-2}$, CO, and H_2 . At this stage, the soot and radiation equations were not solved, and the solution was carried on until a convergence level of approximately 5 percent in cumulative mass residual was reached.
- (2) The soot and radiation equations were solved next. The radiation fluxes appear as sources in the enthalpy equation; and this, in turn, influences the other dependent variables. The solution of the variables in Step (1) was repeated coupled with the soot and radiation equations. The process was continued until a convergence level of approximately 1 percent was reached.
- (3) The NO_x equations were solved next. The solution of the variables in Steps (1) and (2) was repeated, coupled with the NO_x equations. The process was continued until the convergence level desired for the final solution (~0.5 percent) was reached.

The reason for adopting the above stepwise procedure was to cut down on required computer time. Since the soot is generally present only in small concentrations, it will influence the main flow field only slightly and so delaying the solution of the soot and radiation (which is mainly from soot) equations resulted in a considerable saving of computer time. Similarly, the NO_x species have an even smaller influence on the other variables and so their solution was further delayed. Due to the point-by-point nature of the NO_x solution, this solution had to be repeated a number of times to achieve convergence, as explained in Chapter V.

A flow chart of the overall solution procedure is given in Figure 5. The various steps are executed automatically by the program from start to completion.

Computations were performed with both the two-step and four-step hydrocarbon oxidation schemes and with a grid of $10 \times 10 \times 5$ (axial \times radial \times tangential) points. Due to the coarseness of the grid, it was not possible to simulate exactly all of the geometrical details of the combustor. However, the main features were simulated as closely as possible. Due to the large computer times required for the NO_x calculations, as explained in Chapter V, increasing the number of grid points significantly over that used was found to be computationally prohibitive.

The central processor time on a CYBER 730 computer with the two-step hydrocarbon scheme was 0.044 seconds per iteration per internal node (boundary nodes that are not calculated are excluded here) when the NO_x chemical kinetics solution was not activated. For the NO_x solution, the central processor time was an additional 0.2-0.3 second per iteration per internal node. Typically 100-150 iterations were required before the NO_x solution was turned on, after which an additional 50-100 iterations were required to achieve convergence. Thus for the chosen grid ($10 \times 10 \times 5$), a complete run required 3000-5000 seconds depending on the conditions

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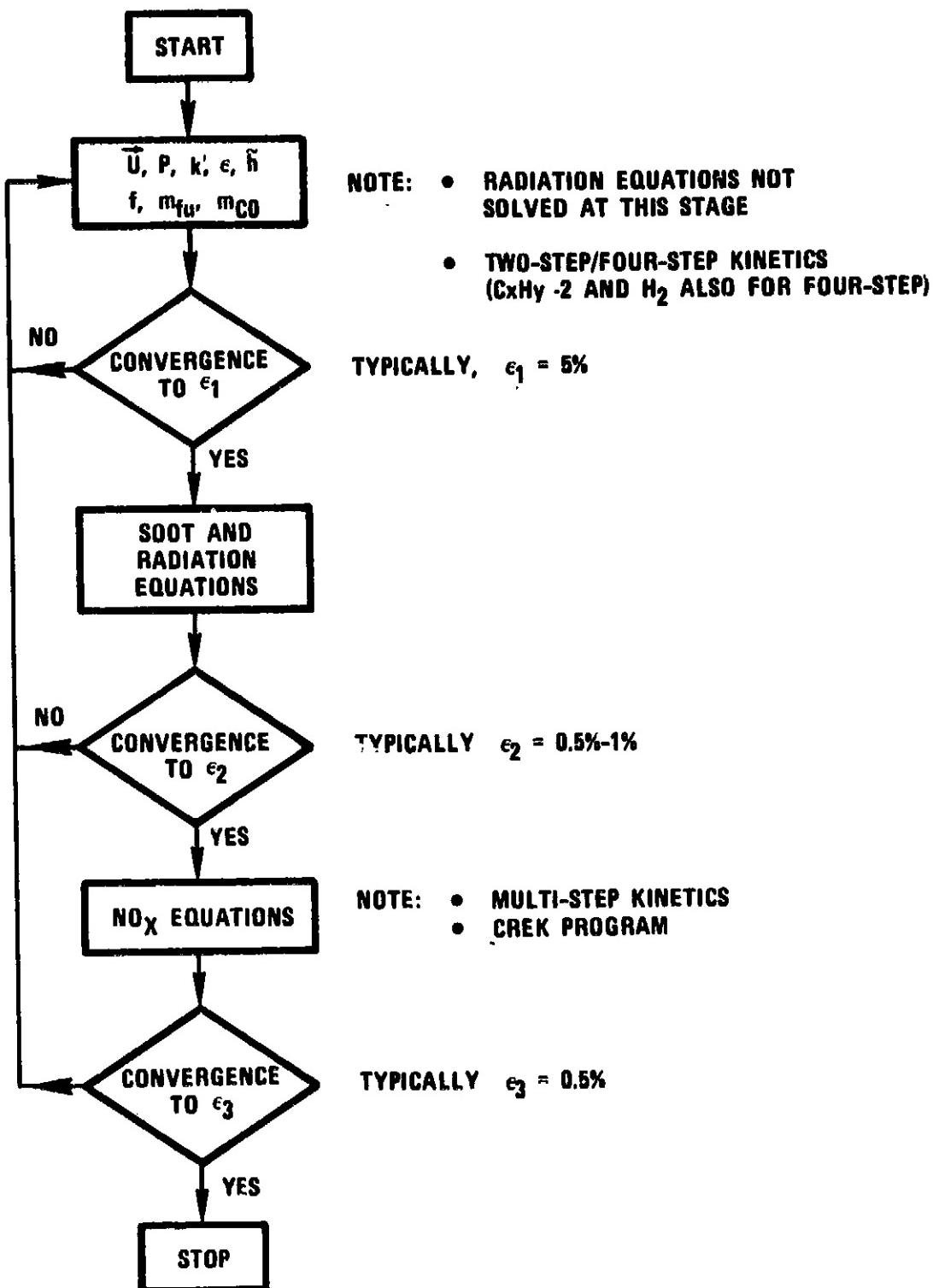


Figure 5. Flowchart of Overall Solution Procedure.

for the run (which influences the number of iterations to convergence), with the bulk of the time spent on NO_x calculations. Since the four-step scheme involved the solution of additional equations for the intermediate hydrocarbon and H_2 , the computation times were about 10-15 percent higher than those with the two-step scheme. The central memory required for the $10 \times 10 \times 5$ grid was 173,500 octal words.

The predicted emissions index for the idle, cruise, and take-off conditions with the two-step and four-step schemes is shown in Tables IIa and IIb. For the idle case, the predicted smoke concentration is very small and much lower than that experimentally observed. The formation of soot, as modeled, is governed by the local temperature and fuel/air ratio and also turbulent fluctuations. Since the temperature and fuel/air ratio are low for the idle case, the model does not predict significant soot formation. Obviously, other factors that have not been modeled and that are not precisely known, govern soot formation under such conditions.

For the cruise and takeoff cases, the emissions indices for soot and NO_x show the correct trends and are reasonably close to the measurements that are available. The differences between the two-step and four-step schemes are not significant in the prediction of the emissions index, which represents an integrated value at the combustor exit. The differences in the two schemes are significant in the primary zone of the combustor.

The predicted radiation flux to the combustor wall for the conditions of idle, cruise, and takeoff is shown in Table IIIa for the two-step scheme and in Table IIIb for the four-step scheme. The values are reported at the primary, secondary, and tertiary zones which are at 6, 21, and 33cm downstream of the fuel nozzle; these correspond to the locations at which measurements were conducted by Claus⁵⁶ for different operating conditions. The predicted radiation fluxes show the correct trends; i.e., the flux is

TABLE IIa. PREDICTED EMISSIONS INDEX WITH TWO-STEP HYDROCARBON OXIDATION SCHEME.

Condition	Emission Index Gm of Emissions/Kg of Fuel	
	Smoke	NO _x
Idle	0.26 E-3 (0.6) ⁵⁵	≈0
Cruise	1.6	15
Takeoff	1.5 (2.8) ⁵⁵	28 (24.4) ⁵⁴

NOTE: Values in parentheses are experimental measurements from indicated reference.

TABLE IIb. PREDICTED EMISSIONS INDEX WITH FOUR-STEP HYDROCARBON OXIDATION SCHEME.

Condition	Emission Index Gm of Emissions/Kg of Fuel	
	Smoke	NO _x
Idle	0.056 (0.6) ⁵⁵	≈0
Cruise	1.3	13
Takeoff	1.2 (2.8) ⁵⁵	27 (24.4) ⁵⁴

NOTE: Values in parentheses are experimental measurements from indicated reference.

TABLE IIIa. PREDICTED WALL RADIATION FLUX WITH
TWO-STEP HYDROCARBON OXIDATION
SCHEME.

Condition	Primary Zone (W/M ²)	Secondary Zone (W/M ²)	Tertiary Zone (W/M ²)
Idle	2.9E4	3.46E4	1.03E4
Cruise	5.55E5	8.98E5	2.23E5
Takeoff	7.89E5	1.33E6	4.26E5

TABLE IIIb. PREDICTED WALL RADIATION FLUX WITH
FOUR-STEP HYDROCARBON OXIDATION
SCHEME.

Condition	Primary Zone (W/M ²)	Secondary Zone (W/M ²)	Tertiary Zone (W/M ²)
Idle	1.06E4	1.35E4	3.19E3
Cruise	3.78E5	9.01E5	2.13E5
Takeoff	6.40E5	1.34E6	3.72E5

maximum in the secondary zone and minimum in the tertiary zone. This trend was experimentally observed by Claus.⁵⁶ The level of the flux also corresponds to that measured by Claus for slightly different conditions. Due to the differences in the conditions for which measurements and predictions were made, a direct comparison of the two is not shown.

For the idle case, since the soot concentrations were predicted to be very low, the predicted radiation fluxes are also towards the low side. The predicted radiation flux with the four-step scheme is lower than that with the two-step scheme for the idle case, but the soot predictions show the opposite trend, i.e., slightly higher with the four-step scheme. This occurs because, in the predictions for the idle case, the radiation from the soot is low and is due to its small concentration. The gas radiation is important and is predicted to be higher with the two-step scheme because of a faster temperature rise.

The computations performed for the three operating conditions of the JT8D combustor show that the present model is capable of producing reasonable predictions of the emissions of smoke and NO_x and of the wall radiation flux.

CHAPTER VIII

CONCLUSIONS

In the present work, a method was formulated for the following:

- o computation of soot and NO_x emissions from a combustor
- o inclusion of the effects of soot on radiant heat transfer, and
- o extension of the two-step hydrocarbon oxidation scheme to a four-step one.

The method was coded into the Garrett 3-D Combustor Performance Program. A description of the program, list of Fortran variables, and program listing have been included in the report to aid the reader in understanding the emissions model.

The computations that were performed show that the method is capable of producing reasonable results. The lack of accurate experimental data has precluded more detailed validation of the model. As reliable experimental data becomes available, further computations will reveal the capabilities and limitations of the model and the modifications necessary to overcome the limitations.

CHAPTER IX

NOMENCLATURE

All symbols were defined in the report at the point when first referenced. The following is a list of symbols used often in the report.

- a = Absorption coefficient
- C_i = Time-mean concentration of species i
- C_p = Specific heat
- D = Particle diameter
- E = Activation energy
- k = Kinetic energy of turbulence
- K_b = Backward reaction rate constant
- K_C = Equilibrium constant
- K_f = Forward reaction rate constant
- m_i = Mass fraction of species i
- n = Nuclei concentration
- n_o = Rate of spontaneous nuclei formation
- N = Concentration of soot particles
- P = Pressure
- R = Reaction rate
- S = Scattering coefficient
- S_ϕ = Source term of dependent variable ϕ
- t = Time
- T = Temperature

\vec{u} = Velocity vector
 ϵ = Emissivity; dissipation rate of turbulence
 ϕ = General dependent variable
 ν = Kinematic viscosity
 μ_t = Effective viscosity
 σ = Stefan-Boltzmann constant
 σ_ϕ = Prandtl/Schmidt number of dependent variable ϕ
 ρ = Density
 λ = Wavelength

Subscripts

fu = Fuel
 i = Species i
 n = Nuclei
 O_2 = Oxygen
 pr = Products
 s = Soot
 ϕ = Dependent variable

Superscripts

$*$ = Fine structure
 $^\circ$ = Surrounding fluid

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**APPENDIX A
DESCRIPTION OF THE 3-D
COMBUSTOR PERFORMANCE PROGRAM**

APPENDIX A

DESCRIPTION OF THE 3-D COMBUSTOR PERFORMANCE PROGRAM

The 3-D performance model is a three-dimensional recirculating-flow program that is capable of analyzing a variety of combustor configurations, including can, can-annular, and annular. The program solves for the three velocity components, U, V, and W, species concentrations, C_XH_Y , C_XH_{Y-2} , C(S), CO, CO_2 , H, H_2 , O, O_2 , OH, H_2O , N, N_2 , NO, NO_2 , turbulence quantities from the k- ϵ turbulence model, and three radiation fluxes. In addition, the use of primitive variables makes modifications to the boundary conditions easy, allowing the user to analyze complex inlet geometries. Also provided is a subroutine for calculating the trajectories and evaporation rates of a fuel-nozzle spray. The functions of the various subroutines are briefly described below.

Program MAIN (a computer listing has been provided in Appendix D) is divided into two basic sections. Up to card MA.167, the routine is concerned with reading the input data and converting it to the program's internal units which are Système International (S.I.). The input sequence is covered in Appendix B so only the units will be discussed. Cards MA.7 to MA.11 are used to define seven arrays which convert lengths associated with dimensions and lengths associated with velocity, energy, mass, temperature, pressure, and angles respectively. By proper specification in the data statements, the user may employ those input units that are most convenient. The output units are always S.I. From card MA.168 on, MAIN's function is to call the other various routines in their proper sequence.

Subroutine INIT performs some preliminary calculations (AL.10 to AL.155), prints the input data (AL.156 to AL.258), and defines

the initial conditions and some of the boundary conditions on the various arrays (AL.259 on). In section AL.48 through AL.78, two arrays, JKIN and IKIN, are defined. They merely contain flags which indicate the locations of mass injection points. Cards AL.261 to AL.272 contain logic for the restart option. If Tape 0 from a previous run is saved and then made available for use during a subsequent run, the program will read the initial and boundary conditions from it.

Subroutine ALLMOD contains several entry points which perform miscellaneous calculations pertaining, usually, to the boundary nodes where modifications to the standard equation are in order. The cyclic nature of the boundary conditions in the θ or K direction is evident in FMOD as well as limits to the species mass fractions. VELMOD allows the inlet swirl velocity to be increased gradually over a number of iterations and assures that overall continuity is maintained at the exit plane. DENMOD makes alterations to the density at the boundaries to maintain the correct mass-flow rate. GAMOD specifies the wall viscosity values as calculated by the wall functions. SOMAS is used to initialize an array DIVG which is used later in the program. The largest entry point SOMOD contains logic for modifying the equation coefficients and source terms when cooling slots, walls, and droplet evaporation are present. Each variable has its own section and accounts for transfer with the walls and mass addition from the evaporating fuel. SOMODZ deals only with the Z-direction radiation equation and is in a section alone as the data storage is slightly different for this variable.

Subroutine OUTPUT is used for printout purposes. The emissions index of SOOT and NO_x is calculated and printed here. Subsequently, subroutine FPRINT is called for the printout of all dependent variables.

Subroutine AUX performs the auxiliary calculations for temperature, density, viscosity, and source terms. Entry DENS uses AU.11 to AU.56 to calculate temperature. Cards AU.52 to AU.56 limit the values calculated in order to account for dissociation and early iteration fluctuations. With known temperature, density is then determined from AU.57 to AU.108. VISCO obtains effective viscosity from turbulent kinetic energy and dissipation and calculates Y+ for use by the wall function routine. GAMMA obtains the effective diffusion coefficients. SOURCE contains all calculations for source terms with the exception of the aforementioned modifications in SOMOD. Again, each variable has its own section, with coding that is quite straightforward and requires no explanation.

Subroutine AUXRAD performs the same function as AUX except that it pertains only to the radiation equations.

Subroutine SPRAY is used to determine the evaporation rate of the fuel-nozzle spray. A large section, from SP.106 to SP.269, deals with locating the droplet, determining free-stream conditions, and handling the situation where the droplet approaches a boundary. Next, various fuel and free-stream properties are evaluated (to SP.292). The drag forces and time step are then determined and used to obtain new velocities and location. If the droplet is below the boiling temperature, no evaporation occurs (SP.340 to SP.347); but, when the boiling temperature is reached, evaporation rates are calculated, and the appropriate entries to the evaporation array (EVAP) are made. Information concerning momentum changes due to evaporation are also stored in their respective arrays and later (SP.382 to SP.425) on a scratch file for use when the three momentum equations are solved.

The coefficients for each variable are generated and the solution routine called in subroutine STRIDE. First, equations for U,

V, and W are handled (ST.117 to ST.632), then the pressure perturbation (P') is obtained (ST.633 to ST.714) and used to correct the velocities (ST.716 to ST.753) so that mass errors are reduced. Then, the remaining variables are solved with the radiation equations having their own special section (ST.915 to ST.937). The chemical kinetics calculations are contained from NOX.230 to NOX.342. Here the inputs to program CREK are prepared and the outputs from CREK are stored in the respective arrays.

STRAD is a subroutine used in the radiation model which performs the same function as STRIDE performed for the other variables.

Subroutines ABSORB, ASYMP, CHEBY, DLECK, EGAS, PENTA, SOOT and SCRTCH (from Ref. 40) are used to compute the absorbtivity of gas-soot mixtures.

SOLVE provides a solution to the equations generated in STRIDE. A full three-dimensional solution would be time consuming and would require enormous computer storage. Therefore, an approximate solution is obtained by "sweeping" through the field several times alternately solving along one direction, while holding the values in the other two fixed. The variable ICTDMA (NV) at S0.36 is used to specify the number of such sweeps. As the program converges, and the variables assume their final values, the solution becomes more accurate. Due to the cyclic nature of the boundary conditions in the θ -direction, a cyclic tri-diagonal matrix algorithm (CTDMA) is used for this direction; the coding sequence is contained in SOLVE2.

Subroutine FPRINT is used for the printout of field values of dependent variables.

The last part of the program contains the chemical kinetics subroutines: CREK, CALC, SPECE, CREKO AND HCPS.

Subroutine CREK is the main routine called from the 3-D program. It controls the solution strategy: equilibrium or kinetic and problems associated with lack of convergence.

Subroutine CALC construct the Newton-Raphson correction matrix for both equilibrium and kinetic states and solves for the corrections by a standard Gaussian elimination procedure. In the present work, modifications have been made to this subroutine in order to incorporate the four-step hydrocarbon oxidation scheme and to compute the reaction rates from the eddy-break-up model.

Subroutine SPECE contains the Newton-Raphson iteration procedure for both equilibrium and kinetic states.

Subroutine CREKO is the initializing subroutine and is used for the input of element, thermodynamic and reaction mechanism data.

Subroutine HCPS is used for computing the enthalpy, constant pressure specific heat and the entropy of the species.

Further details of the chemical kinetics subroutines are contained in Ref. 48.

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**APPENDIX B
PROGRAM INPUT
DESCRIPTION**

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APPENDIX B

PROGRAM INPUT DESCRIPTION

Card Set	Variable	Format	Description
1	TITLE	20A4	Each card is a heading for a particular three-dimensional array that is printed out. These never change (33 cards).
2	TITLE2	10A4	Case title card.
3	LP1	8(I2,8X)	Number of grid nodes in axial (x) direction.
	MPL		Number of grid nodes in radial (y) direction.
	NPL		Number of grid nodes in tangential (z) direction.
	IPLAX		01 For plane geometry; 02 For axisymmetric geometry.
	MODEL		01 For laminar viscosity; 02 For k- ϵ viscosity model.
	MODER		01 For kinetic controlled combustion; 02 for kinetic and turbulence controlled combustion.
	IPAR		01 For absolute pressure; 02 For relative pressure.
	ITRAD		01 No radiation; 02 With radiation; radiation properties specified; 03 With radiation; radiation properties calculated.
4	IU	8(I2,8X)	01 Input units are international system (i.e., meters, kilograms, degrees kelvin, newtons, joules, radians, seconds or combinations thereof); 02 User selected input units.
	MODEN		01 Density is fixed at the value of "Den" on Card Set 19; 02 Density calculated from perfect gas law.
	INTAPE		00 Initial conditions not printed; 08 Initial conditions printed.

Card Set	Variable	Format	Description
	IDW	00 01	Inner boundary is axis of symmetry; Inner boundary is wall.
	IRES	00 01	This is a new case; This is a restart of previous case.
5	ISOLVE	8(I2,8X)	An 01 in proper field indicates that this particular variable will be solved for; an 00 indicates that it will not be. Order of variables: u, v, w, p', k, ϵ , Φ , mfu, mCH, mCO, mH, n, s1, s2, 14*0 (14 species solved by CREK), Rx, Ry, Rz.
6	ICTDMA	8(I2,8X)	Indicates the number of "sweeps" made in the solve routine for each variable. Order of variables as in Card Set 5.
7	IPRINT	8(I2,8X)	An 01 indicates that this variable will be printed, an 00 indicates that it will not be. Order of variables as in Card Set 1.
8	RELAX	8E10.4	Relaxation parameters for each variable. Order of variables as in Card Set 5. In addition, pressure, density, effective viscosity at end of the set.
9	PR	8E10.4	Laminar Prandtl numbers for each variable. Order of variables as in Card Set 5.
10	PREF	8E10.4	Turbulent Prandtl numbers for each variable. Order of variables as in Card Set 5.
11	X	8E10.4	X-coordinates (LP1 values).
12	RI Y	8E10.4	Radius of inner boundary. Y-coordinates as measured from inner boundary (MP1-1) values. Since Y(1) is <u>always</u> 00, RI is read in its place.
13	Z	8E10.4	Z-coordinates (NP1 values).
14	IWEI	8(I2,8X)	I-node at which upstream inclined wall ends.
	JWIO	See Fig. B-1	J-node at which upstream outer inclined wall starts.

Card Set	Variable	Format	Description
	IWE0		I-node at which downstream inclined wall starts.
	JWOO		J-node at which downstream outer inclined wall ends.
15	IWL1	8(I2,8X)	Starting I-nodes of the calculation domain when inclined wall is present. (Skip if IWEI = 2).
16	JWL0	8(I2,8X)	Ending J-nodes of the calculation domain at upstream outer inclined wall. (Skip if IWEI = 2).
17	IWL0	8(I2,8X)	Ending I-nodes of the calculation domain when inclined wall is present. (Skip if IWE0 = L).
18	JWL0	8(I2,8X)	Ending J-nodes of the calculation domain at downstream outer inclined wall. (Skip if IWE0 = L).
19	PRESS DEN	8E10.4	System pressure. The value of density if option MODEN = 01 is selected.
	ABSOR		Absorption coefficient in radiation model (if ITRAD = 2).
	SCATR		Scattering coefficient in radiation model (if ITRAD = 2).
	AKFAC		Internally defined turbulent kinetic energies are AKFAC time the appropriate velocity squared.
	ALFAC		Internally defined turbulent length scales are ALFAC time the appropriate distance.
20	CXX HYX HFU FUMCO	8E10.4	Carbon atoms in fuel molecule. Hydrogen atoms in fuel molecule. Heat of formation of fuel. Initial value assigned to MCO.
21	PREXP1 ARCON1	8E10.4	Preexponent of 1st reaction. Activation energy divided by gas constant of 1st reaction (E/R).
	CR1		Constant in turbulence controlled reaction rate of 1st reaction.

Card Set	Variable	Format	Description
	PREXP2 ARCON2		Pre-exponent of 2nd reaction. Activation energy divided by gas constant of 2nd reaction (E/R).
	CR2		Constant in turbulence controlled reaction rate for 2nd reaction.
22	PREXP3 ARCON3	8E10.4	Pre-exponent of 3rd reaction. Activation energy divided by gas constant of 3rd reaction (E/R).
	CR3		Constant in turbulence controlled reaction rate for 3rd reaction.
	PREXP4 ARCON4		Pre-exponent of 4th reaction. Activation energy divided by gas constant of 4th reaction (E/R)
	CR4		Constant in turbulence controlled reaction rate for 4th reaction
23	AA1 BB1 CC1 AA2 BB2 CC2	8E10.4	Exponent on species concentration in the reaction rate for 1st reaction. Exponent on species concentration in the reaction rate for 2nd reaction.
24	AA3 BB3 CC3 AA4 BB4 CC4	8E10.4	Exponent on species concentration in the reaction rate for 3rd reaction. Exponent on species concentration in the reaction rate for 4th reaction.
25	C1 C2 CD AMU ERROR TCYlw TLIP	8E10.4	Turbulence model constant. Turbulence model constant. Turbulence model constant. The value of the viscosity if option MODEL = 01 is specified. Also the laminar viscosity used in the "wall functions". Program will terminate if total error in mass becomes less than this value. Temperature of cylindrical portion of combustor and of dome. Temperature of cooling slot lip.
26	LASTEP IJUMP	2(I3,7X), 6(I2,8X)	Maximum number of iterations. Number of iterations between array printout.

Card	Set	Variable	Format	Description
		JSW1		J-node at start of dome inlet.
		JSW2		J-node at end of dome inlet.
		NUINJ		Number of axial injection points (cooling slots).
		NVINJ		Number of radial injection points.
27		USW	8E10.4	Axial velocity of dome inlet.
		VSW		Radial velocity of dome inlet.
		SWNO		Ratio of tangential to axial velocity at dome inlet.
		AFSW		Flow rate of fuel and air through dome inlet.
		FSW		Flow rate of fuel through dome inlet.
		TSW		Temperature at dome inlet.
28		NFNZ	2(I2,8X), 6E10.4	00 No liquid fuel nozzle; 01 Liquid fuel nozzle present.
		ISPRAY		Droplet evaporation routine is called. every ISPRAY iterations.
		TFUEL		Initial temperature of liquid fuel.
29		XO	8E10.4	X-location of origin of fuel nozzle spray.
		YO		Y-location of origin of fuel nozzle spray.
		ZO		Z-location of origin of fuel nozzle spray
		ALFA		Nozzle cone angle.
		BETA		Nozzle back angle.
		DELTA		Nozzle down angle.
		THETA1		Initial spray cone segment angle.
		THETA2		Final spray cone segment angle.
		RNSL		Number of spray cone rays.
		WFF		Fuel flow rate.
		SMD		Sauter mean diameter.
		VFUEL		Initial fuel droplet velocity.
		RFUEL		Radius of fuel nozzle. (Skip Set 29 if NFNZ=0)
30		IUINJ	8(I2,8X)	Skip Sets 30-35, if NUINJ=0. I node location of cooling slots
31		JUINJ	8(I2,8X)	J node location of cooling slots.
32		UINJ	8E10.4	Cooling slot axial velocity.
33		WUINJ	8E10.4	Cooling slot tangential velocity.

Card Set	Variable	Format	Description
34	AUINJ	8E10.4	Cooling slot mass flow rate.
35	TUINJ	8E10.4	Cooling slot temperature.
			Skip Sets 36-43, if NVINJ=0.
36	IVINJ	8(I2,8X)	I node location of radial injection.
37	JVINJ	8(I2,8X)	J node location of radial injection
38	KVINJ	8(I2,8X)	K node location of radial injection.
39	VINJ	8E10.4	Radial injection velocity.
40	EVINJ	8E10.4	Radial injection turbulent kinetic energy.
41	DVINJ	8E10.4	Radial injection turbulence length scale.
42	AVINJ	8E10.4	Radial injection mass flow rate.
43	TVINJ	8E10.4	Radial injection temperature.
44	NSOOT	8(I2,8X)	=0, SOOT calculations not performed; =1, SOOT calculations performed. soot calculation started after ERROR falls to SSOOT or after ISOOT number of iterations.
	ISOOT		
	MPART		Number of soot particle sizes.
			Skip Sets 45-48 if NSOOT=0.
45	SSOOT	8E10.4	See ISOOT.
	AO		Constant a_0 in soot nuclei formation rate, equation (6).
	ARCONN		Activation energy divided by gas constant in soot nucleus formation rate, equation (6).
	AAA		Constant a in soot formation rate, equation (8).
	BBB		Constant b in soot formation rate, equation (8).

Card Set	Variable	Format	Description
	FMG		Constant (f-g) in soot nucleus formation rate, equation (7).
	GO		Constant go in soot nucleus formation rate, equation (7).
	RHOP		Particle density.
46	PREXPS	8E10.4	Pre-exponent in soot oxidation rate, equation (11).
	ARCONS		Activation energy divided by gas constant in soot oxidation rate, equation (11).
	ALPHA		Temperature exponent in soot oxidation rate, equation (11).
	AAS		Exponent on fuel concentration in soot oxidation rate, equation (11).
	BBS		Exponent on oxygen concentration in soot oxidation rate, equation (11).
	DHR		Heat of fuel combustion reaction.
	CINCP		Incipient carbon/oxygen ratio for soot formation.
	TINCP		soot calculation bypassed if temperature < TINCP.
47	DPART	8E10.4	soot particle diameters (in microns).
48	FRACP	8E10.4	Relative rates of formation of soot particle sizes.
49	IRAD SRAD	I2,8X, E10.4	Radiation calculation started after ERROR falls to SRAD or after IRAD number of iterations. (Skip if ITRAD=1).
50	NNOX	3(I2,8X),	=0 NO _x calculations not performed; =1 NO _x calculations performed.
	INOX	2E10.4	NO _x calculations started after ERROR falls to SNOX or after INOX number of iterations.
	ITNOX		Number of iterations of NO _x solution at final iteration of flow solution.
	SNOX TNOX		See INOX. NO _x calculation bypassed if temperature < TNOX.

After these 50 card sets, the input to the chemical kinetics program CREK must be provided. This is described below in Tables B-1, B-2 and B-3.

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TABLE B-1. ELEMENTS INPUT CARDS.

Order	Contents	Format	Card Columns
First	ELEMENTS	3A4	1 to 8
Any	One card for each distinct element present in the chemical system. Each card contains: 1) Atomic symbol of element--must agree with that used in THERMØ data. 2) Atomic weight of the element 3) Values of oxidation state of the element (positive, negative or zero).	A2 F10.6 F10.6	1 to 2 10 to 19 20 to 29
Last	Blank Card	--	--

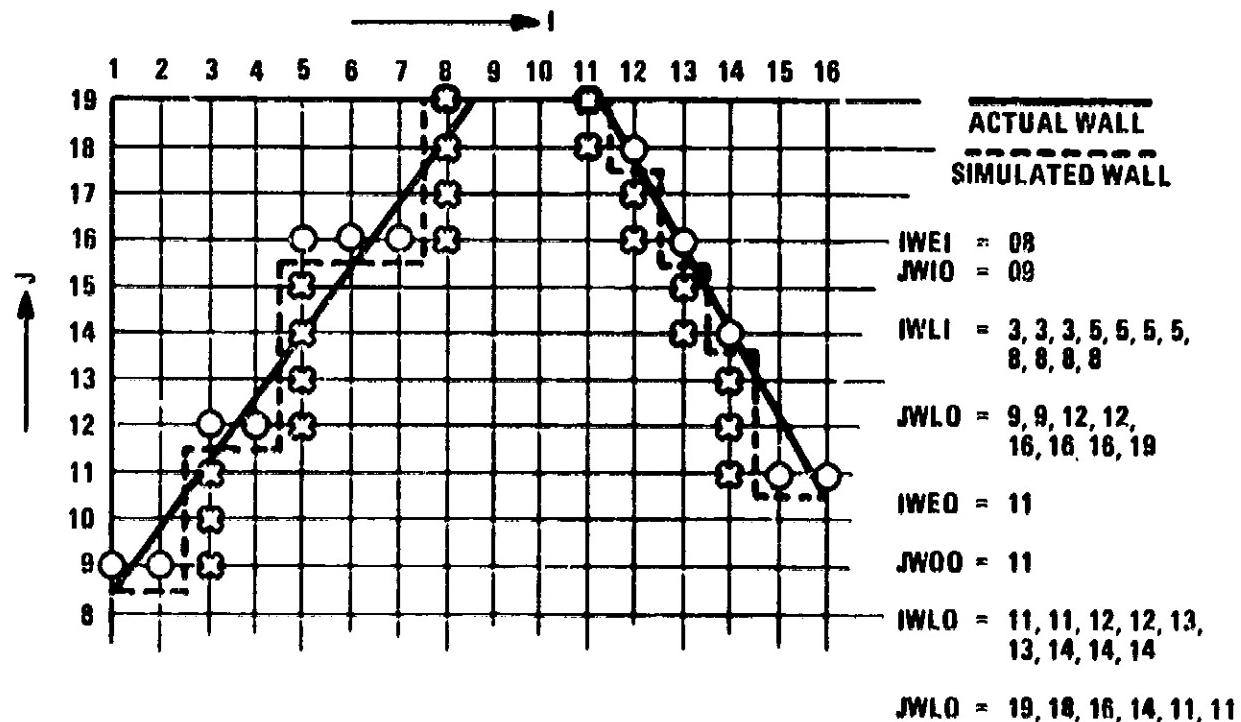


Figure B-1. Definitions of Inclined Wall Indices.

TABLE B-2. THERMO INPUT CARDS.

Order	Contents	Format	Card Columns
First	THERMO	3A4	1 to 6
Any	Sets of four cards <u>in sequence</u> for each species in the chemical system. The card formats for each set are, in order:		
First in set	1) Molecular symbol or name of species 2) Date 3) Atomic Symbols and formula 4) Phase (gas only, letter G) 5) Temperature range, deg K 6) Integer 1	3A4 2A3 4(A2,F3.0) A1 2F10.3 I15	1 to 12 19 to 24 25 to 44 45 46 to 65 80
Second in set	1) Coefficients (z_i , $i=1,5$) for upper temperature range. See Note A. 2) Integer 2	5E15.8 I5	1 to 75 80
Third in set	1) Coefficients z_6 and z_7 for upper temperature range, and z_3 for lower. See Note A. 2) Integer 3	5E15.8 I5	1 to 75 80
Fourth in set	1) Coefficients (z_i , $i=4,7$) for low temperature interval. See Note A. 2) Integer 4	4E15.8 I20	1 to 60 80
Last	Blank Card	--	--

Note A: The coefficients (z_i , $i=1,7$) are those which appear in the polynominal expression for the constant pressure specific heat.

TABLE B-3. MECHANISM INPUT CARDS.

Order	Contents	Format	Card Columns
First	MECHANISM	3A4	1 to 9
Any	One card for each distinct forward (or optionally, reverse) reaction step in the mechanism specified. Each card contains: 1) Molecular symbols of up to three reactant species. See Note A. 2) Molecular symbols of up to three product species. See Note A. 3) Exponent B_j . See Notes B and E. 4) Exponent N_j . See Note B 5) Activation temperature T_j , deg K. See Notes B and E. 6) Options: a) for forward reactions, date or comments, etc. b) for reverse reactions, REVERSE. See Note C. c) for global oxidative pyrolysis of hydrocarbon fuels, GLOBAL. See Note D. d) for rate data in cgs units, CGS. See Note E.	3(2A4) 3(2A4) F8.3 F8.3 F8.3 2A4 2A4 2A4 -- --	1 to 24 25 to 48 49 to 56 57 to 64 65 to 72 73 to 80 73 to 79 73 to 78 -- --
Last	Blank Card		

NOTES:

- A. Symbols must be identical to those used in THERMØ data cards.
- B. As used in modified Arrhenius expression
- $$k_j = 10^{B_j} T^j \exp(-T_j/T), \text{ with units}$$
- $m^3 \text{ kg-mole}^{-1} s^{-1}$ for bimolecular reactions, and
- $m^6 \text{ kg-mole}^{-2} s^{-1}$ for termolecular reactions.
- C. If REVERSE is specified, Columns 1 to 48 are ignored. Card with reverse rate data must therefore follow immediately the card with data for the associated forward reaction, and must be in same units.

TABLE B-3. MECHANISM INPUT CARDS (Contd.).

- D. All GLOBAL cards must precede other cards in MECHANISM data deck.
- E. If CGS is punched in Columns 73-75, B_j must correspond to $\text{cm}^3 \text{ gmol}^{-1} \text{ s}^{-1}$ or $\text{cm}^6 \text{ gmol}^{-2} \text{ s}^{-1}$, and T_j must be the activation energy, kcal/gmol.

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APPENDIX C
LIST OF FORTRAN VARIABLES

In this appendix a description of the Fortran variables is provided. Table C-1 contains the variables in the 3-D Combustor Program and Table C-2 contains the variables in the chemical kinetics program CREK.

TABLE C-1
LIST OF FORTRAN VARIABLES IN 3-D COMBUSTOR PROGRAM

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
A	STRAD	COFFICIENT IN TONA SOLUTION.
AAA	AUX,MAIN	CONSTANT IN SOOT FORMATION (SEE INPUT).
AAS	AUX,MAIN	EXPONENT ON FUEL CONCENTRATION IN SOOT OXIDATION RATE (SEE INPUT).!
AA1	AUX,MAIN INIT	EXPONENT ON SPECIES CONCENTRATION IN FIRST STEP OF HYDROCARBON OXIDATION SCHEME.
AA2	AUX,MAIN INIT	EXPONENT ON SPECIES CONCENTRATION IN SECOND STEP OF HYDROCARBON OXIDATION SCHEME.
AA3	AUX,MAIN INIT	EXPONENT ON SPECIES CONCENTRATION IN THIRD STEP OF HYDROCARBON OXIDATION SCHEME.
AA4	AUX,MAIN INIT	EXPONENT ON SPECIES CONCENTRATION IN FOURTH STEP OF HYDROCARBON OXIDATION SCHEME.
ABSOR	MAIN INIT AUXRAD	ABSORPTION COEFFICIENT (IF ITRAD=2).
ABSP	INIT AUX AUXRAD	ARRAY TO STORE ABSORPTION COEFFICIENT.
ALDEF	AUX,DATA	COEFFICIENTS TO LIMIT TEMPERATURE TO ACCOUNT FOR DISSOCIATION.
ACOND	SPRAY	COEFFICIENT IN THERMAL CONDUCTIVITY CALCULATION.
AEXP1	INIT	EXPONENT ON SPECIES CONCENTRATION IN FIRST STEP OF HYDROCARBON OXIDATION SCHEME(=AA1).
AEXP2	INIT	EXPONENT ON SPECIES CONCENTRATION IN SECOND STEP OF HYDROCARBON OXIDATION SCHEME(=AA2).
AEXP3	INIT	EXPONENT ON SPECIES CONCENTRATION IN THIRD STEP OF HYDROCARBON OXIDATION SCHEME(=AA3).
AEXP4	INIT	EXPONENT ON SPECIES CONCENTRATION IN FOURTH STEP OF HYDROCARBON OXIDATION SCHEME(=AA4).
AFSW	MAIN INIT	AIR+FUEL FLOW THROUGH DOME INLET.

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TABLE C-1 (CONTD.)

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
AK	DATA ALLMOD	VON KARMAN CONSTANT.
AKA,AKB	AUX	RATE CONSTANTS IN SOOT OXIDATION EXPRESSION.
AKFAC	MAIN INIT ALLMOD	INTERNALY DEFINED TURBULENT KINETIC ENERGIES ARE AKFAC TIMES THE APPROPRIATE VELOCITY SQUARED.
AKK,AKT	AUX	RATE CONSTANTS IN SOOT OXIDATION EXPRESSION.
AKZ	AUX	RATE CONSTANT IN SOOT OXIDATION EXPRESSION.
AL	INIT	TURBULENCE LENGTH SCALE.
ALFA	MAIN SPRAY	NOZZLE CONE ANGLE.
ALFAC	MAIN INIT ALLMOD	INTERNALY DEFINED TURBULENT LENGTH SCALES ARE ALFAC TIMES THE APPROPRIATE DISTANCE.
ALIN	INIT	INLET TURBULENCE LENGTH SCALE.
ALNHGT	INIT	LENGTH OF COMBUSTOR.
ALPHA	AUX,MAIN	TEMPERATURE EXPONENT IN SOOT OXIDATION RATE (SEE INPUT).
ALPHAS	AUXRAD	ABSORPTION COEFFICIENT.
ALX,ALXM	STRIDE	CONVECTION FLUX IN X DIRECTION.
ALXP,ALXL	STRIDE	CONVECTION FLUX IN X DIRECTION.
ALY,ALYM	STRIDE	CONVECTION FLUX IN Y DIRECTION.
ALYP,ALYI	STRIDE	CONVECTION FLUX IN Y DIRECTION.
ALZ,ALZM	STRIDE	CONVECTION FLUX IN Z DIRECTION.
ALZF,ALZI	STRIDE	CONVECTION FLUX IN Z DIRECTION.
AMASS	INIT	TOTAL AIR FLOW RATE.
AMT	SPRAY	FUEL EVAPORATION RATE FOR ONE TIME STEP.
AVII	MAIN AUX ALLMOD	LAMINAR VISCOSITY (SEE INPUT).

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TABLE C-1 (CONTD.)

FORTRAN VARIABLE		ROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
AND	AUX		SOOT NUCLEUS FORMATION RATE AT MEAN TEMPERATURE.
ANOD	AUX		SOOT NUCLEUS FORMATION RATE IN FLUID SURROUNDING FINE STRUCTURES.
ANOSTR	AUX		SOOT NUCLEUS FORMATION RATE IN FINE STRUCTURES.
ANUC	ALL		SOOT NUCLEUS CONCENTRATION.
AO	AUX,MAIN		CONSTANT IN SOOT NUCLEUS FORMATION RATE (SEE INPUT).
AP	SOLVE		COEFFICIENT IN TDMA SOLUTION.
APP	SOLVE		COEFFICIENT IN CYCLIC TDMA SOLUTION.
ARCONN	AUX,MAIN		ACTIVATION ENERGY DIVIDED BY GAS CONSTANT IN SOOT NUCLEUS FORMATION RATE (SEE INPUT).
ARCONS	AUX,MAIN		ACTIVATION ENERGY DIVIDED BY GAS CONSTANT IN SOOT OXIDATION RATE (SEE INPUT).
ARCON1	AUX,MAIN INIT		ACTIVATION ENERGY IN FIRST STEP OF HYDROCARBON OXIDATION SCHEME, DIVIDED BY GAS CONSTANT.
ARCON2	AUX,MAIN INIT		ACTIVATION ENERGY IN SECOND STEP OF HYDROCARBON OXIDATION SCHEME, DIVIDED BY GAS CONSTANT.
ARCON3	AUX,MAIN INIT		ACTIVATION ENERGY IN THIRD STEP OF HYDROCARBON OXIDATION SCHEME, DIVIDED BY GAS CONSTANT.
ARCON4	AUX,MAIN INIT		ACTIVATION ENERGY IN FOURTH STEP OF HYDROCARBON OXIDATION SCHEME, DIVIDED BY GAS CONSTANT.
ARFA	ALLMOD STRIDE		AREA OF CONTROL VOLUME SURFACE.
AREAT	AUX		SOOT PARTICLE SURFACE AREA.
ARG	AUX		TEMPORARY USAGE.
ARG	SPRAY		SQUARE OF DROPLET DIAMETER.
ARRHEN	AUX		ARRHENIUS REACTION RATE.
AS	SPRAY		DROPLET SURFACE AREA.
ASH	ALLMOD		ABSOLUTE OF CONTINUITY ERROR.
ASUR	CRFK		SEE TABLE C-2.

TABLE C-1 (CONTD.)

FORTRAN VARIABLE	SUBROUTINE	DEFINITION
	WMFRE	
	DEFINFO OR USED OFTEN	
ASW	INIT	FLOW RATE OF AIR THROUGH DOME INLET.
ASWRLR	INIT	DOME INLET AREA.
AT	SPRAY	QUANTITY USED IN THERMAL CONDUCTIVITY CALCULATION.
AUENJ	MAIN ALLMOD	MASS FLOW RATE THROUGH FILM COOLING SLOT.
AVENJ	MAIN ALLMOD	MASS FLOW RATE THROUGH DILUTION HOLES.
AXM	STRIDE STRAD ALLMOD SOLVE	FINITE-DIFFERENCE COEFFICIENT IN X- DIRECTION.
AXMK	SOLVE	FINITE-DIFFERENCE COEFFICIENT IN X- DIRECTION, USED IN CYCLIC TDMA.
AXP	STRIDE STRAD ALLMOD SOLVE	FINITE-DIFFERENCE COEFFICIENT IN X+ DIRECTION.
AXPK	SOLVE	FINITE-DIFFERENCE COEFFICIENT IN X+ DIRECTION, USED IN CYCLIC TDMA.
AYM	STRIDE STRAD ALLMOD SOLVE	FINITE-DIFFERENCE COEFFICIENT IN Y- DIRECTION.
AYMK	SOLVE	FINITE-DIFFERENCE COEFFICIENT IN Y- DIRECTION, USED IN CYCLIC TDMA.
AYP	STRIDE STRAD ALLMOD SOLVE	FINITE-DIFFERENCE COEFFICIENT IN Y+ DIRECTION.
AYPK	SOLVE	FINITE-DIFFERENCE COEFFICIENT IN Y+ DIRECTION, USED IN CYCLIC TDMA.
AZM	STRIDE STRAD ALLMOD SOLVE	FINITE-DIFFERENCE COEFFICIENT IN Z- DIRECTION.

TABLE C-1 (CONTD.)

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
AZMK	SOLVE	FINITE-DIFFERENCE COEFFICIENT IN Z- DIRECTION, USED IN CYCLIC TDMA.
AZP	STRIDE STRAD ALLMOD SOLVE	FINITE-DIFFERENCE COEFFICIENT IN Z+ DIRECTION.
AZPK	SOLVE	FINITE-DIFFERENCE COEFFICIENT IN Z+ DIRECTION, USED IN CYCLIC TDMA.
A1-A6	AUX	TEMPORARY USAGE.
A4	INIT	TEMPORARY USAGE OF FLOW AREA.
B	STRAD	COEFFICIENT IN TDMA SOLUTION.
B8B	AUX,MAIN	CONSTANT IN SOOT FORMATION (SEE INPUT).
B8S	AUX,MAIN INIT	EXPONENT ON O2 CONCENTRATION IN SOOT OXIDATION RATE (SEE INPUT).
B81	AUX,MAIN INIT	EXPONENT ON SPECIES CONCENTRATION IN FIRST STEP OF HYDROCARBON OXIDATION SCHEME.
B82	AUX,MAIN INIT	EXPONENT ON SPECIES CONCENTRATION IN SECOND STEP OF HYDROCARBON OXIDATION SCHEME.
B83	AUX,MAIN INIT	EXPONENT ON SPECIES CONCENTRATION IN THIRD STEP OF HYDROCARBON OXIDATION SCHEME.
B84	AUX,MAIN INIT	EXPONENT ON SPECIES CONCENTRATION IN FOURTH STEP OF HYDROCARBON OXIDATION SCHEME.
RCOND	SPRAY	COEFFICIENT IN THERMAL CONDUCTIVITY CALCULATION.
BEE	SPRAY	DRIVING FORCE FOR MASS TRANSFER.
BETA	MAIN SPRAY	NOZZLE BACK ANGLE.
BEXP1	INIT	EXPONENT ON SPECIES CONCENTRATION IN FIRST STEP OF HYDROCARBON OXIDATION SCHEME(=B81).
BEXP2	INIT	EXPONENT ON SPECIES CONCENTRATION IN SECOND STEP OF HYDROCARBON OXIDATION SCHEME(=B82).
BEXP3	INIT	EXPONENT ON SPECIES CONCENTRATION IN THIRD STEP OF HYDROCARBON OXIDATION SCHEME(=B83).

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TABLE C-1 (CONTD.)

FORTRAN VARIABLE	SUBROUTINE	DEFINITION
BEXP4	INIT	EXponent ON SPECIES CONCENTRATION IN FOURTH STEP OF HYDROCARBON OXIDATION SCHEME(=BA4).
RK	SOLVE	TEMPORARY USAGE.
BP	SOLVE	COEFFICIENT IN TDMA SOLUTION.
BPP	SOLVE	COEFFICIENT IN CYCLIC TDMA SOLUTION.
RT	SPRAY	QUANTITY USED IN THERMAL CONDUCTIVITY CALCULATION.
CANG	MAIN	CONSTANT TO CONVERT UNITS ON ANGLES.
CARR	AUX	MASS FRACTION OF ELEMENTAL CARBON.
CC1	AUX,MAIN INIT	EXponent ON SPECIES CONCENTRATION IN FIRST STEP OF HYDROCARBON OXIDATION SCHEME.
CC2	AUX,MAIN INIT	EXponent ON SPECIES CONCENTRATION IN SECOND STEP OF HYDROCARBON OXIDATION SCHEME.
CC3	AUX,MAIN INIT	EXponent ON SPECIES CONCENTRATION IN THIRD STEP OF HYDROCARBON OXIDATION SCHEME.
CC4	AUX,MAIN INIT	EXponent ON SPECIES CONCENTRATION IN FOURTH STEP OF HYDROCARBON OXIDATION SCHEME.
CD	AUX ALLMOD	CONSTANT IN TURBULENCE MODEL.
CD0,CD1	SPRAY	DROPLET DRAG COEFFICIENT.
CERU1	INIT	EDDY-BREAK-UP CONSTANT FOR FIRST STEP OF HYDROCARBON OXIDATION SCHEME.
CERU2	INIT	EDDY-BREAK-UP CONSTANT FOR SECOND STEP OF HYDROCARBON OXIDATION SCHEME.
CERU3	INIT	EDDY-BREAK-UP CONSTANT FOR THIRD STEP OF HYDROCARBON OXIDATION SCHEME.
CERU4	INIT	EDDY-BREAK-UP CONSTANT FOR FOURTH STEP OF HYDROCARBON OXIDATION SCHEME.
CENER	MAIN	CONSTANTS TO CONVERT UNITS ON ENERGY.
CEXP1	AUX,INIT	EXponent N SPECIES CONCENTRATION IN FIRST STEP OF HYDROCARBON OXIDATION SCHEME(=CC1).

TABLE C-1 (CONTD.)

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
CEXP2	AUX,INIT	EXponent ON SPECIES CONCENTRATION IN SECOND STEP OF HYDROCARBON OXIDATION SCHEME(=CC2).
CEXP3	AUX,INIT	EXponent ON SPECIES CONCENTRATION IN THIRD STEP OF HYDROCARBON OXIDATION SCHEME(=CC3).
CEXP4	AUX,INIT	EXponent ON SPECIES CONCENTRATION IN FOURTH STEP OF HYDROCARBON OXIDATION SCHEME(=CC4).
CFR	ALLMOD AUX INIT	SKIN FRICTION COEFFICIENT.
CINCP	AUX,MAIN	INCIPENT CARBON/OXYGEN RATIO FOR SOOT FORMATION.
CK	SOLVE	TEMPORARY USAGE.
CLEND	MAIN	CONSTANTS TO CONVERT UNITS ON LENGTHS.
CLENV	MAIN	CONSTANTS TO CONVERT UNITS ON VELOCITIES.
CMASS	MAIN	CONSTANTS TO CONVERT UNITS ON MASS.
CNO	OUTPUT	NOX EMISSIONS INDEX.
COND1	SPRAY	Thermal Conductivity Of Fuel Vapors.
CONS	SPRAY	TEMPORARY USAGE.
CONS2	AUX	TEMPORARY USAGE.
CON2	SPRAY	FRACTION OF FUEL EVAPORATED.
COSA	SPRAY	COSINE OF HALF THE NOZZLE CONE ANGLE.
COSB	SPRAY	COSINE OF NOZZLE BACK ANGLE.
COSD	SPRAY	COSINE OF NOZZLE DOWN ANGLE.
COST	SPRAY	COSINE OF CURRENT SPRAY CONE SEGMENT ANGLE.
CP	AUX ALLMOD	CONSTANT PRESSURE SPECIFIC HEAT.
CPI	INIT AUX	CONSTANT PRESSURE SPECIFIC HEAT.
CPLF	SPRAY	SPECIFIC HEAT OF LIQUID DROPLET.

TABLE C-1 (CONTD.)

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
CPR	AUX	CONSTANT PRESSURE SPECIFIC HEAT.
CPRESS	MAIN	CONSTANTS TO CONVERT UNITS ON PRESSURE.
CPSUM	ALLMOD AUX	CONSTANT PRESSURE SPECIFIC HEAT OF GAS MIXTURE.
CP1	SPRAY	SPECIFIC HEAT.
CR1	AUX,MAIN	EDDY-BREAK-UP CONSTANT IN FIRST STEP OF HYDROCARBON OXIDATION SCHEME(=CERU1).
CR2	AUX,MAIN	EDDY-BREAK-UP CONSTANT IN SECOND STEP OF HYDROCARBON OXIDATION SCHEME(=CERU2).
CR3	AUX,MAIN	EDDY-BREAK-UP CONSTANT IN THIRD STEP OF HYDROCARBON OXIDATION SCHEME(=CFBU3).
CR4	AUX,MAIN	EDDY-BREAK-UP CONSTANT IN FOURTH STEP OF HYDROCARBON OXIDATION SCHEME(=CFBU4).
CSMO	OUTPUT	SMOKE EMISSIONS INDEX.
CTEMP	MAIN	CONSTANT TO CONVERT UNITS ON TEMPERATURE.
CX	STRIDE	TEMPORARY STORAGE FOR CONVECTIVE/DIFFUSIVE FLUX IN X DIRECTION.
CXU,CXUP	STRIDE	TEMPORARY STORAGE FOR CONVECTIVE FLUX IN X DIRECTION.
CXX	INIT AUX MAIN	NUMBER OF CARBON ATOMS IN THE FUEL.
CY	STRIDE	TEMPORARY STORAGE FOR CONVECTIVE/DIFFUSIVE FLUX IN Y DIRECTION.
CYP		NOT USED.
CYU,CYUP	STRIDE	TEMPORARY STORAGE FOR CONVECTIVE FLUX IN Y DIRECTION.
CZ	STRIDE	TEMPORARY STORAGE FOR CONVECTIVE/DIFFUSIVE FLUX IN Z DIRECTION.
CZP		NOT USED.
CZU,CZUP	STRIDE	TEMPORARY STORAGE FOR CONVECTIVE FLUX IN Z DIRECTION.
CA	AUX,MAIN	CONSTANT IN TURBULENCE MODEL.

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TABLE C-1 (CONTD.)

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
C2	AUX,MAIN	CONSTANT IN TURBULENCE MODEL.
DANG	SPRAY	DELTA(ANGLE).
DELTA	SPRAY MAIN	FUEL NOZZLE DOWN ANGLE.
DELTAT	AUX	TEMPERATURE RISE.
DEN	AUX,MAIN	DENSITY (SEE INPUT).
DENOM	SOLVE	TEMPORARY USAGE.
DENST	AUX	DENSITY.
DENSTY	STRIDE	DENSITY.
DEVAP	SPRAY	FRACTION OF FUEL EVAPORATED IN ONE TIME STEP.
DFAC	MAIN STRIDE	QUANTITY USED TO GRADUALLY INTRODUCE 2 DIRECTION DIFFUSION.
DFTW	TSOLVE	DIFFERENTIAL OF HEAT TRANSFER W.R.T. TEMPERATURE.
DHR	AUX,MAIN	HEAT OF FUEL COMBUSTION REACTION.
DIA	SPRAY	INSTANTANEOUS DROPLET DIAMETER.
DIA0	SPRAY	INITIAL DROPLET DIAMETER.
DIST	ALLMOD AUX STRIDE	INTERNOAL DISTANCE.
DIVG	STRIDE ALLMOD	MASS IMBALANCE AT A CONTROL VOLUME.
DK	SOLVE	TEMPORARY USAGE.
DLIM	SPRAY	CONSTANT TO LIMIT TIME STEP.
DM	SPRAY	DROPLET MASS.
DMDOT	OUTPUT	MASS FLOW RATE.
DP	SOLVE	COEFFICIENT IN CYCLIC TOMA SOLUTION.
DPART	AUX,MAIN	SOOT PARTICLE DIAMETERS.

TABLE C-1 (CONTD.)

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
DQCH	TSOLVE	HEAT TRANSFER COEFFICIENT.
DQRH	TSOLVF	DIFFERENTIAL OF RADIATION HEAT TRANSFER W.R.T. TEMPERATURE.
DRHOOP	STPIDE	PARTIAL DERIVATIVE OF DENSITY W.R.T. PRESSURE.
DSACO	AUX	TEMPORARY USAGE IN CO SOURCE TERM.
DSOFU	AUX	TEMPORARY USAGE IN FUEL SOURCE TERM.
DSOH	AUX	TEMPORARY USAGE IN ENTHALPY SOURCE TERM.
DSODT	PUTPUT	TEMPORARY USAGE.
DSOSP	AUX	TEMPORARY USAGE IN CXHY-2 AND H2 SOURCE TERMS.
DSMD	SPRAY	RATIO OF DROPLET DIAMETER TO SMD.
DT	STRIDE	TIME INCREMENT.
DTF	SPRAY	TEMPERATURE RISE OF DROPLET.
DTHTA	SPRAY	DIFFERENCE BETWEEN INITIAL AND FINAL SPRAY CONE SEGMENT ANGLES.
DTI	SPRAY	LIMIT ON TIME STEP TO AVOID NUMERICAL INSTABILITY.
DTI1-7	SPRAY	LIMITS ON TIME STEP TO AVOID NUMERICAL INSTABILITY.
DII	STRIDE SOLVE AUX	PRESSURE-VELOCITY COEFFICIENT FOR U-VELOCITY.
DUDXM	AUX	PARTIAL DERIVATIVE OF U W.R.T. X AT I LOCATION.
DUDXP	AUX	PARTIAL DERIVATIVE OF U W.R.T. X AT I+1 LOCATION.
DUDYM	AUX	PARTIAL DERIVATIVE OF U W.R.T. Y AT I LOCATION.
DUDYP	AUX	PARTIAL DERIVATIVE OF U W.R.T. Y AT I+1 LOCATION.
DUDZM	AUX	PARTIAL DERIVATIVE OF U W.R.T. Z AT I LOCATION.
DUDZP	AUX	PARTIAL DERIVATIVE OF U W.R.T. Z AT I+1 LOCATION.
DUDXJ	AUX	PARTIAL DERIVATIVE OF UI W.R.T. XJ.
DV	STRIDE SOLVE AUX	PRESSURE-VELOCITY COEFFICIENT FOR V-VELOCITY.

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TABLE C-1 (CONTD.)

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
DVDXM	AUX	PARTIAL DERIVATIVE OF V W.R.T. X AT J LOCATION.
DVDXP	AUX	PARTIAL DERIVATIVE OF V W.R.T. X AT J+1 LOCATION.
DVDY	AUX	VELOCITY GRADIENT NEAR A WALL.
DVDYM	AUX	PARTIAL DERIVATIVE OF V W.R.T. Y AT J LOCATION.
DVDYP	AUX	PARTIAL DERIVATIVE OF V W.R.T. Y AT J+1 LOCATION.
DVDZM	AUX	PARTIAL DERIVATIVE OF V W.R.T. Z AT J LOCATION.
DVDZP	AUX	PARTIAL DERIVATIVE OF V W.R.T. Z AT J+1 LOCATION.
DVINJ	INIT MAIN	RADIAL INJECTION TURBULENCE LENGTH SCALE.
DW	STRIDE SOLVE AUX ALLMOD	PRESSURE-VELOCITY COEFFICIENT FOR W-VELOCITY.
DWDXM	AUX	PARTIAL DERIVATIVE OF W W.R.T. X AT K LOCATION.
DWDXP	AUX	PARTIAL DERIVATIVE OF W W.R.T. X AT K+1 LOCATION.
DWDYM	AUX	PARTIAL DERIVATIVE OF W W.R.T. Y AT K LOCATION.
DWDYP	AUX	PARTIAL DERIVATIVE OF W W.R.T. Y AT K+1 LOCATION.
DWDZM	AUX	PARTIAL DERIVATIVE OF W W.R.T. Z AT K LOCATION.
DWDZP	AUX	PARTIAL DERIVATIVE OF W W.R.T. Z AT K+1 LOCATION.
DX	AUX	INTERNODAL DISTANCE IN X DIRECTION.
DX	SPRAY	DISTANCE TRAVELED BY DROPLET IN X DIRECTION.
DY	INIT AUX	INTERNODAL DISTANCE IN Y DIRECTION.
DY	SPRAY	DISTANCE TRAVELED BY DROPLET IN Y DIRECTION.
DZ	AUX INIT	INTERNODAL DISTANCE IN Z DIRECTION.
DZ	SPRAY	DISTANCE TRAVELED BY DROPLET IN Z DIRECTION.
E	ALLMOD DATA	CONSTANT E IN LOG-LAW OF THE WALL.

TABLE C-1 (CONTD.)

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
EDK	STRIDE AUX	DISSIPATION DIVIDED BY TURBULENCE ENERGY.
EDKIJ	STRIDE	DISSIPATION DIVIDED BY TURBULENCE ENERGY AT NODE I,J,K.
EDK2	AUX	DISSIPATION DIVIDED BY TURBULENCE ENERGY SQUARED.
EE	SPRAY	CONSTANT IN DROPLET BOILING POINT CALCULATION.
EMOT	AUX	RATE OF MASS TRANSFER BETWEEN FINE STRUCTURES AND SURROUNDING FLUID.
EMOOTR	AUX	TEMPORARY USAGE.
EMI	INIT AUX TSOLVE ALLMOD	=EMISH/(2.0-EMISH).
EMTSIN	INIT	INLET EMISSIVITY.
EMISR	INIT ALLMOD	GAS EMISSIVITY.
EMISH	ALLMOD INIT	WALL EMISSIVITY.
EMIN	AUX	TEMPORARY USAGE.
EMP	AUX	MASS OF SOOT PARTICLE.
EMPR	AUX	MASS FRACTION OF PRODUCTS.
EMV	STRIDE	TOTAL CONVECTIVE AND DIFFUSIVE MASS INFLOW INTO A FINITE-DIFFERENCE CELL; SEE TABLE C-2.
ENM	AUX	MEAN SOOT PARTICLE CONCENTRATION.
ENND	AUX	SOOT PARTICLE CONCENTRATION IN FLUID SURROUNDING FINE STRUCTURES.
ENNRH1	AUX	ENM DIVIDED BY GAS DENSITY.
ENNSTR	AUX	SOOT PARTICLE CONCENTRATION IN FINE STRUCTURES.
END	AUX	SOOT NUCLEUS CONCENTRATION IN FLUID SURROUNDING FINE STRUCTURES.

TABLE C-1 (CONT'D.)

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
ENRHO	AUX	MEAN SOOT NUCLEUS CONCENTRATION DIVIDED BY GAS DENSITY.
ENSTP	AUX	SOOT NUCLEUS CONCENTRATION IN FINE STRUCTURES.
ENSTR1	AUX	TEMPORARY USAGE.
ENSTR2	AUX	TEMPORARY USAGE.
EP	SOLVE	COEFFICIENT IN CYCLIC TOMA SOLUTION.
FR	CREK	EQUIVALENCE RATIO, SEE TABLE C-2.
ERROR	MAIN	PROGRAM WILL TERMINATE IF TOTAL ERROR IN MASS BECOMES LESS THAN THIS VALUE.
ER1	INIT	ACTIVATION ENERGY FOR THE FIRST STEP OF HYDROCARBON OXIDATION SCHEME, DIVIDED BY GAS CONSTANT (=ARCON1).
ER2	INIT	ACTIVATION ENERGY FOR THE SECOND STEP OF HYDROCARBON OXIDATION SCHEME, DIVIDED BY GAS CONSTANT (=ARCON2).
ER3	INIT	ACTIVATION ENERGY FOR THE THIRD STEP OF HYDROCARBON OXIDATION SCHEME, DIVIDED BY GAS CONSTANT (=ARCON3).
ER4	INIT	ACTIVATION ENERGY FOR THE FOURTH STEP OF HYDROCARBON OXIDATION SCHEME, DIVIDED BY GAS CONSTANT (=ARCON4).
ET	SPRAY	VARIABLE IN DROPLET BOILING POINT CALCULATION.
EVAP	SPRAY ALLMOD STRIKE	EVAPORATION RATE OF LIQUID FUEL.
EVAPIH-W	SPRAY	INTERPHASE MOMENTUM TRANSFER IN X,Y,Z DIRECTIONS.
EVINJ	INIT MAIN	RADIAL INJECTION TURBULENCE ENERGY.
EVSI	SPRAY ALLMOD	ARRAY USED TO STORE INTERPHASE MOMENTUM TRANSFER.
F	ALL	ARRAY USED TO STORE DEPENDENT VARIABLES.
FAC	SPRAY	TEMPORARY USAGE.

TABLE C-1 (CONTD.)

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
FACP	AUXRAD	TEMPORARY USAGE.
FAV	AUX	AVERAGE RADIATION FLUX.
FCH	ALL	INTERMEDIATE HYDROCARBON CONCENTRATION.
FDFU		NOT USED.
FEND	SOLVE	QUANTITY USED IN CYCLIC TDMA.
FEVAP	SPRAY	FRACTION OF FUEL EVAPORATED.
FEXTT	INIT	UNAURNT FUEL MASS FRACTION.
FH2	ALL	HYDROGEN MASS FRACTION.
FK	TINIT	INLET TURBULENCE KINETIC ENERGY.
FKFU		NOT USED.
FL0	INIT	FLOW RATE AT EACH AXIAL STATION.
FL0W	OUTPUT	MASS FLOW RATE.
FL0WIN	TINIT ALLMOD	INLET MASS FLOW RATE.
FL0WOT	ALLMOD	FLOW RATE AT EXIT PLANE.
FLPCO2	INIT AUX AUXRAD	CO2 MASS FRACTION.
FLPE	AUX AUXRAD	EMISSIVE POWER.
FLPH2O	TINIT AUX AUXRAD	H2O MASS FRACTION.
FLPN2	TINIT AUX AUXRAD	N2 MASS FRACTION.
FLPOX	INIT AUX AUXRAD SPRAY	O2 MASS FRACTION.

TABLE C-1 (CONT'D.)

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
FLPTE	AUX AUXRAD	TEMPERATURE.
FLZP	SOLVE	F VALUE AT NODE LZP.
FMA		NOT USED.
FMG	AUX,MAIN	CONSTANT IN SOOT NUCLEUS FORMATION RATE (SEE INPUT).
FMGF	AUX	TEMPORARY USAGE.
FQ	CREK	SEE TABLE C-2.
FRACP	AUX,MAIN	RELATIVE RATES OF FORMATION OF SOOT PARTICLE SIZES.
FRACT	SPRAY	CUMULATIVE MASS FRACTION OF DROPLETS IN DIFFERENT SIZE GROUPS.
FS	ALL	ARRAY USED TO STORE SPECIES MASS FRACTIONS.
FSLP	STRIDE	TEMPORARY STORAGE FOR FSILP%.
FST	INIT	STOICHIOMETRIC VALUE OF MIXTURE FRACTION.
FSTDIC	INIT AUX	STOICHIOMETRIC VALUE OF MIXTURE FRACTION.
FSW	INIT MAIN	FLOW RATE OF FUEL THROUGH DOME INLET.
FTW	TSOLVE	RADIATIVE+CONVECTIVE HEAT TRANSFER.
FUARAT	INIT	FUEL/AIR RATIO.
FUR	INIT AUX AUXRAD	MASS FRACTION OF BURNED FUEL.
FUEL	INIT	FUEL FLOW RATE AT EACH AXIAL STATION.
FUFLF	INIT	MASS FRACTION OF UNBURNED FUEL.
FUFLI	INIT	MIXTURE FRACTION.
FUELS	INIT	Liquid FUEL FLOW RATE AT EACH AXIAL STATION.
FUMCP	INIT MAIN	INITIAL ESTIMATE OF CO MASS FRACTION.

TABLE C-1 (CONTD.)

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
FUMSH	INIT	FUEL/AIR RATIO AT DOME INLET.
FUOX	INIT	MIXTURE FRACTION AT EACH AXIAL STATION.
FUOXSH	INIT	MIXTURE FRACTION AT DOME INLET.
FUT	STRIDE	MIXTURE FRACTION.
FUTOT	INIT	TOTAL FUEL FLOW RATE.
FX	SPRAY	DRAG FORCE ON DROPLET IN X DIRECTION.
FXN	ALL	INTERPOLATION FACTOR FOR X- DIRECTION NODAL DISTANCES.
FXP	ALL	INTERPOLATION FACTOR FOR X+ DIRECTION NODAL DISTANCES.
FY	SPRAY	DRAG FORCE ON DROPLET IN Y DIRECTION.
FYN	ALL	INTERPOLATION FACTOR FOR Y- DIRECTION NODAL DISTANCES.
FYP	ALL	INTERPOLATION FACTOR FOR Y+ DIRECTION NODAL DISTANCES.
FZ	SPRAY	DRAG FORCE ON DROPLET IN Z DIRECTION.
FZN	ALL	INTERPOLATION FACTOR FOR Z- DIRECTION NODAL DISTANCES.
FZP	ALL	INTERPOLATION FACTOR FOR Z+ DIRECTION NODAL DISTANCES.
GAM	ALL	DIFFUSION COEFFICIENT.
GAMAS	AUX	MASS FRACTION OF FLUID IN FINE STRUCTURES.
GANDOL	ALL400	TEMPORARY USAGE.
GAMLP	AUX STRIDE	DIFFUSION COEFFICIENT AT NODE LP.
GAMLXN	AUX	DIFFUSION COEFFICIENT AT NODE LXM.
GAMLYN	AUX	DIFFUSION COEFFICIENT AT NODE LYH.
GAMLZH	AUX	DIFFUSION COEFFICIENT AT NODE LZH.
GAMM	AUX	AVERAGE DIFFUSION COEFFICIENT.
GAMP	AUX	AVERAGE DIFFUSION COEFFICIENT.
GAMPT2	AUX	AVERAGE DIFFUSION COEFFICIENT.

TABLE C-1 (CONTD.)

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
GASCON	AUX,MAIN	UNIVERSAL GAS CONSTANT DIVIDED BY MOLECULAR WEIGHT OF AIR.
GFNR	AUX	GENERATION RATE OF TURBULENCE ENERGY.
GO	AUX,MAIN	CONSTANT IN SOOT NUCLEUS FORMATION RATE (SEE INPUT).
GPSI	AUX	=GAMAS*PSI.
GPSTR	AUX	GPSI DIVIDED BY DENSITY OF FINE STRUCTURES.
H	ALL	ENTHALPY.
HCO	INIT	HEAT OF COMBUSTION OF CO.
HCRAT	INIT	TEMPORARY USAGE.
HDRFL	ALLMOD	TEMPORARY USAGE.
HEIGHT	INIT	CHANNEL HEIGHT OF COMBUSTOR.
HEVAP	SPRAY	HEAT OF VAPORIZATION OF LIQUID FUEL.
HFU	MAIN INIT	HEAT OF FORMATION OF FUEL.
HFUEL	SPRAY	HEAT OF COMBUSTION OF FUEL.
HPI	ALLMOD AUX INIT	TEMPORARY USAGE FOR ENTHALPY.
HSURC	STRIDE	MIXTURE ENTHALPY.
HSUM	AUX ALLMOD INIT STRIDE	ENTHALPY OF GAS MIXTURE.
HT	SPRAY	HEAT TRANSFER COEFFICIENT FOR DROPLET HEATUP.
HTC	ALLMOD AUX	HEAT TRANSFER COEFFICIENT.
HTCEXT		EXTERNAL HEAT TRANSFER COEFFICIENT (NOT USED).
HTCI	TSOLVE	HEAT TRANSFER COEFFICIENT.
HYY	INIT MAIN AUX	NUMBER OF HYDROGEN ATOMS IN FUEL.

TABLE C-1 (CONTD.)

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
H1,H2	INIT	ENTHALPY(TEMPORARY USAGE).
IB	SPRAY	INDEX TO DENOTE LOCATION OF I BOUNDARY.
ICONVG	STRIDE	*0, CHEMICAL KINETICS SOLUTION NOT CONVERGED. *1, CHEMICAL KINETICS SOLUTION CONVERGED.
ICTOMA	SOLVE PAIN	NUMBER OF SWEEPS FOR EACH VARIABLE IN SOLVE (SEE INPUT).
IDCH	DATA, INIT	INDEX FOR INTERMEDIATE HYDROCARBON MASS FRACTION. AUX
IDCO	DATA, INIT	INDEX FOR CO MASS FRACTION. AUX
IDCO2	DATA, INIT	INDEX FOR CO2 MASS FRACTION. AUX
IDFU	DATA, INIT	INDEX FOR FUEL MASS FRACTION. AUX SPRAY STRIDE ALLMOD
IDH1	DATA	INDEX FOR H ATOM MASS FRACTION.
IDH2	DATA, INIT	INDEX FOR H2 MASS FRACTION. AUX
IDH2O	DATA, INIT	INDEX FOR H2O MASS FRACTION. AUX
IDK	AUX	*01 FOR RATE CONTROLLED COMBUSTION, *02 FOR MIXING CONTROLLED COMBUSTION.
IDNO	DATA	INDEX FOR NO MASS FRACTION.
IDNO2	DATA	INDEX FOR NO2 MASS FRACTION.
IDN1	DATA	INDEX FOR N ATOM MASS FRACTION.
IDN2	DATA, INIT	INDEX FOR N2 MASS FRACTION. ALLMOD AUX STRIDE
IDO	DATA	INDEX FOR O ATOM MASS FRACTION.

TABLE C-1 (CONTD.)

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
ID0H	DATA	INDEX FOR OH MASS FRACTION.
ID02	DATA, INIT ALLMOD UX STRIDE	INIT INDEX FOR O2 MASS FRACTION.
IDW	MAIN ALLMOD STRIDE AUX	TYPE OF BOUNDARY AT J=1(SEE INPUT).
IE	ALL	ENDING VALUE OF I (LOCAL VALUE OF INLO).
IEHO	FPRINT	FINDING VALUE OF I FOR PRINTOUT.
IG	SPRAY	DO-LOOP INDEX FOR DROPLET SIZE GROUPS.
IGAM1-2	DATA ALLMOD	INDEX TO DENOTE TYPE OF BOUNDARY CONDITION FOR A DEPENDENT VARIABLE.
IGPNT	SPRAY	INDEX FOR DIAGNOSTIC PRINTOUT.
IHCPS	H_CPS	INDEX FOR CALCULATING THERMODYNAMIC PROPERTIES.
IJUMP	PUTPUT PATN	NUMBER OF ITERATIONS BETWEEN PRINTOUT.
IKIN	INIT ALLMOD AUX STRIDE	INDEX FOR BOUNDARY CONDITIONS.
IL	STRIDE	TEMPORARY USAGE.
IL	SPRAY	DO-LOOP INDEX FOR DROPLET RAYS.
ILC	CREK	SEE TABLE C-2.
ILH	CREK	SEE TABLE C-2.
ILOC	SPRAY	I INDEX FOR DROPLET LOCATION.
IMAT	CREK	SEE TABLE C-2.
IMAX	MAIN ALLMOD	I LOCATION OF MAXIMUM CONTINUITY ERROR.
INCOMP		INDEX TO DENOTE COMPRESSIBILITY(NOT USED).

TABLE C-1 (CONT'D.)

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
IND	STRIDE	INDEX USED IN RADIATION CALCULATIONS.
INDEX	ALL MOD	+1 IF U VELOCITY IS NEGATIVE AT EXIT, OTHERWISE =0.
INDEX	SPRAY	INDEX FOR TYPE OF BOUNDARY.
IND	SOLVE	DO-LOOP INDEX.
INOMAX	SOLVE	NUMBER OF TDM SWEEPS.
INOK	MAIN STRIDE	INDEX TO DECIDE ON NOX CALCULATIONS(SEE SNOX).
INTAPE	MAIN	INDEX FOR INITIAL FIELD PRINTOUT(SEE INPUT).
INV	INIT STRIDE	TEMPORARY USAGE.
IOLD	SPRAY	PREVIOUS I LOCATION OF DROPLET.
IONF	FPRINT	FIRST VALUE OF I FOR PRINTOUT.
IP	STRIDE	TEMPORARY USAGE.
IPAR	MAIN STRIDE	INDEX FOR ABSOLUTE OR RELATIVE PRESSURE(SEE INPUT).
IPLAX	MAIN STRIDE	INDEX FOR PLANE OR AXISYMMETRIC FLOW(SEE INPUT).
IPRINT	FPRINT MAIN	INDEX FOR PRINTOUT OF DEPENDENT VARIABLES (SEE INPUT).
IRAD	MAIN	INDEX FOR RADIATION SOLUTION(SEE SRAD).
IREF	MAIN	I LOCATION OF REFERENCE PRESSURE LOCATION.
IPES	MAIN INIT STRIDE AUX	INDEX FOR RESTARTING SOLUTION(SEE INPUT).
IS	ALL	STARTING VALUE OF I (LOCAL VALUE OF IWLIS).
ISOLVE	STRIDE MAIN AUX	INDEX FOR SOLUTION OF DEPENDENT VARIABLES (SEE INPUT).

TABLE C-1 (CONTD.)

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FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
ISOOT	MAIN	INDEX FOR SOOT SOLUTION(SEE SSOOT).
ISP	MAIN	TEMPORARY USAGE.
ISPRAY	MAIN	NUMBER OF ITERATIONS BETWEEN SPRAY SOLUTIONS.
ISTART	FPRINT	STARTING VALUE OF I FOR PRINTOUT.
ISTEP	MAIN STRIDE AUX OUTPUT	NUMBER OF CURRENT ITERATION.
ISTOP	FPRINT	ENDING DEPENDENT VARIABLE INDEX FOR PRINTOUT.
ISTR	STRIDE	FIRST I LOCATION.
ISTAT	FPRINT	STARTING DEPENDENT VARIABLE INDEX FOR PRINTOUT.
ISTR1	SOLVE STRAD	=IS-1.
ISTUN		INDEX FOR STEADY/UNSTEADY FLOW(NOT USED).
ISUP	SOLVE	=ISTR+L.
ISUM	STRAD	=IS+IE.
ISUM1	SOLVE	=IS+IE.
ISWP	SOLVE STRIDE	INDEX USED FOR Y-TDMA SWEEP DIRECTION.
ITER	CRK	NUMBER OF CURRENT ITERATION OF CRK SOLUTION.
ITNOX	STRIDE MAIN	NUMBER OF ITERATIONS OF NOX SOLUTION AT FINAL ITERATION OF FLOW SOLUTION.
ITR	STRIDE	NUMBER OF CHEMICAL KINETICS ITERATIONS.
ITR	TSOLVE	=1 IF RADIATION IGNORED, =2 IF RADIATION CONSIDERED.
ITRAD	TSOLVE MAIN AUX	INDEX FOR RADIATION SOLUTION(SEE INPUT).
ITWALL	AUX	INDEX FOR WALL TEMPERATURE SOLUTION(SEE INPUT).
ITYPE	SPRAY	=1 FOR HEATING DROPLET, =2 FOR BOILING DROPLET.

TABLE C-1 (CONT'D.)

FORTRAN VARIABLE	SUBROUTINE	DEFINITION
	WHERE DEFINED OR USED OFTEN	
IU	MAIN	INDEX FOR TYPE OF UNITS (SEE INPUT).
IU	SPRAY	=IUTNJ-1.
IUINJ	ALLMOD MAIN INIT	I NODE LOCATION OF COOLING SLOTS.
IWINJ	INIT MAIN ALLMOD	I NODE LOCATION OF RADIAL INJECTION HOLES.
IWEI	MAIN	I NODE AT WHICH UPSTREAM INCLINED WALL ENDS.
IWEO	MAIN	I NODE AT WHICH DOWNSTREAM INCLINED WALL STARTS.
INLI	ALL	STARTING I NODES OF CALCULATION DOMAIN WHEN INCLINED WALL IS PRESENT.
INLO	ALL	ENDING I NODES OF CALCULATION DOMAIN WHEN INCLINED WALL IS PRESENT.
IYY	SOLVE STRIDE	INDEX FOR DIRECTION OF TIME SWEEPS.
JB	SPRAY	INDEX TO DENOTE LOCATION OF J BOUNDARY.
JE	ALL	LOCAL VALUE OF JWLD-1.
JJ	INIT	TEMPORARY USAGE.
JJ	SOLVE STRIDE	BUILDUP INDEX.
JJJ	STRIDE	NUMBER OF REACTION STEPS (JJ OF CRIN) SEE TABLE C-21.
JKIN	INIT ALLMOD AUX STRIDE	INDEX FOR TYPE OF BOUNDARY.
JL	STRIDE	TEMPORARY USAGE.
JLDC	SPRAY	J LOCATION OF DROPLET.
JM	ALL	= (J-1)*IMAX.
JMAT	MAIN ALLMT	J LOCATION OF MAXIMUM CONTINUITY ERROR.

TABLE C-1 (CONTD.)

CURRENT
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FORTRAN SUBROUTINE VARTABLE WHERE DEFINED OR USED OFTEN		DEFINITION
JNOX	MAIN	TEMPORARY USAGE.
JOLD	SPRAY	PREVIOUS J LOCATION OF DROPLET.
JONE	FPRINT	FIRST J VALUE FOR PRINTOUT.
JP	STRIDE	TEMPORARY USAGE.
JPLANE	AUXRAD STRAD ALLMOD	VALUE OF J (INDEX FOR Y LOCATION) WHEN SOLVING 2 DIRECTION RADIATION FLUX.
JREF	MAIN	J LOCATION OF REFERENCE PRESSURE NODE.
JS	ALL	LOCAL VALUE OF JWL _{I+1} .
JSTR	STRAD SOLVE STRIOF	STARTING J VALUE.
JSTR1	SOLVE STRAD	=JS-1.
JSUM	SOLVE	=JSTR+M.
JSUM	STRAD	=JS+JE.
JSUM	FPRINT	=JONE+MP1.
JSUM1	SOLVE	=JS+JE.
JSWP	SOLVE STRIDE	INDEX USED FOR X-TOMA SWEEP DIRECTION.
JSW1	INIT,MAIN	J NODE AT START OF DOME INLET. ALLMOD
JSW2	INIT,MAIN	J NODE AT END OF DOME INLET. ALLMOD
JTRAD	MAIN	TEMPORARY USAGE.
JU	SPRAY	=JUNIJ.
JUNIJ	INIT,MAIN	J NODE LOCATIONS OF COOLING SLOTS. ALLMOD
JVINJ	INIT,MAIN	J NODE LOCATIONS OF RADIAL INJECTION HOLES. ALLMOD

TABLE C-1 (CONT'D.)

ORIGINAL PAGE IS
OF POOR QUALITY

FORTRAN VARIABLE	SHAROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
JWEI	INIT,MAIN J NODE AT WHICH UPSTREAM INNER INCLINED WALL STARTS.	
JWIO	INIT,MAIN J NODE AT WHICH UPSTREAM OUTER INCLINED WALL STARTS.	
JWLI	ALL	STARTING J NODES OF THE CALCULATION DOMAIN AT INNER INCLINED WALL.
JWLO	ALL	ENDING J NODES OF THE CALCULATION DOMAIN AT OUTER INCLINED WALL.
JWOI	INIT,MAIN J NODE AT WHICH DOWNSTREAM INNER INCLINED WALL ENDS. ALLMOD AUX STRIDE	
JWOO	INIT,MAIN J NODE AT WHICH DOWNSTREAM OUTER INCLINED WALL ENDS. ALLMOD AUX STRIDE	
J1,J2	INIT	TEMPORARY VALUES FOR JWLI AND JWLO.
KEND	SOLVE	VALUE OF K AT LAST Z LOCATION.
KENOM1	SOLVE	=KEND-1.
KENOM2	SOLVE	=KEND-2.
KJC	SPRAY	TEMPORARY USAGE.
KJK	ALLMOD PUTPUT	TEMPORARY USAGE.
KJM	ALL	=KM(K)+JM(J).
KK	STRA0	TEMPORARY USAGE.
KLOC	SPRAY	X LOCATION OF DROPLET.
KM	ALL	=(K-1)*NJNK,
KMAX	MAIN ALLMOD	K LOCATION OF MAXIMUM CONTINUITY ERROR.
KMIN	SOLVE	=KSTR+1.
KOLO	SPRAY	PREVIOUS X LOCATION OF DROPLET.

TABLE C-1 (CONTD.)

GIVEN NAME BY
OF FORTRAN QUALITY

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
KONF	FPRINT	FIRST K VALUE FOR PRINTOUT.
KONTR0	AUX	CONTROL INDEX =1 ON FIRST ITERATION, OTHERWISE 2.
KONTR0	STRAD	CONTROL INDEX =1,2,3 WHEN NV=LVRX,LVRY,LVRZ.
KOUNT	TSOLVE	NUMBER OF ITERATIONS ON WALL TEMPERATURE.
KREF	MAIN	K LOCATION OF REFERENCE PRESSURE NODE.
KSTR	STRIDE STRAD AUX SOLVE	FIRST K LOCATION.
KSUM	SOLVE	=KEND+KSTR-2.
KSUM	STRAD	=2+N.
KVINJ	INIT ALLMOD MAIN	K NODE LOCATION OF RADIAL INJECTION HOLE.
L	ALL	=LP1-1.
LADIAR	CREK	SEE TABLE C-2.
LASTEP	MAIN STRIDE	MAXIMUM NUMBER OF ITERATIONS.
LCONVG	CREK	SEE TABLE C-2.
LCV	STRIDE	NUMBER OF CONTROL VOLUMES IN X DIRECTION (=L-1).
LDERUG	CREK	SEE TABLE C-2.
LENER	CREK	„.FALSE., ENERGY EQUATION COMPLETELY DECOUPLED FROM SPECIES EQUATIONS AND SPECIES CONCENTRATIONS OBTAINED AT SPECIFIED TEMPERATURE, „.TRUE., COMPLETE ENERGY EQUATION IS USED.
LEOUIL	CREK	SEE TABLE C-2.
LIJ	ALL	=I+JM(J).
LTJNV	SOLVE	INDEX FOR VALUE AT K=1 PLANE IN F ARRAY.
LIJ2	STRIDE	=LIJ+KM(2).

TABLE C-1 (CONTD.)

ORIGINAL PAGE IS
OF POOR QUALITY

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
LIK	AUXRAD STRAD	= I+KM(K).
LMOP, LMPJ	AUX	TEMPORARY USAGE OF LP TYPE OF INDEX.
LNRG	CREK	SEE TABLE C-2.
LOMP, LOPM	AUX	TEMPORARY USAGE OF LP TYPE OF INDEX.
LOPP	AUX	TEMPORARY USAGE OF LP TYPE OF INDEX.
LP	ALL	= I+JM(J)+KM(K).
LPA	STRIDE	INDEX TO REFER TO Z- LOCATION.
LPC	ALL	TEMPORARY USAGE.
LPCE	SOLVE	TEMPORARY USAGE.
LPCH	AUX AUXRAD STRIDE SPRAY	INDEX USED TO REFER TO INTERMEDIATE HYDROCARBON MASS FRACTION.
LPCH1	STRIDE	INDEX USED TO REFER TO INTERMEDIATE HYDROCARBON MASS FRACTION.
LPCO	AUX AUXRAD STRIDE SPRAY	INDEX USED TO REFER TO CO MASS FRACTION.
LPCO1	STRIDE	INDEX USED TO REFER TO CO MASS FRACTION.
LPCSTR	SOLVE	TEMPORARY USAGE.
LPD	AUX	INDEX USED TO REFER TO DISSIPATION RATE.
LPE	STRIDE	INDEX TO REFER TO X+ LOCATION.
LPF	SOLVE STRIDE STRAD	INDEX FOR REFERING TO VALUE IN F ARRAY.
LPF	FPRINT	DO-LOOP LIMIT FOR PRINTOUT.
LPFAV	AUX STRIDE	INDEX USED TO REFER TO AVERAGE RADIATION FLUX.

TABLE C-1 (CONTD.)

ORIGINAL INDEX
OF PCPA QUALITY

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
LPPFU	AUX AUXRAD STRIDE SPRAY	INDEX USED TO REFER TO UMBURNT FUEL MASS FRACTION.
LPPFUOX	AUX AUXRAD STRIDE SPRAY	INDEX USED TO REFER TO MIXTURE FRACTION.
LPPFU1	STRIDE	INDEX USED TO REFER TO UMBURNT FUEL MASS FRACTION.
LPF1	SOLVE	=LPP+ISTR1.
LPH	AUX STRIDE	INDEX USED TO REFER TO ENTHALPY.
LPHD	AUX	INDEX USED TO REFER TO ENTHALPY.
LPH2	AUX AUXRAD STRIDE SPRAY	INDEX USED TO REFER TO H2 MASS FRACTION.
LPH21	STRIDE	INDEX USED TO REFER TO H2 MASS FRACTION.
LPK	AUX	INDEX USED TO REFER TO TURBULENCE ENERGY.
LPL	FPRINT	DO-LOOP LIMIT FOR PRINTOUT.
LPMD	AUX	TEMPORARY USAGE OF LP TYPE OF INDEX.
LPN	ALLMOD	TEMPORARY USAGE.
LPN	STRIDE	INDEX TO REFER TO Y+ LOCATION.
LPN	AUX	INDEX USED TO REFER TO SOOT NUCLEUS CONCENTRATION.
LPNP1	ALLMOD STRIDE	TEMPORARY USAGE.
LPOM,LPOP	AUX	TEMPORARY USAGE OF LP TYPE OF INDEX.
LPD2	STRIDE	INDEX USED TO REFER TO O2 MASS FRACTION.
LPPO	AUX	TEMPORARY USAGE OF LP TYPE OF INDEX.
LPREF	STRIDE MAIN	LOCATION OF REFERENCE PRESSURE NODE.

TABLE C-1 (CONTD.)

ORIGINAL PAGE IS
OF POOR QUALITY

FORTRAN VARIABLE	SURROUNTE WHERE DEFINED OR USED OFTEN	DEFINITION
LPRX	AUX AUXRAD STRIDE	INDEX USED TO REFER TO X DIRECTION RADIATION FLUX.
LPRY	AUX AUXRAD STRIDE	INDEX USED TO REFER TO Y DIRECTION RADIATION FLUX.
LPRZ	AUXRAD STRIDE	INDEX USED TO REFER TO Z DIRECTION RADIATION FLUX.
LPS	AUX	INDEX USED TO REFER TO SOOT CONCENTRATION.
LPS	STRIDE	INDEX TO REFER TO Y- LOCATION.
LPSTR	SOLVE	TEMPORARY USAGE.
LPS1	AUX	INDEX USED TO REFER TO SOOT CONCENTRATION OF SIZE 1.
LPS2	AUX	INDEX USED TO REFER TO SOOT CONCENTRATION OF SIZE 2.
LPT	STRIDE	INDEX TO REFER TO Z+ LOCATION.
LPTE	AUX AUXRAD SPRAY	INDEX USED TO REFER TO TEMPERATURE.
LPW	ALLMOD STRIDE	INDEX TO REFER TO X- LOCATION.
LP1	ALL	NUMBER OF GRID NODES IN AXIAL (X) DIRECTION.
LP11	STRIDE	TEMPORARY USAGE.
LP2	ALLMOD STRIDF	TEMPORARY USAGE.
LREACT	CREK	SEE TABLE C-2.
LVCH	DATA ALLMOD AUX STRIDE	INDEX FOR INTERMEDIATE HYDROCARBON MASS FRACTION.
LVCH1	DATA STRIDE	INDEX FOR INTERMEDIATE HYDROCARBON MASS FRACTION.
LVCO	DATA ALLMOD AUX STRIDE	INDEX FOR CO MASS FRACTION.

TABLE C-1 (CONT'D.)

ORIGINAL PAGE IS
OF POOR QUALITY

FORTRAN SUBROUTINE VARIABLE		DEFINITION
	WHERE DEFINED OR USED OFTEN	
LVC01	DATA STRIDE	INDEX FOR CO MASS FRACTION.
LVC02	DATA	INDEX FOR CO2 MASS FRACTION.
LVO	DATA ALLMOD AUX	INDEX FOR DISSIPATION RATE OF TURBULENCE.
LVFU	DATA ALLMOD AUX STRIDE	INDEX FOR UNBURNT FUEL MASS FRACTION.
LVFX0X	DATA ALLMOD AUX STRIDE	INDEX FOR MIXTURE FRACTION.
LVFU1	DATA STRIDE	INDEX FOR UNBURNT FUEL MASS FRACTION.
LVH	DATA ALLMOD AUX STRIDE	INDEX FOR ENTHALPY.
LVH1	DATA ALLMOD AUX STRIDE	INDEX FOR H ATOM MASS FRACTION.
LVH2	DATA ALLMOD AUX STRIDE	INDEX FOR H2 MASS FRACTION.
LVH20	DATA	INDEX FOR H2O MASS FRACTION.
LVH21	DATA STRIDE	INDEX FOR H2 MASS FRACTION.
LVR	DATA ALLMOD AUX STRIDE	INDEX FOR TURBULENCE KINETIC ENERGY.
LVN	DATA ALLMOD AUX	INDEX FOR SOOT NUCLEUS CONCENTRATION.

TABLE C-1 (CONTD.)

ORIGINAL PAGE IS
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FORTRAN VARIABLE	DATA WHERE DEFINED OR USED OFTEN	DEFINITION
LVNO	DATA	INDEX FOR NO MASS FRACTION.
LVNO2	DATA	INDEX FOR NO2 MASS FRACTION.
LVN1	DATA	INDEX FOR N ATOM MASS FRACTION.
LVN2	DATA	INDEX FOR N2 MASS FRACTION.
LVO	DATA	INDEX FOR O ATOM MASS FRACTION.
LVOH	DATA STRIDE	INDEX FOR OH MASS FRACTION.
LVO2	DATA STRIDE	INDEX FOR O2 MASS FRACTION.
LVRX	DATA ALLMOD STRIDE	INDEX FOR X DIRECTION RADIATION FLUX.
LVRY	DATA ALLMOD	INDEX FOR Y DIRECTION RADIATION FLUX.
LVRZ	DATA STRIDE	INDEX FOR Z DIRECTION RADIATION FLUX.
LVS1	DATA ALLMOD AUX	INDEX FOR MASS FRACTION OF SOOT PARTICLE SIZE 1.
LVS2	DATA ALLMOD AUX	INDEX FOR MASS FRACTION OF SOOT PARTICLE SIZE 2.
LXM	ALL	INDEX TO REFER TO X- LOCATION.
LXMC	ALLMOD SPRAY	TEMPORARY USAGE.
LXM1	AUX STRIDE	=LXM-NI.
LXP	ALL	INDEX TO REFER TO X+ LOCATION.
LXP1	AUX STRIDE	=LXP-NI.
LYM	ALL	INDEX TO REFER TO Y- LOCATION.

TABLE C-1 (CONTD.)

ORIGINAL PAGE IS
OF POOR QUALITY

FORTRAN SUBROUTINE VARIABLE WHERE DEFINED OR USED OFTEN		DEFINITION
LYNC	ALLMOD SPRAY	TEMPORARY USAGE.
LYM1	AUX	=LYN-1.
LYP	ALL	INDEX TO REFER TO Y+ LOCATION.
LYP1	AUX STRIDE	=LYP-1.
LZM	ALL	INDEX TO REFER TO Z- LOCATION.
LZMC	ALLMOD SPRAY	TEMPORARY USAGE.
LZM1	AUX	=LZM-1.
LZP	ALL	INDEX TO REFER TO Z+ LOCATION.
LZP1	AUX STRIDE	=LZP-1.
M	ALL	=MP1-1.
MAX	AUX STRIDE	LOCAL VALUE OF JWLD-1.
MCV	STRIDE	NUMBER OF CONTROL VOLUMES IN Y DIRECTION.
MIN	AUX	LOCAL VALUE OF JWLI+1.
MM1	STRIDE	SAME AS MCV.
MM1	ALLMOD	TEMPORARY USAGE.
MODEL	AUX,MAIN	INDEX FOR TYPE OF VISCOSITY(SEE INPUT).
MDEN	AUX,MAIN	INDEX FOR TYPE OF DENSITY(SEE INPUT).
MNDER	AUX,MAIN STRIDE	INDEX FOR TYPE OF REACTION RATE(SEE INPUT).
MPART	AUX,MAIN	NUMBER OF SOOT PARTICLE SIZES.
MP1	ALL	NUMBER OF GRID NODES IN RADIAL (Y) DIRECTION.
MW	SPRAY	ARRAY TO STORE MOLECULAR WEIGHTS OF VARIOUS FUELS.
MWCOND	SPRAY	CONSTANT USED IN MOLECULAR WEIGHT CALCULATION.

TABLE C-1 (CONTD.)

ORIGINAL PAGE IS
OF POOR QUALITY

FORTRAN SUBROUTINE VARIABLE WHERE DEFINED OR USED OFTEN		
MWT	SPRAY	MOLECULAR WEIGHT OF FUEL VAPORS.
M1,M2	ALLMOD	TEMPORARY USAGE.
N	ALL	=NP1-1.
NA	CPEK	SEE TABLE C-2.
NCV	STRIDE	NUMBER OF CONTROL VOLUMES IN Z DIRECTION (=N-1).
NDERUG	CPEK	SEE TABLE C-2.
NFNZ	SPRAY MAIN ALLMOD STRIDE INIT	INDEX FOR WHETHER LIQUID FUEL NOZZLE IS PRESENT (SEE INPUT).
NG	SPRAY	NUMBER OF DROPLET SIZE GROUPS.
NGAM	DATA STRIDE AUX	INDEX FOR DIFFUSION COEFFICIENT.
NGLOB	CPEK	SEE TABLE C-2.
NGLOPP	CPEK	SEE TABLE C-2.
NGOTO	STRIDE SOLVE STRAD ALLMOD AUX	INDEX WHICH TAKES VALUES 1,2,3 WHEN U,V,W BEING SOLVED, OTHERWISE IT HAS A VALUE OF 4.
NI	ALL	MAXIMUM NUMBER OF NODES IN X DIRECTION.
NINJ	STRIDE	NINJ.
NINJNK	STRIDE	NINJNK.
NITER	STRIDE	MAXIMUM NUMBER OF CHEMICAL KINETICS ITERATIONS.
NJ	ALL	MAXIMUM NUMBER OF NODES IN Y DIRECTION.
NK	ALL	MAXIMUM NUMBER OF NODES IN Z DIRECTION.
NLM	CPEK	SEE TABLE C-2.
NN	SPRAY	DO-LOOP INDEX OVER FUEL NOZZLES.

TABLE C-1 (CONTD.)

OPTIONAL PARAMETERS
OF POOR QUALITY

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
NNOX	MAIN	INDEX FOR NOX SOLUTION(SEE INPUT).
NNV	DATA STRIDE	MAXIMUM NUMBER OF DEPENDENT VARIABLES.
NP	DATA STRIDE	INDEX FOR PRESSURE.
NP1	ALL	NUMBER OF GRID NODES IN TANGENTIAL (Z) DIRECTION.
NR	CREK	SEE TABLE C-2.
NRHO	DATA AUX	INDEX FOR DENSITY.
NS	ALL	NUMBER OF SPECIES.
NSKIP	FPRINT	TEMPORARY STORAGE FOR IPRINT.
NSL	SPRAY MAIN	NUMBER OF SPRAY CONE RAYS.
NSL2	SPRAY	=NSL(NN).
NSM	CREK	SEE TABLE C-2.
NSOOT	MAIN	INDEX FOR SOOT SOLUTION(SEE INPUT).
NS1,NS2	ALL	TEMPORARY USAGE OF DO-LOOP LIMITS ON SPECIES CONCENTRATIONS.
NTP	OUTPUT	INDEX FOR TAPE NUMBER.
NTPT	STRIDE	=NTP1+NTP2.
NTP1	STRIDE MAIN,INIT AUX	INDEX FOR TAPE NUMBER.
NTP2	STRIDE MAIN,INIT	INDEX FOR TAPE NUMBER.
NTP3	SPRAY MAIN ALLMOD	INDEX FOR TAPE NUMBER.
NUINJ	MAIN,INIT ALLMOD	NUMBER OF COOLING SLOTS.

TABLE C-1 (CONTD.)

ORIGINAL PAGE IS
OF POOR QUALITY

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
NV	ALL	DEPENDENT VARIABLE INDEX.
NVCH	DATA, INIT	INDEX FOR INTERMEDIATE HYDROCARBON MASS FRACTION. ALLMOD STRIDE AUX
NVCO	DATA, INIT	INDEX FOR CO MASS FRACTION. STRIDE AUX
NVCO2	DATA	INDEX FOR CO2 MASS FRACTION.
NVD	DATA, INIT	INDEX FOR DISSIPATION RATE OF TURBULENCE. AUX
NVE		INDEX FOR EMISSIVE POWER.
NVF	ALL	INDEX FOR IDENTIFYING LOCATION IN F ARRAY.
NVFAV	DATA, INIT	INDEX FOR AVERAGE RADIATION FLUX. STRIDE AUX
NVFF	ALLMOD	=NVF(NV).
NVFU	DATA, INIT	INDEX FOR UNBURNED FUEL MASS FRACTION. ALLMOD AUX STRIDE
NVFUCX	DATA, INIT	INDEX FOR MIXTURE FRACTION. ALLMOD STRIDE AUX
NVM	DATA, INIT	INDEX FOR ENTHALPY. STRIDE AUX
NVHP	AUX	INDEX FOR ENTHALPY.
NVH2	DATA, INIT	INDEX FOR H2 MASS FRACTION. STRIDE AUX
NVH2O	DATA	INDEX FOR H2O MASS FRACTION.
NVINJ	MAIN INIT ALLMOD	NUMBER OF RADIAL INJECTION HOLES.

TABLE C-1 (CONT'D.)

ORIGINAL PRINTOUT
OF PART. QUANTITY

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
NVJM	STRAD	=JM(J)+NVM(NVRZ),
NVK	DATA, INIT INDEX FOR TURBULENCE KINETIC ENERGY. ALLMOD AUX	
NVKM	SOLVE STRAD FPRINT	=KM(K)+NVM(NVF(NV)),
NVM	ALL	=(NV-1)*NIONJ+NK,
NVN	DATA, INIT INDEX FOR SOOT NUCLEUS CONCENTRATION. AUX	
NVN2	DATA	INDEX FOR N2 MASS FRACTION.
NVNX	DATA	INDEX FOR O2 MASS FRACTION.
NVRX	DATA, INIT INDEX FOR X DIRECTION RADIATION FLUX. STRIDE	
NVRY	DATA, INIT INDEX FOR Y DIRECTION RADIATION FLUX. STRIDE	
NVRZ	DATA, INIT INDEX FOR Z DIRECTION RADIATION FLUX. STRIDE ALLMOD	
NVS1	DATA, INIT INDEX FOR MASS FRACTION OF SOOT PARTICLE SIZE 1. AUX	
NVS2	DATA, INIT INDEX FOR MASS FRACTION OF SOOT PARTICLE SIZE 2. AUX	
NVT	DATA, INIT INDEX FOR TEMPERATURE. AUX	
NVV	FPRINT	DO-LOOP COUNTER.
NVVV	FPRINT	FIRST DEPENDENT VARIABLE TO BE PRINTED ON A CALL TO FPRINT.
N1	CREK	SEE TABLE C-2.
N2	CREK	SEE TABLE C-2.
N3	CREK	SEE TABLE C-2.

TABLE C-1 (CONTD.)

ORIGINAL PAGE IS
OF POOR QUALITY

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
DGPSI	AUX	TEMPORARY USAGE.
DGPSIR	AUX	TEMPORARY USAGE.
P	ALL	PRESSURE.
PA	CPEK	PRESSURE.
PATH	AUXRAD	PATH LENGTH FOR RADIATION CALCULATIONS.
PRAR	OUTPUT	TEMPORARY USAGE.
PCO2	AUXRAD	CO2 PARTIAL PRESSURE.
PEXP1	INIT	PRE-EXPONENT FACTOR IN FIRST STEP OF HYDROCARBON OXIDATION SCHEME.
PEXP2	INIT	PRE-EXPONENT FACTOR IN SECOND STEP OF HYDROCARBON OXIDATION SCHEME.
PEXP3	INIT	PRE-EXPONENT FACTOR IN THIRD STEP OF HYDROCARBON OXIDATION SCHEME.
PEXP4	INIT	PRE-EXPONENT FACTOR IN FOURTH STEP OF HYDROCARBON OXIDATION SCHEME.
PHI	INIT AUX	FUEL MASS FRACTION/STOICHIOMETRIC MIXTURE FRACTION.
PH2O	AUXRAD	H2O PARTIAL PRESSURE.
PI	SPRAY	=3.14159.
PJAY	ALL,MOD MAIN	PJAY FUNCTION FOR HEAT TRANSFER WALL FUNCTION.
PLAXH1	ALL	IPLAX=1.
PLREF	STRIDE	PRESSURE AT REFERENCE PRESSURE LOCATION.
PO,POT	SPRAY	CONSTANTS IN BOILING POINT CALCULATION.
PO2	AUX	OXYGEN PARTIAL PRESSURE.
PP	ALL	PRESSURE CORRECTION.
PPLN	CPEK	SFF TABLE C-2.
PR	AUX,MAIN ALL,MOD	LAMINAR PRANDTL/SCHMIDT NUMBER.

TABLE C-1 (CONT'D.)

ORIGINAL PAGE IS
OF POOR QUALITY

FORTRAN SUBROUTINE		DEFINITION
VARTABLE	WHERE DEFINED OR USED OFTEN	
PRFF	AUX,MAIN ALLMOD	TURBULENT PRANDTL/SCHMIDT NUMBER.
PRESS	MAIN INIT STRIDE AUX	SYSTEM PRESSURE.
PREXPS	AUX,MAIN	PRE-EXPONENT FACTOR IN SOOT OXIDATION RATE (SEE INPUT).
PREXP1	AUX,MAIN TNIT	PRE-EXPONENT FACTOR IN FIRST STEP OF HYDROCARBON OXIDATION SCHEME(=PEXP1).
PREXP2	AUX,MAIN INIT	PRE-EXPONENT FACTOR IN SECOND STEP OF HYDROCARBON OXIDATION SCHEME(=PEXP2).
PREXP3	AUX,MAIN TNIT	PRE-EXPONENT FACTOR IN THIRD STEP OF HYDROCARBON OXIDATION SCHEME(=PEXP3).
PREXP4	AUX,MAIN INIT	PRE-EXPONENT FACTOR IN FOURTH STEP OF HYDROCARBON OXIDATION SCHEME(=PEXP4).
PRRAT	MAIN	RATIO OF LAMINAR AND TURBULENT PRANDTL NUMBERS.
PR3	SPRAY	PRANDTL NUMBER.
PSI	AUX	FRACTION OF FINE STRUCTURES HEATED ENOUGH TO REACT.
PSIC	AUX	TEMPORARY USAGE IN SOOT OXIDATION RATE.
PT2	SPRAY	=2*PI.
QCH	TSOLVE	CONVECTION HEAT TRANSFER.
QDT	SPRAY	HEAT TRANSFER RATE TO DROPLET.
QRH	TSOLVE	NET RADIATION HEAT TRANSFER FROM WALL.
QQ-04	CREK	SEE TABLE C-2.
R	ALL	RADIUS.
RAD	TSOLVE	RADIATION HEAT FLUX TO WALL.
RADIN	INIT ALLMOD	INLET RADIATION FLUX.
RADSUR	TINIT ALLMOD	RADIATION FLUX AT EACH AREA STATION.

ORIGINAL PAGE IS
OF POOR QUALITY

TABLE C-1 (CONTD.)

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
RATE	SPRAY	DROPLET EVAPURATZON RATE.
RATIO1=9	INIT ALLMOD AUX	CONSTANTS USED IN ELEMENT BALANCE EQUATIONS.
RATIO10=12	INIT ALLMOD AUX	CONSTANTS USED IN ELEMENT BALANCE EQUATIONS.
RDT	STRIDE	ALWAYS EQUAL TO ZERO.
REI	SPRAY	DROPLET REYNOLDS NUMBER.
RELAX	SOLVE MAIN STRIDE AUX	UNDER-RELAXATION FACTORS (SEE INPUT).
RELAXM	SOLVE AUX	=1.-RELAX.
RET	AUX	TURBULENT REYNOLDS NUMBER.
RFUFL	MAIN SPRAY	RADIUS OF FUEL NOZZLE.
RF1,PF2	AUX	SOOT FORMATION RATES.
RGAS	CREK	SEE TABLE C-2.
RGASIN	CREK	SEE TABLE C-2.
RHO	ALL	DENSITY.
RHDA	ALLMOD STRIDE	DENSITY*AREA.
RHOCON	MAIN AUX	PRESSURE DIVIDED BY UNIVERSAL GAS CONSTANT.
RHOINJ	ALLMOD	DENSITY OF DILUTION JET.
RHOLP	AUX	DENSITY AT NODE LP.
RHOI	AUX	DENSITY OF SURROUNDING FLUID.
RHOP	AUX MAIN TINIT	SOOT PARTICLE DENSITY.

TABLE C-1 (CONT'D.)

ORIGINAL PAGE IS
OF POOR QUALITY

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
RHOPP	STRIDE INIT	DENSITY AT NODE P.
RHODSTR	AUX	DENSITY OF FINE STRUCTURES.
RHOSH	INIT ALLMOD	INLET DENSITY.
RHD4	INIT	DENSITY.
RI	STRIDE MAIN	INNER RADIUS OF COMBUSTOR.
RM	STRIDE	RADIUS AT V-VELOCITY LOCATION.
RMV	STRIDE	RADIUS AT V-VELOCITY CONTROL VOLUME SURFACE.
RNC	AUX	TEMPORARY USAGE.
RNG	SPRAY	NUMBER OF DROPLET SIZE GROUPS.
RNSL	SPRAY MAIN INIT	=NSL2, NUMBER OF SPRAY CONE RAYS.
ROA	ALLMOD	DENSITY*AREA.
ROF	SPRAY	DENSITY OF LIQUID FUEL AT BOILING POINT.
ROFO	SPRAY	INITIAL DENSITY OF LIQUID FUEL.
ROST	SPRAY	GAS DENSITY.
RTCD	INIT ALLMOD AUX	SQUARE ROOT OF CD.
RTCDK	ALLMOD	TURBULENCE ENERGY=SQRT(CD).
RVAV	STRIDE	TEMPORARY USAGE.
RVFCX-Z	SPRAY	COORDINATE TRANSFORMATION QUANTITIES.
SRAR	OUTPUT	TEMPORARY USAGE.
SCATR	AUXRAD MAIN INIT	SCATTERING COEFFICIENT (IF ITAD=2).

ORIGINAL PAGE IS
OF POOR QUALITY

TABLE C-1 (CONTD.)

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
SCTR	AUXRAD	ARRAY FOR SCATTERING COEFFICIENT.
SC9	SPRAY	SCHMIDT NUMBER.
SECTOR	INIT	ANGULAR SECTOR.
SEXIT	ALLMOD	EXIT MASS FLOW ERROR.
SFAC	AUX	TEMPORARY USAGE IN CO REACTION RATE.
SHRSTR	ALLMOD	SHEAR STRESS.
SIG	TSOLVE	STEFAN-BOLTZMANN CONSTANT.
SIGMA	AUXRAD DATA ALLMOD INIT AUX	STEFAN-BOLTZMANN CONSTANT.
SINA	SPRAY	SINE OF HALF THE NOZZLE CONE ANGLE.
SINR	SPRAY	SINE OF NOZZLE BACK ANGLE.
SIND	SPRAY	SINE OF NOZZLE DOWN ANGLE.
SINT	SPRAY	SINE OF CURRENT SPRAY CONE SEGMENT ANGLE.
SKE	ALLMOD	TURBULENCE ENERGY AT COOLING SLOT.
SLM	ALLMOD	LENGTH SCALE AT COOLING SLOT.
SM	CREK	SEE TABLE C-2.
SMASS	INIT	TEMPORARY USAGE.
SMAY	ALLMOD MAIN	MAXIMUM OF CONTINUITY ERRORS.
SMCONE	OUTPUT	SMOKE CONCENTRATION.
SMO	SPRAY MAIN	SAUTER MEAN DIAMETER.
SMINV	CREK	SEE TABLE C-2.
SMOND	OUTPUT	SMOKE NUMBER.
SMW	CREK	SEE TABLE C-2.

TABLE C-1 (CONTD.)

ORIGINAL CODE
OF POOR QUALITY

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
SMO	CREK	NOT USED.
SNOX	MAIN	NOX SOLUTION STARTED AFTER ERROR FALLS TO SNOX OR AFTER INOX NUMBER OF ITERATIONS.
S00TK	AUXRAD	SOOT CONCENTRATION.
S00T1	ALL	MASS FRACTION OF SOOT PARTICLE SIZE 1.
S00T2	ALL	MASS FRACTION OF SOOT PARTICLE SIZE 2.
S0R	AUX	PART OF SOURCE TERM.
S0RC0	AUX	PART OF CO SOURCE TERM.
S0R1	AUX	LAMINAR SOURCE TERM.
S0R2	AUX	TURBULENT SOURCE TERM.
S0R3	AUX	LAMINAR SOURCE TERM.
S0R4	AUX	TURBULENT SOURCE TERM.
SP	ALL	PART OF LINEARIZED SOURCE TERM.
SPCH	AUX	PART OF LINEARIZED SOURCE TERM (SP) FOR INTERMEDIATE HYDROCARBON MASS FRACTION.
SPC1,SPC2	AUX	SOOT OXIDATION RATE.
SPFU	AUX	PART OF LINEARIZED SOURCE TERM (SP) FOR FUEL.
SPF1,SPF2	AUX	TEMPORARY USAGE.
SPF2F	AUX	TEMPORARY USAGE.
SPK	SOLVE	PART OF LINEARIZED SOURCE TERM USED IN CYCLIC TOMA.
SQFK	INIT	SQUARE ROOT OF FK.
SRAD	MAIN	RADIATION SOLUTION STARTED AFTER ERROR FALLS TO SRAD OR AFTER IRAD NUMBER OF ITERATIONS.
SREI	SPRAY	SQUARE ROOT OF REI.
SS00T	MAIN	SOOT SOLUTION STARTED AFTER ERROR FALLS TO SS00T OR AFTER ISOOT NUMBER OF ITERATIONS.
SSS	AUX	TEMPORARY USAGE.

TABLE C-1 (CONTD.)

ORIGINAL PAGE IS
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FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
SSUM	ALLMOD MAIN	SUM OF ABSOLUTE CONTINUITY ERRORS.
STORE	SOLVE STRAD	TEMPORARY USAGE.
ST4	INIT	$\bullet \text{SIGMA} = \text{TEMP}^{0.4}$.
SU	ALL	PART OF LINEARIZED SOURCE TERM.
SUCH	AUX	PART OF LINEARIZED SOURCE TERM (SUI) FOR INTERMEDIATE HYDROCARBON MASS FRACTION.
SUFU	AUX	PART OF LINEARIZED SOURCE TERM (SUI) FOR FUEL.
SUF1,SUF2	AUX	TEMPORARY USAGE.
SUK	SOLVE	PART OF LINEARIZED SOURCE TERM USED IN CYCLIC TDMA.
SUN	AUX	TEMPORARY USAGE.
SUM1	MAIN	TEMPORARY USAGE.
SUM2	MAIN	TEMPORARY USAGE.
SWNO	MAIN	RATIO OF TANGENTIAL TO AXIAL VELOCITY AT DOME INLET.
S1	CREK	SEE TABLE C-2.
S2	CREK	SEE TABLE C-2.
T	INIT AUXRAD AUX	TEMPERATURE.
TAN	INIT	ANNULUS TEMPERATURE.
TAUP	AUX	WALL SHEAR STRESS.
TR	SPRAY	LIQUID FUEL BOILING TEMPERATURE.
TCYLW	ALLMOD MAIN	TEMPERATURE OF CYLINDRICAL PORTION OF COMBUSTOR WALL.
TEMP	ALL	TEMPERATURE.
TEMPW	ALLMOD	TEMPERATURE.
TEMTH	INIT	MASS AVERAGED TEMPERATURE AT EACH AXIAL STATION.

TABLE C-1 (CONTD.)

ORIGINAL PAGE IS
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FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
TF	SPRAY	TEMPERATURE OF COMBUSTION PRODUCTS.
TFU	SPRAY	LIQUID DROPLET TEMPERATURE.
TFUEL	MAIN ALLMOD SPRAY	INLET TEMPERATURE OF FUEL.
TGAS	TSOLVE	GAS TEMPERATURE.
THETA	SPRAY	CURRENT SPRAY CONE SEGMENT ANGLE.
THETA1	SPRAY MAIN	INITIAL SPRAY CONE SEGMENT ANGLE.
THETA2	SPRAY MAIN	FINAL SPRAY CONE SEGMENT ANGLE.
TINE	STRIDE	TIME.
TIN	INIT	INITIAL TEMPERATURE AT EACH AXIAL STATION.
TINCP	AUX MAIN	SOOT CALCULATION BYPASSED FOR TEMPERATURE.LE.TINCP.
TINLW	ALLMOD MAIN INIT	TEMPERATURE OF INCLINED WALL PORTION OF COMBUSTOR AND OF DOME.
TITLE	FPRINT MAIN	HEADING FOR DEPENDENT VARIABLE.
TITLE2	OUTPUT MAIN	CASE TITLE CARD.
TK	CREK	SEE TABLE C-2.
TKINV	CREK	SEE TABLE C-2.
TLIP	ALLMOD MAIN	TEMPERATURE OF COOLING SLOT LIP.
TLN	CREK	SEE TABLE C-2.
TMAX	INIT AUX	MAXIMUM TEMPERATURE.
TNEW	INIT	TEMPERATURE ON NEW ITERATION.

TABLE C-1 (CONTD.)

ORIGINAL PAGE IS
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FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
TNOX	MAIN STRIDE	NOX CALCULATION BYPASSED IF TEMPERATURE.LE.TNOX.
TO	AUX	TEMPERATURE OF SURROUNDING FLUID.
TOUT		OUTLET TEMPERATURE (NOT USED).
TS	AUXRAD	TEMPERATURE.
TST	SPRAY	GAS TEMPERATURE.
TSTR	AUX	TEMPERATURE OF FINE STRUCTURES.
TSW	INIT MAIN	TEMPERATURE AT DOME INLET.
TUINJ	ALLMOD MAIN INIT	COOLING SLOT TEMPERATURE.
TVINJ	MAIN INIT	DILUTION JET TEMPERATURE.
TH	TSOLVE	WALL TEMPERATURE.
THN	TSOLVE	WALL TEMPERATURE AT NEW ITERATION.
TH2	TSOLVE	=TH**2.
TX,TX1	STRIDE STRAD	DIFFUSION FLUX IN X DIRECTION.
TY,TY1	STRIDE STRAD	DIFFUSION FLUX IN Y DIRECTION.
TZ	STRIDE STRAD	DIFFUSION FLUX IN Z DIRECTION.
TZFAC	STRIDE	FRACTION OF DIFFUSION FLUX IN Z DIRECTION.
T1	SPRAY	AVERAGE OF TB AND TF.
T4	INIT	TEMPORARY USAGE.
U	ALL	U-VELOCITY.
UADD	ALLMOD	CORRECTION TO EXIT VELOCITIES.
UF	SPRAY	DROPLET VELOCITY IN X DIRECTION AT CURRENT LOCATION.

TABLE C-1 (CONT'D.)

ORIGINAL PAGE IS
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FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	
UFN	SPRAY	DROPLET VELOCITY IN X DIRECTION AT PREVIOUS LOCATION.
UIN	INIT	MEAN U-VELOCITY AT EACH AXIAL STATION.
UINJ	ALLMOD MAIN INIT	COOLING SLOT AXIAL VELOCITY.
ULIM	SPRAY	LIMIT ON DROPLET VELOCITY CHANGE BETWEEN SUCCESSIVE STEPS.
UMASS	INIT	MOMENTUM FLOW THROUGH DOME INLET.
UMEAN	ALLMOD	MEAN EXIT VELOCITY.
UNICON	PATA ALLMOD STRIDE AUX INIT	UNIVERSAL GAS CONSTANT.
UST	SPRAY	GAS VELOCITY IN X DIRECTION.
USH	INIT MAIN	AXIAL VELOCITY OF DOME INLET.
UYN, UYP	AUX	AVERAGE U VELOCITY BETWEEN NEIGHBORING NODES.
UTM, UZP	AUX	AVERAGE U VELOCITY BETWEEN NEIGHBORING NODES.
V	ALL	V-VELOCITY.
VC, VFC	AUX	RESULTANT VELOCITY.
VECX-Z	SPRAY	UNIT VECTORS IN X,Y,Z DIRECTIONS.
VF	SPRAY	DROPLET VELOCITY IN Y DIRECTION AT CURRENT LOCATION.
VFO	SPRAY	DROPLET VELOCITY IN Y DIRECTION AT PREVIOUS LOCATION.
VFU	SPRAY	RESULTANT DROPLET VELOCITY AT CURRENT LOCATION.
VFUEL	SPRAY MAIN	INITIAL FUEL DROPLET VELOCITY.
VINJ	INIT ALLMOD MAIN	RADIAL VELOCITY OF DILUTION JET.
VISC	ALL	VISCOSITY.

TABLE C-1 (CONTD.)

ORIGINAL PAGE IS
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FORTRAN SUBROUTINE VARIABLE WHERE DEFINED OR USED OFTEN		DEFINITION
VISCO	SPRAY	GAS VISCOSITY.
VISCOS	AUX	VISCOSITY.
VMIX	AUX AUXRAD	RECIPROCAL OF AVERAGE MOLECULAR WEIGHT.
VMT2	AUX	AVERAGE V VELOCITY BETWEEN NEIGHBORING NODES.
VOL	STRIDE	VOLUME OF ELEMENTARY CONTROL VOLUME.
VP	AUX	RESULTANT VELOCITY.
VPT2	AUX	AVERAGE V VELOCITY BETWEEN NEIGHBORING NODES.
VR	SPRAY	RESULTANT RELATIVE VELOCITY BETWEEN GAS AND DROPLET.
VST	SPRAY	GAS VELOCITY IN Y DIRECTION.
VSW	INIT MAIN	RADIAL VELOCITY OF DOME INLET.
VXM,VXP	AUX	AVERAGE V VELOCITY BETWEEN NEIGHBORING NODES.
VZM,VZP	AUX	AVERAGE V VELOCITY BETWEEN NEIGHBORING NODES.
W	ALL	W-VELOCITY.
WALKE	ALLMOD	WALL TURBULENCE KINETIC ENERGY.
WC1	INIT AUX	MOLECULAR WEIGHT OF INTERMEDIATE HYDROCARBON.
WC0	INIT,DATA	MOLECULAR WEIGHT OF CO.
WC02	INIT,DATA	MOLECULAR WEIGHT OF CO2.
WC2H4	INIT,DATA	MOLECULAR WEIGHT OF C2H4.
WF	SPRAY	DROPLET VELOCITY IN Z DIRECTION AT CURRENT LOCATION.
WFF	SPRAY MAIN INIT	FUEL FLOW RATE.
WFI	SPRAY	FUEL FLOW RATE ON A PARTICULAR RAY.

TABLE C-1 (CONT'D.)

ORIGINAL PAGE IS
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FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
WFNZ	INIT	TOTAL LIQUID FUEL FLOW RATE.
WFO	SPRAY	DROPLET VELOCITY IN Z DIRECTION AT PREVIOUS LOCATION.
WFU	INIT, DATA	MOLECULAR WEIGHT OF FUEL. AUX
WH2	INIT, DATA	MOLECULAR WEIGHT OF H2. AUX
WH2O	INIT, DATA	MOLECULAR WEIGHT OF H2O. AUX
WIN	ALLMOD	W-VELOCITY THROUGH DOME INLET.
WL7P	STRIDE	TEMPORARY USAGE.
WMNM,WMNP	AUX	AVERAGE W VELOCITY BETWEEN NEIGHBORING NODES.
WN2	INIT, DATA	MOLECULAR WEIGHT OF N2. AUX
WOX	INIT, DATA	MOLECULAR WEIGHT OF O2. AUX
WST	SPRAY	GAS VELOCITY IN Z DIRECTION.
WSW	INIT ALLMOD	TANGENTIAL VELOCITY OF DOME INLET.
WIINJ	ALLMOD MAIN INIT	COOLING SLOT TANGENTIAL VELOCITY.
WXM,WXP	AUX	AVERAGE W VELOCITY BETWEEN NEIGHBORING NODES.
WYM,WYP	AUX	AVERAGE W VELOCITY BETWEEN NEIGHBORING NODES.
X	ALL	AXIAL DISTANCE.
XDIF	STRIDE	INTERMODAL DISTANCE IN X-DIRECTION.
XF	SPRAY	X LOCATION OF DROPLET.
XM	SPRAY	X LOCATION OF CONTROL VOLUME SURFACES.
XM	AUX	X DISTANCE AT X- LOCATION.
XO	MAIN SPRAY	X LOCATION OF ORIGIN OF FUEL NOZZLE SPRAY.

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TABLE C-1 (CONTD.)

FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
XP	AUX	X DISTANCE AT X+ LOCATION.
XS	STRIDE	MAIN CONTROL VOLUME WIDTH IN X DIRECTION.
XSU	STRIDE	U-VELOCITY CONTROL VOLUME WIDTH IN X DIRECTION.
Y	ALL	RADIAL DISTANCE.
YDIF	STRIDE	INTERNODAL DISTANCE IN Y DIRECTION.
YF	SPRAY	Y LOCATION OF DROPLET.
YM	SPRAY	Y LOCATION OF CONTROL VOLUME SURFACES.
YH	AUX	Y DISTANCE AT Y- LOCATION.
YO	MAIN SPRAY	Y LOCATION OF ORIGIN OF FUEL NOZZLE SPRAY.
YP	AUX	Y DISTANCE AT Y+ LOCATION.
YPLUS	ALLMOD	YPLUS IN WALL FUNCTIONS.
YS	STRIDE	MAIN CONTROL VOLUME WIDTH IN Y DIRECTION.
YSR	STRIDE	MAIN CONTROL VOLUME AREA NORMAL TO X DIRECTION.
YSV	STRIDE	V-VELOCITY CONTROL VOLUME WIDTH IN Y DIRECTION.
YSVR	STRIDE	V-VELOCITY CONTROL VOLUME AREA NORMAL TO X DIRECTION.
Y1,Y2	INIT	TEMPORARY USAGE.
Z	ALL	TANGENTIAL DISTANCE.
ZDIF	STRIDE	INTERNODAL DISTANCE IN Z DIRECTION.
ZF	SPRAY	Z LOCATION OF DROPLET.
ZH	SPRAY	Z LOCATION OF CONTROL VOLUME SURFACES.
ZM	AUX	Z DISTANCE AT Z- LOCATION.
ZO	MAIN SPRAY	Z LOCATION OF ORIGIN OF FUEL NOZZLE SPRAY.
ZP	AUX	Z DISTANCE AT Z+ LOCATION.
ZS	STRIDE	MAIN CONTROL VOLUME WIDTH IN Z DIRECTION.

TABLE C-1 (CONT'D.)

ORIGINAL PAGE IS
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FORTRAN VARIABLE	SUBROUTINE WHERE DEFINED OR USED OFTEN	DEFINITION
ZSMALL	SPRAY	ONE HUNDRETH OF AVERAGE ANGULAR GRID SPACING.
ZSW	STRIDE	W-VELOCITY CONTROL VOLUME WIDTH IN Z DIRECTION.

TABLE C-2. LIST OF FORTRAN VARIABLES IN THE CHEMICAL KINETICS PROGRAM CREK.

This list is adapted from Ref. 48 to which the reader is referred for further details.

Fortran Variable	Routines Where Defined Or Used Often	Definition
A	CALC	Elements of Newton-Raphson correction matrix.
AL	CREKO SPECE CALC	Atomic stoichiometric coefficients, AL(I,J) = the number of kg-atoms of element I per kg-mole of species J.
ATOM	ERATIO (SPECE) CREKO	ATOM (1,K) = atomic symbol for element K. ATOM (2,K) = atomic weight of element K. ATOM (3,K) = valence or oxidation state of element K.
ASUB	CREKO	Molecular symbol of each NS species (e.g., CO, H ₂ O, etc.).
BO	SPECE CALC	Atom numbers for reactant mixture, BO(I) = kg-atoms element I per kg reactant mixture.
BX	CREKO CALC	Exponent-on 10 on pre-exponential term of extended Arrhenius forward rate expression, when read from MECHANISM data cards. Later, BX is set = BX*(log _e 10) to avoid repetitive exponentiation on ten.
BX2	CREKO CALC	Same as BX for reverse rate expression.
CPSUM	CALC CREKO HCPS	Non-dimensional mixture constant pressure specific heat capacity.
EMV	CREK CALC	Total convective and diffusive mass inflow rate to the control volume, kg m ⁻³ s ⁻¹ .
ER	CREK ERATIO (SPECE)	Fuel/air equivalence ratio.

TABLE C-2 (Continued).

Fortran Variable	Routines Where Defined Or Used Often	Definition
ETA	SPECE	Self-adjusting under-relaxation parameter.
FQ	CREK CALC	Scaling parameter for Q.
HO	CREKO CALC HCPS	Non-dimensional, ideal-gas enthalpy of each chemical species at given temperature.
HSUBO	CREKO CALC	Convective and diffusive net enthalpy influx rate to the control volume, divided by EMV (i.e., mass-averaged specific enthalpy of reactants entering the control volume), J/kg. HSUBO must be set by the calling program.
HSUM	CREKO CALC	Working variable wherever used.
ID	CREKO CALC	ID(K,J) is the species index number (i=1, NS) of the K-th species (K=1,4) in the J-th reaction (J=1,JJ).
IDCO, IDC02 IDH2, IDH20 IDN2, ID02	CALC	Index number (i=1,NS) of the particular species in the variable name.
IHCPS	CREKO CALC HCPS	Value of IHCPS controls whether or not subroutine HCPS calculates values of non-dimensional one-atmosphere entropy for each species.
ILC, ILH	CREKO CALC	Index number of the elements carbon and hydrogen, respectively.
IMAT	SPECE CALC	Number of rows in Newton-Raphson correction matrix; set in CALC. IMAT=N2 if LEQUIL=.TURE.: IMAT=NQ if LEQUIL=.FALSE..

TABLE C-2 (Continued)

Fortran Variable	Routines Where Defined Or Used Often	Definition
ITER	SPECE	Current value of iteration counter.
ITMAX	SPECE	Controls the maximum number of iterations permitted by each call to CREK. Set by DATA statement in SPECE.
JJ	CREKO CALC	Number of distinct forward reactions considered in reaction mechanism; must be less than or equal to the dimensions of labeled COMMON block REACTS.
LADIAB	CREK CALC	LADIAB must be set by program calling CREK. If = .FALSE., enthalpy source term Q is non-zero, and calling program must specify values of Q0, Q1, Q2, Q3 and Q4 in enthalpy source term.
LCONVG	CREK SPECE	Initially = .FALSE.; set = .TRUE. in SPECE if convergent solution achieved. Controls solution strategy in CREK.
LDEBUG	SPECE CALC	If LDEBUG is set = .TRUE. by the calling program, intermediate output is written on the output record. Default value is .FALSE.
LEQUIL	CREK SPECE CALC	LEQUIL must be set by calling program. If = .TRUE., equilibrium states are calculated; if = .FALSE., kinetic stationary states are calculated.
LNRG	CREK CALC	For LEQUIL = .FALSE. problems only. If = .TRUE., fully coupled energy equation is used.
LREACT	CREK	LREACT = .FALSE. on entry to CREK suppresses calculation of combustion reaction. Default value is .TRUE.

TABLE C-2 (Continued)

Fortran Variable	Routines Where Defined Or Used Often	Definition
NDEBUG	CREK SPECE CALC	When LDEBUG = .TRUE., NDEBUG set from 1 to 5 controls increasing detail of debug output. Default value of NDEBUG = 5.
NGLOB	CREKO CALC	Number of finite-rate global hydrocarbon pyrolysis steps considered.
NGLOBP	CREKO CALC	NGLOB + 1.
NLM	CREKO SPECE CALC	The number of distinct elements considered. Must be less than or equal to corresponding dimensions of labeled COMMON block CEQUIL.
N1,N2,N3	CREKO CALC	N1 = NLM + 1, N2 = NLM + 2, N3 = NLM + 3.
NS	CREKO SPECE CALC	Number of distinct species considered. Must be less than appropriate dimensions in labeled COMMON blocks CEQUIL, CMATRI, CPARAM and CSPECE.
NSM, NQ, NA	CREKO CALC	NSM = NS + 1, NQ = NS + 2, NA = NS + 3.
PA	CREK SPECE CALC	Pressure within control volume, N m ⁻² . Must be set by program calling CREK.
PI	CALC	Lagrange multipliers in reduced Gibbs iteration correction equations.
PPLN	CREK CALC	Loge (P/P ₀).
Q	CALC	Negative of non-dimensional enthalpy source term, determined by values of Q0, Q1, Q2, Q3 and Q4 set by the calling program.

TABLE C-2 (Continued)

Fortran Variable	Routines Where Defined Or Used Often	Definition
Q0, Q1, Q2, Q3, Q4	CALC	Coefficients for enthalpy source term, $-S_H = Q_0 + Q_1 T + Q_2 T^2 + Q_3 T^3 + Q_4 T^4$, $Jm^{-3} s^{-1}$. These values must be set whenever LADIAB = .FALSE. is set by the calling program.
RGAS	CREKO CALC	Universal gas constant, 8314.4 J/(kg-mole) (K).
RGASIN	CREKO CALC	Inverse of RGAS.
RHOP	CREKO CALC	Mass density , kg m ⁻³ .
RT	CALC	$\frac{\partial f_i}{\partial \log T}$
SO	CREKO CALC HCPS	One-atmosphere, ideal-gas entropy of species i.
S1	CREKO CALC	Inlet mole numbers of species i.
S2	CREKO CALC	Mole numbers of species i, kg-moles i/kg. Calling program must set these values as estimates; on return they are solution values.
SM	ALL	Reciprocal mixture molecular weight.
SMINV	CREK CALC	Reciprocal of SM, therefore the mixture molecular weight, kg/(kg-mole).
SMW	CREKO	Molecular weight of species i.
SSAVE	CREK	Array for saving current values of S2.

TABLE C-2 (Continued)

Fortran Variable	Routines Where Defined Or Used Often	Definition
TACT, TACT2	CREKO CALC	Activation temperature (activation energy divided by gas constant) for forward and reverse reactions respectively, degrees K.
TEN, TEN2	CREKO CALC	Exponent-on-temperature in pre-exponential term of rate constant in forward and reverse reactions respectively.
TK	ALL	Temperature T, deg K. Estimate on calling CREK, solution on return. If set equal to zero by program calling CREK, causes CREK to establish estimates for T and S2.
TKINV	CREK CALC	Reciprocal of TK.
TLN	CREKO CALC HCPS	Logarithm of the temperature.
X	CREKO CALC	Current values of the correction variables: Also used as working variable in subroutine CREKO.
X1, X2	CALC	Contact index for forward and reverse reactions j. Dimensionless.
Y	CREKO CALC	Logarithms of variables. Also used as working variable in subroutine CREKO.
Z	CREKO HCPS	Coefficients for calculation of thermochemical data.

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APPENDIX D
LISTING OF THE 3-D COMBUSTOR
PERFORMANCE PROGRAM

APPENDIX D

LISTING OF THE 3-D COMBUSTOR PERFORMANCE PROGRAM

This appendix contains a listing of the 3-D combustor performance program. In order to identify the changes made to the original program of Ref. 1, various correction ident appear at the ends of the changed or newly inserted statements. The meanings of these correction ident are given below:

CREK	
CALC	
SPEC	- Chemical kinetics program CREK
CRKO	
HCPS	
ABSOR	- Radiation-property subroutine
SOOT	- Soot-emissions updates
NASAX	- Corrections to the original program
CTDMA	- Cyclic TDMA updates
NOXXX	- Updates to make the chemical kinetics program CREK CYBER-Compatible
RAD	
TS0	- Radiation updates
NOX	- NO _x -emissions updates for 3-D program
NOXX	- NO _x -emissions updates for CREK program
4STEP	- 4-Step-mechanism updates
COMMENT	- Comment cards
JAN14	
JAN18	- Some additional modifications
FEB2	
MAR2	

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PROGRAM MAIN(INPUT,OUTPUT,TAPE5=INPUT,TAPE6=OUTPUT,TAPE8,TAPE9,
1 TAPE11)
COMMON F(900,7),NU(10,10,5),DV(10,10,5),DW(10,10,5),
1 AMUC(10,10,5),S00T1(10,10,5),S00T2(10,10,5),FCH(10,10,5),
2 FH2(10,10,5),FS(500,14),
1 RHO(10,10,5),VISC(10,10,5),ABSR(10,10,5),SCTR(10,10,5),
1 SU(10,10),SP(10,10),DRHONP(10,10,5),
1 AXP(10,10),AXM(10,10),AYP(10,10),AYM(10,10),AZP(10,10),
2 AZP(10,10),C7(10,10),CY(10,10),CZU(10,10),CYU(10,10),
3 CZP(10,10),CVP(10),DIVG(10,10),NTP1,NTP2
1,AKMK(192),AXPK(192),AYMK(192),AYPK(192),AZMK(192),AZPK(192),
2 SUK(192),SPK(192)
DTMFNSION U(10,10,5),V(10,10,5),W(10,10,5),PP(10,10,5)
DTMFNSION P(10,10,5),TEMP(10,10,5),GAM(10,10,5)
FOUIVALENCE (F(1,1),U(1,1,1)),(F(1,2),V(1,1,1)),(F(1,3),W(1,1,1))
EQUIVALENCE (F(1,4),PP(1,1,1)),(F(1,5),P(1,1,1))
EQUIVALENCE (F(1,6),TEMP(1,1,1)),(F(1,7),GAM(1,1,1))
COMMON/CYL/R(30),RM(30),RHM(30),YSR(30),YSVR(30),IPALX
COMMON/GRID/X(40),Y(30),Z(30),XS(40),YS(30),ZS(30),XSU(40),
1 YSV(30),ZSU(30),X0IF(40),Y0IF(30),Z0IF(30),FXP(40),FXM(40),
2 FYP(30),FYR(30),F7P(30),F2M(30),DT,TIME
COMMON
1/CIMDFX/IDCC,IDFU,IDO2,IDH2,IDH2D,IDCO2,IDH1,IDH2,IDM1,IDM0,IDM02
1,IDO0,IDOM,ICPSS,ILC,ILH,IMAT,ITER,JJJ,N1,N2,N3,NA,NGLOB,NGLOAP,
2 NLM,NG,NSP,NS1,NS2,ICDH
3/CCHFM/CPSUP,HSUM,FQ,PPLN,RGAS,RGASIN,SMINV,TKINV,TLN,LNRG
4/CARAM/ASUB(30,3),EMV,ER,HSUB0,NDEBUG,NS,PA,QQ,Q1,Q2,Q3,Q4,RHOPP,
4 SM,SMU(30),SM0,S1(30),S2(30),TK,LADTAB,LDEBUG,LFEUIL,LPEACT,
4 LENER,EDRJ,LCNVG
DOUBLE PRECISION CPSUM,ENV,ER,FQ,HSUB0,HSUM,PA,PPLN,QQ,Q1,Q2,Q3,
1 Q4,RGAS,RGASIN,RHOPP,SM,SMINV,SHW,S1,S2,TK,TKINV,TLN,SM0
2,FUT,FST
COMMON/STEP4/PEXP1,PEXP2,PEXP3,PEXP4,ER1,ER2,ER3,ER4,CERU1,CERU2,
1 CERU3,CERU4,EXP1,AEXP2,AEXP3,AEXP4,EXP1,REXP2,BEXP3,REXP4,
2 REXP1,CEXP2,CEXP3,CEXP4,FUT,FST
LOGICAL LADTAB,LCNVG,LDEBUG,LEQUIL,LNRG,LREACT,LENER
COMMON/INT/L,N,NCV,LCV,NCV,LPI,MP1,MP1,NT,NJ,NK,NINJ,NINJNK,NV,
1 NNV,NGOTD,K,ISTR,JSTR,KSTR,NVM(35),KM(30),JM(30),ISTEP,
2 ISOLVE(32),IPRINT(33),TITLE(10,33),IXY,ISWP,JSWP,RELAX(35),NP,
3 VRHO,NGAM,IULI(30,5),IWLO(30,5),JWLO(40,5),JWLI(40,5),IWFI,
4 IWFO,MRI,JWII,JWIO,JWDI,JWDO,INW,JKIN(30,30),IKIN(40,30)
COMMON/INDEX/IPAR,LPREF,ISTUN,INCOMP,ITRAD,NVRX,NVRY,NVRZ,JPLANE
1,PLAKM2,LVK,LVD,LVFUOX,LVFU,LVCO,LVH,LVRX,LVRY,LVRZ,NVF(32),
2 IJUMP,IRFS,TITLE2(20),IMAX,JMAX,KMAX,NVCO,FUMCC,NVH20,NVC02,
3 NVN2,NVCH,NVM2
COMMON/CNDR/LVH1,LVH2,LVN1,LVNO,LVNO2,LVO,LVNH,LVH20,LVN2,LVO2,
1 LVCO2,LVFU1,LVC01,NN0X,IN0X,ITNOX,SN0X,TNOX
COMMON/THRM/NVH,NVFU,NV0X,NVFUOX,NVTE,MODFN,IKR,FSTOIC,HFU,CP,
1 GASCON,RHOCN,UNICON,PRSS,NVFV,TCYLW,TINLW,TIP,ACOEF(4),
2 T4,OFAC,WFU,WCO,WNOX,WH20,HN2,HYY,CXX,RATIO1,RATIO2,
3 RATIO3,RATIO4,HCO,TAN,ITWALL
COMMON/CTDPA/KEND,ICTDMA(32)
COMMON/MIS/AMU,OPEN,SMAX,SSUM,LASTEP,HTCENT,CFR,EMISH,EMISIN,
1 FMTSR,TOUT,RTCD,EM1,RADIN,RADSUR,FMA,FK,SGFK,
2 FKFU,FDFFU,TFUEL,MFN2,FLD(40),TEMTH(40),H(40),FUEL(40),FUDX(40),
2 UTM(40),TIN(40),FUELS(40),SFKIT,IGAM1(29),IGAM2(29)
COMMON/TIIR/NVK,NVD,C1,C2,CD,AK,QUICKJ(3,3),AKFAC,ALFAC,
1 MDEL,PR(92),PRF(32),PJAY(32),E
COMMON/RAD/NVE,SIGMA,ARSOR,SCATR
COMMON/REACT/ARCON1,PREXP1,CR1,ARCON2,PREXP2,CR2,MODER
COMMON/DRDPL/FVAP(192),NTP4,NFM2,K0(3),Y0(3),Z0(3),ALFA(3),
1 BETA(3),DELTA(3),THETA1(3),THETA2(3),NSL(3),MFF(3),SM0(3),
2 VFUEL(3),RFUEL(3),FVSU(64),HEVAP
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RFAD(5,100) IWEI, JWI0, IWE0, JW00
IF (IWEI.EQ.2) GO TO 82
RFAD(5,100) (JWL)(J,4), J=JWI0, MP1)
RFAD(5,100) (JWL0(I,4), I=1, XWEI)
82 CONTINUE
IF (IWE0.EQ.1) GO TO 83
RFAD(5,100) (JWL0(J,4), J=JW00, MP1)
READ(5,100) (JWL0(I,4), I=IWE0, LP1)
83 CONTINUE
GO TO (23, 24), IPAR
24 IREF=L
JREF=M
KREF=N
LPREF=NM(KREF)+JM(JREF)+IREF
23 CONTINUE
DO 25 J=1, MP1
GO TO (260, 265), IPLAK
260 RIJ)=1.0
GO TO 25
265 RIJ)=RI+Y(IJ)
27 CONTINUE
C+-----+-----+-----+-----+-----+-----+-----+-----+-----+-----+-----+
CALL STRID1
C+-----+-----+-----+-----+-----+-----+-----+-----+-----+-----+-----+
CHAPTER 3 -----DEPENDENT VARIABLES-----+-----+-----+-----+-----+-----+
READ (5,101) PRESS, DEN, ARSDR, SCATR, AKFAC, ALFAC
READ (5,101) CKX, HYY, HFU, FUNCO
READ (5,101) PREXP1, ARCON1, CR1, PREXP2, ARCON2, CR2
READ(5,101) PREXP3, ARCON3, CR3, PREXP4, ARCON4, CR4
READ(5,101) AA1, BB1, CC1, AA2, BB2, CC2
RFAD(5,101) AA3, BB3, CC3, AA4, BB4, CC4
READ (5,101) C1, C2, CD, AMU, ERROR, TCYLW, TINLW, TLIP
READ (5,101) LASTFP, IJUMP, JSW1, JSW2, NUINJ, NVINJ
103 FORMAT (2(I3, 7X), 6(I2, 8X))
READ (5,101) USW, VSW, SWND, AFSW, FSW, TSW
C-----FUEL INJECTION DATA.
READ (5,102) NFNZ, ISPRAY, TFUEL
102 FORMAT (2(I2, 8X), 6E10.4)
IF (NFN7.LE.0) GO TO 110
DO 115 I=1, NFNZ
READ (5,103) X0(I), Y0(I), Z0(I), ALFA(I), BETA(I), DELTA(I), THETA1(I),
1 THETA2(I), RNSL, WFF(I), SMD(I), VFUEL(I), RFUEL(I)
115 NSL(I)=IFIX(RNSL)
DO 120 II=1, NFNZ
Y0(II)=X0(II)*CLEND(IU)
Y0(II)=Y0(II)*CLEND(IU)
GO TO (125, 130), IPLAK
125 Z0(II)=Z0(II)*CLEND(IU)
GO TO 135
130 Z0(II)=Z0(II)*CANG(IU)
129 ALFACT(I)=ALFA(II)*CANG(IU)
BETA(II)=BETA(II)*CANG(IU)
DELTA(II)=DELTA(II)*CANG(IU)
THETA1(II)=THETA1(II)*CANG(IU)
THETA2(II)=THETA2(II)*CANG(IU)
WFF(I)=WFF(I)*CMASS(IU)
RFUEL(I)=RFUEL(I)*CLEND(IU)
120 VFUEL(I)=VFUEL(I)*CLENV(IU)
110 CONTINUE
TFUEL=TFUEL+CTEMP(IU)
AMU=AMU*CMASS(IU)/CLENV(IU)
PRESS=PRESS*CPRESS(IU)
DEN=DEN*CMASS(IU)/CLEND(IU)/CLEND(IU)/CLEND(IU)
TCYLW=TCYLW+CTEMP(IU)

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TINLW=TINLW+CTEMP(IU)                               MA    117
TLTP=TLIP+CTEMP(IU)                                MA    118
USM=USM+CLENV(IU)                                 MA    119
VSM=VSM+CLENV(IU)                                 MA    120
AFSM=AESM+CHASS(IU)                                MA    121
FSM=FSM+CHASS(IU)                                 MA    122
TSW=TSW+CTEMP(IU)                                 MA    123
COMMENT 2
C-----FILM COOLING DATA.
IF (NUINJ.LE.0) GO TO 85
READ (5,100) (UINJ(I),I=1,NUINJ)                  MA    124
READ (5,100) (UINJ(I),I=1,NUINJ)                  MA    125
READ (5,100) (UINJ(I),I=1,NUINJ)                  MA    126
READ (5,101) (UINJ(I),I=1,NUINJ)                  MA    127
READ (5,101) (UINJ(I),I=1,NUINJ)                  MA    128
READ (5,101) (UINJ(I),I=1,NUINJ)                  MA    129
READ (5,101) (UINJ(I),I=1,NUINJ)                  MA    130
DO 239 II=1,NUINJ
UINJ(II)=UINJ(II)+CLENV(IU)
WUINJ(II)=WUINJ(II)+CLENV(IU)
AUINJ(II)=AUINJ(II)+CHASS(IU)
235 TUINJ(II)=TUINJ(II)+CTEMP(IU)
COMMENT 3
C-----DILUTION JET DATA.
85 IF (NVINJ.LE.0) GO TO 86
READ (5,100) (VINJ(I),I=1,NVINJ)                  MA    136
READ (5,100) (VINJ(I),I=1,NVINJ)                  MA    137
READ (5,100) (VINJ(I),I=1,NVINJ)                  MA    138
READ (5,100) (VINJ(I),I=1,NVINJ)                  MA    139
READ (5,101) (VINJ(I),I=1,NVINJ)                  MA    140
READ (5,101) (EVINJ(I),I=1,NVINJ)                 MA    141
READ (5,101) (DVINJ(I),I=1,NVINJ)                 MA    142
READ (5,101) (AVINJ(I),I=1,NVINJ)                 MA    143
READ (5,101) (TVINJ(I),I=1,NVINJ)                 MA    144
DO 240 II=1,NVINJ
VINJ(II)=VINJ(II)+CLENV(IU)
EVINJ(II)=EVINJ(II)+CLENV(IU)+CLENV(IU)
DVINJ(II)=DVINJ(II)+CLENV(IU)
AVINJ(II)=AVINJ(II)+CHASS(IU)
240 TVINJ(II)=TVINJ(II)+CTEMP(IU)
89 READ(5,100)NSOOT,ISOOT,MPART
C-----SOOT DATA.
TF(NSOOT,EQ.0)GO TO 910
READ(5,101)SSOOT,A0,ARCONN,AAA,BBB,FMG,GO,RHOP
READ(5,101)PREXP,ARCONN,ALPHA,AAS,BBS,DHR,CINCP,TINCP
READ(5,101)(DPART(I),I=1,MPART)
READ(5,101)(FRACP(I),I=1,MPART)
RHOP=RHOP*CHASS(IU)/(CLEND(IU)**3)
DHR=DHR*CFNER(IU)/CHASS(IU)
910 CONTINUE
COMMENT 5
C-----RADIATION DATA.
IF(ITRAO,NE,1)READ(5,105)IRAD,SRAD
105 FORMAT(12.0X,E10.4)
C-----NOX DATA.
READ(5,104)NNOX,INOX,ITNOX,SNOX,TNOX
104 FORMAT(12.0X),2E10.4)
TNOX=TNOX+CTEMP(IU)
CALL CREKO
WFU=17.0*CX*HYV
ISTFP=IRES
DFAC=1.0
SUM1=.01
SUM2=.05
CHAPTER 4 ----- MATERIAL CONSTANTS -----
PRFF(LVD)=AKBAA/(C2-C1)/SORT(CD)
DO 93 NV=2,NNV
PRRAT=PR(NV)/PREF(NV)
93 PJJY(NV)=E0*(PRRAT-1.)/PRRAT**.25
MA    151

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RHCON=PRESS/UNICON
GASCON=UNICON*(0.232/MOX+0.768/MN2)
CHAPTER 5 -----INITIAL VALUES-----
CALL START
IF(INTAPE.NE.C)CALL OUTPUT(INTAPE)
JTRAD=ITRAD
ITRAD=1
JNOX=1
SSUM=1.0E30
C----- MAIN LOOP STARTS -----
60 CONTINUE
IF(JSOOT.EQ.0)GO TO 64
C----START SOOT CALCULATION.
TF(ISTEP.LT.ISOOT.AND.SSUM.GT.SSOOT)GO TO 64
DO 66 II=1,MPART
ISOLVE(LVS1+II-1)=1
66 IPRINT(29+II)=1
ISOLVF(LVN)=1
GO TO 63
64 DO 67 II=1,MPART
ISOLVE(LVS1+II-1)=0
67 IPRINT(29+II)=0
ISOLVF(LVN)=0
IPRINT(23)=0
63 IF(JTRAD.EQ.1)GO TO 65
C----START RADIATION CALCULATION.
TF(ISTEP.GE.IRAD.OR.SSUM.LE.SRAD)ITRAD=JTRAD
IF(ITRAD.F0.1)GO TO 65
ISOLVF(LVRX)=1
ISOLVE(LVRY)=1
ISOLVE(LVR7)=1
IPRINT(11)=1
IPRINT(12)=1
IPRINT(13)=1
IPRINT(14)=1
GO TO 69
69 CONTINUE
ISOLVF(LVRX)=C
ISOLVE(LVRY)=C
ISOLVF(LVRZ)=0
IPRINT(11)=0
IPRINT(12)=0
IPRINT(13)=C
IPRINT(14)=0
69 CONTINUE
IF(JNOX.EQ.0)GO TO 70
C----START NOX CALCULATION.
IF(INNOX.EQ.0)GO TO 60
IF(ISTEP.LT.INOX.AND.SSUM.GE.SNOX)GO TO 60
ISOLVE(LVFU)=0
ISOLVF(LVCO)=0
ISOLVF(LVCH)=0
ISOLVE(LVH2)=C
ISOLVF(LVH1)=1
JNOX=0
INOX=ISTEP
GO TO 70
60 ISOLVE(LVH1)=0
70 CONTINUE
C-----+
IF(ISTEP.F0.100) ISOLVE(LVK)=9
IF(ISTEP.EC.100) ISOLVF(LVD)=9
CALL DENS
ISP=ISPRAY

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	MA	162
	NASAK	0
	MA	164
	MA	165
	NASAX	9
	SOOT	22
	SOOT	23
	NOX	26
	SOOT	24
	MA	167
	MA	168
	SOOT	25
	COMMENT	7
	SOOT	26
	SOOT	27
	SOOT	28
	SOOT	29
	SOOT	30
	SOOT	31
	SOOT	32
	SOOT	33
	SOOT	34
	SOOT	35
	SOOT	36
	RAD	7
	COMMENT	8
	SOOT	38
	RAD	8
	RAD	9
	RAD	10
	RAD	11
	RAD	12
	RAD	13
	RAD	14
	RAD	15
	RAD	16
	SOOT	39
	RAD	17
	RAD	18
	RAD	19
	RAD	20
	RAD	21
	RAD	22
	RAD	23
	RAD	24
	NOX	27
	COMMENT	9
	NOX	28
	NOX	29
	NOX	30
	NOX	31
	4STEP	22
	4STEP	23
	NOX	32
	NOX	33
	NOX	34
	NOX	35
	NOX	36
	NOX	37
	MA	169
	MA	170
	MA	171
	MA	172
	MA	173

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? UIN(40),TIN(40),FUELS(40),SEXIT,IGAM1(29),IGAM2(29)		
COMMON/TURB/NVK,NVD,C1,C2,CD,AK,DUODXJ(3,3),AKFAC,ALFAC,	4STEP	13
1 MODEL,PR(32),PRFF(32),PJAY(32),E	CONGEN	6
COMMON/RAD/NVE,SIGMA,ABSOR,SCATR	4STEP	14
COMMON/REACT/ARCON1,PREXP1,CR1,ARCON2,PREXP2,CR2,MODER	CONGEN	8
COMMON/DRDPL/EVAP(192),NTP4,NFNZ,XO(3),YO(3),ZO(3),ALFA(3),	CONGEN	9
1 RETA(3),DELTA(3),THETA1(3),THETA2(3),MSL(3),WFF(3),SND(3),	CONGEN	10
2 VFUFL(3),RFUEL(3),EVSU(64),HEVAP	CONGEN	11
COMMON/INJECT/FLNWIN,IUINJ(20),JIINJ(20),UINJ(20),WIINJ(20),	CONGEN	12
1 AUINJ(20),TUINJ(20),IVINJ(20),JVINJ(20),KVINJ(20),VINJ(20),	CONGEN	13
2 EVINJ(20),DVINJ(20),AVINJ(20),TVINJ(20),WIINJ,WVINJ,JSW1,JSW2,	CONGEN	14
3 USW,VSW,AFSW,FSW,TSM,MSW,SWNO,RHOSW	CONGEN	15
COMMON/CSDCT/LVN,MVS1,MVS2,ISOOT,SSOOT,NSOOT,AD,ARCONN,AAA,BBB,FNG	CONGEN	16
1,GO,MRART,DPART(2),FRACP(2),RHOP,ARCONS,PREXPS,ALPHA,AAS,BBS,DHR	SOOT	8
2,LVN,LVS1,LVS2,CINCP,TINCP,FUTOT	SOOT	9
COMMON/CRAD/IPAD,SRAD	SOOT	10
COMMON/CFDUR/PREP3,ARCON3,CR3,PREXP4,ARCON4,CR4,AA1,BB1,CC1,	SOOT	11
1 AA2,AB2,CC2,AA3,BB3,CC3,AA4,BB4,CC4,RATIO5,RATIO6,RATIO7,	4STEP	12
2 RATIO6,RATIO9,RATO10,RATO11,RATO12,WCH,WH2,WC2H4,LVCH,LVCH1,LVH21	4STEP	13
DATA NI,NJ,NK,NNV/10,10,5,29/	4STEP	17
DATA AK,E/.43,9./	4STEP	24
DATA UNICON,SIGMA/0314.,5.669E-08/	MA	203
DATA NVK,NVD,NVFUOX,NVFU,NVCH,NVCD,NVH2,NVTE,NVH,NVN,MVS1,MVS2	MA	204
1/4,5,4,5,14,6,9,11,12,13/	4STEP	25
DATA NVFAV,NVRX,NVRY,NVRZ/10,1,2,3/	MA	206
DATA IDFC,IDC2,IDN2,IDCO,IDCW,IDH2,IDH20,IDC02,IDH1,IDN1,IDNO,	4STEP	27
1 IDN02,IDO,IOOM/1,2,3,4,5,6,7,8,9,10,11,12,13,14/	4STEP	28
DATA NVFF/1,2,3,4,5,4,5,14,8,19,9,11,12,13,16,17,18,19,20,21,22,	4STEP	29
1 23,24,25,26,27,28,29,1,2,3/	4STEP	30
DATA LVK,LVD,LVFUOX,LVFU,LVCH,LVC0,LVH2,LVH,LVN,LVS1,LVS2/3,6,	4STEP	31
1 7,8,9,10,11,12,13,14,15/	4STEP	32
DATA LVFU1,LVC02,LVN2,LVC01,LVCH1,LVH21,LVH20,LVC02,LVH1,LVN1,	4STEP	33
1 LVNO,LVNQ2,LVQ,LVOM/16,17,18,19,20,21,22,23,24,25,26,27,28,29/	4STEP	34
DATA LVRX,LVRY,LVRZ/30,31,32/	4STEP	35
DATA NVH20,NVEX,NVCD2,NVN2/1,2,3,4/	MA	210
DATA NP,NRHO,NGAM/33,34,35/	4STEP	36
DATA WC02,WCD,WDX,WH2D,WN2,WH2,WC2H4/44.,28.,32.,18.,28.,2.,20./	4STEP	37
DATA IGAM1,IGAM2/1,0,3*1,24*0,0,4*1,24*0/	4STEP	38
DATA ACDEF/-1306.01,6620.37,-6167.00,1336.65/	NA	214
END	NA	215
SUBROUTINE INIT	NASAX	10
COMMON F(500,7),DU(10,10,5),DV(10,10,5),DW(10,10,5),	COMFA	2
1 ANUC(10,10,5),SOUT1(10,10,5),SOUT2(10,10,5),FCM(10,10,5),	4STEP	1
2 FH2(10,10,5),FS(500,14),	4STEP	2
1 RH0(10,10,5),VISCI(10,10,5),ABSR(10,10,5),SCTR(10,10,5),	RAD	1
1 CU(10,10),SP(10,10),DRH0DP(10,10,5),	RAD	2
1 AXP(10,10),AXP(10,10),AYP(10,10),AYH(10,10),AZP(10,10),	COMFA	4
2 ATM(10,10),CZ(10,10),CY(10),CZU(10,10),CYU(10),	COMFA	5
3 CZP(10,10),CYP(10),DIVG(10,10),NTP1,NTP2	COMFA	6
1,AKPK(192),AXPK(192),AYMK(192),AYPK(192),AZMK(192),AZPK(192),	CTOMA	1
2 SHK(192),SPK(192)	CTOPA	2
DIMENSION U(10,10,5),V(10,10,5),W(10,10,5),PP(10,10,5)	COMFA	7
DIMENSION P(10,10,5),TEMP(10,10,5),GAM(10,10,5)	COMFA	8
EQUIVALENCE (F(1,1),U(1,1,1)),(F(1,2),V(1,1,1)),(F(1,3),W(1,1,1))	COMFA	9
EQUIVALENCE (F(1,4),P(1,1,1)),(F(1,5),P(1,1,1))	COMFA	10
EQUIVALENCE (F(1,6),TEMP(1,1,1)),(F(1,7),GAM(1,1,1))	COMFA	11
COMMON/CYL/R130),RM(30),RMV(30),YSR(30),YSVR(30),IPMAX	COMMON	2
COMMON/GRD/X(40),Y(30),Z(30),XS(40),YS(30),ZS(30),XSU(40),	COMMON	3
1 YSV(30),ZSH(30),XDIF(40),YDIF(30),ZDIF(30),FXP(40),FXM(40),	COMMON	4
2 FYP(30),FYM(30),FZP(30),FZN(30),DT,TIME	COMMON	5
COMMON	NOX	2
1/CINDEX/IDCF,IDFU,IDO2,IDN2,IDH20,IDC02,IDH1,IDH2,ION1,IDNO,IDNO2	NOX	3
1,IDO,IDOH,IMCPS,ILC,ILH,IMAT,ITER,JJJ,N1,N2,N3,NA,NGLOB,NGLOBF,	NOX	4
2 NLM,NQ,NSM,NS1,NS2,ICHC	4STEP	3

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RATIO9=HYY*WH2/(2.0*WFU)	4STEP	45
RAT010=(HYY-2.0)*WH2/(2.0*WCH)	4STEP	46
PATO11=CXX*WCD/WCH	4STEP	47
RATO12=WH2/WFU	4STEP	48
FSTDIC=RAT012/(RATIO1+RATIO2)	AL	49
HFU=HFU/1.987	NOX	50
CFR=.003	AL	51
EMISW=.0	AL	52
EMISIN=.1	AL	53
EMISR=.1	AL	54
UMASS=0.	AL	55
SMASS=1.E-30	AL	56
ASH=AFSW-FSW	AL	57
FUMSW=FSW/AFSW	AL	58
FUNXSW=FUMSW	AL	59
WSW=SWN0*USW	AL	60
UMASS=AFSW*USW	AL	61
SPASS=AFSW	AL	62
FK=AMAX1(10.,AKFAC*(UMASS/SMASS)+0.2)*FLOAT(MODEL-1)	AL	63
SQFR=SORT(FK)	AL	64
ASURLR=0.	AL	65
DO 10 J=JSW1,JSW2	AL	66
10 ASURLR=ASURLR+YSR(J)*(Z(NP1)-Z(1))	AL	67
ALIN=.5*ALFAC*(Y(JSW2)+Y(JSW2+1)-Y(JSW1)+Y(JSW1-1))	AL	68
RHOSW=AFSW/ASURLR/USW	AL	69
RTCD=SGRT(CD)	AL	70
DO 40 I=1,LP1	AL	71
40 FUELS(I)=0.	AL	72
C----FUEL INJECTION.	COMMENT	73
IF (NFMZ.LE.0) GO TO 40	AL	74
DO 165 II=1,NFMZ	AL	75
DO 165 I=2,L	AL	76
IF (XO(I),GT,0.5*(X(I)+X(I+1))) GO TO 165	AL	77
FUELS(I)=FUELS(I)+WFF(I)	AL	78
165 CONTINUE	AL	79
40 FUELS(LP1)=FUELS(L)	AL	80
WFN2=FUELS(LP1)	AL	81
C----BOUNDRY CONDITIONS.	COMMENT	82
DO 80 K=1,NP1	AL	83
DO 80 J=1,MPI	AL	84
82 JKIN(J,K)=0	AL	85
DO 80 I=1,LP1	AL	86
80 IKIN(T,K)=0	AL	87
DO 80 K=1,NP1	AL	88
DO 80 J=JSW1,JSW2	AL	89
85 JKIN(J,K)=1	AL	90
84 CONTINUE	AL	91
C----DILUTION JETS.	COMMENT	92
80 IF (INVINJ.LE.0) GO TO 92	AL	93
80 94 II=1,NVINJ	AL	94
I=IVINJ(T)	AL	95
J=JVINJ(T)	AL	96
K=KVINJ(T)	AL	97
IF (J,EQ,JWLI(I,4)) GO TO 96	AL	98
IKIN(T,K)=IKIN(I,K)+2	AL	99
GO TO 94	AL	100
96 IKIN(I,K)=IKIN(I,K)+1	AL	101
94 CONTINUE	AL	102
C----FILM COOLING SLOTS.	COMMENT	103
97 IF (NUINJ.LE.0) GO TO 199	AL	104
DO 198 II=1,NUINJ	AL	105
I=TUTNJ(T)-1	AL	106
J=JUTNJ(T)	AL	107
IF (J,EQ,JWLI(I,4)+1) GO TO 197	AL	108

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    DO 196 K=1,NP1          AL      72
196  IKIN(I,K)=IKIN(I,K)+2   AL      73
      GO TO 198           AL      74
197  DO 199 K=1,NP1          AL      75
198  IKIN(I,K)=IKIN(I,K)+1   AL      76
199  CONTINUE              AL      77
200  CONTINUE              AL      78
C ----- COMPUTE TOTAL FLOW RATE -----          AL      79
201  DO 499 I=1,LPI          AL      80
      FLO(I)=0.             AL      81
      FUEL(I)=0.             AL      82
499  TEMTH(I)=0.            AL      83
      FLO(I)=AFSW            AL      84
      FUEL(I)=FSW             AL      85
      TEMTH(I)=AFSH+TSW       AL      86
C ----- AXIAL INJECTION          AL      87
202  IF (NUINJ.LE.0) GO TO 104        AL      88
203  DO 106 II=1,NUINJ          AL      89
      I=IIINJ(II)-1          AL      90
      FLO(I)=FLO(I)+AUINJ(II)  AL      91
104  TEMTH(I)=TEMTH(I)+TUINJ(II)*AUINJ(II)  AL      92
C ----- RADIAL INJECTION          AL      93
205  IF (NVINJ.LE.0) GO TO 106        AL      94
206  DO 110 II=1,NVINJ          AL      95
      I=IVINJ(II)            AL      96
      FLO(I)=FLO(I)+AVINJ(II)  AL      97
110  TEMTH(I)=TEMTH(I)+TVINJ(II)*AVINJ(II)  AL      98
207  CONTINUEF                  AL      99
C ----- FLOW RATE AT EACH I-STATION          AL     100
208  DO 139 I=2,LPI          AL     101
      FLO(I)=FLO(I-1)+FLO(I)  AL     102
      FUEL(I)=FUEL(I-1)+FUEL(I)  AL     103
139  TEMTH(I)=TEMTH(I-1)+TEMTH(I)  AL     104
      FLOWIN=FLO(LPI)+WFNZ      AL     105
209  DO 145 I=1,LPI          AL     106
      FUUX(I)=FUEL(I)/FLO(I)  AL     107
      FUTOT=FUEL(LPI)+WFNZ      AL     108
      AMASS=FLO(LPI)-FUEL(LPI)  AL     109
      FUARAT=FUTOT/AMASS      AL     110
210  DO 150 I=1,LPI          AL     111
      FUEL1=(FUEL(I)+FUELS(I))/(FLO(I)+FUELS(I))  AL     112
      FUEL2=AMAX1(FUEL1-RATIO2*(1.-FUEL1)/RATIO1,0.)  AL     113
      PHT=FUEL2/FSTCIC        AL     114
      THCP5=3                 NOX     49
      NS1=IDFU                NOX     50
      NS2=IDN2                NOX     51
      TK=TSW                  NOX     52
      TKINV=1.000/TK          NOX     53
      S2(TDFU)=FUFLI/SNW(IDFU)  NOX     54
      S2(TD02)=(1.0-FUEL1)*RATE02/SNW(TD02)  NOX     55
      S2(TDN2)=(1.0-FUFLI)*(1.0-RATIO2)/SNW(TDN2)  NOX     56
      CALL HCPS                NOX     57
      H1=HSUM*UNICCR*TK        NOX     58
      TIN(I)=TSW               AL     117
      FUB=FUEL1-FUEL2          AL     118
      FLPC02=WC02*(CXX*FUB/WFU-CXX*FUNCO/WCH-FUNCO/WCO)  4STEP   49
      FLPOX=RATIO1+FUEL2*RATIO2*FUNCO+RATIO2*(RATIO1+RATIO2)*FUEL1  AL     120
      1+(RATIO3+RATIC6)*FUNCO  4STEP   50
      FLPOX=AMAX1(FLPOX,0.)    AL     121
      FLPH2O=C(.5*WH2O+(HYY*FUB/WFU-(RATE07+1.01*FUNCO))  4STEP   51
      FLPH2O=1.0-FUEL2-FLPC02-3.0*FUNCO-FLPOX-FI.PH2O  4STEP   52
      IHCP5=4                 NOX     59
      NS1=IDFU                NOX     60
      NS2=IDC02                NOX     61

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S2(IDFUI)=FUEL/FMW(IDFUI)
S2(IDO2)=FLPQH/SMW(IDO2)
S2(IDN2)=FLPN2/SMW(IDN2)
S2(IDC1)=FUNC0/SMW(IDC0)
S2(IDC1)=FUNCC/SMW(IDC1)
S2(IDH2)=FUNCE/SMW(IDH2)
S2(IDH20)=FLPH20/SMW(IDH20)
S2(IDC02)=FLPC02/SMW(IDC02)

C-----IGNITION SEQUENCE.
DO 151 II=1,10
T=TIN(I)
TK=T
TKINV=1.000/TK
CALL MCPS
H2=HSUM*UNICON*TK
CPI=CPSUM*UNICCN
THFW=T+(H1-H2)/CPI
TMAX=ACDEF(1)+PHI*(ACDEF(2)+PHI*(ACDEF(3)+PHI*ACDEF(4)))
TMAX=AMAX1(TMAX,2000.)
TNEW=AMIN1(TNEW,TMAX)
IF (ARS(TIN(I)-TNEW),LT.10.) GO TO 150
151 TIN(I)=TNEW
WRTTE (6,156)
156 FORMAT (' **ERROR=100**')
150 CONTINUE
T4=TIN(LP1)
IMCPS=1
NS1=1002
NS2=10N2
TK=T4
TKINV=1.000/TK
S2(IDO2)=RATIC2/SMW(IDO2)
S2(IDN2)=(1.0-RATT02)/SMW(IDN2)
CALL MCPS
CP=CPSUM*UNICCN

C-----AVERAGE U-VELOCITY AT EACH I-SECTION.
DO 231 I=3,LPI
J1=JWL(I,1)
J2=JWL(I,1)
RH04=PRESS/GASCON/TIN(I-1)
A4=.5*(Z(NP1)-Z(1))*(RM(J2)**2-RM(J1+1)**2)
IF (IPLAX,F0,2) GO TO 231
Y1=.5*(Y(J1)+Y(J1+1))
IF (J1,F0,1) Y1=Y(J1)
Y2=.5*(Y(J2)+Y(J2-1))
IF (J2,F0,MP1) Y2=Y(J2)
A4=(Z(NP1)-Z(1))*(Y2-Y1)
231 UIN(I)=FLD(I-1)/RH04/A4
EMI=EMISW/(2.*EMISW)
RADIN=EMISIN*SIGMA*TSW004
RADSUR=EMISR*SIGMA*T4004
C ----- PRINTOUT INPUT DATA -----
WRTTE (6,1004) TITLE2
1004 FORMAT(1H1,24X,20A4/29X,00(1H-1))
MC RAT=MCRAT,MFU,MFU
WRTTE (6,2010) MC RAT,MFU,MFU
2010 FORMAT (2X,'PHYSICAL INPUT'/8X,14(1H-1)/10X,'1.FUEL-'/,
4 30X,'HYDROGEN-CARBON RATIO-----',1PE12.4,/,
2 30X,'MOLECULAR WEIGHT-----',1PE12.4,' (KG/KGMOLE)''/',
3 30X,'HEAT OF FORMATION-----',1PE12.4,' (CAL/GMOLE)''')
JJ=1
WRTTE (6,2014) JJ,FSW
2014 FORMAT (30X,'INLET-',1X,'MASS FLOW RATE-----',1PE12.4,
1  '(KG/S)')


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WRITE (6,2020) PRESS							
2020 FORMAT (10X,'2.AIR -')							
3 30X,'PRESSURE-----',1PE12.4,' (NEW/SQ.M)')	AL	169					
WRITE (6,2024) JJ,ASW,JD,USW,BJ,SWNO	AL	170					
2024 FORMAT (30X,'INLET-',11,', MASS FLOW RATE-----',1PE12.4,	AL	171					
1 1 , '(M/S)/30X,'INLET-',11,', AXIAL VELOCITY-----',1PE12.4,	AL	172					
2 1 , '(M/S)/30X,'INLET-',11,', SWIRL NUMBER-----',	AL	173					
3 1PE12.4)	AL	174					
HEIGHT=2.0(Y(NP1)=Y(1))	AL	175					
ALNHT=X(LP1)-X(1)	AL	176					
SECTOR=2(NP1)-2(1)	AL	177					
WRITE (6,2025) HEIGHT,ALNHT,SECTOR	AL	178					
2025 FORMAT (2X,'IT. GEOMETRICAL INPUT')/8X,10(1H-)/	AL	179					
1 30X,'CHANNEL HEIGHT OF COMBUSTOR-----',1PE12.4,' (M)')	AL	180					
2 30X,'LENGTH OF COMBUSTOR-----',1PE12.4,' (M)')	AL	181					
2 30X,'ANGULAR SECTOR-----',1PE12.4,' (RAD-M1)')	AL	182					
WRITE (6,2029) JJ,ASWRLR	AL	183					
2029 FORMAT (30X,'INLET-',11,', FLOW AREA-----',1PE12.4,	AL	184					
1 1 ,(SQ.M)')	AL	185					
IF (NUINJ+NVINJ+NFNZ.GT.0) WRITE (6,2030)	AL	186					
2030 FORMAT (2X,'III. AIR INJECTIONNS')/8X,14(1H-)	AL	187					
IF (NUINJ.LE.0) GO TO 770	AL	188					
WRITE (6,2031)	AL	189					
2031 FORMAT (10X,'1.FILM COOLING AIR-')	AL	190					
WRITE (6,2033)	AL	191					
2033 FORMAT (25X,'SLOT NO',4X,'I',5X,'J',4X,'K',8X,'U-VELOCITY',	AL	192					
1 5X,'V-VELOCITY',5X,'W-VELOCITY',6X,'MASS FLOW',6X,'FUEL FLOW'/	AL	193					
2 50X,'(M/S)',10X,'(M/S)',10X,'(M/S)',10X,'(KG/S)',9X,'(KG/S)')	AL	194					
DO 772 II=1,NUINJ	AL	195					
I=IUINJ(II)	AL	196					
J=JVINJ(II)	AL	197					
772 WRITE (6,2090) II,I,J,KUDEF,UINJ(II),UDEF,WUINJ(II),AVINJ(II)	AL	198					
770 IF (VINIJ.LE.C1) GO TO 774	AL	199					
WRITE (6,2034)	AL	200					
2034 FORMAT (/10X,'2.DILUTION AND SECONDARY AIR-')	AL	201					
WRITE (6,2033)	AL	202					
DO 776 II=1,NVINJ	AL	203					
I=IVINJ(II)	AL	204					
K=KVINJ(II)	AL	205					
J=JVINJ(II)	AL	206					
776 WRITE (6,2090) II,I,J,K,UDEF,VINJ(II),UDEF,AVINJ(II)	AL	207					
774 CONTINUE	AL	208					
2090 FORMAT (27X,13,4X,13,3X,13,2X,13,8X,1PE10.3,4(5X,1PE10.3))	AL	209					
810 IF (NFNZ.LE.0) GO TO 813	AL	210					
WRITE (6,811)	AL	211					
811 FORMAT (/10X,'3.FUEL NOZZLES-/12X,'X0',8X,'Y0',8X,'Z0',6X,'ALFA',	AL	212					
1 5X,'BETA',5X,'DELTA',4X,'THETA1',4X,'THETA2',7X,'NSL',8X,'WF',	AL	213					
2 7X,'SMO',5X,'VFUEL')/12X,'(M)',7X,'(M)',6X,'(N-R)',4X,'(RAD)',	AL	214					
3 5X,'(RAD)',5X,'(RAD)',5X,'(RAD)',5X,'(RAD)',8X,'(M/S)',6X,'(KG/S)',	AL	215					
4 3X,'(MICRON)',2X,'(M/S)')	AL	216					
DO 811 I=1,NFNZ	AL	217					
RNSL=FLOAT(NSL(I))	AL	218					
811 WRITE (6,811) X0(I),Y0(I),Z0(I),ALFA(I),BETA(I),DELTA(I),	AL	219					
1 THETA1(I),THETA2(I),RNSL,WFF(I),SMO(I),VFUEL(I)	AL	220					
811 FORMAT (9X,1P12E10.2)	AL	221					
812 CONTINUE	AL	222					
812 WRITE (6,2037) FUTOT,ANASS,FUARAT	AL	223					
2037 FORMAT (/2X,'IV. AIR-FUEL BALANCE')/8X,16(1H-)/	AL	224					
1 30X,'TOTAL FUEL FLOW RATE-----',1PE12.4,' (KG/S)')	AL	225					
2 30X,'TOTAL AIR FLOW RATE-----',1PE12.4,' (KG/S)')	AL	226					
3 30X,'FUEL TO AIR RATIO-----',1PE12.4,'/')	AL	227					
WRITE (6,2040) CP,ARCON1,PREXP1,CRI1,ARCON2,PREXP2,CR2,	AL	228					
1 C1,C2,CD	AL	229					
2040 FORMAT (2X,'V. SOME IMPORTANT QUANTITIES')/8X,24(1H-)/	SOOT	230					
	AL	49					
	AL	232					

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1 30X,*SPECIFIC HEAT-----',1PE12.4,I (J/KG-K)** AL 233
2 30X,*ACTIVATION ENERGY (1ST) -----',1PE12.4,I (K)** AL 234
3 30X,*PRE-EXPONENT (1ST) -----',1PE12.4,I AL 235
3 30X,*EDDY BREAKUP CONSTANT (1ST) -----',1PE12.4,I AL 236
7 30X,*ACTIVATION ENERGY (2ND) -----',1PE12.4,I (K)** AL 237
6 30X,*PRE-EXPONENT (2ND) -----',1PE12.4,I AL 238
9 30X,*EDDY BREAKUP CONSTANT (2ND) -----',1PE12.4,I AL 239
4 30X,*TURB. CONSTANT (C1) -----',1PE12.4,I AL 240
4 30X,*TURB. CONSTANT (C2) -----',1PE12.4,I AL 241
4 30X,*TURB. CONSTANT (CD) -----',1PE12.4,I SOOT 50
      WRITE(6,2062)PREXP3,ARCON3,CR3,PREXP4,ARCON4,CR4
2062 FORMAT(30X,*PRE-EXPONENT (3RD) -----',1PE12.4,I 4STEP 55
1 30X,*ACTIVATION ENERGY (3RD) -----',1PE12.4,I 4STEP 56
1 30X,*EDDY BREAKUP CONSTANT (3RD) -----',1PE12.4,I 4STEP 57
1 30X,*PRE-EXPONENT (4TH) -----',1PE12.4,I 4STEP 58
1 30X,*ACTIVATION ENERGY (4TH) -----',1PE12.4,I 4STEP 59
1 30X,*EDDY BREAKUP CONSTANT (4TH) -----',1PE12.4,I 4STEP 60
      WRITE(6,2064)AA1,BB1,CC1,AA2,BB2,CC2,AA3,BB3,CC3,AA4,BB4,CC4
2064 FORMAT(30X,*SPECIES EXPONENTS,A,B,C(1ST) ---,1P3E12.4/I 4STEP 63
1 30X,*SPECIES EXPONENTS,A,B,C(2ND) ---,1P3E12.4/I 4STEP 64
1 30X,*SPECIES EXPONENTS,A,B,C(3RD) ---,1P3E12.4/I 4STEP 65
1 30X,*SPECIES EXPONENTS,A,B,C(4TH) ---,1P3E12.4/I 4STEP 66
C-----UNIT CONVERSION FOR 4-STEP RATE CONSTANTS.
      PREXP1=PREXP1*((WFU**((1.0-AA1)))/((WDX**BB1)*(WC2H4**CC1)))
1*(10.0**(-3.0*(AA1+BB1+CC1)))
      PREXP2=PREXP2*((WC2H4**((1.0-AA2)))/((WDX**BB2)*(WFU**CC2)))
1*(10.0**(-3.0*(AA2+BB2+CC2)))
      PREXP3=PREXP3*((WC0**((1.0-AA3)))/((WDX**BB3)*(WH2O**CC3)))
1*(10.0**(-3.0*(AA3+BB3+CC3)))
      PREXP4=PREXP4*((WH2O**((1.0-AA4)))/((WDX**BB4)*(WC2H4**CC4)))
1*(10.0**(-3.0*(AA4+BB4+CC4)))
      PEKP1=ALOG(PREXP1*((WFU**((AA1-1.0)))*(WDX**BB1)*(WC2H4**CC1)))
      PEKP2=ALOG(PREXP2*((WC2H4**((AA2-1.0)))*(WDX**BB2)*(WFU**CC2)))
      PEKP3=ALOG(PREXP3*((WC0**((AA3-1.0)))*(WDX**BB3)*(WH2O**CC3)))
      PEKP4=ALOG(PREXP4*((WH2O**((AA4-1.0)))*(WDX**BB4)*(WC2H4**CC4)))
      ER1=ARCON1
      FR2=ARCON2
      ER3=ARCON3
      ER4=ARCON4
      CFBU1=CR1
      CERU2=CR2
      CERU3=CR3
      CERU4=CR4
      AEXP1=AA1
      AEXP2=AA2
      AEXP3=AA3
      AEXP4=AA4
      REXP1=BB1
      REXP2=BB2
      REXP3=BB3
      REXP4=BB4
      CFKP1=CC1
      CFKP2=CC2
      CFKP3=CC3
      CFKP4=CC4
      FST=FSTOIC
      IF(IITRAD.EQ.2)WRITE(6,2041)ARSOR,SCATR
2041 FORMAT(
3 30X,*ABSORPTION COEFFICIENT-----',1PE12.4,I AL 243
4 30X,*SCATTERING COEFFICIENT-----',1PE12.4,I AL 244
      IITRAD,EQ.3)WRITE(6,2043)
2043 FORMAT(30X,*ABSORPTION AND SCATTERING COEFFICIENTS CALCULATED*)/
      TFINSOOT,FQ,C1GO TO 401
      WRITE(6,2045)(DPART(T),T=1,MPART)
      SOOT 51
      SOOT 52
      AL 243
      AL 244
      SOOT 53
      SOOT 54
      SOOT 55
      SOOT 56

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2045 FORMAT(30X,*SOOT PARTICLE DIAMETERS(MICRONS)*,1PE12.4,/)
  WRITE(6,2047)(FRACP(I),I=1,MPART)
2047 FORMAT(30X,*RELATIVE FORMATION RATES -----*,1PE12.4,/)
  DO 2049 II=1,MPART
    DPART(II)=1.0E-6*DPART(II)
2049 FRACP(II)=0.01*FRACP(II)
  WRITE(6,2054)AD,ARCONN,PREXPS,ARCONS,ALPHA,AAS,BDS,AAA,BBB,FMG,
  1 GD,RHCP
2054 FORMAT(30X,*PRE-EXPONENT (NUCLEI) -----*,1PE12.4,/
  1   30X,*ACTIVATION ENERGY (NUCLEI) -----*,1PF12.4,/
  2   30X,*PREF-EXPONENT (SOOT) -----*,1PE12.4,/
  3   30X,*ACTIVATION ENERGY (SOOT) -----*,1PF12.4,/
  4   30X,*TEMPERATURE EXPONENT (SOOT) -----*,1PE12.4,/
  5   30X,*FUEL EXPONENT (SOOT) -----*,1PE12.4,/
  6   30X,*OXYGEN EXPONENT (SOOT) -----*,1PE12.4,/
  7   30X,*CONSTANTS IN SOOT FORMATION --,/
  8   35X,*A = *,1PE12.4,5X,*B = *,1PE12.4,/
  9   30X,*CONSTANTS IN NUCLEI FORMATION --,/
  1   35X,*F-G = *,1PE12.4,5X,*G0 = *,1PE12.4,/
  ?   30X,*PARTICLE DENSITY -----*,1PE12.4,* KG/M3*,/)
  WRITE(6,402)ISOOT,SSOOT,CINCP,TINCP
402 FORMAT(30X,*SOOT CALCULATION STARTED AFTER ISTEP,GE.0,I3,
  1 * OR SSUM.LF.0,1PE8.2/30X,*SOOT CALCULATION BYPASSED IF C/N RATIO
  1 LT.4,1PE8.2,* OR IF TEMPERATURE LT.0,1PE8.2)
401 CONTINUE
  IF(ITRAD.NE.1)WRITE(6,365)IRAD,SRAD
365 FORMAT(30X,*RADIATION INCLUDED AFTER ISTEP,GE.0,I3,
  1 * OR SSUM.LF.0,1PE8.2)
  IF(NNOX.NE.0)WRITE(6,403)INOX,SNOX,TNOX
403 FORMAT(30X,*NOX CALCULATIONS STARTED AFTER ISTEP,GE.0,I3,
  1 * OR SSUM.LE.0,1PE8.2/30X,*NOX CALCULATION BYPASSED IF TEMPERATUR
  IE LT.4,1PE8.2)
  WRITE(6,2042)(RELAX(I),I=1,39)
2042 FORMAT(/8X,*RELAXATION PARAMETERS*/8X,2I(1H-)/(5X,1P10E12.3))
  GO TO (2050,2051), MODEL
2050 WRITE(6,2052)(PR(I),I=1,32)
  GO TO 2053
2051 WRITE(6,2052)(PREF(I),I=1,32)
2052 FORMAT(/8X,*PRANDTL NUMBERS*/8X,13(1H-)/(5X,1P10E12.3))
2053 CONTINUE
  WRITE(6,2044)(X(I),I=1,LP1)
2044 FORMAT(/8X,*X-COORDINATES*/8X,13(1H-)/(5X,1P10E12.3))
  WRITE(6,2046)R(1),(Y(J),J=2,MP1)
2046 FORMAT(/8X,*Y-COORDINATES*/8X,13(1H-)/(5X,1P10E12.3))
  WRITE(6,2047)(Z(K),K=1,MP1)
2048 FORMAT(/8X,*Z-COORDINATES*/8X,13(1H-)/(5X,1P10E12.3))
C +-----+-----+-----+-----+-----+-----+-----+
C ----- RESTART OPTIONS
C ----- IF (IRES.EQ.0) GO TO 201
  REWIND NTP1
  DO 202 II=1,2
202 READ(NTPI)
C ----- HERE PP IS PHI, P IS MFUP, DU IS MC0
  READ(NTPI)PP,P,DU
C ----- HERE DV IS ENTHALPY, DW IS FAV
  READ(NTPI)DV,DW
C ----- HERE U IS FX, V IS FY, W IS FZ
  READ(NTPI)U,V,W
  READ(NTPI)TEPP,RHO
  READ(NTPI)FC1,FC2
  READ(NTPI)AMUC,SOOT1,SOOT2
  READ(NTPI)FS
C ----- ABSORPTION AND SCATTERING COEFFICIENTS.
  DO 203 K=1,MP1

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DO 203 J=1,NP1
DO 203 I=1,LPI
ABSR(I,J,K)=ABSOR
203 SCTR(I,J,K)=SCATR
RETURN
C ===== ZERO ARRAYS
201 DO 204 NV=1,N
DO 204 K=1,NP1
DO 204 J=1,NP1
KJM=KM(K)+JM(J)
DO 204 I=1,LPI
ABSR(I,J,K)=ABSOR
SCTR(I,J,K)=SCATR
LP=KJM+I
204 F(ILP,NV)=0.
DO 205 K=2,N
DO 205 J=2,M
KJM=KM(K)+JP(J)
DO 205 I=2,L
LP=KJM+I
C-----SPECIES CONCENTRATIONS.
207 INV=LVO2,LVOM
207 F(ILP,INV)=1,F=15
F(ILP,NVS1)=1.E-5
F(ILP,NVS2)=1.E-6
209 F(ILP,NVN)=1.E0
C +----- U,V,W AND PRESSURE +-----+
DO 491 K=1,NP1
DO 491 J=2,M
IS=IWLI(I,J,4)
IE=IWLO(I,J,4)
DO 491 I=IS,IE
IF (I,EQ.IS) GO TO 492
U(I,J,K)=UIN(I)
492 W(I,J,K)=0.0
IF (J,EQ.JWLI(I,4)+1) GO TO 491
V(I,J,K)=0.0
491 CONTINUE
IF (IPAR.EQ.2) GO TO 259
DO 209 K=1,NP1
DO 209 J=1,NP1
IS=IWLI(I,J,5)
IE=IWLC(I,J,5)
DO 209 I=IS,IE
209 P(I,J,K)=PRESS
C ----- BOUNDARY NCDES
255 DO 240 K=1,NP1
IF (IDW,EQ.1) GO TO 241
DO 242 I=3,LPI
J=JWLI(I,4)
Uff,J,K)=IN(I)
242 CONTINUE
241 CONTINUE
DO 244 J=JSW1,JSW2
I=IWLI(I,J,4)-1
Uff+1,J,K)=USW
V(I,J,K)=VSW
244 V(I,J+1,K)=VSH
247 CONTINUE
DO 245 J=1,NP1
I=IWLO(I,J,4)+1
IF (J,LE,JWCI,OR,J,GE,JWCO) GO TO 245
Uff,J,K)=U(I-1,J,K)
245 CONTINUE

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RAD	28
RAD	29
AL	272
AL	273
4STEP	104
AL	275
AL	276
AL	277
AL	278
RAD	30
RAO	31
AL	279
AL	280
SOOT	90
SOOT	91
SOOT	92
SOOT	93
SOOT	94
COMMENT	19
NOX	91
NOX	92
SOOT	93
SOOT	96
SOOT	97
AL	201
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SOOT	98
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C ----- INJECTION POINTS		AL 319
C-----FILM COOLING SLOTS.		COMMENT 20
IF (NUINJ.LE.0) GO TO 240		AL 320
DO 246 II=1,NUINJ		AL 321
I=IUINJ(II)		AL 322
J=JUINJ(II)		AL 323
U(I,J,K)=UINJ(II)		AL 324
U(I-1,J,K)=0.		AL 325
245 W(I-1,J,K)=WUINJ(II)		AL 326
240 CONTINUE		AL 327
C ----- DILUTION JETS.		COMMENT 21
IF (NVINJ.LE.0) GO TO 249		AL 328
DO 250 II=1,NVINJ		AL 329
I=IVINJ(II)		AL 330
J=JVINJ(II)		AL 331
K=KVINJ(II)		AL 332
V(I,J,K)=VINJ(II)		AL 333
IF (J.EQ.JWL(I,4)) V(I,J+1,K)=VINJ(II)		AL 334
250 CONTINUE		AL 335
249 CONTINUE		AL 336
REWIND NTP1		AL 337
WRITE (NTP1) U,V,W,P		AL 338
C +---+---+---+---+ TURBULENT KINETIC ENERGY AND DISSIPATION +---+---+---+---+		AL 339
DO 437 K=1,NP1		AL 340
DO 418 J=1,MP1		AL 341
KJM=KM(K)+JM(J)		AL 342
IS=IWLI(J,5)		AL 343
IE=IWLD(J,5)		AL 344
DO 418 I=IS,IE		AL 345
LP=KJM+I		AL 346
F(LP,NVK)=FK		AL 347
DY=Y(JWL(I,4))-Y(J)		AL 348
IF (IDW.EQ.1) DY=AMIN1(Y(JWL(I,4))-Y(J),Y(J)-Y(JWL(I,4)))		AL 349
DY=AMAX1(DY,0.)		AL 350
AL=ALFAC*DY		AL 351
418 F(LP,NVD)=CD*FK**1.5/(AL+1.E-30)		AL 352
DO 775 J=JSW1,JSW2		AL 353
LP=KM(K)+JM(J)+IWLI(J,4)-1		AL 354
775 F(LP,NVD)=CD*FK**1.5/ALIN		AL 355
C ----- INJECTION POINTS.		COMMENT 22
C-----FILM COOLING SLOTS.		COMMENT 23
IF (NUINJ.LE.0) GO TO 437		AL 356
DO 270 II=1,NUINJ		AL 357
I=IUINJ(II)-1		AL 358
J=JUINJ(II)		AL 359
LP=KM(K)+JM(J)+I		AL 360
F(LP,NVK)=ARFAC*(UINJ(II)**2+WUINJ(II)**2)		AL 361
AL=ALFAC*YS(J)		AL 362
270 F(LP,NVD)=CD*F(LP,NVK)**1.5/(AL+1.E-30)		AL 363
437 CONTINUE		AL 364
C ----- DILUTION JETS.		COMMENT 24
IF (NVINJ.LE.0) GO TO 272		AL 365
DO 274 II=1,NVINJ		AL 366
I=IVINJ(II)		AL 367
J=JVINJ(II)		AL 368
K=KVINJ(II)		AL 369
LP=KJM+I		AL 370
F(LP,NVK)=EVINJ(II)		AL 371
274 F(LP,NVD)=CD*F(LP,NVK)**1.5/(DVINJ(II)+1.E-30)		AL 372
*77 CONTINUE		AL 373
C ----- HERE PP IS RF, P IS DISSIPATION		AL 374
WRITE (NTP1) PP,P		AL 375
C +---+---+---+---+---+---+---+---+ PHX,FUEL,CO AND TEMP +---+---+---+---+---+---+		AL 376
DO 404 K=1,NP1		AL 377

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DO 404 J=1,MPI
  KJM=KMK(K)+JM(J)
  TS=IWLI(J,5)
  IE=IWLD(J,9)
  DO 405 I=IS,IE
    LP=KJM+I
    F(LP,NVFOUX)=TIN(I)
    IS=IWLI(J,4)
    IE=IWLD(J,4)
    DO 404 I=IS,IE
      LP=KJM+I
      F(LP,NVFUOX)=FUOX(I)
      F(LP,NVFU)=AMAX1(0.,F(LP,NVFUOX)-RATIO2*(1.-F(LP,NVFUOX))/RATIO1)
      F(LP,NVCH)=FUNCO
      F(LP,NVH2)=FUPCO
  404 F(LP,NVCC)=FUPCO
C ----- BOUNDARY NODES
  DO 495 K=1,NPI
  DO 206 I=1,LP1
    J=JWLT(I,4)
    LP=KMK(K)+JM(J)+I
    IF (IDW,EO,0) GO TO 217
    TEMP(I,J,K)=TCYLW
    IF (J,EO,1) GO TO 206
    TEMP(I,J,K)=TINLW
  208 F(LP,NVFUOX)=0.
    F(LP,NVFU)=0.
    F(LP,NVCO)=0.
    F(LP,NVCH)=0.0
    F(LP,NVH2)=0.0
    GO TO 216
  217 TEMP(I,J,K)=TIN(I)
    F(LP,NVFUOX)=FUOX(I)
    FEXIT=FUOX(I)-RATIO2*(1.-FUOX(I))/RATIO1
    F(LP,NVFU)=AMAX1(FEXIT,0.)
    F(LP,NVCC)=0.
    F(LP,NVCH)=0.0
    F(LP,NVH2)=0.0
  216 J=IWLD(I,4)
    LP=KMK(K)+JM(J)+I
    TEMP(I,J,K)=TCYLW
    IF (J,EO,MP1) GO TO 444
    TEMP(I,J,K)=TINLW
  444 F(LP,NVFU)=0.
    F(LP,NVCO)=0.
    F(LP,NVCH)=0.0
    F(LP,NVH2)=0.0
  206 F(LP,NVFUOX)=0.
  DO 210 J=1,MP1
    I=IWLT(J,4)-1
    LP=KMK(K)+JM(J)+I
    IF (J,EE,JSW1.AND.J,LE,JSW2) GO TO 212
    TEMP(I,J,K)=TINLW
    F(LP,NVFUOX)=0.
    F(LP,NVFU)=0.
    F(LP,NVCO)=0.
    F(LP,NVCH)=0.0
    F(LP,NVH2)=0.0
    GO TO 219
  212 TEMP(I,J,K)=TSW
    F(LP,NVFUOX)=FUOXSW
    F(LP,NVFU)=FUMSW
    F(LP,NVCO)=0.
    F(LP,NVCH)=0.0
  219

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F(LP,NVH2)=0.0          4STEP    116
213 I=IWLO(J,4)+1      AL        431
LP=KM(K)+JM(J)+I      AL        432
IF (J,GT,JW01,AND,J,LT,JW00) GO TO 214
TEMP(I,J,K)=TINLW      AL        433
F(LP,NVFUOX)=0.0       AL        434
F(LP,NVFU)=0.0          AL        435
F(LP,NVCO)=0.0          AL        436
F(LP,NVCH)=0.0          AL        437
F(LP,NVH2)=0.0          4STEP    117
GO TO 210               4STEP    118
214 F(LP,NVFUOX)=FUOX(LP1)
FEKIT=FUOX(LP1)-RATIO2*(1.-FUOX(LP1))/RATIO1
F(LP,NVFU)=AMAX1(FFKIT,0.)
F(LP,NVTE)=TIN(I)
F(LP,NVCO)=0.0          AL        438
F(LP,NVCH)=0.0          AL        439
F(LP,NVH2)=0.0          4STEP    119
210 CONTINUE              4STEP    120
C ---- INJECTION POINTS
C ---- FILM COOLING SLOTS.
IF (NUINJ,LE,0) GO TO 495
DO 218 II=1,NUINJ
I=IUINJ(II)-1
J=JUINJ(II)
LP=KM(K)+JM(J)+I
F(LP,NVFUOX)=0.0
F(LP,NVFU)=0.0
F(LP,NVCO)=0.0
F(LP,NVCH)=0.0
F(LP,NVH2)=0.0
218 TEMP(I,J,K)=TUINJ(II)
495 CONTINUE
C ---- DILUTION JETS.
IF (NVINJ,LE,0) GO TO 220
DO 222 III=1,NVINJ
I=IVINJ(III)
J=JVINJ(III)
K=KVINJ(III)
LP=KM(K)+JM(J)+I
F(LP,NVFUOX)=0.0
F(LP,NVFU)=0.0
F(LP,NVCO)=0.0
F(LP,NVCH)=0.0
F(LP,NVH2)=0.0
222 TEMP(I,J,K)=TVINJ(III)
220 CONTINUE
C ----- HERE PP IS PHI, P IS VFU AND DU IS MCO
WRITE (NTP1) PP,P,DU
C +-----+-----+-----+-----+-----+-----+-----+-----+
DO 276 K=1,NPI
DO 276 J=1,NPI
IS=IWLI(J,5)
IE=IWLO(J,5)
KJM=KM(K)+JM(J)
DO 276 I=IS,IE
LP=KJM+I
T=TEMP(I,J,K)
FUR=F(LP,NVFUOX)-F(LP,NVFU)
FLPOX=RATIO1+F(LP,NVFU)+RATIO3+F(LP,NVCO)+RATIO2-(RATIO1+RATIO2)*
 1 F(LP,NVFUOX)+RATIO5+F(LP,NVCH)+RATIO6+F(LP,NVH2)
FLPOX=AMAX1(FLPOX,0.)
FLPH2D=0.5*WH2D*(HYY*FUB/VFU-RATIO7*(F(LP,NVCH)-F(LP,NVH2))
FLPCO2=MCO2*(CXX*FUR/VFU-CXX*F(LP,NVCH)/VCH-F(LP,NVCO)/VCO)
4STEP    121
4STEP    122
AL        434
AL        435
AL        436
AL        437
AL        438
AL        439
AL        440
AL        441
AL        442
AL        443
AL        444
AL        445
COMMENT   25
AL        446
AL        447
AL        448
AL        449
AL        450
AL        451
AL        452
AL        453
AL        454
AL        455
COMMENT   26
AL        456
AL        457
AL        458
AL        459
AL        460
AL        461
AL        462
AL        463
AL        464
4STEP    123
4STEP    124
AL        465
AL        466
AL        467
AL        468
AL        469
AL        470
AL        471
AL        472
AL        473
AL        474
AL        475
AL        476
AL        477
AL        478
AL        479
4STEP    125
AL        480
4STEP    126
4STEP    127

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FLPN2=1.-F(LP,NVFU)-FLPC02-F(LP,NVC0)-FLPOX-FLPH20
1-F(LP,NVCH)-F(LP,NVM2)
1HCPS=3
NS1=1NU
NS2=1DC02
TK=T
TKINV=1.000/TK
FS(LP,1DFU)=F(LP,NVFU)
FS(LP,1D02)=FLPOX
FS(LP,1DH2)=FLPN2
FS(LP,1DC01)=F(LP,NVC0)
FS(LP,1DC1)=F(LP,NVCH)
FS(LP,1DH2)=F(LP,NVM2)
FS(LP,1DH20)=FLPH20
FS(LP,1DC02)=FLPC02
DO 277 II=NS1,NS2
277 S2(II)=FS(LP,II)/SMW(II)
CALL HCPS
HPI=HSUM0UNICCN0TK
F(LP,NVM)=HPI
276 CONTINUE
C +-----+-----+-----+-----+-----+-----+-----+-----+-----+
C      HERE DV IS ENTHALPY, DW IS FAV
      DO 791 K=1,NP1
      DO 791 J=1,NP1
      KJM=KM(K)+JP(J)
      IS=IWLI(J,5)
      IE=IWLO(J,5)
      DO 791 I=IS,IE
      LP=KJM+I
      ST4=SIGMAUTEMP(I,J,K)*04
      F(LP,NVRX)=ST4
      F(LP,NVRY)=ST4
      F(LP,NVRZ)=ST4
      791 F(LP,NVFAV)=ST4
C ----- HERE DV IS ENTHALPY, DW IS FAV
      WRITE (NTP1) DV,DW
C ----- HERE U IS FX, V IS FY, W IS FZ
      WRITE (NTP1) U,V,W
      WRITE (NTP1) TEMP,RHO
C-----SPECIFCS AND SOOT CONCENTRATIONS.
      WRITE(NTP1)FCM,FH2
      WRITE(NTP1)AMUC,SCOT1,SOOT2
      WRITE(NTP1)FS
      RETURN
      END
      SUBROUTINE ALLMOD
      COMMON F(500,7),DU(10,10,5),DV(10,10,5),DW(10,10,5),
1 AMUC(10,10,5),SOOT1(10,10,5),SOOT2(10,10,5),FCM(10,10,5),
2 FH2(10,10,5),FS(500,14),
1 KHN(1C,10,5),VTSC(10,10,5),ABSR(10,10,5),SCTR(10,10,5),
1 SV(10,10),SP(10,10),DRHNDP(10,10,5),
1 AXPK(10,10),AXM(10,10),AYP(10,10),AYM(10,10),ATP(10,10),
2 ATM(10,10),CZ(10,10),CY(10),CZU(10,10),CYU(10),
2 CZP(10,10),CYP(10),DIVG(10,10),NTP1,NTP2
1,AMHK(192),AXPK(192),AYMK(192),AYPK(192),AZHK(192),AZPK(192),
2,SK(192),SPK(192)
      DIMENSION U(10,10,5),V(10,10,5),W(10,10,5),PP(10,10,5)
      DIMENSION P(1C,10,5),TEMP(10,10,5),GAM(10,10,5)
      EQUIVALENCE (F(1,1),U(1,1,1)),(F(1,2),V(1,1,1)),(F(1,3),W(1,1,1))
      EQUIVALENCE (F(1,4),PP(1,1,1)),(F(1,5),P(1,1,1))
      EQUIVALENCE (F(1,6),TEMP(1,1,1)),(F(1,7),GAM(1,1,1))
      COMMON/CYL/R(30),RM(30),RMV(30),YSR(30),YSVR(30),IPAK
      COMMON/GRID/X(40),Y(30),Z(30),XS(40),YS(30),ZS(30),XSU(40),
1 YSV(30),ZSW(30),X0IF(40),Y0IF(30),Z0IF(30),FKP(40),FXN(40),
COMMON

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2	FYP(30),FYH(30),FZP(30),FZH(30),OT,TIME	COMMON	5
	CMMMN	NOX	2
1	CINDFR/IDCO, IDFU, IDO2, IDN2, IDH2D, IDCO2, IDH1, IDH2, IDN1, IDN2, IDN02	NOX	3
2	IDO, IDCH, INCPS, ILC, ILH, TMAT, ITER, JJJ, M1, M2, M3, MA, NGLOR, NGLORP,	NOX	4
?	NLM, NO, NSM, NS1, NS2, IDCH	4STEP	3
3	CCHEMI/CPSUM, HSUM, FO, PPLH, RGAS, RGASIN, SHINV, TKINV, TLH, LNRG	NOX	6
4	CPARAP/ASUB(30,3), EMV, ER, HSU0, HDERUG, MS, PA, Q0, Q1, Q2, Q3, Q4, RHOPP,	NOX	7
4	SM, SHW(30), SMO, S1(30), S2(30), TK, LADTAB, LDEBUG, LEQUIL, LREACT,	NOX	8
4	LENER, EDKIJ, LCONVG	NOX	9
	DOUBLE PRECISION CPSUM, EMV, FR, FO, HSU0, HSUM, PA, PPLH, Q0, Q1, Q2, Q3,	NOX	10
1	Q4, RGAS, RGASIN, RHOPP, SH, SHINV, SHW, S1, S2, TK, TKINV, TLH, SMO	NOX	11
2	FUT, FST	4STEP	4
	COMMON/STEP4/PEXP1, PEXP2, PEXP3, PEXP4, ER1, ER2, ER3, ER4, CEBU1, CEBU2,	4STEP	5
1	CEBU3, CEBU4, AEXP1, AEXP2, AEXP3, AEXP4, BEXP1, BEXP2, BEXP3, BEXP4,	4STEP	6
2	CEXP1, CEKP2, CEXP3, CEXP4, FUT, FST	4STEP	7
	LOGICAL LADIAS, LCONVG, LDERUG, LEQUIL, LNRG, LREACT, LENER	NOX	12
	COMMON/INT/L, P, N, LCV, MCV, NCV, LP1, MP1, NP1, NI, NJ, MJ, MK, MINJ, MINJNK, NV,	COMMON	6
1	NMV, NGOF0, N, ISTR, JSTR, KSTR, HV4(39), KN(30), JM(30), ISTEP,	4STEP	8
2	ISOLVF(32), IPPINT(33), TITLE(10,33), XY, ISWP, JSWP, RELAK(35), NP,	4STEP	9
3	MRHO, NGAM, INLI(30,5), INLO(30,5), JWLO(40,5), JWL1(40,5), INL1,	COMMON	9
4	TWD, PM1, JWI1, JWI2, JWI3, JWI4, JWI5, JWI6, JKIN(30,3), IKIN(40,3),	COMMON	10
	COMMON/INDEX/IPAR, LPREF, ISTUM, INCOMP, ITAD, NVRX, NVRY, NVRZ, JPLANE	COMMON	11
1	PLAXM1, LVK, LVD, LVFUD, LVFU, LVCO, LVH, LVRK, LVRY, LVRZ, NVF(32),	4STEP	10
2	TJUMP, IRFS, TITLE2(20), IMAX, JMAX, KMAX, NVCO, FUNCO, NVH20, NVCO2,	COMMON	13
3	NVN2, NVCH, NVH2	4STEP	11
	COMMON/CNOX/LVH1, LVH2, LVN1, LVN0, LVN02, LVO, LVOH, LVH20, LVN2, LVO2,	NOX	16
1	LVCO2, LVFUD1, LVCO1, NNOX, INOX, ITNOX, SHOK, THOK	NOX	17
	COMMON/THERP/NVH, NVFU, NVOX, NVFU0, NVTE, MODEN, IDK, FSTOIC, HFU, CP,	COMMON	19
1	GASCON, RHOCEN, UNICON, PRESS, NVFAV, TCYLW, TINLW, TLIP, ACOEF(4),	COMMON	16
2	T4, DFAC, WFU, WC02, WCO, WDX, WH20, WN2, HVY, CXX, RATIO1, RATIO2,	COMMON	17
3	RATIO3, RATIO4, HCO, TAN, ITWALL	COMMON	10
	COMMON/CTDMA/KEND, ICTDMA(32)	4STEP	12
	COMMON/MIS/APIU, DEN, SNAK, SSUM, LASTEP, HTCEXT, CTR, EMISH, EMISIM,	COMGEN	2
1	EMISR, TOUT, RTCD, EMI, RADIN, RADSUR, FMA, FM, SQFK,	COMGEN	9
2	FKFU, FDFU, TFUEL, WFN7, FLO(40), TERM(40), H(40), FUEL(40), FUOK(40),	COMGEN	4
2	UTN(40), TIM(40), FUELS(40), SEXIT, IGAMI(29), IGAM2(29)	4STEP	13
	COMMON/TURB/NVK, NVD, C1, C2, CO, AK, DUOIJXJ(3,3), AKFAC, ALFAC,	COMGEN	6
1	MODEL, PR(32), PREF(32), PJAY(32), E	4STEP	14
	COMMON/RAD/NVE, SIGMA, ABSOR, SCATR	COMGEN	8
	COMMON/REACT/ARCON1, PREXP1, CR1, ARCON2, PREXP2, CR2, MODER	COMGEN	9
	COMMON/DROPL/EVAP(192), NTP4, NFH2, X0(31), Y0(3), Z0(3), ALFA(3),	COMGEN	10
1	BETA(3), DELTA(3), THETA1(3), THETA2(3), NSL(3), WFF(3), TMD(3),	COMGEN	11
2	VFUEL(3), RFUEL(3), EVSU(64), HEVAP	COMGEN	12
	COMMON/INJECT/FLOWIN, IWINJ(20), JWINJ(20), UWINJ(20), WWINJ(20),	COMGEN	13
1	AUINJ(20), TUINJ(20), IVINJ(20), JVINJ(20), KVINJ(20), VINJ(20),	COMGEN	14
2	EVINJ(20), OVINJ(20), AVINJ(20), TVINJ(20), HUINJ, NVINJ, JSW1, JSW2,	COMGEN	15
3	USH, VSH, AFSH, FSH, TSW, WSW, S, ND, RHOSW	COMGEN	16
	COMMON/CSOOT/NVM, NVS1, NVS2, ISOOT, SSOOT, NSOOT, AD, ARCONN, AAA, BB0, FMG	SOOT	8
1	GO, MPART, DPART(2), FRACP(2), RHOP, ARCONS, PREXP5, ALPHA, AAS, RDS, DHR	SOOT	9
2	LVN, LVS1, LVS2, CINC, TINC, FUTOT	SOOT	10
	COMMON/CRAD/TRAD, SRAD	SOOT	11
	COMMON/CFOUR/PREXP3, ARCON3, CR3, PREXP4, ARCON4, CR4, AA1, BB1, CC1,	4STEP	12
1	AA2, BB2, CC2, AA3, BB3, CC3, AA4, BB4, CC4, RATIO5, RATIO6, RATIO7,	4STEP	13
2	RATIO8, RATIO9, RAT010, RAT011, RAT012, WCH, WH2, WC2H4, LVCH, LVCH1, LVH21	4STEP	16
C	** * AL	4STEP	17
	ENTRY FMOD	AL	512
C	-----FMTRY FMOD IS USED TO UPDATE BOUNDARY VALUES AND TO LIMIT	AL	513
C	SPECIES MASS FRACTIONS TO LIE BETWEEN 0.0 AND 1.0.	COMMENT	20
	NVFF=NVF(NV)	COMMENT	29
	IF(NV, NF, LVN1)0 TO 1210	AL	514
C	-----NUCLEI CONCENTRATION.	SOOT	102
	DO 1211 K=2,N	SOOT	103
	DO 1211 J=2,P	SOOT	104
	KJM=KM(K1+JM(J))	SOOT	105

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00 1211 I=2,L
LP=KJM+J
1211 F(LP,NVFF)=AMAX1(F(LP,NVFF),1.0)
1210 IF(NV.LT.LVS1.OR.NV.GT.LVS2)GO TO 1310
C----SOOT CONCENTRATION.
00 1311 K=2,N
00 1311 J=2,M
KJM=KM(K)+JM(J)
00 1311 I=2,L
LP=KJM+I
F(LP,NVFF)=AMAX1(F(LP,NVFF),1.E-30)
1311 F(LP,NVFF)=AMIN1(F(LP,NVFF),1.0)
1310 CONTINUE
C----SYMMETRY AXIS UPDATING.
IF(NV.EQ.2)GF TO 2044
00 1005 J=1,MP1
00 1005 K=2,N
LP=LP1+JM(J)+KM(K)
LPW=LP-1
1005 F(LP,NVFF)=F(LPW,NVFF)
IF(IDW,NE,0)GC TO 1044
00 1006 I=2,LP1
00 1006 K=2,N
LP=I+KM(K)
LPN=LP+JM(2)
1006 F(LP,NVFF)=F(LPN,NVFF)
C----- CYCLIC BOUNDARY CONDITIONS -----
00 1002 J=1,MP1
00 1002 I=1,LP1
LIJ=I+JM(J)
LP2=I+JM(J)+KM(2)
LPN=LIJ+KM(N)
LPNP1=LIJ+KM(NP1)
F(LIJ,NVFF)=F(LPN,NVFF)
F(LPNP1,NVFF)=F(LP2,NVFF)
1002 CONTINUE
1001 CONTINUE
IF(NV,NE,LVFUOX)GO TO 1010
C----MIXTURE FRACTION.
00 1020 K=1,MP1
00 1020 J=1,MP1
KJM=KM(K)+JM(J)
00 1020 I=1,LP1
LP=KJM+I
F(LP,NVFF)=AMAX1(F(LP,NVFF),0.1)
F(LP,NVFF)=AMIN1(F(LP,NVFF),1.0)
1020 CONTINUE
GO TO 1036
1010 IF(NV,NE,LVFU)GO TO 1030
C----FUEL CONCENTRATION.
00 1031 K=1,MP1
00 1031 J=1,MP1
KJM=KM(K)+JM(J)
00 1031 I=1,LP1
LP=KJM+I
F(LP,NVFF)=AMIN1(F(LP,NVFF),F(LP,NVFUOK))
1031 F(LP,NVFF)=AMAX1(F(LP,NVFF),0.0)
GO TO 1036
1030 IF(NV,NE,LVCH)GO TO 1032
C----INTERMEDIATE HYDROCARBON CONCENTRATION.
00 1033 K=1,MP1
00 1033 J=1,MP1
KJM=KM(K)+JM(J)
00 1033 I=1,LP1

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LP=KJM+1
F(LP,NVFF)=AMIN1(F(LP,NVFF),RATI00*(F(LP,NVFUDX)-F(LP,NVFUI)))
1033 F(LP,NVFF)=AMAX1(F(LP,NVFF),1.0E-2)
GO TO 1030
1032 IF(INV,NE,LVCH1) GO TO 1034
C-----LU CONCENTRATION.
DO 1035 K=1,NPI
DO 1035 J=1,MP1
KJM=KM(K)+JM(J)
DO 1035 I=1,LP1
LP=KJM+1
F(LP,NVFF)=AMIN1(F(LP,NVFF),RATI04*(F(LP,NVFUDX)-F(LP,NVFUI))
1-RATI01*(F(LP,NVCH1))
1035 F(LP,NVFF)=AMAX1(F(LP,NVFF),1.0E-2)
GO TO 1036
1034 IF(INV,NE,LVH2) GO TO 1030
C-----L2 CONCENTRATION.
DO 1037 K=1,NPI
DO 1037 J=1,MP1
KJM=KM(K)+JM(J)
DO 1037 I=1,LP1
LP=KJM+1
F(LP,NVFF)=AMIN1(F(LP,NVFF),RATI09*(F(LP,NVFUDX)-F(LP,NVFUI))
1-RATI04*(F(LP,NVCH1))
1037 F(LP,NVFF)=AMAX1(F(LP,NVFF),1.0E-2)
1036 CONTINUE
RETURN
C ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** * AL 537
ENTRY VELMOD
C-----ENTRY VELMOD IS USED FOR VELOCITY MODIFICATIONS.
C
C-----INTRODUCE SWIRL GRADUALLY.
DO 1000 K=1,NPI
DO 1000 J=JSW1,JSW2
WIN=WSWR(J)/R(JSW2)
I=LWLI(J,4)-1
W(I,J,K)=W(I,J,K)+0.02*WIN
IF (ABS(W(I,J,K)),GT,ABS(WIN)) W(I,J,K)=WIN
1000 CONTINUE
1003 CONTINUE
DO 2005 J=2,M
DO 2005 I=2,L
W(I,J,2)=W(I,J,NPI)
2007 DW(I,J,2)=DW(I,J,NPI)
2005 CONTINUE
C ----- SATISFY CONTINUITY AT EXIT PLANE
RHUA=0.0
FLJN0T=U,J
INDEX=0
DO 752 K=2,N
JS=JWL1(LP1+4)+1
JE=JWL0(LP1+4)-2
DO 752 J=JS,JE
RHJ(LP1,J,K)=RHO(L,J,K)
KUA=YSH(J)*ZS(K)*RHO(LP1,J,K)
RHJA=RHUA+RDA
FLJNUT=FLJN0T+U(L,J,K)*RUA
IF (U(L,J,K),GE,0.0) GO TO 755
INDEX=1
755 CONTINUE
UADD=(FLJNIN-FLJN0T)/RHUA
SEXIT=1.-FLJNUT/FLJNIN
UMAN=FLJNIN/RHUA
DO 750 K=2,N

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JS=JWL(I(LP1,4)+1          971
JE=JWL0(LP1,4)-1           972
DO 756 J=JS,JE              973
U(LP1,J,K)=AMAX1(0.0,U(L,J,K)+UADD)      NASAK 21
756 CONTINUE
RETURN
C   00 00 00 00 00 00 00 00 00 00 00 00 00 00 00 00 * AL 570
ENTRY DFNMD0
C----FENTRY DFNMD0 IS USED FOR MODIFYING DENSITIES AT RADIAL
C    INJECTION HOLES, INLET SWIRLER, AND FILM COOLING SLOTS.
C
C    IF (INVIND.LE.0) GO TO 750
C----RADIAL INJECTION.
DO 749 II=1,NVINJ           AL 579
I=IVINJ(II)
K=KVINJ(II)
J=JVINJ(II)
M1=J
IF (J.EQ.JWL(I,4)) M1=J+1
AREA=XS(I)*RM(M1)*ZSI(K)
RHODINJ=AVINJ(II)/ABS(VINJ(II))/AREA
749 RHO(I,J,K)=RHODINJ
750 CONTINUE
C----CYCLIC BOUNDARY CONDITIONS.
DO 2060 J=2,M               AL 580
DO 2060 I=2,L               AL 581
RHO(I,J,NP1)=.5*(RHO(I,J,2)+RHO(I,J,M))
RHO(I,J,1)=RHO(I,J,NP1)
2060 CONTINUE
C----INLET SWIRLER.
DO 760 K=1,NP1              AL 582
DO 2061 J=JSW1,JSW2         AL 583
I=IWL(I,J,4)-1             AL 584
2061 RHO(I,J,K)=RHOSW
2099 CONTINUE
C----FILM COOLING SLOTS.
2064 IF (NUINJ.LE.0) GO TO 760
DO 759 II=1,NUINJ           AL 585
I=IUINJ(II)-1
J=JUINJ(II)
AREA=YSR(J)*(Z(NP1)-Z(1))
759 RHO(I,J,K)=2.*AUTND(II)/AREA/UINJ(II)-RHO(I+1,J,K)
760 CONTINUE
RETURN
C   00 00 00 00 00 00 00 00 00 00 00 00 00 00 00 00 * AL 586
ENTRY GAM0D
C----FENTRY GAM0D IS USED TO CALCULATE WALL GAMAS FROM THE WALL
C    FUNCTIONS.
C
DO 3000 K=1,NP1             AL 587
DO 3007 I=1,LP1              AL 588
J=JWL0(I,4)
IF (IKIN(I,K).EQ.2.OR.IKIN(I,K).EQ.3) GO TO 3003
IF (IGAM1(NV).EQ.0) GO TO 3003
YPLUS=VTSC(I,J,K)
IF (YPLUS.GT.21.5) GO TO 3001
GAM(I,J,K)=AMU/PR(NV)
GO TO 3002
3001 GAM(I,J,K)=AMU*YPLUS/PREF(NV)/(ALOG(E*YPLUS)/AK+PDAT(NV))
GO TO 3002
3003 GAM(I,J,K)=0.
3002 J=JWL(I,4)
IF (IDW.EQ.0.CR.IKIN(I,K).EQ.1.OR.IKIN(I,K).EQ.3) GO TO 3004
IF (IGAM1(NV).EQ.0) GO TO 3004

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YPLUS=VISC(I,J,K)
IF (YPLUS.GT.11.5) GO TO 3006
GAM(I,J,K)=AMU/PR(NV)
GO TO 3007
3006 GAM(I,J,K)=AMU*YPLUS/PREF(NV)/(ALOG(E*YPLUS)/AK+PJAY(NV))
GO TO 3007
3004 GAM(I,J,K)=0.
3007 CONTINUE
DO 3000 J=2,M
I=IWLI(J,4)-1
IF (JKIN(J,K).EQ.1) GO TO 3009
IF (IGAM2(NV).EQ.0) GO TO 3009
YPLUS=VISC(I,J,K)
IF (YPLUS.GT.11.5) GO TO 3019
GAM(I,J,K)=AMU/PR(NV)
GO TO 3013
3019 GAM(I,J,K)=AMU*YPLUS/PREF(NV)/(ALOG(E*YPLUS)/AK+PJAY(NV))
GO TO 3012
3009 GAM(I,J,K)=0.
3011 I=IWLO(J,4)+1
IF (J.GT.JNCL.AND.J.LT.JWNO) GO TO 3012
IF (IGAM2(NV).EQ.0) GO TO 3012
YPLUS=VISC(I,J,K)
IF (YPLUS.GT.11.5) GO TO 3013
GAM(I,J,K)=AMU/PR(NV)
GO TO 3000
3013 GAM(I,J,K)=AMU*YPLUS/PREF(NV)/(ALOG(E*YPLUS)/AK+PJAY(NV))
GO TO 3000
3012 GAM(I,J,K)=0.
3000 CONTINUE
CYCLIC BOUNDARY CONDITIONS.
DO 3014 I=2,L
DO 3014 J=2,M
GAM(I,J,1)=.5*(GAM(I,J,2)+GAM(I,J,M))
GAM(I,J,NP1)=GAM(I,J,1)
IF (NV.EQ.3) GAM(I,J,NP1)=GAM(I,J,2)
3014 CONTINUE
RETURN
C ** 00 00 00 00 00 00 00 00 00 00 00 00 00 00 00 00
C-----ENTRY SCMAS
C-----ENTRY SCMAS IS USED TO INCLUDE THE SPRAY EVAPORATION TERM
C-----IN THE VARIOUS EQUATIONS.
C
DO 124 I=1,LPI
DO 124 J=1,MPI
124 DIVG(I,J)=0.
GO TO (266,267,268,269), NGOTO
C ----- U-VELOCITY
266 CONTINUE
270 IF (MFNZ.LE.0) GO TO 271
DO 273 J=2,M
KJK=(K-2)*(NJ-2)+(NJ-2)+(J-2)*(NI-2)
IS=IWLI(J,NGOTO)
IE=IWLO(J,NGOTO)
DO 273 I=IS,IE
LPC=KJK+(I-1)
LYNC=LPC-1
DIVG(I,J)=DIVG(I,J)-FXR(I-1)*EVAP(LXMC1-FKP(I)*EVAP(LPC))
IF (I.EQ.3) DIVG(I,J)=DIVG(I,J)-FXP(2)*EVAP(LXMC1)
IF (I.EQ.1) DIVG(I,J)=DIVG(I,J)-FXM(L)*EVAP(LPC)
273 CONTINUE
271 CONTINUE
RETURN
C ----- V-VELOCITY

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267 CONTINUE
274 IF (INFNZ,LE,0) GO TO 276
   DO 277 J=3,M
      KJK=(K-2)*(NI-2)+(NJ-2)+(J-2)*(NI-2)
      IS=IWLI(J,NGOTO)
      IE=IWLO(J,NGOTO)
      DO 277 I=IS,IE
         LPC=KJK+(I-1)
         LYMC=LPC-(NI-2)
         DIVG(I,J)=DIVG(I,J)-FYM(J-1)*EVAP(LYMC)-FYP(J)*EVAP(LPC)
         IF (J.EQ.3) DIVG(I,J)=DIVG(I,J)-FYP(2)*EVAP(LYMC)
         IF (J.EQ.M) DIVG(I,J)=DIVG(I,J)-FYR(M)*EVAP(LPC)
277 CONTINUE
276 CONTINUE
   RETURN
C ----- W-VELOCITY
268 CONTINUE
278 IF (INFNZ,LE,0) GO TO 281
   DO 282 J=2,M
      KJK=(K-2)*(NI-2)+(NJ-2)+(J-2)*(NI-2)
      IS=IWLI(J,NGOTO)
      IE=IWLC(J,NGOTO)
      DO 282 I=IS,IE
         LPC=KJK+(I-1)
         LZMC=LPC-(NI-2)+(NJ-2)
         LIJ=(J-2)+(NI-2)+(I-1)
         DIVG(I,J)=DIVG(I,J)-FZM(K-1)*EVAP(LZMC)
         IF (K.LT.NP1) DIVG(I,J)=DIVG(I,J)-FZP(K)*EVAP(LPC)
         IF (K.EQ.NP1) DIVG(I,J)=DIVG(I,J)-FZP(2)*EVAP(LIJ)
282 CONTINUE
281 CONTINUE
   RETURN
C ----- OTHER VARIABLES
269 CONTINUE
283 IF (INFNZ,LE,0) GO TO 285
   DO 286 J=2,M
      KJK=(K-2)*(NI-2)+(NJ-2)+(J-2)*(NI-2)
      IS=IWLI(J,NGOTO)
      IE=IWLO(J,NGOTO)
      DO 286 I=IS,IE
         LDC=KJK+(I-1)
         DIVG(I,J)=DIVG(I,J)-EVAP(LDC)
286 CONTINUE
285 CONTINUE
   RETURN
C   *   *   *   *   *   *   *   *   *   *   *   *   *   *   *   *   *   *   *
C ENTRY SOMOD
C-----ENTRY SOMOD IS USED TO INTRODUCE THE BOUNDARY CONDITIONS
C BY MODIFYING THE SOURCE TERMS.
C
COME HERE FOR SLOT COEFFICIENT MODS.
54 IF (NUINJ,LE,0) GO TO 92
   DO 49 II=1,NUINJ
      I=IUTNJ(II)
      J=JUTNJ(II)
      IF (J.EQ.JWLI(I,4)+1) GO TO 149
      M1=J-1
      IF (INV,EQ,1) AYP(I,M1)=.5*AYP(I,M1)
      IF (INV,EQ,1) AYP(I-1,M1)=.5*AYP(I-1,M1)
      IF (INV,GT,2) AYP(I-1,M1)=0.
      IF (INV,NF,1) AYP(I-2,J)=0.
      IF (INV,FQ,LVRX) AXM(I,J)=0.
      GO TO 49
149 M1=J+1

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IF (INV.EQ.1) AYM(I,M1)=.5*AYM(I,M1)
IF (INV.EQ.1) AYM(I-1,M1)=.5*AYM(I-1,M1)
IF (INV.GT.2) AYM(I-1,M1)=0.
IF (INV.NE.1) AXP(I-2,J)=0.
IF (INV.EQ.LVRX) AXM(I,J)=0.
49 CONTINUE
50 CONTINUE
C +---+---+---+---+---+---+---+---+---+---+---+---+---+---+---+---+---+
C----- PRESSURE PERTABATION +---+---+---+---+---+---+---+---+---+---+---+
IF (INV.NF,4) GO TO 200
C-----SLOT MODIFICATIONS.
C-----COMMENT 50
IF (INUINJ.LE.0) GO TO 99
DO 98 II=1,NUINJ
I=IUINJ(II)-1
J=JUINJ(II)
SU(I,J)=0.
98 SP(I,J)=-1.E30
99 CONTINUE
COME HERE FOR DROPLET EVAPORATION TERMS
IF (NFNZ.LE.0) GO TO 344
DO 346 J=2,N
KJK=(K-2)*(NI-2)*(NJ-2)+(J-2)*(NI-2)
IS=IWLI(J,NGOTO)
IE=IWLO(J,NGOTO)
DO 346 I=IS,IE
LPC=KJK*(I-1)
346 SU(I,J)=SU(I,J)+EVAP(LPC)
344 CONTINUE
C-----CALCULATE THE MAXIMUM AND SUM OF CONTINUITY ERRORS.
C-----COMMENT 59
IF (K.NE.2) GO TO 101
SMAX=0.
SSUM=0.
101 CONTINUE
DO 100 J=2,N
IS=IWLI(J,NGOTO)
IE=IWLO(J,NGOTO)
DO 100 I=IS,IE
ASU=ARS(SU(I,J))
SSUM=SSUM+ASU
IF (ASU.LT.SMAX) GO TO 100
IMAX=I
JMAX=J
KMAX=K
SMAX=ASU
100 CONTINUE
IF (K.NE.N) GO TO 102
SMAX=SMAX/FLOWIN
SSUM=SSUM/FLOWIN
102 CONTINUE
200 CONTINUE
C +---+---+---+---+---+---+---+---+---+---+---+---+---+---+---+---+---+
C----- TURBULENCE DISSIPATION +---+---+---+---+---+---+---+---+---+---+---+
IF (INV.NE.LVD) GO TO 300
COME HERE FOR CYLINDRICAL WALL SOURCE TERMS
DO 201 I=2,L
J=JWLI(I,NGOTC)-1
IF (IKIN(I,K).EQ.2.OR.IKIN(I,K).EQ.3) GO TO 1201
DIST=.2*YDIF(J+1)
IF (J.EQ.M) DIST=YDIF(MP1)
L=KM(K)+JM(J)+1
RTCDK=RTCD*F(ILP,NVK)
SU(I,J)=3.E30*RTCDK*SORT(RTCDK)/(AK*DIST)
SP(I,J)=-1.E90
1201 IF (IDWI=201,201,1200
1204 J=JWLI(I,NGOTC)+1
IF (IKIN(I,K).EQ.1.OR.IKIN(I,K).EQ.3) GO TO 201

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DIST=.5*YDIF(J)
IF (J.EQ.2) DIST=YDIF(2)
LP=KM(K)+JM(J)+I
RTCDK=RTCD+F(LP,NVK)
SU(I,J)=1.E30+RTCDK*SQRT(RTCDK)/(AK*DIST)
SP(I,J)=-1.E30
201 CONTINUE
COME HERE FOR SLOT MODIFICATIONS
IF (NUINJ.LE.C) GO TO 710
DO 709 II=1,NUINJ
I=IUINJ(II)-1
J=JIUINJ(II)
M1=J-1
IF (J.EQ.JWL(I,NGOTO)+1) M1=J+1
M2=AMAX0(M1,J)
LP=KM(K)+JM(M1)+I
RTCDK=RTCD+F(LP,NVK)
SKE=AKFAC*(UINJ(II)**2+MUINJ(II)**2)
SLN=ALFAC*VS(J)
SU(I,J)=1.E30*CD+SKE**1.5/(SLN+1.E-30)
SP(I,J)=-1.E30
SU(I,M1)=1.E30+RTCDK*SQRT(RTCDK)/(AK+.5*YDIF(M2))
SP(I,M1)=-1.E30
709 CONTINUE
710 CONTINUE
COME HERE FOR INLET WALL SOURCE TERMS
DO 202 J=2,M1
I=IWLT(J,NGOTC)
IF (JKIN(J,K).EQ.1) GO TO 1202
LP=I+JM(J)+KM(K)
RTCDK=RTCD+F(LP,NVK)
DIST=.5*XDIF(I)
IF (I.EQ.2) DIST=XDIF(2)
SU(I,J)=1.E30+RTCDK*SQRT(RTCDK)/(AK*DIST)
SP(I,J)=-1.E30
1202 I=IWLD(J,NGOTC)
IF (J.GT.JWC1.AND.J.LT.JW001) GO TO 202
LP=I+JM(J)+KM(K)
RTCDK=RTCD+F(LP,NVK)
DIST=.5*XDIF(I+1)
IF (I.EQ.1) DIST=XDIF(LP1)
SU(I,J)=1.E30+RTCDK*SQRT(RTCDK)/(AK*DIST)
SP(I,J)=-1.E30
202 CONTINUE
C +---+---+---+---+---+---+---+---+---+---+---+---+---+---+---+---+
300 IF (INV.NE.1) GO TO 400
COME HERE FOR SLOT MODIFICATIONS
IF (NUINJ.LE.C) GO TO 720
DO 719 II=1,NUINJ
I=IUINJ(II)
J=JIUINJ(II)
SU(I,J)=1.E30*UINJ(II)
SP(I,J)=-1.E30
719 SP(I,J)=-1.E30
720 CONTINUE
COME HERE FOR DROPLET EVAPORATION TERMS
IF (NFMZ.LE.C) GO TO 321
IF (K.EQ.2) REWIND NTP4
READ (NTP4) EVSU
DO 322 J=2,M
KJK=(K-2)+(NI-2)*(NJ-2)+(J-2)*(NI-2)
IS=IWLT(J,NGOTC)
IF=IWLC(J,NGOTC)
DO 322 I=IS,IF

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S2(IDN2)=(1.0-RATIO2)/SMW(IDN2)
CALL HCPS
HPI=HSUM*UNICON*TK
SU(I,J)=1.E300*HPI
736 SP(I,J)=1.E30
802 CONTINUE
COME HERE FOR INLET WALL SOURCE TERMS
DO 803 J=2,M
I=IWLI(J,NGOTO)
IF (JKIN(J,K),EQ,1) GO TO 1803
HTC=.5*(W(I,J,K)+W(I,J,K+1))*RHOC(I,J,K)*CFR
HTC=ABS(HTC)
AREA=YSR(J)*ZS(K)
SU(I,J)=SU(I,J)+HTC*AREA*CPO(TINLW-TEMP(I,J,K))
1803 I=IWLD(J,NGOTO)
IF (J.GT.JWDL.AND.J.LT.JWDL) GO TO 803
LP=I+JMC(J)+KMC(K)
HTC=.5*(W(I,J,K)+W(I,J,K+1))*RHOC(I,J,K)*CFR
HTC=ABS(HTC)
AREA=YSR(J)*ZS(K)
SU(I,J)=SU(I,J)+HTC*AREA*CPO(TINLW-TEMP(I,J,K))
803 CONTINUE
COME HERE FOR CROPLET EVAPORATION TERMS
IF (NFNZ.LE.0) GO TO 319
DO 316 J=2,M
KJK=(K-2)*(NI-2)*(NJ-2)+(J-2)*(NI-2)
IS=IWLI(J,NGOTO)
IE=IWLD(J,NGOTO)
DO 316 I=IS,IE
LPC=KJK+(I-1)
IHCPSS=3
MS1=IDFU
MS2=IDFU
TK=TFUEL
TKINV=1.000/TK
S2(IDFU)=1.000/SPW(IDFU)
HDFU=HSUM*UNICON*TK
SU(I,J)=SU(I,J)+EVAP(LPC)*HDFU
316 SP(I,J)=SP(I,J)-EVAP(LPC)
315 CONTINUE
C   +-----+-----+-----+-----+-----+-----+-----+-----+-----+-----+-----+
900 IF (INV.NE.LVFUOX) GO TO 850
COME HERE FOR SLOT MODIFICATIONS
IF (NUINJ.LE.0) GO TO 851
DO 737 II=1,NUINJ
I=TUINJ(II)-1
J=JUINJ(II)
SU(I,J)=0.
737 SP(I,J)=-1.E30
851 CONTINUE
COME HERE FOR DROPLET EVAPORATION TERMS
IF (NFNZ.LE.0) GO TO 317
DO 318 J=2,M
KJK=(K-2)*(NI-2)*(NJ-2)+(J-2)*(NI-2)
IS=IWLI(J,NGOTO)
IE=IWLD(J,NGOTO)
DO 318 I=IS,IE
LPC=KJK+(I-1)
SU(I,J)=SU(I,J)+EVAP(LPC)
318 SP(I,J)=SP(I,J)-EVAP(LPC)
317 CONTINUE
C   +-----+-----+-----+-----+-----+-----+-----+-----+-----+-----+-----+-----+
950 IF (INV.NE.LVFU) GO TO 951
COME HERE FOR SLOT MODIFICATIONS

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IF (NUINJ,LF,0) GO TO 899
DO 742 II=1,NUINJ
I=IUINJ(II)-1
J=JUINJ(II)
742 SP(I,J)=1.E30
899 CONTINUE
COME HERE FOR DROPLET EVAPORATION TERMS
IF (NFMZ,LF,0) GO TO 319
DO 320 J=2,M
KJK=(K-2)*(NI-2)*(NJ-2)+(J-2)*(NI-2)
IS=IWLI(J,NGOTO)
IE=IWLC(J,NGOTO)
DO 320 I=IS,IE
LPC=KJK+(I-1)
SUI(I,J)=SUI(I,J)+EVAP(LPC)
320 SP(I,J)=SP(I,J)-EVAP(LPC)
319 CONTINUE
C   +--+ +--+ +--+ +--+ +--+ +--+ +--+ +--+ +--+
941 IF(NV,NE,LVCO,AND,NV,NE,LVCH,AND,NV,NE,LVH2,AND,NV,NE,LVH1)GO TO 1 950
COME HERE FOR SLOT MODIFICATION
IF(NUINJ,LF,0) GO TO 959
DO 952 II=1,NUINJ
I=IUINJ(II)-1
J=JUINJ(II)
SUI(I,J)=0.
952 SP(I,J)=1.E30
959 CONTINUE
COME HERE FOR DROPLET EVAPORATION TERMS
951 IF (NFMZ,LF,0) GO TO 950
DO 957 J=2,M
KJK=(K-2)*(NI-2)*(NJ-2)+(J-2)*(NI-2)
IS=IWLI(J,NGOTO)
IE=IWLC(J,NGOTO)
DO 957 I=IS,IE
LPC=KJK+(I-1)
957 SP(I,J)=SP(I,J)-EVAP(LPC)
C   +--+ +--+ +--+ +--+ +--+ +--+ +--+ +--+ +--+
950 IF(NV,NE,LVN)GO TO 1200
COME HERE FOR SLOT MODIFICATIONS
IF(NUINJ,LF,0)GO TO 1203
DO 1207 II=1,NUINJ
I=IUINJ(II)-1
J=JUINJ(II)
SUI(I,J)=0.0
1207 SP(I,J)=-1.0E30
COME HERE FOR DROPLET EVAPORATION TERMS
1203 IF(NFMZ,LF,C1)GO TO 1205
DO 1206 J=2,P
KJK=(K-2)*(NI-2)*(NJ-2)+(J-2)*(NI-2)
IS=IWLI(J,NGOTO)
IE=IWLC(J,NGOTO)
DO 1206 I=IS,IE
LPC=KJK+I-1
1206 SP(I,J)=SP(I,J)-EVAP(LPC)
1205 CONTINUE
RETURN
C   +--+ +--+ +--+ +--+ +--+ +--+ +--+ +--+ +--+
1200 IF(NV,LT,LVS1,OR,NV,GT,LVS2)GO TO 1300
COME HERE FOR SLOT MODIFICATIONS
IF(NUINJ,LF,0)GO TO 1303
DO 1306 II=1,NUINJ
I=IUINJ(II)-1
J=JUINJ(II)

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      SU(I,J)=0.0
1308 SP(I,J)=1.0E30
COME HERE FOR DRLPLFT EVAPORATION TERMS
1303 IF(NFNZ,LE,C)GO TO 1305
DO 1306 J=2,M
KJR=(K-2)*(NI-2)*(NJ-2)*(J-2)*(NI-2)
IS=IWLI(J,NGOTD)
IE=IWLO(J,NGOTD)
DO 1306 I=IS,IE
LPC=KJK+I-1
1306 SP(I,J)=SP(I,J)-EVAP(LPC)
1305 CONTINUE
RETURN
C +--+ +--+ +--+ +--+ +--+ +--+ +--+ +--+ +--+ X-DIRECTION RADIATION +--+ +--+ +--+ +--+ +--+ +--+ +--+
1300 IF(NV,NE,LVRX)GO TO 910
C-----INLET BOUNDARY.
DO 901 A=2,M
I=IWLI(J,NGOTC)
IF (JKIN(J,K),EQ,1) GO TO 902
TEMPH=TEMP(I-1,J,K)
SU(I,J)=SU(I,J)+EMI*SIGMA*TEMPH##4
SP(I,J)=SP(I,J)-EMI
GO TO 1901
902 CONTINUE
SU(I,J)=SU(I,J)+RADIN
SP(I,J)=SP(I,J)-1.
C-----OUTLET BOUNDARY.
1901 I=.WLO(J,NGOTC)
II (J.GT.JWOI.AND.J.LT.JWOO) GO TO 1902
TEMPH=TEMP(I+1,J,K)
SU(I,J)=SU(I,J)+EMI*SIGMA*TEMPH##4
SP(I,J)=SP(I,J)-EMI
GO TO 901
1902 CONTINUE
SU(L,J)=SU(L,J)+RADSUR
SP(L,J)=SP(L,J)-1.
901 CONTINUE
COME HERE FOR SLOT MODIFICATIONS
IF (NUINJ,LE,C) GO TO 903
DO 743 II=1,NUINJ
I=IWINJ(II)-1
J=JUINJ(II)
SU(I+1,J)=SU(I+1,J)+EMISR*SIGMA*TEMP(I,J,K)##4
SP(I+1,J)=SP(I+1,J)-1
TEMPH=TLIP
SU(I-1,J)=SU(I-1,J)+EMI*SIGMA*TEMPH##4
743 SP(I-1,J)=SP(I-1,J)-EMI
903 CONTINUE
C +--+ +--+ +--+ +--+ +--+ +--+ +--+ +--+ +--+ Y-DIRECTION RADIATION +--+ +--+ +--+ +--+ +--+ +--+ +--+
910 IF (NV,NE,LVRY) GO TO 920
DO 911 I=2,L
C-----TOP WALL.
J=JWL(I,NGOTC)-1
IF (IKIN(I,K),EQ,2,OR.IKIN(I,K),EQ,3) GO TO 904
TEMPH=TEMP(I,J+1,K)
SU(I,J)=SU(I,J)+EMI*SIGMA*TEMPH##4*RH(J+1)
SP(I,J)=SP(I,J)-EMI*RH(J+1)
GO TO 903
904 SU(I,J)=SU(I,J)+RADIM*RH(J+1)
SP(I,J)=SP(I,J)-RH(J+1)
905 IF (IDW) 911,911,1911
C-----BOTTOM WALL.
1911 J=JWL(I,NGOTD)+1
IF (IKIN(I,K),EQ,1,OR.IKIN(I,K),EQ,3) GO TO 906

```

	SOOT	145
	SOOT	146
	SOOT	147
	SOOT	148
	SOOT	149
	SOOT	150
	SOOT	151
	SOOT	152
	SOOT	153
	SOOT	154
	SOOT	155
	SOOT	156
	SOOT	157
	AL	1089
	SOOT	158
COMMENT		60
	AL	1091
	AL	1092
	AL	1093
	AL	1094
	AL	1095
	AL	1096
	AL	1097
	AL	1098
	AL	1099
	AL	1100
COMMENT		61
	AL	1101
	AL	1102
	AL	1103
	AL	1104
	AL	1105
	AL	1106
	AL	1107
	AL	1108
	AL	1109
	AL	1110
	AL	1111
	AL	1112
	AL	1113
	AL	1114
	AL	1115
	AL	1116
	AL	1117
	AL	1118
	AL	1119
	AL	1120
	AL	1121
	AL	1122
	AL	1123
	AL	1124
COMMENT		62
	AL	1125
	AL	1126
	AL	1127
	AL	1128
	AL	1129
	AL	1130
	NASAX	24
	NASAX	25
	AL	1133
COMMENT		63
	AL	1134
	AL	1135

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CALL FPRINT (1,3,1)
CALL FPRINT (3,3,4)
IF(ISTEP.EQ.0)GO TO 300
IF(MSOOT.EQ.0)GO TO 227
C-----SOOT EMISSIONS INDEX AND SMOKE NUMBER.
FLOW=0.0
PBAR=0.0
SBAR=0.0
DO 225 K=2,N
DO 225 J=2,P
LP=KM(K)+JP(J)+L
DMOOT=RHO(LP1,J,K)*YSR(J)*ZS(K)*U(LP1,J,K)
FLOW=FLOW+DMOOT
DSOOT=DMOOT*(SOOT1(L,J,K)+SOOT2(L,J,K))
SBAR=SBAR+DSOOT
225 PRAR=PBAR+DSOOT*RHO(LP1,J,K)
PRAR=PRAR+1.0E-30
FLOW=FLOW+1.0E-30
CSMO=1000.0*SBAR/FUTOT
SMCONC=1.0E6*PRAR/FLOW
SMONO=12.9847*ALOG(SMCONC)+12.045
SMONO=AMAX1(SMONO,0.0)
227 IF(MNOX.EQ.0)GO TO 300
C-----NOX EMISSIONS INDEX.
PRAR=0.0
DO 301 K=2,N
DO 301 J=2,N
LP=KM(K)+JP(J)+L
301 PRAR=PRAR+RHC(LP1,J,K)*YSR(J)*ZS(K)*U(LP1,J,K)*(F(LP,LVNO)+46./30.*1+F(LP,LVNO2))
CN1=1000.0*PRAR/FUTOT
300 CONTINUE
C ---- HFRF PP IS ACTUALLY KE, P IS ACTUALLY DISSIPATION
READ (NTP) PP,P
DO 25 K=1,NP1
DO 25 J=1,NP1
KJM=KM(K)+JM(J)
DO 25 I=1,LPI
LP=KJM+I
25 F(LP,NVD)=CD*F(LP,NVK)**1.5/(F(LP,NVD)+1.0E-30)
CALL FPRINT (NVK,NVD,5)
C ----- HFRF PP IS PHE, P IS MFU, DU IS MCO
READ (NTP) PP,P,DU
CALL FPRINT (NVFUOX,NVTE,7)
CALL FPRINT (NVCO,NVCO,15)
DO 50 K=1,NP1
DO 50 J=1,NP1
KJM=KM(K)+JM(J)
DO 50 I=1,LPI
LP=KJM+I
FUR=F(LP,NVFUDX)-F(LP,NVFU)
F(LP,NVFUD2)=FS(LP,IOCO2)
F(LP,NVHDX)=FS(LP,IOO2)
F(LP,NVH2D)=FS(LP,IOH20)
F(LP,NVN2)=FS(LP,ION21)
50 CONTINUE
CALL FPRINT (NVH20,NVN2,16)
IF (NFN2.LT.0) GO TO 35
DO 37 K=1,NP1
DO 37 J=1,NP1
KJM=KM(K)+JM(J)
DO 37 I=1,LPI
LP=KJM+I
37 F(LP,NVFUDX)=C.

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	OU	12
	OU	13
	NOX	127
	SOOT	139
	COMMENT	69
	SOOT	160
	SOOT	161
	SOOT	162
	SOOT	163
	SOOT	164
	SOOT	165
	SOOT	166
	SOOT	167
	SOOT	168
	SOOT	169
	SOOT	170
	SOOT	171
	SOOT	172
	SOOT	173
	SOOT	174
	SOOT	175
	SOOT	176
	NOX	128
	COMMENT	70
	NOX	129
	NOX	130
	NOX	131
	NOX	132
	NOX	133
	NOX	134
	NOX	135
	NOX	136
	OU	14
	OU	15
	OU	16
	OU	17
	OU	18
	OU	19
	OU	20
	OU	21
	OU	22
	OU	23
	OU	24
	OU	25
	OU	26
	OU	27
	OU	28
	OU	29
	OU	30
	OU	31
	OU	32
	NOX	137
	NOX	138
	NOX	139
	NOX	140
	OU	40
	OU	41
	OU	42
	OU	43
	OU	44
	OU	45
	OU	46
	OU	47
	OU	48

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C-----SPRAY EVAPORATION RATES.          COMMENT    71
DO 39 K=2,N                           OU        49
DO 39 J=2,M                           OU        50
KJM=KM(K)+JP(J)
KJK=(K-2)*(NI-2)*(NJ-2)*(J-2)*(NI-2)   OU        51
DO 39 I=2,L                           OU        52
LP=KJM+I                           OU        53
LPC=LPC+(I-1)
39 F(LP,NVFUDX)=EVAP(LPC)
CALL FPRINT (NVFUDX,NVFUDX,22)         OU        54
39 CONTINUE                         OU        55
C ----- MFR E DV IS ENTHALPY, DW IS FAV
READ (NTP) DV,DW                      OU        56
CALL FPRINT (NVH,NVFAV,10)             OU        57
C ----- MFR U IS FX, V IS FY, W IS FZ
READ (NTP) U,V,W                      OU        58
CALL FPRINT (NVFX,NVYZ,12)            OU        59
C ----- RHO AND VISCOSITY
CALL FPRINT(3C,30,20)                  4STEP    179
NV=4
DO 56 K=1,NP1                         OU        60
DO 56 J=1,NP1                         OU        61
KJM=KM(K)+JM(J)
DO 56 I=1,LP1                         OU        62
LP=KJM+I                           OU        63
56 F(LP,7)=0.
CALL GAMMA                          OU        64
CALL FPRINT (7,T,21)                  OU        65
REWIND NTP1                          OU        66
DO 46 II=1,2                         OU        67
46 READ (NTP1)
C ----- HERE PP IS PHI, P IS MFU, DU IS MCQ
READ (NTP1) PP,P,DU                  OU        68
CALL FPRINT(11,13,?3)                4STEP    179
CALL FPRINT(24,29,26)                4STEP    176
CALL FPRINT(14,15,32)                4STEP    177
1 IF(ISTEP.GT.0.AND.NSOOT.NE.0)WRITE(6,226)SMONO,SMCONC,CSNO
226 FORMAT(1HO,10(1H4),5X,*SMOKE NUMBER = *, E10.2,5X,10(1H4)/1HO,
1 10(1H4),5X,*SMOKE CONCENTRATION = *,E10.2,1X,0MG/M3, OR*,E10.2,
2 1X,0GM.OF SMOKE/KG.OF FUEL*,5X,10(1H4)/)
IF(ISTEP.GT.C.AND.NNOX.NE.0)WRITE(6,302)CMO
302 FORMAT(1HO,10(1H4),5X,*NOX EMISSIONS INDEX = *,E10.2,1X,
1 *GM.OF NO2/KG.OF FUEL*,5X,10(1H4)/)
15 CONTINUE                         OU        69
WRITE(6,19)
19 FORMAT (1HO,4HSTEP,5X,4HSMAX,7X,4HSUM,6X,9HSEKIT,5X,
1 1HPL(2,M,2),3X,8HP(L,M,2),3X,8HU(I,J,K),3X,8HV(I,J,K),3X,
2 8HW(I,J,K),2X,8HT(I,J,K),2X,10HRHO(I,J,K),2X,7HI J K)
20 CONTINUE                         OU        70
RETURN
END
SUBROUTINE AUX
COMMON F(3500),DU(500),DV(500),DW(500),
1 AMUC(500),SOOT1(500),SOOT2(500),FCM(500),FH2(500),FS(500,14),
1 RH0(500),VTSC(500),ABSR(500),SCTR(500),SU(100),SP(100),
1 DRHDP(500),
1 AXP(.00),AYP(100),AYP(100),AYM(100),AZP(100),
2 AYM(100),CY(100),CYU(100),CYU(100),
3 CZP(100),CTP(10),DIVG(100),NTP1,NTP2
1,AYMK(192),AZPK(192),AYMK(192),AYPK(192),AZMK(192),AZPK(192),
2 SUK(192),SPK(192)
DIMENSION U(500),V(500),W(500),PP(500),P(500),TEMP(500)
DIMENSION GM(500)
FOH(VALENCE (F(1),U(1)),(F(501),V(1)),(F(1001),W(1)))
COMMENT    71
COMMENT    49
COMMENT    50
COMMENT    51
COMMENT    52
COMMENT    53
COMMENT    54
COMMENT    55
COMMENT    56
COMMENT    57
COMMENT    58
COMMENT    59
COMMENT    60
COMMENT    61
COMMENT    62
COMMENT    63
COMMENT    64
COMMENT    65
COMMENT    66
COMMENT    67
COMMENT    68
COMMENT    69
COMMENT    70
COMMENT    71
COMMENT    72
COMMENT    73
COMMENT    74
COMMENT    75
COMMENT    76
COMMENT    77
COMMENT    78
COMMENT    79
COMMENT    80
COMMENT    SOOT    179
COMMENT    81
COMMENT    82
COMMENT    83
COMMENT    84
COMMENT    85
COMMENT    86
COMMENT    87
COMMENT    88
COMMENT    AU     2
COMMENT    COMFB  2
4STEP    179
RAD      3
RAD      4
COMFR   4
COMFB   5
COMFB   6
CTOMA   3
CTOMA   4
COMFB   7
COMFR   8
COMFR   9

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EQUIVALENCE (F(19C1),PP(1)),(F(2001),P(1)),(F(2901),TEMP(1))	COMMON	10
EQUIVALENCE (F(3001),GAM(1))	COMMON	11
COMMON/CYL/R(30),PM(30),RMV(30),YSR(30),YSVR(30),IPLAX	COMMON	2
COMMON/GRID/X(40),Y(30),Z(30),XS(40),YS(30),TS(40),XSU(40),	COMMON	3
1 YSV(30),ZSW(30),XDTF(40),YDEF(30),ZDIF(30),FXP(40),FKM(40),	COMMON	4
2 FYP(30),FYH(30),F7P(30),FZM(30),DT,TIME	COMMON	5
COMMON	NOX	2
1/CTMDFX/IDCC,INFU,IND2,IND2,IND2,IND2,IND2,IND2,IND2,IND2	NOX	3
1,IND,INDH,IHCPS,ILC,ILH,IMAT,ITER,JJJ,N1,N2,N3,NA,NGLOR,NGLORP,	NOX	4
2 NLM,NO,NSP,NS1,NS2,INDH	4STEP	3
3/CCHEMI/CPSUM,HSUM,FQ,PPLN,RGAS,RGASIN,SHINV,TINV,LNRG	NOX	6
4/CPARAM/ASUR(30,31),FMV,ER,HSUB0,NDEBUG,MS,PA,QQ,Q1,Q2,Q3,Q4,RHOPP,	NOX	7
4 SM,SHW(30),SM0,S1(30),S2(30),TK,LADIAB,LDEBUG,LEQUIL,LREACT,	NOX	8
4 LENER,FDKID,LCONVG	NOX	9
DOUBLE PRECISION CPSUM,EMV,ER,FQ,HSUB0,HSUM,PA,PPLN,QQ,Q1,Q2,Q3,	NOX	10
1 Q4,RGAS,RGASIN,RHOPP,SH,SHINV,SHW,S1,S2,TK,TINV,TLM,SM0	NOX	11
2,FIUT,FST	4STEP	4
COMMON/STEP4/PEXP1,PEXP2,PEXP3,PEXP4,ER1,ER2,ER3,ER4,C8U1,C8U2,	4STEP	5
1 CERU3,CFRU4,AEXP1,AEXP2,AEXP3,AEXP4,BEXP1,BEXP2,BEXP3,BEXP4,	4STEP	6
2 CEXP1,CEXP2,CEXP3,CEXP4,FUT,FST	4STEP	7
LOGICAL LADIAB,LCPNVG,LDEBUG,LEQUIL,LNRG,LREACT,LENER	NOX	12
COMMON/INT/L,P,N,LCV,MCV,N,V,LPI,MP1,MP1,NI,NJ,NK,NINJ,NINJK,NV,	COMMON	6
1 NNV,NGOTO,K,ISTR,JSTR,KSTR,NVM(35),KM(30),JM(30),ISTEP,	4STEP	8
2 ISOLVF(32),IPRINT(33),TITLE(10,33),IXY,ISWP,JSWP,RELAX(35),NP,	4STEP	9
3 NRHO,NGAM,IWLI(30,5),IWLD(30,5),JWLD(40,5),JWLII(40,5),IWEI,	COMMON	9
4 INFO,NN1,JWII,JWDI,JWOO,ICM,JKIM(30,30),IKIM(40,30)	COMMON	10
COMMON/INDEX/IPAR,LPREF,ISTUN,INCOMP,ITRAD,MVRX,MVRY,MVRZ,JPLANE	COMMON	11
1,PLAYM1,LVK,LVD,LVFUOK,LVFU,LVCO,LVH,LVRX,LVRY,LVRZ,NVF(32),	4STEP	10
2 IJUMP,IRFS,TITLE2(20),TMAX,JMAX,KMAX,MVCO,MVH20,MVC02,	COMMON	13
3 MVN2,MVCH,MVH2	4STEP	11
COMMON/CNOX/LVH1,LVH2,LVN1,LVNO,LVNO2,LVD,LVOM,LVH20,LVN2,LVO2,	NOX	16
1 LVCO2,LVFU1,LVCO1,NNOX,INOX,ITNOX,SNOK,TNOX	NOX	17
COMMON/THERP/NVH,NVFU,NVFX,NVFOOK,NVTE,NOEN,IOK,FSTOIC,HFU,CP,	COMMON	15
1 GASCON,RHCCN,UNICON,PRESS,MVFAV,TCYLW,TINLW,TLIP,ACDEF(4),	COMMON	16
2 T4,DFAC,WFU,WCO2,WCO,WFX,WHD,WN2,HYY,CKX,RATIO1,RATIO2,	COMMON	17
3 RATIO3,RATIC4,MCO,TAN,ITWALL	COMMON	18
COMMON/CTDMA/REND,ICTDMA(32)	4STEP	12
COMMON/RIS/APU,DEM,SHAK,SSUM,LASTEP,HTCEXT,CFR,EMISH,EMISIN,	COMGEN	2
1 EMISR,TOUT,RTCD,EMI,RADIN,RADSUR,FMF,SKF,	COMGEN	3
2 EFKU,FDFU,TFUEL,WFNZ,FLD(40),TEMTH(40),H(40),FUEL(40),FUOK(40)	COMGEN	4
2 UTN(40),TIM(40),FUELS(40),SEXIT,IGAM1(29),IGAM2(29)	4STEP	13
COMMON/TURB/MVK,NVD,C1,C2,CD,AK,DUIDXJ(3,3),AKFAC,ALFAC,	COMGEN	6
1 MODEL,PR(32),PREF(32),PJAY(32),E	4STEP	14
COMMON/RAD/NVE,STGMA,ABSOR,SCATR	COMGEN	8
COMMON/REACT/ARCON1,PREXP1,CR1,ARCON2,PREXP2,CR2,MODER	COMGEN	9
COMMON/DRDPL/EVAP(192),NTP4,MFNZ,KO(3),YO(3),ZO(3),ALFA(3),	COMGEN	10
1 BETA(3),DETA(3),THETA1(3),THETA2(3),NSL(3),WFF(3),SMO(3),	COMGEN	11
2 VFUFL(3),RFUFL(3),EVSU(64),HEVAP	COMGEN	12
COMMON/INJEC/FLOWIN,IUINJ(20),JIINJ(20),UIINJ(20),WIINJ(20),	COMGEN	13
1 AUINJ(20),TUINJ(20),IVINJ(20),JVINJ(20),KVINJ(20),VINJ(20),	COMGEN	14
2 EVINJ(20),AVINJ(20),TVINJ(20),NUINJ,MVINJ,JSW1,JSW2,	COMGEN	15
3 USW,VSW,AFSW,FSW,TSW,WSW,SWH,RHOSW	COMGEN	16
COMMON/CSOOT/NVN,MVS1,MVS2,ISOOT,SSOOT,NSOOT,AO,ARCONN,AAA,BBB,FMG	SOOT	8
1,GO,MPART,OPART(2),FRACP(2),RHOP,ARCONS,PREXP5,ALPHA,AAS,RBS,DRH	SOOT	9
2,LVN,LVS1,LVS2,CINCP,TINCP,FUTOT	SOOT	10
COMMON/CRAD/IRAD,SRAD	SOOT	11
COMMON/CFDUP/PREP3,ARCON3,CR3,PREXP4,ARCON4,CR4,AA1,BR1,CC1,	4STEP	15
1 AA2,BB2,CC2,AA3,BB3,CC3,A44,B44,CC4,RATIO5,RATIO6,RATIO7,	4STEP	16
2 RATIO8,R47109,RATO10,RATO11,RATO12,MCH,W42,WC2H,LVCH,LVCH1,LVH21	4STEP	17
COMMON/CLDR/FDK(192)	NOX	146
DIMENS:DM GENR(500),SFU(500),SPFU(500),EDK2(192)	NOX	147
DIMENS:DN SUCH(500),SPCH(500)	4STEP	170
*** REWARE OF EQUIVALENCE STATEMENTS ***	AU	7
EQUIVALENCE (GENR(1),DU(1)),(SFU(1),DV(1)),(SPFU(1),DN(1))	AU	8

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TMAX=AMAX1(TMAX,2000.)
TEMP(LP)=AMIN1(TEMP(LP),TMAX)
1050 TEMP(LP)=AMAX1(TEMP(LP),100.)
C ----- HERE DU IS U, DV IS V, DW IS W
1034 RFWIND NTP1
READ (NTP1) DU,DV,DW,P
1048 RFAD (NTP1)
C ----- HERE PP IS PHI, DU IS MFU, DV IS MCQ
READ (NTP1) PP,DU,DV
RFAD(NTP1)
READ(NTP1)DW,P
REWIND NTP1
READ(NTP1)U,V,W
CALCULATE WALL TEMPERATURE.
DO 1052 K=2,N
DO 1058 I=2,L
IF(IKIN(I,K).EQ.2.OR.IKIN(I,K).EQ.3)GO TO 1054
J=JWL(I,I,4)-1
LP=I+JM(J)+KM(K)
LPRY=LP+NVM(5)
VEC=0.25*((U(LP)+U(LP+1))**2+(W(LP)+W(LP+1))**2)
HTC=CFR*RHO(LP)*CP*SQRT(VEC)
TEMP(LP+NI)=TSOLVE(TEMP(LP+NI),TEMP(LP),F(LPRY),HTC,SIGMA,EMI,
1 ITRAD)
1054 IF(IKIN(I,K).EQ.1.OR.IKIN(I,K).EQ.3)GO TO 1058
IF(IDW,F0.0)GO TO 1058
J=JWL(I,I,4)+1
LP=I+JM(J)+KM(K)
LPRY=LP+NVM(5)
VEC=0.25*((U(LP)+U(LP+1))**2+(W(LP)+W(LP+1))**2)
HTC=CFR*RHO(LP)*CP*SQRT(VEC)
TEMP(LP+NI)=TSOLVE(TEMP(LP+NI),TEMP(LP),F(LPRY),HTC,SIGMA,EMI,
1 ITRAD)
1058 CONTINUE
DO 1052 J=2,M
IF(JKTN(J,K).EQ.1)GO TO 1059
LP=IWLI(J,4)+JM(J)+KM(K)
LPRY=LP+NVM(10)
VEC=0.25*((V(LP)+V(LP+NI))**2+(W(LP)+W(LP+NI))**2)
HTC=CFR*RHO(LP)*CP*SQRT(VEC)
TEMP(LP-1)=TSOLVE(TEMP(LP-1),TEMP(LP),F(LPRY),HTC,SIGMA,EMI,ITRAD)
1059 IF(J.GT.JWDI.AND.J.LT.JWDD)GO TO 1072
LP=IWLI(J,4)+JM(J)+KM(K)
LPRY=LP+NVM(10)
VEC=0.25*((V(LP)+V(LP+NI))**2+(W(LP)+W(LP+NI))**2)
HTC=CFR*RHO(LP)*CP*SQRT(VEC)
TEMP(LP+1)=TSOLVE(TEMP(LP+1),TEMP(LP),F(LPRY),HTC,SIGMA,EMI,ITRAD)
1072 CONTINUE
REWIND NTP1
READ(NTP1)U,V,W,P
IF(ISOLVE(LVFU).EQ.0)GO TO 1200
GO TO (1060,1062,1064), MODEM
1060 DO 1061 K=1,NP1
C-----DENSITY=CONSTANT, MODEM=1.
DO 1061 J=1,NP1
KJM=KM(K)+JM(J)
IS=IWLI(J,3)
IE=IWLC(J,3)
DO 1061 I=IS,IE
LP=KJM+I
RH0(ILP)=DFN
1061 CONTINUE
GO TO 1200

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1062 DO 1063 K=1,NP1
C-----DENSITY=FUNCTION(NCOMPOSITION,TEMPERATURE), MODEN=2.
    DO 1063 J=1,MP1
        KJM=KM(K)+JM(J)
        IS=IWLI(J,5)
        IE=IWLC(J,2)
        DO 1063 I=IS,IE
            LP=KJM+I
            LPTE=LP+NVM(NVTE)
            LPFU=LP+NVM(NVFUDX)
C ----- CAUTION HERE
            LPFU=LP+NVM(NVFUDX+3)
            LPC0=LPC0+NVM(NVCO+1)
            LPCH=LPC0+NVM(NVCH)
            LPH2=LPC0+NVM(NVH2)
            FUR=F(LPFUDX)-F(LPFU)
            FLPH2D=0.5*WH2D*(HYY*FUB/WFU-RATIO7*F(LPCH)-F(LPH2))
            FLPC02=WC02*(CKX*FUB/WFU-CKX*F(LPCH)/WCH-F(LPC0)/WC0)
            FLPOX=RATIO1*F(LPFU)+RATIO3*F(LPC0)+RATIO2-(RATIO2+RATIO1)*
1 F(LPFUDX)+RATIO5*F(LPCH)+RATIO6*F(LPH2)
            FLPOX=AMAX1(FLPOX,0.)
            FLPN2=1.0-F(LPFU)-FLPC02-F(LPC0)-FLPOX-FLPH2D-F(LPCH)-F(LPH2)
1008 CONTINUE
            RLPTE=F(LPTE)
            RLPTE=AMAX1(RLPTE,100.)
            VMIX=F(LPFU)/WFU+FLPC02/WC02+F(LPC0)/WC0+FLPOX/WOX+FLPH2D/WH2D+
1 FLPN2/WH2+F(LPCH)/WCH+F(LPH2)/WH2
            DENST=RHODCN/(VMIX*RLPTE)
            GO TO (1009,1010),KONTRO
1009 RHO(LP)=DENST
1010 RHO(LP)=RELAX(NRHO1)*DENST+RELAXM*RHO(LP)
1063 CONTINUE
1064 CONTINUE
1200 CONTINUE
    CALL DENMOD
    RETURN
C   00 00 00 00 00 00 00 00 00 00 00 00 00 00 00 00 00 00 + AU 100
C   ENTRY VISCC
C-----ENTRY VISCC IS USED TO CALCULATE THE EFFECTIVE VISCOSITY
C   AND YPLUS AT WALL BOUNDARIES.
C   COMMENT 109
C   COMMENT 110
C   COMMENT 79
C   COMMENT 60
C   COMMENT 81
C ----- HERE DU IS KE, DV IS DISS
    RFAD(INTP1) DU,DV
    RELAXM=1.-RELAX(NGAM)
    KONYRD=2
    IF (ISTEP.EQ.IRES) KONTRO=1
    DO 2000 K=1,NP1
    DO 2000 J=2,M
        KJM=KM(K)+JM(J)
        IS=IWLI(J,4)
        IE=IWLC(J,4)
        DO 2000 I=IS,IE
            LP=KJM+I
            GO TO (2001,2002),MODEL
2001 CONTINUE
C-----CONSTANT VISCOSITY, MODEL=1, LAMINAR.
    VISCLP=AMU
    GO TO 2000
2002 CONTINUE
    LPK=LP+NVM(NVK+4)
    LPD=LP+NVM(NVD+4)
C-----VISCOSITY FROM K-E MODEL, MODEL=2, TURBULENT.
    VISCOS=RHO(LP)*CD0*F(LPK)*42/(F(LP0)+1.E-30)
    GO TO (2003,2004),KONTRO

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2003 VISC(LP)=VISCOS          AU 132
2004 VISC(LP)=RELAX(NGAM)*VISCOS+RELAXNO*VISC(LP)    AU 133
2000 CONTINUE                   AU 134
C ----- CALCULATE YPLUS        AU 135
DO 2020 K=1,NPI                AU 136
DO 2022 I=1,LP1                 AU 137
J=JWL(I,4)                      AU 138
LP=KM(K)+JM(J)+I               AU 139
LPK=LP+NVM(NVK+4)               AU 140
DIST=.5*YDIF(J)                 AU 141
IF (J.EQ.MP1) DIST=YDIF(MP1)     AU 142
YPLUS=RHO(LP-NI)*SURT(F(LPK-NI)*RTCD)*DIST/AMU   AU 143
VISC(LP)=YPLUS                  AU 144
J=JWL(I,I,4)                    AU 145
LP=KM(K)+JM(J)+I               AU 146
LPK=LP+NVM(NVK+4)               AU 147
DIST=.5*YDIF(J+1)               AU 148
IF (J.EQ.1) DIST=YDIF(2)         AU 149
YPLUS=RHO(LP+NI)*SURT(F(LPK+NI)*RTCD)*DIST/AMU   AU 150
VISC(LP)=YPLUS                  AU 151
2022 CONTINUE                   AU 152
DO 2024 J=2,M                   AU 153
I=IWLT(I,J,4)-1                AU 154
LP=KM(K)+JM(J)+I               AU 155
LPK=LP+NVM(NVK+4)               AU 156
DIST=.5*YDIF(I+1)               AU 157
IF (I.EQ.1) DIST=XDIF(2)         AU 158
YPLUS=RHO(LP+1)*SURT(F(LPK+1)*RTCD)*DIST/AMU   AU 159
VISC(LP)=YPLUS                  AU 160
I=IWLO(I,J,4)+1                AU 161
LP=KM(K)+JM(J)+I               AU 162
LPK=LP+NVM(NVK+4)               AU 163
DIST=.5*XDIF(I)                 AU 164
IF (I.EQ.LP1) DIST=XDIF(LP1)     AU 165
YPLUS=RHO(LP-1)*SURT(F(LPK-1)*RTCD)*DIST/AMU   AU 166
VISC(LP)=YPLUS                  AU 167
2024 CONTINUE                   AU 168
2020 CONTINUE                   AU 169
DO 3005 K=2,N                   AU 170
DO 3005 J=2,M                   AU 171
KJM=KM(K)+JM(J)                AU 172
IS=IWLT(I,J,4)                 AU 173
IE=IWLC(I,J,4)                 AU 174
DO 3005 I=IS,IE                 AU 175
LP=KJM+I                        AU 176
LPK=LP+NVM(NVK+4)               AU 177
LPD=LP+NVM(NVD+4)               AU 178
LPC=I-1+(J-2)*(NI-2)+(K-2)*(NI-2)*(NJ-2)       AU 179
ENDP(LPC)=F(LPD)/(F(LPK)**2+1.0E-30)           SOUT 180
3005 FOK(LPC)=F(LPD)/(F(LPK)+1.E-30)            AU 181
RETURN                           AU 182
C ** ** ** ** ** ** ** ** ** * AU 182
ENTRY GAMMA                      AU 183
C-----ENTRY GAMMA IS USED TO CALCULATE THE DIFFUSION COEFFICIENTS. COMMENT 184
C
DO 3000 K=1,NPI                 COMMENT 185
DO 3000 J=2,M                     AU 186
KJM=KM(K)+JM(J)                 AU 187
IS=IWLT(I,J,4)                  AU 188
IE=IWLO(I,J,4)                  AU 189
DO 3000 I=IS,IE                  AU 190
LP=KJM+I                        AU 191
DO TO (3001,3002),NODFL        AU 192
3001 CONTINUE

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      GAM(LP)=VISC(LP)/PR(NV)
      GO TO 3000
3002 CONTINUE
      GAM(LP)=VISC(LP)/PREF(NV)
3000 CONTINUE
      CALL GAMOD
3004 CONTINUE
      RETURN
C   *   *   *   *   *   *   *   *   *   *   *   *   *   *   *   *   *   *
C   ENTRY SOURCE
C-----FNTRY SOURCE IS USED TO CALCULATE THE SOURCE TERMS FOR
C   THE DEPENDENT VARIABLES.
C
CAUTION NOT ALL SOURCE TERMS ARE VALID - AT BOUNDARY NODES -
CHECK AND MODIFY ACCORDINGLY IN S0M0D
GO TO (100,200,300,400),NGOTO
C   *   *   *   *   *   *   *   *   *   *   *   *   *   *   *   *   *   *
C   SOURCE TERMS FOR U-VELOCITY      +---+---+---+---+---+
100 DO 101 J=2,N
      IS=IWLI(J,NGOTO)
      IE=IWLP(J,NGOTO)
      DO 101 I=IS,IE
      LIJ=JM(J)+I
      LP=LIJ+KM(K)
      EXP=LP+1
      LXM=LP-1
      DUDXP=(U(LXP)-U(LP))/XS(I)
      DUDXM=(U(LP)-U(LXM))/XS(I-1)
      GAMLP=GAM(LP)
      GAMLXM=GAM(LXM)
      IF (I.EQ.IS) GAMLXM=GAM(LXM-1)
      IF (I.EQ.IE) GAMLP=GAM(LP+1)
      SU(LIJ)=(GAMLP*DUDXP-GAMLXM*DUDXM)/XSU(I)
      LYP=LP+NI
      LYX=LP-NI
      LYPI=LYP-1
      LYMI=LYM-1
      GAMP=0.25*(GAM(LP)+GAM(LXM)+GAM(LYP)+GAM(LYMI))
      GAMM=0.25*(GAM(LP)+GAM(LXM)+GAM(LYM)+GAM(LYMI))
      DWDXP=(V(LYP)-V(LYPI))/XDIF(I)
      DWDXM=(V(LP)-V(LXM))/XDIF(I)
      SU(LIJ)=SU(LIJ)+(GAMP*Dwdxpm(j+1)-GAMM*Dwdxmrn(j))/YSR(j)
      LZP=LP+NI+N
      LZM=LZP-NINJ
      LZP1=LZP-1
      LZM1=LZM-1
      GAMP=0.25*(GAM(LP)+GAM(LXM)+GAM(LZP)+GAM(LZP1))
      GAMM=0.25*(GAM(LP)+GAM(LXM)+GAM(LZM)+GAM(LZM1))
      DWDXP=(W(LZP)-W(LZP1))/XDIF(I)
      DWDXM=(W(LP)-W(LXM))/XDIF(I)
      SU(LIJ)=SU(LIJ)+(GAMP*Dwdxpm(j+1)-GAMM*Dwdxmrn(j))/YSR(j)
      SP(LIJ)=0.
101 CONTINUE
      GO TO 5000
C   *   *   *   *   *   *   *   *   *   *   *   *   *   *   *   *   *   *
C   SOURCE TERMS FOR V-VELOCITY      +---+---+---+---+---+
200 DO 201 J=3,N
      IS=IWLI(J,NGOTO)
      IE=IWLO(J,NGOTO)
      DO 201 I=IS,IE
      LIJ=JM(J)+I
      LP=LIJ+KM(K)
      LYP=LP+NI
      LYX=LP-NI
      DVNDXP=(V(LYP)-V(LP))/YS(I)
      DVNDXM=(V(LP)-V(LXM))/YS(I-1)

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GAMLP=GAM(LP)
GAMLYM=GAM(LYM)
IF (J.EQ.JWL1(I,NGOTO)+1) GAMLYM=GAM(LYM-NI)
IF (J.EQ.JWL0(I,NGOTO)-1) GAMLP=GAM(LP+NI)
SU(LIJ)=(GAMLP*DWDYDPMV(J+1)-GAMLYM*DWDYHDMV(J))/YSVR(J)
LXP=LP+1
LXM=L_P-1
LXP1=LXP-NT
LXM1=LXM-NI
GAMP=0.25*(GAM(LP)+GAM(LYM)+GAM(LXP)+GAM(LXP1))
GAMM=0.25*(GAM(LP)+GAM(LYM)+GAM(LXM)+GAM(LXM1))
DUJYP=(U(LXP)-U(LXP1))/YDIF(J)
DUOYM=(U(LP)-U(LYM))/YDIF(J)
SU(LIJ)=SU(LIJ)+(GAMP*DUJYP-GAMM*DUOYM)/XS(I)
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DVDZM=(V(LP)-V(LZM))/ZDIF(K)	AU	318
SU(LIJ)=SU(LIJ)+GAMP*DVDZP-GAMM*DVDZM)/VS(R(J))	AU	319
WMMR=0.5*(W(LP)+W(LYM))	AU	320
WMMP=0.5*(W(LP)+W(LYP))	AU	321
SH(LIJ)=SU(LIJ)+PLAXM1*(GAMM*WMMR-GAMP*WMMP)/VS(R(J))	AU	322
VPT2=V(LP)+V(LYP)	AU	323
VMT2=V(LZN)+V(LZH+NI)	AU	324
SU(LIJ)=SH(LIJ)+PLAXM1*(GAM(LP)*VPT2-VMT2*GAM(LZN))/VS(R(J))/R(J)/	AU	325
2*VS(R(J))/ZSW(K)	AU	326
GAMP=0.5*(GAM(LP)+GAM(LZN))	AU	327
SU(LIJ)=SU(LIJ)+PLAXM1*(GAMP/R(J)+((WMMP-WMMR)/VS(J))+0.5*(VPT2-VMT2	AU	328
1)/R(J))/ZSW(K))	AU	329
SP(LIJ)=-GAMP/R(J)/R(J)+PLAXM1	AU	330
301 CONTINUE	AU	331
GO TO 5000	AU	332
C SOURCE TERMS FOR TURBULENT KINETIC ENERGY	AU	333
400 CONTINUE	AU	334
IF (MV,NE,LVK) GO TO 500	AU	335
DO 401 J=2,N	AU	336
IS=IWLI(J,NGOTO)	AU	337
IE=IWLO(J,NGOTO)	AU	338
DO 401 I=IS,IE	AU	339
MIN=JWLII(I,NGOTO)+1	AU	340
MAX=JWL0(I,NGOTO)-1	AU	341
LIJ=JM(J)+I	AU	342
LP=LJ+KM(K)	AU	343
LYP=LP+1	AU	344
LYP=LP+NI	AU	345
LZP=LP+MINJ	AU	346
LXM=LP-1	AU	347
LXM=LP-NI	AU	348
LZN=LP-NINJ	AU	349
LPP0=LYP+1	AU	350
LPN0=LXM+1	AU	351
LPN0=LZN+1	AU	352
LPOP=LZP+1	AU	353
LPOP=LZP+1	AU	354
LXN0=LXM+NI	AU	355
LOPP=LZP+NI	AU	356
LOPN=LZN+NI	AU	357
LMOP=LXM+NINJ	AU	358
LMOP=LXM+NINJ	AU	359
CALCULATE THE PRODUCTION TERM	AU	360
DUIDXJ(1,1)=(U(LXP)-U(LP))/XS(I)	AU	361
DUIDXJ(2,2)=(V(LYP)-V(LP))/VS(J)	AU	362
DUIDXJ(3,3)=(W(LZP)-W(LP))/ZS(K)/R(J)	AU	363
1+PLAXM1*C.5*(V(LP)+V(LYP))/R(J)	AU	364
IF (I-IS) 411,412,411	AU	365
411 VXM=0.5*(V(LXP)+V(LMPO))	AU	366
WXM=0.5*(W(LXM)+W(LMOP))	AU	367
XM=X(I-1)	AU	368
GO TO 413	AU	369
412 VXM=0.5*(V(LP)+V(LYP))	AU	370
WXM=0.5*(W(LP)+W(LZP))	AU	371
XM=X(I)	AU	372
413 IF (I-IE) 414,415,414	AU	373
414 VXP=0.5*(V(LXP)+V(LPP0))	AU	374
WXP=0.5*(W(LXP)+W(LPOP))	AU	375
XP=X(I+1)	AU	376
GO TO 416	AU	377
415 VXP=0.5*(V(LP)+V(LYP))	AU	378
WXP=0.5*(W(LP)+W(LZP))	AU	379
XP=X(I)	AU	380
416 DX=XP-XM	AU	381
DUIDXJ(2,1)=(VXP-VXM)/DX	AU	382

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        DUIDXJ(3,1)=(WXP-WXM)/DX          AU    382
        IF (J-MIN) 421,422,421          AU    383
421      WYM=0.5*(W(LTM)+W(LMP))      AU    384
        UYM=.5*(U(LTP)+U(LPM))        AU    385
        YP=Y(J-1)                      AU    386
        GO TO 423                      AU    387
422      WYP=0.5*(W(LP)+W(LZP))       AU    388
        UYP=0.5*(U(LP)+U(LXP))       AU    389
        YM=Y(J)                        AU    390
423      TF (J-MAX) 424,425,424      AU    391
424      WYP=0.5*(W(LTP)+W(LPP))     AU    392
        UYP=0.5*(U(LTP)+U(LPP))     AU    393
        YP=Y(J+1)                      AU    394
        GO TO 426                      AU    395
425      WYP=0.5*(W(LP)+W(LZP))     AU    396
        UYP=0.5*(U(LP)+U(LXP))     AU    397
        YP=Y(J)                        AU    398
426      DY=YP-YM                  AU    399
        DUIDXJ(3,2)=(WYP-WYM)/DY-PLAXM100.5*(W(LP)+W(LZP))/R(J)  AU    400
        DUIDXJ(1,2)=(UYP-UYM)/DY
        TFIK=21 431,432,431          AU    401
431      U7M=0.5*(U(LZM)+U(LPM))    AU    402
        V7M=0.5*(V(L7M)+V(LPM))    AU    403
        ZM=Z(K)                        AU    404
        ?M=Z(K-1)                      AU    405
        GO TO 433                      AU    406
432      U2M=0.5*(U(LP)+U(LXP))    AU    407
        V2M=0.5*(V(LP)+V(LYP))    AU    408
        ZM=Z(K)                        AU    409
433      TFIK=N 434,435,434          AU    410
434      U2P=0.5*(U(LZP)+U(LPP))    AU    411
        V2P=0.5*(V(LZP)+V(LPP))    AU    412
        ZP=Z(K+1)                      AU    413
        GO TO 436                      AU    414
435      U2P=0.5*(U(LP)+U(LXP))    AU    415
        V2P=0.5*(V(LP)+V(LYP))    AU    416
        ZP=Z(K)                        AU    417
436      DZ=ZP-ZM                  AU    418
        DUIDXJ(1,3)=(U2P-U2M)/DZ/R(J)  AU    419
        DUIDXJ(2,3)=(V2P-V2M)/DZ/R(J)  AU    420
        SUM=0.                         AU    421
        DO 402 II=1,3                 AU    422
        DO 402 JJ=1,3                 AU    423
402      SUM=SUM+(DUIDXJ(II,JJ)+DUIDXJ(JJ,II))+DUIDXJ(IX,JJ)  AU    424
        GENR(LP)=SUM                  AU    425
CALCULATE THE SOURCE TERM
        LPK=LP+NVM(NVK)                AU    426
        LPM=LP+NVM(NVD)                AU    427
        SUMLTJ=RHQ(LP)*CDRF(LPK)**2/(F(LPK)+1.E-30)*SUM  AU    428
        SP(LIJ)=RHQ(LP)*F(LPU)/(F(LPK)+1.E-30)              AU    429
C-----MODIFICATIONS OF THE SOURCE TERMS AT WALL BOUNDARIES.  COMMENT 89
        IF (I,LT,IS) GO TO 440          AU    430
        IF (JKIN(J,K),EQ,1) GO TO 440          AU    431
        DIST=.5*XDF(I)                AU    432
        IF (T,EQ,2) DIST=XDF(2)          AU    433
        VP=.5*SQRT((V(LP)+V(LYP))**2+(W(LP)+W(LZP))**2)  AU    434
        TAUP=AMAX1(GAM(LXM)*VP/DIST,1.E-20)          AU    435
        GAM(LXP)=0.                         AU    436
        VXP=V(LP)+V(LYP)+V(LXP)+V(LPP)          AU    437
        WXP=W(LP)+W(LZP)+W(LXP)+W(LPP)          AU    438
        VC=.25*SQRT(VXP**2+WXP**2)          AU    439
        DVDT=VC/XS(I)                  AU    440
        SUCLIJ=TAUP*DVTY          AU    441
        SP(LIJ)=RHQ(LP)*RHQ(LP)*CDRF(LPK)*DVDT/TAUP          AU    442
440      IF (T,LT,IE) GO TO 442          AU    443
                                         AU    444

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LPC=I-1+(J-2)*(NI-2)+(K-KSTR)*(NI-2)*(NJ-2)          AU      509
LPFU=LP+NVM(NVFM)          AU      510
LPFUNX=LP+NVM(NVFUOX)      AU      511
LPCH=LP+NVM(NVCH)          4STEP   194
LPH2=LP+NVM(NVH2)          4STEP   195
LPTE=LP+NVM(NVTE)          AU      512
FLPTE=F(LPTE)              AU      513
FLPTF=AMAX1(FLPTE,100.)    AU      514
F(LPFU)=AMIN1(F(LPFU),F(LPFUOX))                    AU      515
LPC0=LP+NVM(NVCO)          AU      516
FLPOY=RATIO1*F(LPFU)+RATIO3*F(LPC0)+RATIO2-(RATIO2+RATIO1)*
1 F(LPFUOX)+RATIO5*F(LPCH)+RATIO6*F(LPH2)          4STEP   196
FLPOX=AMAX1(FLPOX,0.)     AU      517
RHOLP=ABS(RHO(LP))        AU      518
ARRHEN=PRXP1*EXP(-ARCON1/FLPTE)                      4STEP   197
SOR1=((F(LPFU)*RHOLP)*AA1)*((FLPOX*RHOLP)*BB1)*((F(LPCH)*RHOLP))
1*CC1*ARRHEN               4STEP   198
4STEP   199
GO TO 611,612,MODER      AU      520
611 SOR=SOP1              AU      521
GO TO 602                AU      522
612 LPK=LP+NVM(NVK)        AU      523
LPD=LP+NVM(NVD)          AU      524
PHI=F(LPFU)              4STEP   200
SOR2=-CR1+PHI*RHO(LP)*EDK(LPC)
SOR=AMAX1(SOR1,SOR2)      AU      525
602 FUB=AMAX1(0.,((RATIO2+RATIO1)*F(LPFUOX)-RATIO2-RATIO3*F(LPC0)
1-RATIO5*F(LPCH)-RATIO6*F(LPH2))/RATIO1)            4STEP   201
FUR=AMIN1(F(LPFU),FUB)  4STEP   202
DSDFU=SOR/(F(LPFU)-FUB+1.E-30)                      4STEP   203
SUILIJ=SOR-DSDFU+F(LPFU)                                AU      526
SP(LIJ)=DSDFU          AU      527
SUFH(LP)=SUILIJ          AU      528
SPFUL(LP)=SP(LIJ)        AU      529
501 CONTINUE             AU      530
GO TO 5000              AU      531
C +-----+-----+-----+-----+-----+-----+-----+-----+-----+-----+-----+
700 CONTINUE             AU      540
IF (NV,NE,LVH) GO TO 800          AU      541
DO 701 J=2,M          AU      542
TS=IWLT(j,NGCTD)        AU      543
IF =IWLD(j,NGCTD)        AU      544
DO 701 I=IS,IF          AU      545
LIJ=JN(j)+I          AU      546
SUILIJ=0.          AU      547
SP(LIJ)=0.          AU      548
IF(ITTAD,EQ.1)GO TO 701          RAO    72
LP=L(TJ)KM(K)          AU      549
LPH=LP+NVM(NVH)          AU      550
LPFAV=LP+NVM(NM*AV)      AU      551
LPTE=LP+NVM(NVTE)        AU      552
FLPTE=F(LPTE)          AU      553
FLPE=$IGMA*FLPTE*004
FAV=F(LPFAV)
SOR=6.0*ABS(RLP)*(FAV-FLPE)          RAO    73
T0=(FAV/$IGMA)**.29
T0=T0+.001
DSOH=SCR/(CP*(FLPTE-T0))
SUILIJ=SUILIJ+SOR-DSOH*F(LPH)
SP(LIJ)=SP(LIJ)+DSOH
701 CONTINUE             AU      560
GO TO 5000              AU      561
C +-----+-----+-----+-----+-----+-----+-----+-----+-----+-----+-----+
800 CONTINUE             AU      562
IF (NV,NE,LVFUOX) GO TO 900          AU      563
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00 801 J=2,M          AU      570
IS=IWLI(J,MGET0)     AU      571
IF=IWLO(J,MGET0)     AU      572
00 901 I=1$,IF        AU      573
LTJ=JM(J)+I          AU      574
SU(LTJ)=0.            AU      575
SP(LIJ)=0.            AU      576
801 CONTINUE          AU      577
GO TO 9000            AU      578
C-----+----- SOURCE TERM FOR CO +-----+
900 IF(NV,NF,LVC0) GO TO 950          AU      579
SFAC=2.48*(1.0-FSTOIC)/FSTOIC        4STEP   205
DO 901 J=2,M          AU      580
IS=IWLI(J,MGET0)     AU      581
IE=IWLO(J,MGET0)     AU      582
00 901 I=1$,IF        AU      583
IJ=JM(J)+I          AU      584
LP=LJ+NM(K)          AU      585
LPC=I-1+(J-2)*(NI-2)+(K-KSTR)*(NI-2)*(NJ-2)    AU      586
LPC0=LPC+NVP(NVCO)        AU      587
LPFU0X=LP+NVM(NVFU0X)        AU      588
LPFU=LP+NVM(NVFU)          AU      589
LPTE=LP+NVM(NVTE)          AU      590
LPCH=LP+NVM(NVCH)          AU      591
LPH2=LP+NVM(NVH2)          AU      592
FLPTE=F(LPTE)          AU      593
FLPTE=AMAX1(FLPTE,100.)    AU      594
FLPOX=RATIO1+F(LPC0)+RATIO2+F(LPC4)+RATIO2-(RATIO2+RATIO1)*
1 F(LPC0)+RATIO3+F(LPC4)+RATIO6+F(LPH2)        4STEP   206
FLPOX=AMAX1(FLPOX,0.)        AU      595
FU0=F(LPFU0X)-F(LPFU)        AU      596
FLPH2D=0.5*W20*(HY+FB/NF-U-RATIO7+F(LPCH)-F(LPH2))  4STEP   210
FLPH2D=AMAX1(0.0,FLPH2D)        AU      597
RHOLP=APS(RHO(LP))          AU      598
ARRHEN=-PREXP3*EXP(-ARCON3/FLPTE)        4STEP   211
SOR3=((FLPC0)+RHOLP)*AA3*((FLPOX+RHOLP)*RB3)*((FLPH2D+RHOLP))
1*CC3)*ARRHEN        4STEP   212
SSS=7.93*EXP(-F(LPFU0X)+SFAC/(1.0-F(LPFU0X)))    4STEP   213
SSS=AMIN1(SSS,1.0)          AU      599
SOR3=SOR3+SSS            AU      600
GO TO (911,912),MODER        AU      601
911 SORCO=SOR3          AU      602
GO TO 902              AU      603
912 CONTINUE          AU      604
PHI=AMIN1(F(LPC0),FLPOX/RATIO3)        AU      605
SOR4=-CR3*PHI+RHO(LP)*EOK(LPC)        AU      606
SORCO=AMAX1(SOR3,SOR4)        4STEP   220
902 FUR=AMAX1(0.,((RATIO2+RATIO3)*F(LPFU0X)-RATIO2-RATIO1)*F(LPTE)
1-RATIO5+F(LPCH)-RATIO6+F(LPH2)+1/RATIO3)    4STEP   221
FUR=AMIN1(F(LPC0),FUR)        4STEP   222
DSDC0=SORCO/(F(LPC0)+FUR+1.E-30)        4STEP   223
SU(LIJ)=DSDC0*(FLPC0+FLC11*FUCHILP)+SPCHC1*(1-(LPCH))  4STEP   224
SP(LIJ)=DSDC0          AU      611
901 CONTINUE          AU      612
GO TO 950              AU      613
950 IF(NV,NF,LVC0) GO TO 960          AU      614
C-----+----- SOURCE TERMS FOR CRMY=2 +-----+
DO 951 J=2,M          4STEP   225
IS=IWLI(J,MGET0)     4STEP   226
IE=IWLO(J,MGET0)     4STEP   227
00 951 I=1$,IF        4STEP   228
IJ=JM(J)+I          4STEP   229
LP=LJ+NM(K)          4STEP   230
LPC=I-1+(J-2)*(NI-2)+(K-KSTR)*(NI-2)*(NJ-2)    4STEP   231

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LPC0=LP+NVM(NVCO) 4STEP 296
LPFUOX=LP+NVM(NVFUOX) 4STEP 297
LPFU=LP+NVM(NVFU) 4STEP 298
LPTE=LP+NVM(NVTE) 4STEP 299
LPCH=LP+NVM(NVCH) 4STEP 299
LPH2=LP+NVM(NVH2) 4STEP 299
FLPTE=F(LPTE)
FLPTE=AMAX1(FLPTE,100.) 4STEP 299
FLPOX=RATIO1+F(LPFU)+RATIO3+F(LPC0)+RATIO2-(RATIO2+RATIO1)* 4STEP 299
1 F(LPFUOX)+RATIO5+F(LPCH)+RATIO6+F(LPH2) 4STEP 299
FLPOX=AMAX1(FLPOX,0.0) 4STEP 299
ARRHEN=-PREXP2*EXP(-ARCON2/FLPTE) 4STEP 299
RHOLP=AUS(RHOLP) 4STEP 299
SOR1=((F(LPCH)+RHOLP)**AA2)*(FLPOX+RHOLP)**BB2*((F(LPFU)+RHOLP 4STEP 299
1+1.E-30)**CC2)*ARRHEN 4STEP 299
IF(NODER.EQ.2)GO TO 952 4STEP 299
SOR=SOR1 4STEP 299
GO TO 953 4STEP 299
952 PHI=AMIN1(F(LPCH),FLPOX/RATIO5) 4STEP 299
SOR2=CR2*PHI*RHOLP*FDK(LPC) 4STEP 299
SOR=AMAX1(SOR1,SOR2) 4STEP 299
953 FUB=AMAX1(C.,((RATIO2+RATIO1)*F(LPFUOX)-RATIO2-RATIO3+F(LPC0) 4STEP 299
1-RATIO1+F(LPFU)-RATIO6+F(LPH2))/RATIO5) 4STEP 299
FUR=AMIN1(F(LPCH),FUB) 4STEP 299
DSDSP=SOR/(F(LPCH))-FUR+1.E-30 4STEP 299
SUCH(LP)=SOR-DSDSP+F(LPCH) 4STEP 299
SPCH(LP)=DSDSP 4STEP 299
SU(LIJ)=SUCH(LP)-RATIO0*(SUFLU(LP)+SPFU(LP)*F(LPFU)) 4STEP 299
SP(LIJ)=DSDSP 4STEP 299
951 CONTINUE 4STEP 299
GO TO 9000 4STEP 299
960 IF(NV.NE.LVH2)GO TO 1000 4STEP 299
-----SOURCE TERMS FOR H2----- 4STEP 299
DO 961 J=2,N 4STEP 299
IS=IWLI(J,N60TN) 4STEP 299
IF=IWLO(J,N60TO) 4STEP 299
DO 961 I=IS,IF 4STEP 299
LIJ=JM(J)+I 4STEP 299
LP=LIJ-KM(K) 4STEP 299
LP=LIJ-KM(K) 4STEP 299
LP=1+(J-2)*(NI-2)+(K-KSTR)*(NI-2)+MJ-2 4STEP 299
LPC0=LP+NVM(NVCO) 4STEP 299
LPFUOX=LP+NVM(NVFUOX) 4STEP 299
LPFU=LP+NVM(NVFU) 4STEP 299
LPTE=LP+NVM(NVTE) 4STEP 299
LPCH=LP+NVM(NVCH) 4STEP 299
LPH2=LP+NVM(NVH2) 4STEP 299
FLPTE=F(LPTE)
FLPTE=AMAX1(FLPTE,100.) 4STEP 299
FLPOX=RATIO1+F(LPFU)+RATIO3+F(LPC0)+RATIO2-(RATIO2+RATIO1)* 4STEP 299
1 F(LPFUOX)+RATIO5+F(LPCH)+RATIO6+F(LPH2) 4STEP 299
FLPOX=AMAX1(FLPOX,0.0) 4STEP 299
ARRHEN=-PREXP4*EXP(-ARCON4/FLPTE) 4STEP 299
RHOLP=AUS(RHOLP) 4STEP 299
SOR1=((F(LPH2)+RHOLP)**AA4)*(FLPOX+RHOLP)**BB4*((F(LPCH)+RHOLP 4STEP 299
1+1.E-30)**CC4)*ARRHEN 4STEP 299
IF(NODER.EQ.2)GO TO 962 4STEP 299
SOR=SOR1 4STEP 299
GO TO 963 4STEP 299
962 PHI=AMIN1(F(LPH2),FLPOX/RATIO6) 4STEP 299
SOR2=CR4*PHI*RHOLP*FDK(LPC) 4STEP 299
SOR=AMAX1(SOR1,SOR2) 4STEP 299
963 FUR=AMAX1(C.,((RATIO2+RATIO1)*F(LPFUOX)-RATIO2-RATIO3+F(LPC0) 4STEP 299
1-RATIO1+F(LPFU)-RATIO5+F(LPCH))/RATIO6) 4STEP 299
FUR=AMIN1(F(LPH2),FUR) 4STEP 299

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D9DSP=SU/(F(LPH2)-FUB+1.E-30)          4STEP    300
S1(L1J1)=SDR-D9DSP*F(LPH2)-RAT012*(SUFLP1+SPFLP1*F(LPFU)) 4STEP    301
1-RAT010*(SUCH(LP)+SPCH(LP)*F(LPCH)) 4STEP    302
SP(L1J1)=D9DSP 4STEP    303
961 CONTINUE 4STEP    304
GO TO 5000  SOOT    107
C----- SOURCE TERM FOR NUCLEI CONCENTRATION -----
1000 IF(NV,NF,LVN160 TO 2100
DO 1001 J=2,M  SOOT    108
TS=TWL((J,NGOTO)
IE=IWLO(J,NGOTO)
DO 1001 I=1S,IF  SOOT    109
LTJ=JNE(J)+I  SOOT    110
LP=LTJ+KMK(K)
LPFU=LP+NVN(NVFUDX)
LPFD=LPCD+NVN(NVCD)
LPTE=LPCD+NVN(NVTE)
LPCH=LPCD+NVN(NVCH)
LPH2=LPCD+NVN(NVH2)
T=F(LPTE)
FLPOX=RATIO1+F(LPFU)+RATIO3*F(LPCD)+RATIO2-(RATIO2+RATIO1)*
1 F(LPFUDX)+RATIO2*F(LPCH)+RATIO6*F(LPH2)  SOOT    201
FLPOX=SMAX1(FLPOX,1.E-30)  SOOT    202
CARB=F(LPFUDX)*12.0*CXX/WFU  SOOT    203
LPC=I-1+(J-2)*(NI-2)+(K-KSTR)*(NI-2)*(NJ-2)  SOOT    204
LPS1=LP+NVN(NVS1)  SOOT    205
LPS2=LP+NVN(NVS2)  SOOT    206
LPN=LP+NVN(NVN)  SOOT    207
FUR=F(LPFUDX)-F(LPFU)  SOOT    208
FLPC02=WC02*(CXX*FUB/WFU-CXX*F(LPCH)/WCH-F(LPCD)/WC0) 4STEP    209
FLPH20=0.5*WH20*(HYT*FUB/WFU-RATIO7*F(LPCH)-F(LPH2)) 4STEP    210
FLPN2=1.0-F(LPFU)-FLPC02-F(LPCD)-FLPOX-FLPH20-F(LPCH)-F(LPH2) 4STEP    211
VMIX=F(LPFU)/WFU+FLPC02/WC02+F(LPCD)/WC0+FLPOX/NOX+FLPH20/WH20  SOOT    212
1+FLPN2/WH2+F(LPCH)/WCH+F(LPH2)/WH2 4STEP    213
RET=(AMU*EDR2(LPC)/RHO(LP))+0.25  SOOT    214
EMDOT=23.6*RET*EDR(LPC)  SOOT    215
EMPR=FUB*(1.0+RATIO1)  SOOT    216
PST=EMPR/(EMPR+F(LPFU)+(1.0+RATIO1))  SOOT    217
FMIN=AMIN1(F(LPFU),FLPOX/RATIO1)  SOOT    218
FMAX=AMIN1(F(LPFU),FLPOX/RATIO1)  SOOT    219
C-----BYPASS CALCULATION IF TEMP.LT.TINCPC, OR IF
C CARBON/OXYGEN RATIO LT.CINCP (TINCPC AND CINCP INPUT BY USER).
1 IF(T.LT.TINCPC) GO TO 1006  COMMENT    90
1 IF(CARB/FLPC02.LT.CINCP) GO TO 1006  COMMENT    91
1 F(LPS1)/DPART(1)+3+F(LPS2)/(DPART(2)+1.E-30)*3)  SOOT    220
1/(F(LPS1)+F(LPS2))  SOOT    221
EMP=RHCP*(3.14159/(6.0*EMP))  SOOT    222
AND=AD*RHO(LP)*F(LPFU)*EXP(-ARCONN/F(LPTE))  SOOT    223
GAMAS=AMIN1(1.0,9.7*RET*3)  SOOT    224
GPST=GAMAS*PST  SOOT    225
NGPST=1.0-GPST  SOOT    226
1NGPS=1  NOX    167
NS1=IDFU  NOX    168
NS2=TOCO2  NOX    169
C-----CALCULATE MIXTURE CP.
TK=T  COMMENT    92
TKTNV=1.000/TK  NOX    170
DO 1012 II=NS1,NS2  NOX    171
1012 S2(II)=FS(LP,II)/SMW(II)  NOX    172
CALL HCPS  NOX    173
CPR=CPSUM*UNICON  NOX    174
DELTAT=DHR*EMPIN/CPR  NOX    175
TSTR=F(LPTE)*DELTAT  SOOT    231
RH0STR=RHOCON/IVMIX*TSTR  SOOT    232
RH0STR=RHOCON/IVMIX*TSTR  SOOT    233

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TO=F(LPTE)-DELTAT*GPSI/OGPSI	SOOT	234
TO=AMAX1(TO,100.0)	SOOT	235
RHOO=RHOCON/(VMIX*TO)	SOOT	236
ANOSTR=A0*RHO0*F(LPFU)*EXP(-ARCONN/TSTR)	SOOT	237
AN0P=A0*RHO0*F(LPFU)*EXP(-ARCONN/T0)	SOOT	238
GPSIR=GPSI/RHOSTR	SOOT	239
OGPSIR=OGPSI/RHO0	SOOT	240
ENRHO=F(LPNT)/RHO(LP)	SOOT	241
EMD0TR=EMD0TR*RHOSTR/(GPSI*OGPSI)	SOOT	242
FNN=(F(LPS1)+F(LPS2))*RHO(LP)/EMP	SOOT	243
ENNRHO=FNN/RHO(LP)	SOOT	244
A1=(ANOSTR+EMD0TR*ENRHO)/GO	SOOT	245
A2=(FMG-FMD0TR/RHOSTR)/GO	SOOT	246
A3=EMD0TR*(A1/RHOSTR)	SOOT	247
A4=EMD0TR*(A2/RHOSTR-ENNRHO)	SOOT	248
A5=-RRB*A1	SOOT	249
A6=AAA-BBR*A2	SOOT	250
ARG=SORT(ARS((A4-A5)*2+4.0*A6*A3))	SOOT	251
ENSTR1=(A4-A5+ARG)/(2.0*A6)	SOOT	252
ENSTR2=(A4-A5-ARG)/(2.0*A6)	SOOT	253
ENSTR=ENSTR1	SOOT	254
IF(ENSTR1.LT.0.0)ENSTR=ENSTR2	SOOT	255
ENSTR=AMIN1(ENSTR,ENRHO/GPSIR)	SOOT	256
FNSTR=AMAX1(ENSTR,ENRHO*RHOSTR)	SOOT	257
ENSTR=AMAX1(1.0,ENSTR)	SOOT	258
ENNSTR=(A1+A2*ENSTR)/ENSTR	SOOT	259
ENNSTR=AMIN1(ENNSTR,AAA/BBB)	SOOT	260
ENNSTR=AMIN1(ENNSTR,ENNRHO/GPSIR)	SOOT	261
FNNSTR=AMAX1(1.0,ENNSTR)	SOOT	262
END=(ENRHO-ENNSTR*GPSIR)/OGPSIR	SOOT	263
END=AMAX1(1.0,FNO)	SOOT	264
ENNO=(ENNPHO-ENNSTR*GPSIR)/OGPSIR	SOOT	265
FNNO=AMAX1(1.0,ENNO)	SOOT	266
FMGF=FMG*F(LPNT)	SOOT	267
SUF1=A0D*FMGF	SOOT	268
SPF1=GC*EMH	SOOT	269
SUF2=(ANOSTR*GPSIR+AN0P*OGPSIR+GO*ENSTR*GPSIR*(ENNO-ENNSTR))	SOOT	270
1*RHO(LP)+FMGF	SOOT	271
SPF2=GO*FNNO	SOOT	272
RF1=SUF1-SPF1*F(LPNT)	SOOT	273
RF2=SUF2-SPF2*F(LPNT)	SOOT	274
C-----FORMATION RATE.	COMMENT	93
IF(RF1.GT.RF2)GO TO 1004	SOOT	275
SU(LTJ)=SUF1	SOOT	276
SP(LIJ)=SPF1	SOOT	277
GO TO 1005	SOOT	278
1004 SU(LIJ)=SUF2	SOOT	279
SP(LIJ)=SPF2	SOOT	280
GO TO 10C9	SOOT	281
100A SU(LIJ)=0.0	SOOT	282
SP(LIJ)=0.0	SOOT	283
C-----OXIDATION RATE.	COMMENT	94
1005 RNC=EMD0TR*PSI*FMPMIN/(F(LPFU)+1.E-30)	SOOT	284
SP(LIJ)=SP(LIJ)-RNC	SOOT	285
1001 CONTINUE	SOOT	286
GO TO 3000	SOOT	287
***** SOURCE TERM FOR SOOT CONCENTRATION *****	SOOT	288
1100 IF(NV.LT.LVS1.OR.NV.GT.LVS2)GO TO 1300	SOOT	289
IT=NV-LVS1+1	SOOT	290
CONS2=6.0/(RHOP*DPART(IT))	SOOT	291
DO 1101 J=2,M	SOOT	292
IS=IWLC(J,NGOT0)	SOOT	293
IF=IVLC(J,NGOT0)	SOOT	294
DO 1101 I=IS,IF	SOOT	295

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L(J=JNE(J)+I
LP=L(J+KMK(K)
LPFU0X=LP+NM(NVFU0X)
LPFU=LP+NM(NVFU)
LPC0=LP+NM(NVCO)
LPTE=LP+NM(PNTE)
LPCH=LP+NM(NVCH)
LPH2=LP+NM(NVH2)
T=F(LPTE)
FLPOX=RATIO1+F(LPFU)+RATIO3+F(LPC0)+RATIO2-(RATIO2+RATIO1)*
1 F(LPFU0X)+RATIO5+F(LPCH)+RATIO6+F(LPH2)
FLPOX=AMAX1(FLPOX,1.E-30)
CARB=F(LPFU0X)+12.0*CKX/WFU
LPC=I-1+(J-2)*(NI-2)+(K-KSTR)*(NI-2)+(HJ-2)
LPS1=LP+NM(NVS1)
LPS2=LP+NM(NVS2)
LPS=LPS1+NM(NV)
LPN=LP+NM(NVN)
FUB=F(LPFU0X)-F(LPFU)
FLPC02=WC02*(CKX+FUB/WFU-CXX*F(LPCH)/WCH-F(LPC0)/WC0)
FLPH20=0.5*WH20*(HY+FUB/WFU-RATIO7+F(LPCH))-F(LPH2)
FLPN2=1.0-F(LPFU)-FLPC02-F(LPC0)-FLPOX-FLPH20-F(LPCH)-F(LPH2)
VMIX=F(LPFU)/WFU+FLPC02/WC02+F(LPC0)/WC0+FLPOX/WOX+FLPH20/WH20
1+FLPN2/WN2+F(LPCH)/WCH+F(LPH2)/WH2
RET=(ANU*EDK2(LPC)/RHO(LPI))**0.25
FM00T=29.6*RET*EDK(LPC)
EMPR=FUB*(1.0+RATIO1)
PSI=EMPR/(EMPR+F(LPFU)*(1.0+RATIO1))
FMIN=AMIN1(F(LPFU),FLPOX/RATIO1)
C----BYPASS CALCULATION IF TEMP.LT.TINCP, OR IF
C CARBON/OXYGEN RATIO LT.CINCP (TINCP AND CINCP INPUT BY USER).
C IF(T.LT.TINCP)GO TO 1106
1 IF(CARB/FLPOX.LT.CINCP)GO TO 1106
FMP=(F(LPS1)/DPART(1)**3+F(LPS2)/(DPART(2)+1.E-30)**3)
1/F(LPS1)+F(LPS2))
FMP=RHO*1.4159/(6.0*EMPR)
AN0=A0*RHO(LP)+F(LPFU)*EXP(-ARCONN/F(LPTE))
GAMAS=AMIN1(1.0,9.7*RET**3)
GPSI=GAMAS*PSI
OGPSI=1.0-GPSI
INCPS=1
NS1=TDFU
NS2=IOCO2
C----CALCULATE MIXTURE CP.
TK=T
TKINV=1.000/TK
D9 1013 II=NS1,NS2
1013 S2(TF)=FS(LP,II)/SM(II)
CALL HCPS
CPR=CPUSUM*UNICON
DELTAT=DHR*EMIN/CPR
TSTR=F(LPTE)+DELTAT
RHOSTR=RHOCON/(VMIX*TSTR)
TO=F(LPTE)-DELTAT*GPST/OGPST
TO=AMAX1(TO,100.0)
RHOD0=RHOCON/(VMIX*TO)
AN0STR=A0*RHO*STR+F(LPFU)*EXP(-ARCONN/TSTR)
AN0D0=A0*RHO*DF(LPFU)*EXP(-ARCONN/TO)
GPSIR=GPST/RHOSTR
OGPSTR=OGPST/RHO0
ENRHO=F(LPN)/RHO(LPI)
EMD0TR=EMD0T*RHOSTR/GPST
ENM=(F(LPS1)+F(LPS2))/RHO(LPI)/EMP
ENMRHO=ENM/RHC(LPI)

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SOOT	296
SOOT	297
SOOT	298
SOOT	299
SOOT	300
SOOT	301
4STEP	312
4STEP	313
SOOT	302
SOOT	303
4STEP	314
SOOT	305
SOOT	306
SOOT	307
SOOT	308
SOOT	309
SOOT	310
SOOT	311
SOOT	312
4STEP	315
4STEP	316
4STEP	317
SOOT	318
4STEP	318
SOOT	318
SOOT	319
SOOT	320
SOOT	321
SOOT	322
COMMENT	95
COMMENT	96
SOOT	323
SOOT	324
SOOT	325
SOOT	326
SOOT	327
SOOT	328
SOOT	329
SOOT	330
SOOT	331
NOX	176
NOX	177
NOX	178
COMMENT	97
NOX	179
NOX	180
NOX	181
NOX	182
NOX	183
NOX	184
SOOT	334
SOOT	335
SOOT	336
SOOT	337
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SOOT	346
SOOT	347

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A1=(ANQSTR+EMDDOTR+ENRHQ)/GO
 A2=(FMG-FMDDOTR/RHOSTR)/GO
 A3=FMDDOTR+A1/RHOSTR
 A4=EMDDOTR*(A2/RHOSTR-ENNRHO)
 A5=-RBRPAZ
 A6=AAA-RBB+A2
 ARG=SORTI(ARS((A4-A5)*02+4,0DAB0A3))
 ENSTR1=(A4-A5+ARG)/(2.0*AG)
 ENSTR2=(A4-A5-ARG)/(2.0*AG)
 ENSTR=ENSTR1
 TF(ENSTR).LT.0.01ENSTR=ENSTR2
 ENSTR=A MIN1(ENSTR,ENRHQ/GPSIR)
 ENSTR=A MAX1(ENSTR,ENRHQ+RHOSTR)
 ENSTR=A MAX1(1.0,ENSTR)
 ENNSTR=(A1+A2*ENSTR)/ENSTR
 ENNSTR=A MIN1(ENNSTR,AAA/BBB)
 ENNSTR=A MIN1(ENNSTR,ENRHQ/GPSIR)
 ENNSTR=A MAX1(1.0,ENNSTR)
 FNO=(ENRHQ-FNSTR*GPSIR)/OGPSIR
 ENO=A MAX1(1.0,ENO)
 ENNO=(ENRHQ-ENNSTR*GPSIR)/OGPSIR
 FNNO=A MAX1(1.0,ENNO)
 C-----QUASI GLOBAL FORMATION RATE.
 SUF1=PREXPS*F(LPTE)*ALPHA*(RHQ(LP)*F(LPFU))+AAS*(RHQ(LP)*FLPOX)
 1000AS*EXP(-ARCONS/F(LPTE))*FRACP(II)
 C-----TURBULENT FORMATION RATE.
 SUF2=EMPO*(AAA+F(LPM)+RBB+ENNSTR*GPSIR+RHQ(LP)*(ENO-ENSTR))
 10FRACP(II)
 SPF2=RHO(LP)+RBB+ENO*FRACP(II)
 SPF2F=SPF2*F(LPS)
 SUF2=A MAX1(SUF2,SPF2F)
 RF2=SUF2-SPF2F
 TF(SUF),GT,RF2!60 TO 1104
 SU(LIJ)=SUF1
 SP(LIJ)=0.0
 GO TO 1105
 1104 SU(LIJ)=SUF2
 SP(LIJ)=SPF2
 GO TO 1105
 1105 SU(LIJ)=0.0
 SP(LIJ)=0.0
 C-----SURFACE OXIDATION RATE.
 1105 AREAT=CDS2*RHO(LP)
 AKA=2000.0*EXP(-19100./F(LPTE))
 AKR=4.4E-1*EXP(-7640./F(LPTE))
 AK7=21.38*EXP(2060./F(LPTE))
 AXT=1.51E6*EXP(-46800./F(LPTE))
 P02=FLPOX*PRESS/(VMIX*92.0*101329.0)
 PSIC=1.0/(1.0+AKT/(AKB*P02))
 AKK=AKA*P02/(1.0+AKZ*P02)
 SPC1=12.0*AREAT*(AKK*PSIC+AKB*P02*(1.0-PSIC))
 C-----TURBULENT OXIDATION RATE.
 SPC2=EMDDOT*PSI*FMMIN*RHT(LP)/(F(LPFU)+1.E-30)
 SPC1=APTN1(SPC1,SPC2)
 SP(LIJ)=SP(LIJ)-SPC1
 1101 CONTINUE
 GO TO 5000
 C----- OTHER SPECIES - H2O, OH, N, NO, NO2
 C----- THESE SOURCES CALCULATED IN KINETICS PROGRAM CREK.
 1200 IF(NV,NE,LVH1)60 TO 1400
 DO 1201 J=2,N
 IS=IWLC(J,NGCTO)
 IF=IWLC(J,NGCTO)
 1201
 1300

00 1201 I=IS,IE
 LIJ=I+JM(J)
 SU(LIJ)=0.0
 1201 SP(LIJ)=0.0
 GO TO 5000
 1400 CONTINUE
 5000 CONTINUE
 RETURN
 FND
 SUBROUTINE AUXRAD
 COMMON F(300),DU(300),DV(300),DW(300),
 1 ANUC(900),S00T1(900),S00T2(900),FCM(900),FH2(900),FS(900,14),
 1 RHO(500),VIS(500),ABSR(500),SCTR(500),SU(100),SP(100),
 1 DRHNDP(500),
 1 AXPK(100),AXPM(100),AYP(100),AYM(100),AZP(100),
 2 AZM(100),C7(100),CY(10),CZU(100),CYU(10),
 3 C7P(100),CYP(10),DIV6(100),NTP1,NTP2
 1, AXMK(192),AXPK(192),AYMK(192),AYPK(192),AZMK(192),AZPK(192),
 2 SUK(192),SPK(192)
 DIMENSION U(500),V(500),W(500),PP(500),P(500),TEMP(500)
 DIMENSION GAM(500)
 EQUIVALENCE (F(1),U(1)),(F(501),V(1)),(F(1001),W(1))
 EQUIVALENCE (F(1501),PP(1)),(F(2001),P(1)),(F(2501),TEMP(1))
 EQUIVALENCE (F(3001),GAM(1))
 COMMON/CYL/R(30),RM(30),RMV(30),YSR(30),YSVR(30),IPLAK
 COMMON/GR ID/X(40),Y(30),Z(30),XS(40),YS(30),ZS(30),XSU(40),
 1 YSV(30),ZSH(30),XOIF(40),YOIF(30),ZOIF(30),FXP(40),FXM(40),
 2 FYP(30),FYR(30),FZP(30),FZN(30),DT,TIME
 COMMON
 1/CINDEX/IDCO, IDFU, IDO2, IDN2, IDH20, IDCO2, IDH1, IDH2, IDN1, IDNO, IDNO2
 1, IDP, IDOH, IMCPS, ILC, ILH, IMAT, ITER, JJJ, N1, N2, N3, NA, NGLOB, NGLBP,
 2 NLM, NQ, NSP, NS1, NS2, IDCH
 3/CCHEM/CPSUM,HSUM,FQ,PPLN,RGAS,RGASIN,SMINV,TKINV,TLN,LNRG
 4/CPARAM/ASUB(30,31),EMV,ER,HSUB0,NOEBUG,NS,PA,Q0,Q1,Q2,Q3,Q4,RHOFP,
 4 SM,SMW(30),SPO,S1(30),S2(30),TK,LADIA0,LDEBUG,LEQUIT,LREACT,
 4 LENER,EDKIJ,LCONVG
 DOUBLE PRECISION CPSUM,EMV,ER,FQ,HSUB0,HSUM,PA,PPLN,Q0,Q1,Q2,Q3,
 1 Q4,RGAS,RGASIN,RHOFP,SM,SMINV,SMW,S1,S2,TK,TKINV,TLN,SM0
 2,FUT,FST
 COMMON/STEP4/PEXP1,PEXP2,PEXP3,PEXP4,ER1,ER2,ER3,ER4,CEBU1,CEBU2,
 1 CEBU3,CFBU4,AEXP1,AEXP2,AEXP3,AEXP4,BEXP1,BEXP2,BEXP3,BEXP4,
 2 CEXP1,CEXP2,CEXP3,CEXP4,FUT,FST
 LOGICAL LADIA0,LCONVG,LDEBUG,LEQUIT,LNRG,LREACT,LENER
 COMMON/INT/L,R,N,LCV,MCV,NCV,LP1,MP1,NP1,NI,NJ,NK,NINJ,NINJNK,NV,
 1 MMV,NGOTO,K,ISTR,JSTR,KSTR,NVM(35),NM(30),JM(30),ISTFP,
 2 ISOLVE(32),IPRINT(33),TITLE(10,33),IKV,ISWP,JSWP,RELAX(35),NP,
 3 MRHO,NGAP,INLJ(30,5),JWLJ(30,5),JWL(40,5),JVL(40,5),IWEI,
 4 INFO,MM1,JWIT,JWTO,JWOT,JW0,JDW,JKIN(30,30),IKIN(40,30)
 COMMON/INDEX/IPAR,LPREF,ISTUN,IMCOP,ITRAD,NVRX,NVRY,NVRZ,JPLANE
 1,PLAKM1,LVK,LVD,LVFUDX,LVFU,LVCO,LVH,LVRK,LVRY,LVRZ,NVF(32),
 2,IJUMP,IRES,TITLE2(20),IMAX,JMAX,KMAX,NVCO,FUMCO,NVH20,NVC02,
 3 NVN2,NVCH,NVH2
 COMMON/CNOX/LVH1,LVH2,LVN1,LVN02,LVO,LV0H,LVH20,LVN2,LVD2,
 1 LVC02,LVFU1,LVC01,NNOX,INOX,ITNOX,SN0X,TNOX
 COMMON/THERP/NVH,NVFU,NVOX,NVFUDX,NVTF,MDEN,IDK,FSTOIC,NFU,CP,
 1 GASCON,RHOCON,UNICON,PRESS,NVFAV,TCYLM,TINLM,TLIP,ACDEF(4),
 2 T4,DFAC,WFU,WCO2,WCO,WDX,WH20,WN2,MYY,CXX,RATIO1,RATIO2,
 3 RATIO3,RATIC4,HCO,TAN,ITWALL
 COMMON/CTDMA/KEND,ICTDMA(32)
 COMMON/MIS/AMU,DEM,SMAX,SSUM,LASTEP,HTCEXT,CFR,EMISW,EMISIN,
 1 FMISR,TOUT,RTCD,EMI,RADIN,RADSUR,FMA,FR,SOFR,
 2 FKFU,FDFU,TFUEL,WFN2,FLD(40),TFMTM(40),H(40),FUEL(40),FUDX(40),
 2 HIN(40),TIN(40),FUELS(40),SEXIT,IGAM1(29),IGAM2(29)
 COMMON/TURB/NVH,NVD,C1,C2,CD,AK,DUDOKJ(3,3),AKFAC,ALFAC,

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NOX	189
NOX	190
NOX	191
NOX	192
NOX	193
NOX	194
AU	615
AU	616
AU	617
AUR	2
COMFB	2
4STEP	18
RAD	3
RAD	4
COMFB	4
COMFB	5
COMFB	6
CTOMA	3
CTOMA	4
COMFB	7
COMFB	8
COMFB	9
COMFB	10
COMFB	11
COMMON	2
COMMON	3
COMMON	4
COMMON	5
COMMON	6
COMMON	7
COMMON	8
COMMON	9
COMMON	10
COMMON	11
NOX	2
NOX	3
NOX	4
4STEP	3
NOX	6
NOX	7
NOX	8
NOX	9
NOX	10
NOX	11
4STEP	4
4STEP	5
4STEP	6
4STEP	7
NOX	12
COMMON	6
4STEP	8
4STEP	9
COMMON	9
COMMON	10
COMMON	11
4STEP	10
COMMON	12
4STEP	11
NOX	16
NOX	17
COMMON	19
COMMON	20
COMMON	21
COMMON	22
COMMON	23
COMMON	24
4STEP	13
COMMON	6

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1 MODEL,PR(32),PREF(32),PJAY(32),E
COMMON/PAD/NVE,SIGMA,ABSOR,SCATR
COMMON/REACT/ARCON1,PREXP1,CR1,ARCON2,PREXP2,CR2,MODER
COMMON/DRNPL/EVAP(192),NTP4,NFNZ,KD(3),YD(3),ZD(3),ALFA(3),
1 DELTA(3),THETA1(3),THETA2(3),NSL(3),WFF(3),SMDF(3),
2 VFIIFL(3),RFUEL(3),EVSU(64),HEVAP
COMMON/INJECT/LOWIN,IWINJ(20),JWINJ(20),UWINJ(20),WWINJ(20),
1 AWINJ(20),TIWINJ(20),IVINJ(20),JVINJ(20),KVINJ(20),VINJ(20),
2 FVINJ(20),DVINJ(20),AVINJ(20),TVINJ(20),NURNJ,NVINJ,JSW1,JSW2,
3 NSW,VSW,AFSW,FSW,TSW,WSW,SWH,RHOSW
COMMON/CSORT/NVN,NVS1,NVS2,ISOOT,SSOOT,NSOOT,AD,ARCONN,AAA,BBB,FNG
1,GO,MPART,DPART(2),FRACP(2),RHOP,ARCONS,PREXPS,ALPHA,AAB,BAB,DHR
2,LVN,LVS1,LVS2,CINCP,TINCP,FUTOT
COMMON/CRAD/IPAD,SRAD
COMMON/CFOUR/PREXP3,ARCON3,CR3,PREXP4,ARCON4,CR4,AA1,BB1,CC1,
1 AA2,BB2,CC2,AA3,BB3,CC3,AA4,BB4,CC4,RATIO9,RATIO6,RATIO7,
2 RATIO8,RATIO9,RATIO10,RATO11,RATO12,WCH,WH2,WC2H4,LVCH1,LVH21
C   00 00 00 00 00 00 00 00 00 00 00 00 00 00 00 00 00 00 00 00 00
FNTRY GAMRAD
C-----FNTRY GAMRAD IS USED TO CALCULATE THE GAMAS IN THE RADIATION
C-----EQUATIONS.
C
IF (NV,EQ,1) GO TO 3100
DO 4002 K=1,NPI
DO 4002 J=1,MP1
KJM=KM(K)+JP(J)
IS=IWLI(J,4)
IE=IWLC(J,4)
DO 4002 I=IS,IE
LP=KJM+I
C-----VALUES OF ABSORPTION AND SCATTERING COEFFICIENTS FOR
C   ITRAD=2.
ARSR(LP)=ABSR
4002 SCTR(LP)=SCATR
TF(ITRAD,NE,2)GO TO 4001
C-----ABSORPTION COEFFICIENT CALCULATED FROM SUBROUTINE ABSOR
C   (ITRAD=3).
DO 4000 K=2,N
DO 4000 J=2,M
KJM=KM(K)+JP(J)
IS=IWLI(J,4)
IE=IWLC(J,4)
DO 4000 I=IS,IE
LP=KJM+I
TS=TEMP(ILP)
TS=AMAX1(TS,300.0)
TS=AMIN1(TS,2000.0)
T+TS
PATH=2.0*Y(MP1)
C-----SOOT CONCENTRATION.
SOTK=7.0*(SCET1(LP)+SOOT2(LP))*RHO(LP)/(RHOP*0.94E-6)
LPFU=LP+NVM(NVFU)
LPFU0X=LP+NVM(NVFU0X)
LPCO=LP+NVM(NVCO)
LPCH=LP+NVM(NVCH)
LPH2=LP+NVM(NVH2)
FIR=F(LPFUK)-F(LPFU)
C-----CO2 AND H2O CONCENTRATIONS.
FLPCO2=WC02*(CYR*FIR/WFU-CYR*F(LPCH)/WCH-F(LPCO)/WC01)
FLPCO2=AMAX1(1.0,F-20,FLPCO2)
FLPOX=AMAX1(0.0,RATIO1*F(LPFU)+RATIO3*F(LPCO)+RATIO2
1-(RATIO1+RATIO2)*F(LPFU0X)+RATIO5*F(LPCH)+RATIO6*F(LPH2))
FLPH2O=C.5*WH2O*(HYT*FIR/WFU-RATIO7*F(LPCH)-F(LPH2))
FLPH2O=AMAX1(1.0,F-20,FLPH2O)
4STEP      14
COMGEN     8
COMGEN     9
COMGEN    10
COMGEN    11
COMGEN    12
COMGEN    13
COMGEN    14
COMGEN    15
COMGEN    16
COMGEN    17
SOOT      8
SOOT      9
SOOT    10
SOOT    11
SOOT    12
SOOT    13
SOOT    14
SOOT    15
SOOT    16
AUR      6
AUR      7
COMMENT 105
COMMENT 106
COMMENT 107
AUR      8
RAD      74
RAD      75
RAD      76
RAD      77
RAD      78
RAD      79
RAD      80
COMMENT 108
COMMENT 109
RAD      81
RAD      82
RAD      83
COMMENT 110
COMMENT 111
RAD      84
RAD      85
RAD      86
RAD      87
RAD      88
RAD      89
RAD      90
RAD      91
RAD      92
RAD      93
RAD      94
RAD      95
RAD      96
RAD      97
RAD      98
RAD      99
RAD      100
COMMENT 112
RAD      101
RAD      102
RAD      103
4STEP 319
4STEP 320
RAD      100
COMMENT 113
4STEP 321
RAD      102
RAD      103
4STEP 322
4STEP 323
RAD      106

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FLPM2=1.0-F(LPFU)-FLPC02-F(LPC0)-FLPOX-FLPH20-F(LPCH)-F(LPH2)
FLPN2=AMAX1(0.0,FLPH2)
VMTX=F(LPFU)/MFU+FLPC02/MC02+F(LPC0)/MC0+FLPOX/MOX+FLPH20/MH20
1+FLPN2/MH2+F(LPCH)/MCH+F(LPH2)/MH2
PC02=FLPC02/(VMTX*MC02)
PH20=FLPH20/(VMTX*MH20)
PC02=APIN1(PC02,1.0-PH20)
FACP=5.97*T/TS
PATH=AMIN1(PATH,FACP/PC02)
PATH=AMIN1(PATH,FACP/PH20)
CALL APSORR(TS,T,PATH,SQTK,PC02,PH20,ALPHAS)
ALPHAS=AMIN1(ALPHAS,0.999)
ABSR(LP)=ALOG(1.0-ALPHAS)/PATH

4000 CONTINUE
4001 CONTINUE
CALCULATE GAMMA FOR X-DIRECTION FLUX.
DO 3000 K=1,NP1
DO 3000 J=1,MP1
KJM=KM(K)+JM(J)
IS=IWLI(J,4)
IE=IWLO(J,4)
DO 3000 I=IS,IE
LP=KJM+I
GAM(LP)=1.0/(ABSR(LP)+SCTR(LP))
3000 CONTINUE
GO TO 3200
CALCULATE GAMMA FOR Y-DIRECTION FLUX.
3100 DO 3200 K=1,NP1
DO 3200 J=1,MP1
KJM=KM(K)+JM(J)
IS=IWLI(J,4)
IE=IWLO(J,4)
DO 3200 I=IS,IE
LP=KJM+I
GAM(LP)=1.0/(ABSR(LP)+SCTR(LP)+1.0/(ER(J)+1.E-30))
3200 CONTINUE
3300 RETURN
C ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** * AUR 29
      FNTRY SORAD
C-----FNTRY SORAD IS USED TO CALCULATE THE SOURCE TERMS IN THE
C RADIATION EQUATIONS.
C
IF (INV,EQ,LVR2) GO TO 300
C-----X- AND Y-DIRECTION FLUXES.
DO 101 J=2,N
IS=IWLI(J,MGOTO)
IE=IWLO(J,MGOTO)
DO 101 I=IS,IE
LTJ=JM(J)+I
LP=LTJ+KM(K)
LPRX=LP+NVN(MVRX)
LPRY=LP+NVN(MVRY)
LPRZ=LP+NVN(MVRZ)
LPTE=LP+NVN(MVTE)
FLPTE=F(LPTE)
FLPE=SIGMAOFIPTE*0.4
SU(LIJ)=ABSR(LP)+FLPE+SCTR(LP)*(F(LPRX)+F(LPRY)+F(LPRZ))/3.
SP(LIJ)=(ABSR(LP)+SCTR(LP))
101 CONTINUE
RETURN
300 CONTINUE
C-----Z-DIRECTION FLUX.
DO 301 K=2,N
KJM=KM(K)+JM(JPLANE)

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IS=IWLI(JPLANE,NGATO)
IF=IWLO(JPLANE,NGATO)
DO 301 I=IS,IF
  LIK=JMK+I
  LP=KJM+I
  LPRX=LPOHVM(NVRX)
  LPRY=LPOHVM(NVRY)
  LPRZ=LPOHVM(NVRZ)
  LPTF=LPOHVM(NVTF)
  FLPTF=F(LPTF)
  FLPE=SIGMA*FLPTF*94
  SU(LIK)=ABSR(LP)+FLPE+SCTR(LP)*(F(LPRX)+F(LPRY)+F(LPRZ))/3.
  SP(LIK)=(ABSR(L')+SCTR(LP))
301 CONTINUE
RETURN
END
SUBROUTINE SPRAY
C ***** SUBROUTINE SPRAY *****
C SURROUNTING FOR AIRTRIP CODE WHICH CALCULATES THE TRAJECTORY
C AND EVAPORATION RATES FOR A FUEL NOZZLE SPRAY. WRITTEN NOV. 1976
C *****
COMMON F(3500),DU(500),DV(500),DM(500),
  1 ANUC(500),SOOT1(500),SOOT2(500),FCH(500),FH2(500),FS(500,14),
  1 RHO(500),VIS(500),ABSR(500),SCTR(500),SU(100),SP(100),
  1 DRHOOP(500),
  1 AXP(100),AXM(100),AYP(100),AZP(100),
  2 AZM(100),CZ(100),CYU(100),CYU(10),
  3 C7P(100),CYP(100),DIVG(100),NTP1,NTP2
  1,AKMK(192),AXPK(192),AYPK(192),AZMK(192),AZPK(192),
  2 SUK(192),SPK(192)
  DIMENSION U(500),V(500),W(500),PP(500),P(500),TEMP(500)
  DIMENSION GAM(500)
  EQUIVALENCE (F(1),U(1)),(F(501),V(1)),(F(1001),W(1))
  EQUIVALENCE (F(1501),PP(1)),(F(2001),P(1)),(F(2501),TEMP(1))
  EQUIVALENCE (F(3001),GAM(1))
  COMMON/CYL/R(30),RM(30),RNV(30),YSR(30),YSVR(30),IPLAX
  COMMON/GRID/X(40),Y(30),Z(30),XS(40),YS(30),ZS(30)+XSU(40),
  1 YSV(30),ZSW(30),XDIF(40),YDIF(30),ZDIF(30),FXP(40),FXM(40),
  2 FYP(30),FYM(30),FPZ(30),FZM(30),DT,TIME
  COMMON
  1/CINDEX/IDCC,IDFU,IDO2,IDM2,IDH20,IDC02,IDH1,IDH2,IDN1,IDNO,EDNO2
  1,IDD,IDRH,ICHPS,ILC,ILH,IMAT,ITER,JJJ,M1,M2,M3,NA,NGLOE,NGLNP,
  2 NLM,NG,NSM,NS1,NS2,IOCH
  3/CCHEMI/CPSUM,HSUM,FQ,PPLN,RGAS,RGASIN,SINV,TINV,TLN,LNRG
  4/CPARAM/ASUB(30,3),EMV,ER,HSUB0,NDEBUG,NS,PA,QQ,Q1,Q2,Q3,Q4,RHOPP,
  4 SH,SHW(30),SM0,S1(30),S2(30),TK,LADTAB,LDEBUG,L_EQUI,LRATE,
  4 LENER,EDKT,IJ,LCQNYG
  DOUBLE PRECISION CPSUM,EMV,ER,FQ,HSUB0,HSUM,PA,PPLN,QQ,Q1,Q2,Q3,
  1 Q4,RGAS,RGASIN,RHOPP,SH,SHINV,S1,S2,TK,TINV,TLN,SM0
  2,FUT,FST
  COMMON/STEP4/PEXP1,PEXP2,PEXP3,PEXP4,ER1,ER2,ER3,ER4,CB01,CB02,
  1 CERU3,CERU4,AEXP1,AEXP2,AEXP3,AEXP4,BEXP1,BEXP2,BEXP3,BEXP4,
  2 CFXP1,CFXP2,CFXP3,CFXP4,FUT,FST
  LOGICAL LADTAB,LCQNYG,LDEBUG,L_EQUI,LRATE,LENER
  COMMON/INT/L,M,N,LCV,NCV,NCV,LP1,MP1,MP1,NI,ND,NK,NINJ,NINJNK,NV,
  1 NMV,NGOTO,N,ISTR,JSTR,KSTR,NVM(35),NM(30),JN(30),ISTEP,
  2 ISOLVE(32),IPRINT(33),TITLE(10,33),IXY,ISWP,JSWP,RELAX(35),MP,
  3 NMHD,NGAM,INL(30,5),IWLO(30,5),JWL(40,5),JWL(-3,5),IWEI,
  4 IWE0,MM1,JW1,JW0,JW01,JW00,JDW,JKIN(30,30),IKIN(40,30)
  COMMON/INDEX/IPAR,LPREF,ISTUN,INCMP,ITRD,MRK1,MRK2,MRK3,JPLANE
  1,PLAVM1,LVR1,LVD,LVFUD,LVFU,LVC0,LV4,LVR1,LVRY,LVR2,LVF(32),
  2,IJUMP,IRES,TITLE2(20),IMAX,JMAX,KMAX,NVC0,FUNCO,NVH20,NVC02,
  3 NVN2,NVCH,NVH2
  COMMON/CMOX/LVH1,LVH2,LVN1,LVND,LVND2,LVD,LVOD,LVH20,LVN2,LV02,

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XH(1)=X(1)	SP	47
DO 115 I=2,L	SP	48
115 XM(I)=XM(I-1)+XS(I)	SP	49
XM(LPI)=XM(L)	SP	50
YM(1)=Y(1)	SP	51
DO 17 J=2,M	SP	52
17 YM(J)=YM(J-1)+YS(J)	SP	53
YM(MP1)=YM(M)	SP	54
ZM(1)=Z(1)	SP	55
DO 19 K=2,N	SP	56
19 ZM(K)=ZM(K-1)+ZS(K)	SP	57
ZM(NP1)=ZM(N)	SP	58
C #####	SP	59
C -----LOOP OVER FUEL NOZZLES	SP	60
DO 2000 NH=1,NFH7	SP	61
RFF=0.	SP	62
NSL2=NSL(NH)	SP	63
RNSL=NSL2	SP	64
WFT=WFF(NH)/RNSL	SP	65
C -----CALCULATE UNIT VECTORS OF SPRAY LINES	SP	66
SINA=SIN(ALFA(NH)/2.)	SP	67
SINR=SIN(BETA(NH))	SP	68
SIND=SIN(DELTA(NH))	SP	69
COSA=COS(ALFA(NH)/2.)	SP	70
COSR=COS(BETA(NH))	SP	71
COSD=COS(DELTA(NH))	SP	72
DTHETA=THETA2(NH)-THETA1(NH)	SP	73
IF (DTHETA.LT.0.0) DTHETA=DTHETA+PT2	SP	74
DANG=DTHETA/(RNSL-1.)	SP	75
IF (DTHETA.GT.0.9*PT2) DANG=DTHETA/RNSL	SP	76
THETA=THETA1(NH)	SP	77
DO 10 IL=1,NSL2	SP	78
SINT=SIN(THETA)	SP	79
COST=COS(THETA)	SP	80
THFTA=THETA+DANG	SP	81
IF (THETA.GT.PT2) THETA=THETA-PT2	SP	82
VFCX(IL)=-SINA*SINT+COSB-COSA*SINB	SP	83
VECY(IL)=SINA*COST+COSD+SINA*SINT*SINB*SIND-COSA*COSD*SIND	SP	84
VFC7(IL)=SINA*COST*SIND-SINA*SINT*SINB*COSD+COSA*COSP+COSD	SP	85
RVECX(IL)=-SINT*COSA	SP	86
RVECY(IL)=COST*COSD+SINT*SINB*SIND	SP	87
RVEC7(IL)=COST*SIND-SINT*SINB*COSD	SP	88
10 CONTINUE	SP	89
C#####	SP	90
C-----START CALCULATIONS FOR EVAPORATION RATES-----	SP	91
DO 1750 IL=1,NSL2	SP	92
DO 2000 IG=1,NG	SP	93
UF=VFCX(IL)*VFUEL(NH)	SP	94
VF=VECY(IL)*VFUEL(NH)	SP	95
VR=VEC7(IL)*VFUEL(NH)	SP	96
DIA=SD(NH)*1.E-6*DSND(IG)	SP	97
TFU=TFUFL	SP	98
ITYPF=1	SP	99
DTAO=DTIA	SP	100
CON2=0.	SP	101
TGPNT=-10	SP	102
IF (ISTEP.NE.1GPNT) GO TO 7746	SP	103
WRITE (6,7747)	SP	104
7747 FORMAT (1/10X,'UF',10X,'VF',10X,'WF',9X,'UST',9X,'VST',9X,'NST',1 1 7X,'FEVAP',10X,'XF',10X,'YF',10X,'ZF')	SP	105
1746 CONTINUE	SP	106
FEVAP=0.	SP	107
DO 21 I=1,LPI	SP	108
ILOC=I	SP	109
	SP	110

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IF (X0(NN).GT.XM(I)) GO TO 11      SP    111
GO TO 12                            SP    112
11 CONTINUE                          SP    113
12 DO 13 J=1,NP1                    SP    114
    JLOC=J
    IF (Y0(NN).GT.YM(J)) GO TO 13
    GO TO 14
13 CONTINUE                          SP    115
14 DO 15 K=1,NP1                    SP    116
    KLOC=K
    IF (Z0(NN).GT.ZM(K)) GO TO 15
    GO TO 16
15 CONTINUE                          SP    117
16 XF=X0(NN)+RFUEL(NN)*RVECX(IL)   SP    118
    YF=Y0(NN)+RFUEL(NN)*RVECY(IL)
    ZF=ZF(NN)+RFUEL(NN)*RVECZ(IL)/(R(1)+PLAXM1*YF)
C-----LOCATION OF THE DROPLET-----
110 CONTINUE                         SP    119
    ILOC=JLOC
    JLOC=JLOC
    KLOC=KLOC
C -----X DROPLET LOCATION          SP    120
    IF (XF.GE.XM(ILOC-1).AND.XF.LT.XM(ILOC)) GO TO 27
    DO 22 I=1,LP1
        ILOC=I
        IF (XF.GT.XM(I)) GO TO 22
        GO TO 27
22 CONTINUE                           SP    121
C -----Y DROPLET LOCATION          SP    122
27 IF (YF.GE.YM(JLOC-1).AND.YF.LT.YM(JLOC)) GO TO 23
    DO 24 J=1,NP1
        JLOC=J
        IF (YF.GT.YM(J)) GO TO 24
        GO TO 23
24 CONTINUE                           SP    123
C -----Z DROPLET LOCATION          SP    124
23 IF (ZF.GE.ZM(KLOC-1).AND.ZF.LT.ZM(KLOC)) GO TO 63
    DO 26 K=1,NP1
        KLOC=K
        IF (ZF.GT.ZM(K)) GO TO 26
        GO TO 48
26 CONTINUE                           SP    125
48 IF (KLOC.GT.1) GO TO 28
    KLOC=N
    ZF=Z(NP1)-ZSMALL
28 IF (KLOC.LT.NP1) GO TO 63
    KLOC=?
    ZF=Z(1)+ZSMALL
C -----DROPLET NEAR A WALL         SP    126
63 INDX=0
    IF (ILOC.GE.IWLI(JLOC,4)) GO TO 49
    ILOC=ILOC
    XF=AMAX1(XF,XM(ILOC-1)+DIA/2.)
    XF=AMIN1(XF,XM(ILOC)-DIA/2.)
    INDX=1
49 IF (ILOC.LE.IWLI(JLOC,4)) GO TO 47
    IF (JLOC.GT.JW01.AND.JLOC.LT.JW00) GO TO 1000
    ILOC=ICLD
    XF=AMAX1(XF,XM(ILOC-1)+DIA/2.)
    YF=AMIN1(YF,XM(ILOC)-DIA/2.)
    INDX=?
47 IF (JLOC.GT.JWLI(ILOC,4)) GO TO 44
    IF (INDX.EQ.0) GO TO 50
    JLOC=JLOC

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YF=AMAX1(YF,YM(JLOC-1)+DIA/2.)
YF=AMIN1(YF,YM(JLOC)-DIA/2.)
INDX=3
44 IF (JLOC.LT.JWLO(JLOC,4)) GO TO 41
JLOC=JOLD
YF=AMAX1(YF,YM(JLOC-1)+DIA/2.)
YF=AMIN1(YF,YM(JLOC)-DIA/2.)
INDX=4
C -----CHECK FOR SLOTS
41 IF (NUINJ.LE.0) GO TO 45
DO 149 II=1,NUINJ
IU=IUINJ(II)-1
JU=JUINJ(II)
IF (ILOC,F0,IU,AND,JLOC,E0,JU) GO TO 50
149 CONTINUE
45 CONTINUE
GO TO 60
C -----DROPLET HAS HIT SOLID BOUNDARY
50 ILOC=ICLO
JLOC=JOLD
KLOC=KOLD
DEVAP=1.-FEVAP
UF=0.
VF=0.
WF=0.
FX=0.
FY=0.
FT=0.
GO TO 249
C -----NO BOUNDARIES HAVE BEEN HIT
60 CONTINUE
LP=KM(KLOC)+JM(JLOC)+ILOC
LYP=LP+1
LYP=LP+NI
L7P=LP+NUINJ
LPTE=LP+NVM(NVTE)
LPFUOK=LP+NVM(NVFUOK)
C ----- CAREFUL HERE
LPFU=LP+NVM(NVFU+3)
LPCD=LP+NVM(NVCD+1)
LPCH=LP+NVM(NVCH)
LPH2=LP+NVM(NVH2)
C -----FREESTREAM PROPERTIES
ROST=RHO(LP)
TST=F(LPTE)
UST=FXP(ILOC)*U(LP)+FXM(ILOC)*U(LXP)
VST=FYP(JLOC)*V(LP)+FYM(JLOC)*V(LYP)
WST=F7P(KLOC)*W(LP)+F7M(KLOC)*W(L7P)
IR=IWLT(JLOC,4)
IF (XF.GE.X(IR)) GO TO 51
IF (JKIN(JLOC,KLOC),E0,1) GO TO 51
FAC=(X(F-1)/(X(IR)-X(IR-1)))**.14286
UST=0.
VST=VST+FAC
WST=WST+FAC
IF (INDR,NE,1) GO TO 51
UF=UST
VF=VST
WF=WST
51 IR=IWLO(JLOC,4)
IF (XF,LE,X(IR)) GO TO 56
IF (JLOC,GT,JWDI,AND,JLOC,LT,JWDD) GO TO 56
FAC=(X(M(IR))-XF)/(X(M(IR))-X(IR)))**.14286
UST=0.

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VST=WST*FAC SP 237
WST=WST*FAC SP 238
IF (INDX,NE,2) GO TO 56 SP 239
UF=UST SP 240
VF=VST SP 241
WF=WST SP 242
56 JR=JWL((ILOC,4) SP 243
IF (YF,LE,Y(JR+1)) GO TO 53 SP 244
IF (IKIN(ILOC,KLOC),EQ,1,JR,IKIN(ILOC,KLOC),EQ,3) GO TO 53 SP 245
FAC=((YF-YM(JB))/(Y(JR+1)-YM(JB)))**.14286 SP 246
UST=UST*FAC SP 247
VST=0. SP 248
WST=WST*FAC SP 249
IF (INDX,NE,3) GO TO 53 SP 250
UF=UST SP 251
VF=VST SP 252
WF=WST SP 253
SP 254
53 JR=JWL((ILOC,4) SP 255
IF (YF,LE,Y(JR-1)) GO TO 54 SP 256
IF (IKIN(ILOC,KLOC),EQ,2,01,IKIN(ILOC,JLOC),EQ,3) GO TO 54 SP 257
FAC=((YM(JB-1)-YF)/(YM(JB-1)-Y(JR-1)))**.14286 SP 258
UST=UST*FAC SP 259
VST=0. SP 260
WST=WST*FAC SP 261
IF (INDX,NE,4) GO TO 54 SP 262
UF=UST SP 263
VF=VST SP 264
WF=WST SP 265
54 CONTINUE SP 266
IF (ABS(UF).LT.1.E-30,AND,ABS(VF).LT.1.E-30,AND,ABS(UST).LT.1.E-30, AND,ABS(WST).LT.1.E-30, AND,ABS(FEVAP).LT.1.E-30, AND,ABS(TF).LT.1.E-30, AND,ABS(POT).LT.1.E-30) GO TO 50 SP 267
1 AND,ANS(VST),LT,1,E-30) GO TO 50 SP 268
FLPOX=RATIO1+F(LPFU)+RATIO3+F(LPCD)+RATIO2-(RATIO2+RATIO1)* SP 269
1 F(LPFUN)+RATIO5+F(LPCH)+RATIO36+F(LPH2) 4STEP SP 270
FLPOX=AMAX1(FLPOX,0.) SP 271
IF (ISTEP,NF,IGPNT) GO TO 7744 SP 272
WRITE (6,7745) UF,VF,WF,UST,VST,WST,FEVAP,KF,YF,ZF SP 273
7745 FORMAT (10E12.4) SP 274
7744 CONTINUE SP 275
C ----BOILING TEMPERATURE OF FUEL----- SP 276
POT=P0(4) SP 277
ET=EE(4) SP 278
IF(FEVAP,GE,0.9) GO TO 200 SP 279
POT=TAR(FEVAP,FRACT,P0,4) SP 280
ET=TAR(FEVAP,FRACT,EE,4) SP 281
200 TR=ET+ALCG(PRESS)+POT SP 282
T1=(TR+TF)/2. SP 283
TFU=AMIN1(TFU,TB) SP 284
C----DENSITY OF LIQUID FUEL AT TB SP 285
RDF=1.076/(1.+1.076/.773-1.1*(1.-.67*FEVAP)) SP 286
RDF=1000.+(RDF+.208-.00072*TFU) SP 287
C----MOLECULAR WEIGHT OF FUEL VAPORS SP 288
MWT=TAR(FEVAP,FRACT,MW,7) SP 289
AT=TAR(MWT,MCOND,ACOND,4) SP 290
300 RT=TAR(PWT,MCOND,RCOND,4) SP 291
C----THERMAL CONDUCTIVITY AND SPECIFIC HEAT OF FUEL VAPORS SP 292
COND1=1.729*(AT+RT+T1) NOX 193
THCP5=1 NOX 194
NS1=TFNU NOX 195
NS2=TFNU NOX 196
TK=T1 NOX 197
TKINV=1.000/TK NOX 198
S2(TDFU)=1.000/SMW(TDFU) NOX 199
CALL HCPS NOX 200
CP1=CPSUM*UNICON NOX 201
CP1=CP1*1.000 NOX 202

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400 CONDI=0.4*COND1+0.6*0.064*SQRT(T1/1111.)
C ----RELATIVE VEL, REYNOLDS NO., DRAG COEF AND FORCE COMPONENTS
  VR=SQRT((UF-UST)**2+(VF-VST)**2+(WF-WST)**2)
  VISCO=4.464E-5*SORT(TST/1111.)
  REI=RNST*VR*ODIA/VISCO
  SREI=SORT(REI)
  COS=2.0
  IF (REI.GT.22.16.AND.REI.LE.80.) COS=27./REI**0.04
  IF (REI.GT.80..AND.REI.LT.10000.) COS=.271*REI**0.217
  CO1=AMAX1(COS/2.,COS/(1.+BEE))
  CONS=CO1*3.14159/4.*DIA**2/2.*RNST
  DM=PI*DIA**3*ROF/6.
  FX=CONS*VR*(UST-UF)
  FY=CONS*VR*(VST-VF)+PLAXM1*DM*WF*WF/R(JLOC)
  FZ=CONS*VR*(WST-WF)-PLAXM1*DM*VF*WF/R(JLOC)
  VFU=SORT(UF**2+VF**2+WF**2)
  FAC=AMAX1(1.0,25./((VR*VR)+1.E-20))
  DTI1=ULIM*VFU*DM+FAC/(ABS(FX)+1.E-30)
  DTI2=ULIM*VFU*DM+FAC/(ABS(FY)+1.E-30)
  DTI3=ULIM*VFU*DM+FAC/(ABS(FZ)+1.E-30)
  DTI4=DLIM/(CON2+1.E-30)
  DTI5=KS1(JLOC)/IARS(UF)+1.E-20
  DTI6=YS(JLOC)/IARS(VF)+1.E-20
  DTI7=R(JLOC)*PSIKLLOC/(ABS(WF)+1.E-20)
  DTI=AMIN1(DTI1,DTI2,DTI3,DTI4,DTI5,DTI6,DTI7)
  CONS=DM/DTI
C-----VELOCITY AND LOCATION OF THE DROPLET
  UF0=UF
  VF0=VF
  WF0=WF
  UF=UF+FX/CONS
  VF=VF+FY/CONS
  WF=WF+FZ/CONS
  IF (UF0.GT.UST) UF=AMAX1(UF,UST-.001)
  IF (UF0.LT.UST) UF=AMIN1(UF,UST+.001)
  IF (VF0.GT.VST) VF=AMAX1(VF,VST-.001)
  IF (VF0.LT.VST) VF=AMIN1(VF,VST+.001)
  IF (WF0.GT.WST) WF=AMAX1(WF,WST-.001)
  IF (WF0.LT.WST) WF=AMIN1(WF,WST+.001)
  DX=.5*(UF+UF0)*DTI
  DY=.5*(VF+VF0)*DTI
  DZ=.5*(WF+WF0)*DTI
  XF=XF+DX
  YF=YF+DY
  ZF=DZ/R(JLOC)
  IF (TFU.GE.TB) ITYPE=2
  GO TO (10P,199), ITYPE
C----- HEATING DROPLET -----
C ----HEAT TRANSFER
  100 HT=COND1*(2.+6*PR3*SREI)/DIA
  AS=PI*DIA*DIA
  QDOT=AS*HT*(TST-TFU)
  CPLF=840.5+4.1372*TFU
  DTF=DTI*QDOT/DM/CPLF
  TFU=TFU+DTF
  GO TO 11C
C ----- BOILING DROPLET -----
C ----MASS TRANSFER NUMBER
  100 TF (FLPFUC1)=FSTOIC) 210,209,201 .
  201 RFE=AMAX1(CP1*(TST-TB)/MEVAP,0.)
  GO TO 219
  205 RFE=FLPNX/RATIO1
  GO TO 219
  210 RFE=(FLPNX*HFUEL/RATIO1+AMAX1(CP1*(TST-TB),0.))/MEVAP

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215 RATE=0./RDF*COND1/CP1+ALOG(1.+BEE)*(1.+0.276*SREI*SCRI) SP 356
C-----FRACTION EVAPORATED SP 357
  CON2=1.9/RDF/DIA00030*RDF/DIA*RATE SP 358
  DFVAP=CON2*DTI SP 359
240 FEVAP=FEVAP+DEVAP SP 360
  IF (FFVAP.LT.1.0) GO TO 250 SP 361
  DEVAP=DEVAP-FEVAP+1. SP 362
  FEVAP=1. SP 363
C ----NEW DROPLET DIAMETER SP 364
250 ARG=DIA*DIA-RATE*DTI SP 365
  IF (ARG.GT.0.0) GO TO 262 SP 366
  DEVAP=DEVAP+1.-FEVAP SP 367
  FEVAP=1.0 SP 368
  GO TO 292 SP 369
262 DIA=SORT(ARG) SP 370
C ----- FUEL EVAPORATION FLOW RATE SP 371
272 AMT=DEVAP*WFI/RNG SP 372
  LPC=ILPC-1+(JLOC-2)*(NI-2)+(KLOC-2)*(NI-2)+(NJ-2) SP 373
  EVAP(LPC)=EVAP(LPC)+AMT SP 374
  EVAPU(LPC)=EVAPU(LPC)+AMT*UF SP 375
  EVAPV(LPC)=EVAPV(LPC)+AMT*VF SP 376
  EVAPH(LPC)=EVAPH(LPC)+AMT*UF SP 377
  900 IF (FEVAP.LT.0.99) GO TO 110 SP 378
1000 CONTINUE SP 379
2900 CONTINUE SP 380
C ***** STORE MOMENTUM DATA ON TAPE4 SP 381
C ----- STORE MOMENTUM DATA ON TAPE4 SP 382
  RFWIND NTP4 SP 383
  00 1100 K=2,N SP 384
  00 1110 J=2,M SP 385
  KJC=(K-2)*(NI-2)*(NJ-2)+(J-2)*(NI-2) SP 386
  00 1110 I=3,L SP 387
  LIJ=(J-2)*(NI-2)+(I-1) SP 388
  LPC=KJC+(I-1) SP 389
  LYNC=LPC-1 SP 390
  EVSU(LIJ)=FXN(I-1)*EVAPU(LYNC)+SXP(I)*EVAPU(LPC) SP 391
  IF (I.EQ.3) EVSU(LIJ)=EVSU(LIJ)+FYP(2)*EVAPU(LYNC) SP 392
  IF (I.EQ.1) EVSU(LIJ)=EVSU(LIJ)+FXN(L)*EVAPU(LPC) SP 393
1110 CONTINUE SP 394
  WRITE (NTP4) EVSU SP 395
1100 CONTINUE SP 396
  00 1200 K=2,N SP 397
  00 1210 J=3,M SP 398
  KJC=(K-2)*(NI-2)*(NJ-2)+(J-2)*(NI-2) SP 399
  00 1210 I=2,L SP 400
  LIJ=(J-2)*(NI-2)+(I-1) SP 401
  LPC=KJC+(I-1) SP 402
  LYNC=LPC-(NI-2) SP 403
  EVSU(LIJ)=FYN(J-1)*EVAPV(LYNC)+FYP(J)*EVAPV(LPC) SP 404
  IF (J.EQ.3) EVSU(LIJ)=EVSU(LIJ)+FYP(2)*EVAPV(LYNC) SP 405
  IF (J.EQ.1) EVSU(LIJ)=EVSU(LIJ)+FYH(N)*EVAPV(LPC) SP 406
1210 CONTINUE SP 407
  WRITE (NTP4) EVSU SP 408
1200 CONTINUE SP 409
  00 1300 K=3,NP1 SP 410
  00 1310 J=2,M SP 411
  KJC=(K-2)*(NI-2)*(NJ-2)+(J-2)*(NI-2) SP 412
  00 1310 I=2,L SP 413
  LIJ=(J-2)*(NI-2)+(I-1) SP 414
  LPC=KJC+(I-1) SP 415
  LYNC=LPC-(NI-2)*(NJ-2) SP 416
  EVSU(LIJ)=F2N(K-1)*EVAPH(LYNC) SP 417
  IF (K.EQ.NP1) GO TO 1309 SP 418
  EVSU(LIJ)=EVSU(LIJ)+F2P(K)*EVAPH(LPC) SP 419

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GO TO 1310
1300 FVSU(LIJ)=EVSU(LIJ)+FZP(2)*EVAPM(LIJ)
1310 CONTINUE
WRITE (NTP4) EVSU
1300 CONTINUE
RETURN
END
FUNCTION TAB (X,XX,YY,NTAB)
DIMENSION XX(11),YY(11)
IF (NTAB.GT.0) GO TO 5
TAB=0.0
RETURN
5 F=1.
IF (XX(1).GT.XX(2)) F=-F
DO 10 J=1,NTAB
I=J
IF (F*(XX(I)-X)<0.40) 10,40,20
10 CONTINUE
20 IF (I.NE.1) GO TO 30
I=2
30 J=I-1
DEL=XX(I)-XX(J)
IF (DEL.FO.0.0) GO TO 50
TAB=(YY(I)*(X-XX(J))-YY(J)*(X-XX(I)))/DEL
RETURN
40 TAB=YY(I)
RETURN
50 WRITE (6,60) X,I,J
60 FORMAT (* 000 ERROR IN SUBROUTINE TAB ***,E15.4,2I5)
STOP
END
SUBROUTINE STRIDE
COMMON/CEDK/EOK(192)
COMMON F(3500),DU(500),DV(500),DW(500),
1 AMUC(500),SOOT1(500),SOOT2(500),FCH(500),FH2(500),FS(500,14),
1 RHO(500),VIS(500),ABSR(500),SCTR(500),SU(100),SP(100),
1 DRHOPP(500),
1 AXP(100),AYM(100),AYP(100),AZP(100),
2 AZM(100),CY(100),C7U(100),CYU(100),
3 CZP(100),CYP(100),DIVG(100),NTP1,NTP2
1,AYMK(192),AXPK(192),AYMK(192),AYPK(192),AZMK(192),AZPK(192),
2 SUK(192),SPK(192)
DIMENSION U(500),V(500),W(500),PP(500),P(500),TEMP(500)
DIMENSION GAM(500)
EQUIVALENCE (F(1),U(1)),(F(501),V(1)),(F(1001),W(1))
EQUIVALENCE (F(1901),PP(1)),(F(2001),P(1)),(F(2501),TEMP(1))
EQUIVALENCE (F(3001),GAM(1))
COMMON/CYL/R(30),RM(30),RMRV(30),YSR(30),YSVR(30),IPLAK
COMMON/GRID/X(40),Y(30),Z(30),XS(40),YS(30),ZS(30),XSU(40),
1 YSV(30),ZSW(30),X0IF(40),Y0IF(30),Z0IF(30),FXP(40),FXH(40),
2 FYP(30),FYH(30),F7P(30),FZH(30),DT,TIME
COMMON
1/CINDEX/I0CC,I0FU,I0D2,I0N2,I0H2D,I0C02,I0H1,I0H2,I0N1,I0N0,I0N02
1,I0D,I0H,I0CPS,I0L,I0H,I0AT,I0T,J0J,N1,M2,N3,NA,NGL0B,NGL0BP,
2 NLH,NQ,NSP,NS1,NS2,I0CH
3/CCHFT/CPSUM,H$UM,FQ,PPLN,RGAS,RGASIN,SHINV,TKINV,TLN,LHRG
4/CPARAM/ASUR(30,3),ENV,EP,HSUB0,MDERUG,NS,PA=00,01,02,03,04,RHOPP,
4 SM,SMH(30),SM0,S1(30),S2(30),TK,LADEAR,LDERUG,LFACT,
4 LENE*,FDKIJ,LCORVG
      DECIMAL PRECISION CPSUM,ENV,EP,FQ,HSUB0,HSUM,PA,PPLN,00,01,02,03,
1 04,RGAS,RGASIN,RHOPP,SM,SHINV,SMH,S1,S2,TK,TKINV,TLN,SM0
2,FUT,FST
COMMON/STFP4/PEXP1,PEXP2,PEXP3,PEXP4,ER1,ER2,ER3,ER4,CERU1,CERU2,
1 CERU3,CERU4,AEXP1,AEXP2,AEXP3,AEXP4,BEXP1,BEXP2,BEXP3,BEXP4

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RAD	3
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COMFR	9
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COMFR	11
COMMON	2
COMMON	3
COMMON	4
COMMON	5
NOX	2
NOX	3
NOX	4
4STEP	3
NOX	6
NOX	7
NOX	8
NOX	9
NOX	10
NOX	11
4STEP	4
4STEP	5
4STEP	6

2	CEXP1,CEXP2,CEXP3,CEXP4,FUT,FST	4STEP	7
	LOGICAL LADTAB,LCONVG,LDEBUG,L_EQUIL,LWRG,LREACT,LENER	NOX	12
	COMMON/INT/L,M,N,LCV,NCV,NP1,NP1,NI,NJ,NK,NINJ,NINJNK,NV,	COMMON	6
1	NNV,NGDTN,K,ISTR,JSTR,KSTR,NVM(39),NM(39),JM(39),ISTFP,	4STEP	8
2	ISOLVE(32),IPRINT(33),TITLE(10,33),IXY,ISWP,JSWP,RELAX(33),NP,	4STEP	9
3	NRHO,NGAM,INLI(30,5),INLO(30,5),JNL(40,5),JNL(40,5),IWEI,	COMMON	9
4	INED,MM1,JNT1,JNTQ,JM01,JM00,TDN,JKIN(30,30),IKIN(40,30)	COMMON	10
	COMMON/INDEX/IPAR,LPREF,ISTUN,INCIMP,ITRAD,NVRX,NVRT,NVRZ,JPLANE	COMMON	11
1	PLAM1,LVK,LVD,LVFUO,X,LVFU,LVCO,LVH,LVRX,LVRY,LVRZ,NVF(32),	4STEP	10
2	TJUMP,IRES,TITLE2(20),IMAX,JMAX,KMAX,NVCO,FUNC0,NVH20,NVC02,	COMMON	13
3	NVN2,NVCH,NVN2	4STEP	11
	COMMON/CNOX/LVH1,LVH2,LVN1,LVN02,LVO,LVOH,LVH20,LVN2,LVO2,	NOX	16
1	LVC02,LVFU1,LVC01,MNOX,INOX,ITNOX,SNOK,TNOX	NOX	17
	COMMON/THERM/NVN,NVFU,NVOK,NVFUOK,NVTE,MODEM,1DK,FSTOIC,HFU,CP,	COMMON	19
1	GASCON,RHOCON,UNICON,PRESS,NVFAV,TCYLW,TINLW,TLIP,ACOEFC(4),	COMMON	16
2	T4,DFAC,WFU,WCO,WCO,WCO,WH20,NVN2,NVY,CXX,RAT101,RATIO2,	COMMON	17
3	RATIO3,RATIC4,HCO,TAN,ITWALL	COMMON	18
	COMMON/CTDMA/KEND,ICTDMA(32)	4STEP	12
	COMMON/MIS/AMU,DEM,SMAK,SSUM,LASTEP,HTCEXT,CFR,EMISH,EMISIM,	CONGEN	2
1	EMISP,TPUT,RTCD,EMI,RADTH,RADSUR,FMA,FK,SQFK,	CONGEN	3
2	FKFU,FDFU,TFUEL,WFNZ,FL(40),TENTH(40),H(40),FUEL(40),FUO(40)	CONGEN	4
2	UTN(40),TIN(40),FUELS(40),SEKIT,IGAM1(29),IGAM2(29)	4STEP	13
	COMMON/TURB/NVK,NVD,C1,C2,CD,AK,OUIDXJ(3,3),AKFAC,ALFAC,	CONGEN	6
1	MODEL,PR(32),PREF(32),PJAY(32),E	4STEP	14
	COMMON/RAD/NVE,SIGMA,ABSOR,SCATR	CONGEN	8
	COMMON/REACT/ARCON1,PREXP1,CR1,ARCON2,PREXP2,CR2,MODER	CONGEN	9
	COMMON/DRDPL/EVAP(192),NTP4,NFMZ,KD(3),YD(3),ZD(3),ALFA(3),	CONGEN	10
1	BETA(3),DELTA(3),THETA1(3),THETA2(3),MSL(3),WFF(3),SND(3),	CONGEN	11
2	VFUEL(3),RFUEL(3),EVSU(64),HEVAP	CONGEN	12
	COMMON/INJEC/FLOWIN,INJIN(20),JINJ(20),UTINJ(20),WIINJ(20),	CONGEN	13
1	AUTNJ(20),THINJ(20),IVINJ(20),JVINJ(20),KVINJ(20),VINJ(20),	CONGEN	14
2	EVINJ(20),DVINJ(20),AVINJ(20),TVINJ(20),NUINJ,NVINJ,JSW1,JSW2,	CONGEN	15
3	USh,VSh,AFSh,FSW,TSW,WSW,SWH,RHSH	CONGEN	16
	COMMON/CSOC/AVN,NVS1,NVS2,ISOOT,SSOOT,NSOOT,AQ,ARCONN,AAA,BBS,FMG	SOOT	8
1	GO,MPART,DPART(2),FRACP(2),RHOP,ARCONS,PREXP5,ALPHA,AAS,BBS,DHR	SOOT	9
2	LVN,LVS1,LVS2,CTINCP,TINCP,FUTOT	SOOT	10
	COMMON/CRAD/IPAD,SRAD	SOOT	11
	COMMON/CFOUR/PREXP3,ARCON3,CR3,PREXP4,ARCON4,CR4,AA1,BB1,CC1,	4STEP	15
1	AA2,BB2,CC2,AA3,BB3,CC3,AA4,BB4,CC4,RATIO5,RATIO6,RATIC7,	4STEP	16
2	RATIO8,RATIC9,RAT010,RAT011,RAT012,WCh,WH2,WC2H4,LVCh,LVCh1,LVH21	4STEP	17
	ENTRY STRIO	ST	5
C----	ENTRY STRIO IS USED FOR PRELIMINARY CALCULATIONS.	COMMENT	121
C		COMMENT	122
	IXY=1	ST	6
	ISWP=1	ST	7
	JSWP=1	ST	8
	TINF=0,	ST	9
	L=LP1-1	ST	10
	M=NP1-1	S:	11
	M=NP1-1	ST	12
	LCV=L-1	ST	13
	NCV=M-1	ST	14
	NCV=M-1	ST	15
	NN1=M-1	ST	16
	NNJ=NINJ	ST	17
	NINJNK=NINJNK	ST	18
	NVM(1)=0	ST	19
1	DO 1 NV=2,NGAM	ST	20
	NVM(NV)=NVM(NV-1)+NINJNK	ST	21
	KM(1)=0	ST	22
2	DO 2 K=2,NP1	ST	23
	KM(K)=KM(K-1)+NINJ	ST	24
	JM(J)=0	ST	25
	MAX=MAX0(NP1,LP1)	ST	26

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3	DO 3 J=2,MAX	ST	27
	JM(J)=JM(J-1)+NI	ST	28
	RETURN	ST	29
C	00 *	ST	30
	ENTRY STRID1	ST	31
C	*****ENTRY STRID1 IS USED TO CALCULATE INTER-MODAL DISTANCES.	COMMENT	123
C	CONTROL VOLUME AREAS AND VOLUMES.	COMMENT	124
C	*****X=GRID0.	COMMENT	125
	DO 101 I=2,LP1	COMMENT	126
101	XDIF(I)=X(I)-X(I-1)	ST	32
	DO 111 I=2,L	ST	33
111	XS(I)=0.5*(X(I+1)-X(I-1))	ST	34
	XS(2)=XS(2)+0.5*XDIF(2)	ST	35
	XS(L)=XS(L)+0.5*XDIF(LP1)	ST	36
	DO 121 I=3,L	ST	37
	XSU(I)=XDIF(I)	ST	38
	FXP(I)=XDIF(I)/(2.*XS(I))	ST	39
121	FXM(I)=1.0-FXP(I)	ST	40
	XSU(3)=XSU(3)+XDIF(2)	ST	41
	XSU(L)=XSU(L)+XDIF(LP1)	ST	42
	FXP(2)=FXP(3)	ST	43
	FXM(2)=1.0-FXP(2)	ST	44
	FXP(L)=FXP(L-1)	ST	45
	FXM(L)=1.0-FXP(L)	ST	46
C	*****Y=GRID0.	COMMENT	127
	DO 102 J=2,MP1	ST	47
102	YDIF(J)= Y(J)- Y(J-1)	ST	48
	DO 112 J=2,M	ST	49
112	YS(J)= 0.5*(Y(J+1)-Y(J-1))	ST	50
	YS(2)=YS(2)+0.5*YDIF(2)	ST	51
	YS(M)=YS(M)+0.5*YDIF(MP1)	ST	52
	RM(2)=R(1)	ST	53
	DO 122 J=3,M	ST	54
	RM(J)=.5*(R(J)+R(J-1))	ST	55
	RMV(J+1)=R(J)	ST	56
	YSV(J)=YDIF(J)	ST	57
	FYP(J)=YDIF(J)/(2.*YS(J))	ST	58
122	FYM(J)=1.0-FYP(J)	ST	59
	RM(MP1)=R(MP1)	ST	60
	RMV(3)=R(1)	ST	61
	RMV(MP1)=R(MP1)	ST	62
	YSV(3)=YSV(3)+YDIF(2)	ST	63
	YSV(M)=YSV(M)+YDIF(MP1)	ST	64
	FYP(2)=FYP(3)	ST	65
	FYM(2)=1.0-FYP(2)	ST	66
	FYP(M)=FYP(M-1)	ST	67
	FYM(M)=1.0-FYP(M)	ST	68
	DO 132 J=2,P	ST	69
132	YSR(J)=.5*(RM(J+1)+RM(J))+YS(J)	ST	70
	DO 142 J=3,P	ST	71
142	YSVR(J)=.5*(RMV(J+1)+RMV(J))+YSV(J)	ST	72
C	*****Z=GRID0.	COMMENT	128
	DO 103 K=2,MP1	ST	73
103	ZDIF(K)=Z(K)-Z(K-1)	ST	74
	DO 113 K=2,N	ST	75
113	ZS(K)=0.5*(Z(K+1)-Z(K-1))	ST	76
	ZS(2)=ZS(2)+0.5*ZDIF(2)	ST	77
	ZS(MP1)=ZS(2)	ST	78
	ZSV(K)=ZDIF(K)	ST	79
	FZP(K)=ZDIF(K)/(2.*ZS(K))	ST	80
123	FZM(K)=1.0-FZP(K)	ST	81
		ST	82
		ST	83
		ST	84

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7SW(NP1)=2DIF(2)+2DIF(NP1)
7FP(NP1)=2DIF(2)/ZS(NP1)
7FM(NP1)=1,-FZP(NP1)
7T(2)=2DIF(2)/ZS(2)
7TM(2)=1,-F2P(2)
C-----BOUNDARY CONDITION INDICES.
ON 290 I=1,LP1
1P=M1NO(I+1,LP1)
1L=MAXO(I-1,1)
JWL(I,I,1)=MIN(JWL(I,I,4),JWL(I,IL,4))
JWL(I,I,2)=JWL(I,I,4)+1
JWL(I,I,3)=JWL(I,I,4)
JWL(I,I,5)=MINC(JWL(I,P,4),JWL(I,I,4),JWL(I,IL,4))
JWL(I,I,1)=M1NO(JWL(I,I,4),JWL(I,IL,4))
JWL(I,I,2)=JWL(I,I,4)
JWL(I,I,3)=JWL(I,I,4)
JWL(I,I,5)=MAXC(JWL(I,P,4),JWL(I,I,4),JWL(I,IL,4))
290 CONTINUE
ON 292 J=1,NP1
JP=M1NO(J+1,NP1)
JL=MAXO(J-1,1)
IWL(I,J,1)=IWL(I,J,4)+1
IWL(I,J,2)=MAXC(IWL(I,J,4),IWL(JL,4))
IWL(I,J,3)=IWL(I,J,4)
IWL(I,J,5)=MINC(IWL(I,JP,4),IWL(I,J,4),IWL(I,JL,4))-1
IWL(I,J,1)=IWL(I,J,4)
IWL(I,J,2)=MINC(IWL(I,J,4),IWL(JL,4))
IWL(I,J,3)=IWL(I,J,4)
IWL(I,J,5)=MAXC(IWL(I,JP,4),IWL(I,J,4),IWL(I,JL,4))+1
292 CONTINUE
RETURN
C ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** * ST
C ENTRY STRID2
C-----ENTRY STRID2 IS USED TO CALCULATE THE FINITE-DIFFERENCE
C COEFFICIENTS AXP, AKN, AVP, AYH, AZP, AND AZR.
C
C +---+---+---+---+---+---+---+---+ U-VELOCITY +---+---+---+---+---+---+---+
ON 360 LP=1,NINJNH
360 DU(LP)=0.0
TF(ISOLVE(1)) 303,302,303
303 TF(MODITSTEP,ISOLVE(1)) 302,304,302
304 CONTINUE
1STA=3
2STA=2
3STA=2
NV=1
NGATO=1
C-----OBTAIN DIFFUSION COEFFICIENTS.
CALL GAMMA
ON 30 J=2,M
TS=IWL(I,J,NGATO)
TF=IWLO(J,NGATO)
T2FAC=R(E(J))/R(H)+DFAC*(R(J)-R(H))/)
ON 30 I=TS,TF
1P=JN(E(J))+1
L7P=1 P+NINJ
LP11=LP-1
L7P1=L7P-1
ARFA=RSU(I,J)*VS(J)
AL7=RHO(I,LP1)*W(L7P)*AREA
AL71=RHO(I,LP11)*W(L7P1)*AREA
AL72=RHO(E(J)+AL21)
AL7=AL7/2.
T7=.5*(GAM(LP)+GAM(LP11))*AREA*T2FAC/(ZSW(NP1)*R(J))

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T7=AMAX1(T2,ARS(ALZ))
C7U(LP)=Z,0ALZ
30 C7(LP)=T7+AL7
DO 301 K=2,M
C-----OBTAIN SOURCE TERMS AND EVAPORATION RATES.
CALL SOURCE
CALL SCMAS
DO 31 I=3,L
JS=JWL(I),NGOT01+1
ARS=XSU(I)*ZS(K)*RM(JS)
LP=KMH(K)+JM(JS)+I
LYM=LP-M
LXM1=LXM-1
LXM=LP-1
IF (JWL(I)=4,FO,JS-1) GO TO 150
ALY=.5*(RHO(LP)+RHO(LYM))*V(LP)*AREA
TY=.5*(GAM(LP)+GAM(LYM))*AREA/YDIF(JS)
GO TO 192
150 ALY=RHO(LYM)*V(LP)*AREA
DIST=.5*YDIF(JS)
IF (JS,EO,2) DIST=YDIF(2)
TY=GAM(LYM)*AREA/DIST
152 IF (JWL(I)=3,4),FO,JS-1) GO TO 154
ALY1=.5*(RHO(LXM)+RHO(LXM1))*V(LXM)*AREA
TY1=.5*(GAM(LXM)+GAM(LXM1))*AREA/YDIF(JS)
GO TO 156
154 ALY1=RHO(LXM1)*V(LXM)*AREA
DIST=.5*YDIF(JS)
IF (JS,EO,2) DIST=YDIF(JS)
TY1=GAM(LXM1)*AREA/DIST
156 ALY=.5*(ALY+ALY1)
TY=.5*(TY+TY1)
TY=AMAX1(TY,-ALY)
CYU(I)=ALY
31 CY(I)=TY+ALY
DO 32 J=2,M
KJM=KM(K)+JPC(J)
AREA=VSP(J)*ZS(K)
IS=IWLI(J,NGOT01)
IE=IWLC(J,NGCT01)
I=IS-1
LXP=KJM+IS
LP=LP-1
LXM=LP-1
200 ALXM=RHO(LXM)*U(LP)*AREA
ALXP=0.
TX=GAM(LXM)*AREA/XS(I)
CXIJ=ALXM
202 TX=AMAX1(TX,ALXP)
TX=AMAX1(TX,-ALXM)
CX=TX+ALXM
TZFAC=R(J)/(R(M)+DFAC*(R(J)-R(M)))
DO 32 I=IS,IE
MAX=JWL(I),NGOT01-1
LTJ=JPC(J)+I
LP=KJM+I
LYP=LP+1
LYP=LP+M
L7P=LP+MINJ
LP11=LP-1
LYP1=LYP-1
L7P1=L7P-1
AXM(LIJ)=CX
AYM(LIJ)=CY(I)
ST 144
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ST COMMENT 134
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ALM(LIJ)=CZ(LIJ)	ST	207
AREA=YSR(J)*ZS(K)	ST	208
IF (I.EQ.J) GO TO 33	ST	209
ALX=RHO(LP)*AREA*(FRP(I)*U(LXP)+FXM(I)*U(LP))	ST	210
ALXP=FP*(I)*ALX	ST	211
ALXM=FM*(I)*ALX	ST	212
TX=GAM(LP)*AREA/XS(I)	ST	213
CXUP=ALX	ST	214
GO TO 34	ST	215
33 ALXP=RHO(LP)*U(LXP)*AREA	ST	216
ALXM=0.	ST	217
TY=GAM(LP)*AREA/XS(L)	ST	218
CXUP=ALXP	ST	219
34 TX=AMAX1(TX,ALXP)	ST	220
TX=AMAX1(TX,-ALXM)	ST	221
ALXP(IJ)=TX-ALXP	ST	222
CX=CXUP	ST	223
DIVG(LIJ)=DIVG(LIJ)+CXUP-CXU	ST	224
CXU=CXUP	ST	225
AREA=7S(K)*XSU(I)*RM(J+1)	ST	226
IF (J.EQ.MAX) GO TO 33	ST	227
ALY=.25*(RHC(LP)+RHO(LYP))*V(LYP)*AREA	ST	228
ALY1=.25*(RHO(LP11)+RHO(LYP1))*V(LYP1)*AREA	ST	229
ALY=.5*(ALY+ALY1)	ST	230
TY=.25*(GAM(LP)+GAM(LYP)+GAM(LP11)+GAM(LYP1))*AREA/YDIF(J+1)	ST	231
TY=AMAX1(TY,ABS(ALY))	ST	232
CYUP=2.*ALY	ST	233
GO TO 36	ST	234
35 IF (JWLO(I,4).EQ.MAX+1) GO TO 157	ST	235
ALY=.5*(RHO(LP)+RHO(LYP))*V(LYP)*AREA	ST	236
TY=.5*(GAM(LP)+GAM(LYP))*AREA/YDIF(MAX+1)	ST	237
GO TO 158	ST	238
157 ALY=RHC(LYP)*V(LYP)*AREA	ST	239
DIST=.5*YDIF(MAX+1)	ST	240
IF (MAX.EQ.M) DIST=YDIF(MP1)	ST	241
TY=GAM(LYP)*AREA/DIST	ST	242
158 IF (JWLO(I-1,4).EQ.MAX+1) GO TO 159	ST	243
ALY1=.5*(RHO(LP11)+RHO(LYP1))*V(LYP1)*AREA	ST	244
TY=.5*(GAM(LP11)+GAM(LYP1))*AREA/YDIF(MAX+1)	ST	245
GO TO 160	ST	246
159 ALY1=RHO(LYP1)*V(LYP1)*AREA	ST	247
DIST=.5*YDIF(MAX+1)	ST	248
IF (MAX.EQ.M) DIST=YDIF(MP1)	ST	249
TY1=GAM(LYP1)*AREA/DIST	ST	250
160 ALY=.5*(ALY+ALY1)	ST	251
TY=.5*(TY+TY1)	ST	252
TY=AMAX1(TY,ALY)	ST	253
CYUP=ALY	ST	254
36 AYP(IJ)=TY-ALY	ST	255
CY(I)=TY+ALY	ST	256
DIVG(LIJ)=DIVG(LIJ)+CYUP-CYU(I)	ST	257
CYU(I)=CYUP	ST	258
AREA=XSU(I)*YS(J)	ST	259
TF(K,F0,M) GO TO 37	ST	260
ALZ=.25*(RHC(LP)+RHO(LZP))*W(LZP)*AREA	ST	261
ALZ1=.25*(RHO(LP11)+RHO(LZP1))*W(LZP1)*AREA	ST	262
ALZ=.5*(ALZ+ALZ1)	ST	263
GAMLP=.25*(GAM(LP)+GAM(LZP)+GAM(LP11)+GAM(LZP1))	ST	264
TZ=GAMLP*AREA*ZFAC/(ZDIF(K+1)*R(J))	ST	265
TZ=AMAX1(TZ,ARS(ALZ))	ST	266
CZUP=2.*ALZ	ST	267
GO TO 38	ST	268
37 ALZ=RHC(LZP)*W(LZP)*AREA	ST	269
ALZ1=RHO(LZP1)*W(LZP1)*AREA	ST	270

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AL2=.5*(AL2+AL7)	ST	271
AL7=AL7/2.	ST	272
TZ=.5*(GAM(LZP)+GAM(LZP1))*AREA*TZFAC/(ZSW(NP1)*R(J))	ST	273
TZ=AMAX1(TZ,ABS(AL7))	ST	274
CZUP=2.*AL2	ST	275
38 A7P(LIJ)=TZ-AL7	ST	276
CZILIJ=TZ+AL2	ST	277
DIVG(LIJ)=DIVG(LIJ)+CZUP-CZULIJ	ST	278
CZULIJ=CZUP	ST	279
VOL=KSU(I)*VSU(J)*ZS(K)	ST	280
IF (I.EQ.IWL1(J,NGOTO),AND,I.GT.3) VOL=VOL*(1.+.5*XSU(I-1)/KSU(I))	ST	281
IF (I.EQ.IWL0(J,NGOTO),AND,I.LT.1) VOL=VOL*(1.+.5*XSU(I+1)/KSU(I))	ST	282
LXM=LPM-1	ST	283
39 RDT=0.	ST	284
392 DIVG(LIJ)=AMAX1(RDT,DIVG(LIJ))	ST	285
DU(LP)=VOL/VDF(I)	ST	286
SU(LIJ)=SU(LIJ)*VOL+DU(LP)*(PLKRI-PLP1)+DIVG(LIJ)*U(LP)	ST	287
SP(LIJ)=SP(LIJ)*VOL-DIVG(LIJ)	ST	288
92 CONTINUE	ST	289
C----SOURCE TERM MODIFICATIONS - BOUNDARY CONDITIONS.	COMMENT	135
CALL SCMOD	ST	290
C----SOLVE FINITE-DIFFERENCE EQUATIONS IN SOLVE1 AND SOLVE2.	COMMENT	136
CALL SOLVF1	ST	291
301 CONTINUE	ST	292
CALL SOLVE2	ST	293
CALL FROD	ST	294
302 CONTINUE	ST	295
440 LP=1,NINJNK	ST	296
460 DV(LP)=0.0	ST	297
TF(ISCLVE(2)) 403,402,403	ST	298
403 TF(MOD(ISTEP,ISOLVE(2))) 402,404,402	ST	299
404 CONTINUE	ST	300
ISTR=2	ST	301
JSTR=3	ST	302
KSTR=2	ST	303
NV=2	ST	304
NGOTO=2	ST	305
C----OBTAIN DIFFUSION COEFFICIENTS.	COMMENT	137
CALL GAMMA	ST	307
DO 40 J=3,N	ST	308
IS=IWLI(J,NGOTO)	ST	309
IF=IWLO(J,NGOTO)	ST	310
TZFAC=RN(J)/(RR(N)+DFAC*(RN(J)-RN(N)))	ST	311
DO 40 I=IS,IE	ST	312
LP=JN(J)+I	ST	313
LZP=LP+NINJ	ST	314
LP11=LP-NI	ST	315
L7P1=LZP-NI	ST	316
AREA=XS(I)*VSU(J)	ST	317
AL2=RHC(LP)*W(L7P1)*AREA	ST	318
AL71=RHO(LP11)*W(LZP1)*AREA	ST	319
AL7=.5*(AL2+AL71)	ST	320
AL2=AL7/2.	ST	321
TZ=.5*(GAM(LP)+GAM(LP11))*AREA*TZFAC/(ZSW(NP1)*RN(J))	ST	322
TZ=AMAX1(TZ,ABS(AL7))	ST	323
CZULP1=2.*AL7	ST	324
40 CZ(LP)=TZ+AL2	ST	325
DO 401 K=2,N	ST	326
C----OBTAIN SOURCE TERMS AND EVAPORATION RATES.	COMMENT	138
CALL SOURCE	ST	327
CALL SCMAS	ST	328
DO 41 I=2,L	ST	329
J=JWL(I,K,NGOTO)	ST	330

AREA=ZS(K)*XSET)*ORMV(J+1)	ORIGINAL PAGE IS OF POOR QUALITY	ST	333
LP=KN(K)+JM(J)+I		ST	332
LYP=LP+NI		ST	331
LYN=LP-NI		ST	330
206 ALYM=RHO(LYM)+VELP1*AREA+		ST	329
ALYP=0,		ST	328
TY=GAM(LYM)+AREA/YS(J)		ST	327
CYU(I)=ALYN		ST	326
208 TY=AMAX1(TY,ALYP)		ST	325
TY=AMAX1(TY,-ALYM)		ST	324
41 CY(I)=TY+ALYM		ST	323
DO 42 J=3,N		ST	322
KJM=KN(K)+JM(J)		ST	321
IS=IWLI(J,NGOTO)		ST	320
IE=IWLO(J,NGOTO)		ST	319
LXP=KJM+IS		ST	318
LP=LXP-1		ST	317
LP11=LP-NI		ST	316
LXP1=LXP-NI		ST	315
AREA=YSVR(J)+ZS(K)		ST	314
IF (IMLI(J,4),EQ,IS) GO TO 162		ST	313
ALK=.5*(RHO(LP)+RHO(LXP))+U(LXP)*AREA		ST	312
TX=.5*(GAM(LP)+GAM(LXP))*AREA/XDIF(IS)		ST	311
GO TO 163		ST	310
162 ALK=RHO(LP)*U(LXP)*AREA		ST	309
DIST=.5*XDIF(IS)		ST	308
IF (IS,EQ,2) DIST=XDIF(2)		ST	307
TX=GAM(LP)*AREA/DIST		ST	306
163 IF (IWLI(J-1,4),EQ,IS) GO TO 164		ST	305
ALK1=.5*(RHO(LP11)+RHO(LXP1))+U(LXP1)*AREA		ST	304
TX1=.5*(GAM(LP11)+GAM(LXP1))*AREA/XDIF(IS)		ST	303
GO TO 165		ST	302
164 ALK1=RHO(LP11)*U(LXP1)*AREA		ST	301
DIST=.5*XDIF(IS)		ST	300
IF (IS,EQ,2) DIST=XDIF(2)		ST	299
TX1=GAM(LP11)*AREA/DIST		ST	298
165 ALK=.5*(ALK+ALK1)		ST	297
TX=.5*(TX+TX1)		ST	296
TX=AMAX1(TX,-ALK)		ST	295
CYU=ALK		ST	294
CX=TX+ALK		ST	293
TZFA=RM(J)/(RM(H)+DFAC*(RM(J)-RM(H)))		ST	292
DO 42 I=IS,IE		ST	291
MAX=JWLO(I,NGOTO)-1		ST	290
LTJ=JM(J)+I		ST	289
LP=KJM+I		ST	288
LXP=LP+1		ST	287
LYP=LP+NI		ST	286
L7P=LP+NI		ST	285
LP11=LP-NI		ST	284
L7P1=L7P-NI		ST	283
AXM(LIJ)=CX		ST	282
AYM(LIJ)=CY(I)		ST	281
AZM(LIJ)=CZ(LIJ)		ST	280
AREA=YSVR(J)+ZS(K)		ST	279
IF (I,EQ,IE) GO TO 43		ST	278
ALK=.25*(RHO(LP)+RHO(LXP))+U(LXP)*AREA		ST	277
ALK1=.25*(RHO(LP11)+RHO(LXP1))+U(LXP1)*AREA		ST	276
ALK=.5*(ALK+ALK1)		ST	275
TX=.25*(GAM(LP)+GAM(LXP)+GAM(LP11)+GAM(LXP1))*AREA/XDIF(I+1)		ST	274
TX=AMAX1(TX,ARS(ALK))		ST	273
CXUP=.5*ALK		ST	272
GO TO 44		ST	271

43	IF ((WLO(I,J,4),EQ,IE) GO TO 167	ST	395
	ALX=.5*(RHO(LP)+RHO(LXP))+U(LXP)*AREA	ST	396
	TX=.5*(GAM(LP)+GAM(LXP))*AREA/XDIF(I+1)	ST	397
	GO TO 168	ST	398
167	ALK=RHO(LXP)*U(LXP)*AREA	ST	399
	DIST=.5*XDIF(I+1)	ST	400
	IF (I,EQ,L) DIST=XDIF(LP1)	ST	401
	TX=GAM(LP)*AREA/DIST	ST	402
168	IF ((WLO(I,J-1,4),EQ,IE) GO TO 169	ST	403
	ALX1=.5*(RHO(LP1)+RHO(LXP1))+U(LXP1)*AREA	ST	404
	TX1=.5*(GAM(LP1)+GAM(LXP1))*AREA/XDIF(I+1)	ST	405
	GO TO 170	ST	406
169	ALX1=RHO(LXP1)*U(LXP1)*AREA	ST	407
	DIST=.5*XDIF(I+1)	ST	408
	IF (I,EQ,L) DIST=XDIF(LP1)	ST	409
	TX1=GAM(LXP1)*AREA/DIST	ST	410
170	ALK=.5*(ALX+ALX1)	ST	411
	TX=.5*(TX+TX1)	ST	412
	TX=AMAX3(TX,ALX)	ST	413
	CXUP=ALK	ST	414
44	AX=(L,I,J)=TX-ALK	ST	415
	CT=TX+ALK	ST	416
	DIVG(L,I,J)=DIVG(L,I,J)+CXUP-CXU	ST	417
	CXU=CXUP	ST	418
	ARFA=7S(K)*XS(I)*RNV(J+1)	ST	419
	IF (J,EQ,JWLO(I,NGOTO)-1) GO TO 45	ST	420
	ALY=RHO(LP)*AREA*(FYP(J)*V(LYP)+FYH(J)*V(LP))	ST	421
	ALYP=FYP(J)*ALY	ST	422
	ALYM=FYH(J)*ALY	ST	423
	TY=GAM(LP)*AREA/YS(J)	ST	424
	CYUP=ALY	ST	425
	GO TO 46	ST	426
45	ALYP=RHO(LYP)*V(LYP)*AREA	ST	427
	ALYM=0,	ST	428
	TY=GAM(LYP)*AREA/YS(J)	ST	429
	CYUP=ALYP	ST	430
46	TY=AMAX3(TY,ALYP)	ST	431
	TY=AMAX3(TY,-A,YM)	ST	432
	AYP(L,I,J)=TY-ALYP	ST	433
	CY(I)=TY+1LYM	ST	434
	DIVG(L,I,J)=DIVG(L,I,J)+CYUP-CYU(I)	ST	435
	CYU(I)=CYUP	ST	436
	AREA=XS(I)*YS(V(J))	ST	437
	TF(K,FQ,N) GO TO 47	ST	438
	AL7=.25*(RHO(LP)+RHO(LZP))*W(LZP)*AREA	ST	439
	AL71=.25*(RHO(LP1)+RHO(LZP1))*W(LZP1)*AREA	ST	440
	AL7=.5*(AL7+AL71)	ST	441
	GAMLP=.25*(GAM(LP)+GAM(LZP)+GAM(LP1)+GAM(LZP1))	ST	442
	T7=GAMLP*AREA*TZFAC/120*F(K+1)*RN(J))	ST	443
	T7=AMAX1(T7,ARS(AL71))	ST	444
	CZUP=2.*AL7	ST	445
	GO TO 48	ST	446
47	ALZ=RHO(LZP)*W(LZP)*AREA	ST	447
	AL71=RHO(LZP1)*W(LZP1)*AREA	ST	448
	AL7=.5*(ALZ+AL71)	ST	449
	AL7=AL7/2.	ST	450
	T7=GAM(LZP)*AREA*TZFAC/(ZSH(NP1)*RN(J))	ST	451
	T7=AMAX1(T7,ARS(AL71))	ST	452
	CZUP=-.9AL7	ST	453
48	A7P(L,I,J)=T7-AL7	ST	454
	C7(L,I,J)=TZ+ALZ	ST	455
	DIVG(L,I,J)=DIVG(L,I,J)+CZUP-CZU(L,I,J)	ST	456
	C7U(L,I,J)=CZUP	ST	457
	VOL=KRE(I)*YSVR(J)*ZS(K)	ST	458

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ALY=.54(ALY+ALY1)	ST	519
0.9ST=.54YDIF(J)	ST	520
XF=CJ.FQ.21 DIST=YDIF(2)	ST	521
TY=.5*(GAM(LP)+GAM(LP11))*AREA/DIST	ST	522
TX=AMAX1(TY,-ALY)	ST	523
CYU(I)=ALY	ST	524
51 CY(I)=TY+ALY	ST	525
DO 52 J=2,M	ST	526
KJM=KJM(K)+JPC(J)	ST	527
IS=IMLIX(J,NGOTO)	ST	528
IF=IMLIC(J,NGOTO)	ST	529
LYP=KJM+IS	ST	530
LP=LXP+1	ST	531
LP1=LXP-NINJ	ST	532
LXP1=LXP-NINJ	ST	533
AREA=YSR(J)*ZSW(K)	ST	534
ALX=RHO(LP)*U(LXP)*AREA	ST	535
ALK1=RHO(LP11)*U(LXP1)*AREA	ST	536
ALK=.5*(ALX+ALK1)	ST	537
DIST=.5*XNDF(I)	ST	538
IF (IS.EQ.2) DIST=XDIF(2)	ST	539
TX=.5*(GAM(LP)+GAM(LP11))*AREA/DIST	ST	540
TX=AMAX1(TX,-ALK)	ST	541
CXU=ALX	ST	542
CX=TR+ALX	ST	543
TZFAC=1.0	ST	544
DO 52 I=IS,IF	ST	545
MAX=JMLD(I,NGOTO)-1	ST	546
LIJ=JME(J)+I	ST	547
LP=KJM+I	ST	548
LXP=LP+NINJ	ST	549
LXP1=LXP-NINJ	ST	550
LYP=LYP-NINJ	ST	551
AXM(LIJ)=CX	ST	552
AYM(LIJ)=CY(I)	ST	553
ATM(LIJ)=C7(LIJ)	ST	554
AREA=YSR(J)*ZSW(K)	ST	555
IF (I.EQ.IF) GO TO 53	ST	556
ALK=.25*(RHO(LP)+RHO(LXP))+U(LXP)*AREA	ST	557
ALK1=.25*(RHO(LP11)+RHO(LXP1))+U(LXP1)*AREA	ST	558
ALK=.5*(ALX+ALK1)	ST	559
TX=.25*(GAM(LP)+GAM(LXP)+GAM(LP11)+GAM(LXP1))*AREA/XDIF(I+1)	ST	560
TX=AMAX1(TX,ARS(ALX))	ST	561
CXUP=2.0*ALX	ST	562
GO TO 54	ST	563
53 ALX=RHF(LXP)*U(LXP)*AREA	S"	564
ALK1=RHO(LXP1)*U(LXP1)*AREA	ST	565
ALK=.5*(ALY+ALK1)	ST	566
DIST=.5*XNDF(I+1)	ST	567
IF (I.EQ.I) DIST=XDIF(LP1)	ST	568
IF (I.EQ.I) DIST=XDIF(LP1)	ST	569
TX=.5*(GAM(LXP)+GAM(LXP1))*AREA/DIST	ST	570
TX=AMAX1(TX,ALK)	ST	571
CXUP=ALX	ST	572
54 AXP(LIJ)=TX-ALX	ST	573
CX=TX+ALX	ST	574
DIVG(LIJ)=DIVG(LIJ)+CXUP-CXU	ST	575
CXU=CXUP	ST	576
AREA=.75V(K)*RS(I)*RM(J+1)	ST	577
IF (J,FQ,MAX) GO TO 53	ST	578
ALY=.25*(RHO(LP)+RHO(LYP))*V(LYP)*AREA	ST	579
ALY1=.25*(RHO(LP11)+RHO(LYP1))*V(LYP1)*AREA	ST	580
	ST	581
	ST	582

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ALY=.5*(ALY+ALY1)	ST	583
TY=.25*(GAM(LP)+GAM(LYP)+GAM(LP11)+GAM(LYP1))*AREA/YDIF(J+1)	ST	584
TY=AMAX1(TY,ARS(ALY))	ST	585
CYUP=2.*ALY	ST	586
GO TO 56	ST	587
55 ALY=RHO(LYP)*V(LYP)*AREA	ST	588
ALY1=RHO(LYP1)*V(LYP1)*AREA	ST	589
ALY=.5*(ALY+ALY1)	ST	590
DIST=.5*YDIF(J+1)	ST	591
IF (J,EQ,M) DIST=YDIF(MP1)	ST	592
TY=.5*(GAM(LYP)+GAM(LYP1))*AREA/DIST	ST	593
TY=AMAX1(TY,ALY1)	ST	594
CYUP=ALY	ST	595
56 AYP(LIJ)=TY-ALY	ST	596
CY(I)=TY+ALY	ST	597
DIVG(LIJ)=DIVG(LIJ)+CYUP-CYU(I)	ST	598
CYU(I)=CYUP	ST	599
AREA=XS(I)*YS(J)	ST	600
DENSTY=RHO(LP)	ST	601
IF (K,EQ,NP1) DENSTY=RHO(LIJ+NINJ)	ST	602
IF (K,EQ,NP1) WLZP=W(LIJ+2*NINJ)	ST	603
IF (K,LT,NP1) WLZP=W(LZP)	ST	604
ALZ=DENSTY*AREA+(F2P(K)*WLZP+F2M(K)*W(LP))	ST	605
ALZP=F2P(K)*ALZ	ST	606
ALZM=F2M(K)*ALZ	ST	607
TZ=GAM(LP)*AREA*TZFACT/(2S(K)*R(J))	ST	608
CZUP=ALZ	ST	609
TZ=AMAX1(TZ,ALZP)	ST	610
TZ=AMAX1(TZ,-ALZM)	ST	611
AZP(LIJ)=TZ-ALZP	ST	612
CZ(LIJ)=TZ+ALZM	ST	613
DIVG(LIJ)=DIVG(LIJ)+CZUP-CZU(LIJ)	ST	614
CZU(LIJ)=CZUP	ST	615
VOL=XS(I)*YSR(J)*ZSW(K)	ST	616
L7M=LP-NINJ	ST	617
59 RDT=0.	ST	618
592 DIVG(LIJ)=AMAX1(RDT,DIVG(LIJ))	ST	619
DW(LP)=VOL/ZDIF(K)/R(J)	ST	620
IF (K,EQ,NP1) DW(LP)=DW(LP)*ZDIF(K)/ZSW(K)	ST	621
SU(LIJ)=SU(LIJ)*VOL+DW(LP)*(P(LZM)-P(LP))+DIVG(LIJ)*W(LP)	ST	622
SP(LIJ)=SP(LIJ)*VOL-DIVG(LIJ)	ST	623
IF (TPLAX,EQ,1) GO TO 52	NASAX	37
RVAV=0.125*(RHO(LP)+RHO(LP-NINJ))*(V(LP)+V(LP-NINJ)+V(LP+NJ))	NASAX	38
+V(LP-NINJ+NJ)*VOLR(J)	NASAX	39
IF (RVAV,LT,0.0) GO TO 57	NASAX	40
SP(LIJ)=SP(LIJ)-RVAV	NASAX	41
GO TO 52	NASAX	42
57 SU(LIJ)=SU(LIJ)-RVAV*W(LP)	NASAX	43
52 CONTINUE	ST	626
C---- SOURCE TERM MODIFICATIONS - BOUNDARY CONDITIONS.	COMMENT	143
CALL SCMD	ST	627
C---- SOLVE FINITE-DIFFERENCE EQUATIONS IN SOLVE1 AND SOLVE2.	COMMENT	144
CALL SOLVE1	ST	628
501 CONTINUE	ST	629
CALL SOLVE2	ST	630
502 CONTINUE	ST	631
CALL VELMOD	ST	632
C +----- PRESSURE PERTABATION EQUATION ----- C	ST	633
NGOTD=4	ST	634
TF(SOLVE(4)) 603,602,603	ST	635
603 IF(NOD(ISTEP,ISOLVE(4))) 602,604,602	ST	636
604 CONTINUE	ST	637
DO 605 LP=1,NINJNK	ST	638
605 PP(LP)=0.0	ST	639

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ISTR=2	ST	640
JSTR=2	ST	641
KSTR=2	ST	642
NV=4	ST	643
A000 CONTINUE	ST	644
CALCULATE CONTINUITY ERRORS.	COMMENT	149
DO 60 J=2,N	ST	645
TS=IWLI(J,NGOTO)	ST	646
IE=IWLE(J,NGOTO)	ST	647
DO 60 I=TS,IE	ST	648
LP=JN(J)+1	ST	649
LZP=LP+NINJ	ST	650
RHDA=RHO(LP)*XS(I)*YS(J)	ST	651
CXU(LP)=RHOA*DULZP	ST	652
60 C7(LP)=RHDA*DULZP	ST	653
DO 601 K=2,N	ST	654
DO 61 I=2,L	ST	655
J=JWL(I,J,NGOTO)+1	ST	656
LP=KMK(K)+JM(J-1)+I	ST	657
LYP=LP+NI	ST	658
RHDA=RHO(LP)*ZS(K)*XS(I)*RM(J)	ST	659
CYU(I)=RHOA*DULYP	ST	660
61 CY(I)=RHDA*DULYP	ST	661
DO 62 J=2,M	ST	662
KJM=KMK(K)+JM(J)	ST	663
TS=IWLI(J,NGOTO)	ST	664
IE=IWLE(J,NGOTO)	ST	665
LP=KJM+IS-1	ST	666
LXP=LP+1	ST	667
RHDA=RHO(LP)*YSR(J)*ZS(K)	ST	668
CXU=RHOA*DULXP	ST	669
CY=RHOA*DULXP	ST	670
DO 62 I=IS,IE	ST	671
MAY=JWL(I,J,NGOTO)-1	ST	672
LIJ=JM(J)+I	ST	673
LP=KJM+I	ST	674
LXP=LP+1	ST	675
LYP=LP+NI	ST	676
LZP=LP+NINJ	ST	677
AXM(LIJ)=CX	ST	678
AYM(LIJ)=CY(I)	ST	679
AZM(LIJ)=C2(LIJ)	ST	680
IF (I,FO,IE) GO TO 63	ST	681
RHDA=0.5*(RHO(LP)+RHO(LXP))*YSR(J)*ZS(K)	ST	682
GO TO 64	ST	683
63 RHDA=RHO(LXP)*YSR(J)*ZS(K)	ST	684
64 CX=RHOA*DULXP	ST	685
CXUP=RHOA*DULXP	ST	686
SU(LIJ)=CXU-CXUP	ST	687
CXU=CXUP	ST	688
AXP(LIJ)=CX	ST	689
IF (J,EQ,MAY) GO TO 65	ST	690
RHDA=0.5*(RHO(LP)+RHO(LYP))*ZS(K)*XS(I)*RM(J+1)	ST	691
GO TO 6A	ST	692
65 RHDA=RHO(LYP)*ZS(K)*XS(I)*RM(J+1)	ST	693
66 CY(I)=RHOA*DULYP	ST	694
CYUP=RHOA*DULYP	ST	695
SU(LIJ)=SU(LIJ)+CYU(I)-CYUP	ST	696
CYU(I)=CYUP	ST	697
AYP(LIJ)=CY(I)	ST	698
IF(K,FO,M) GO TO 67	ST	699
RHDA=0.5*(RHO(LP)+RHO(LZP))*XS(I)*YS(J)	ST	700
GO TO 6B	ST	701
67 RHDA=RHO(LZP)*XS(I)*YS(J)	ST	702

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C	---- HERE PP IS KE, P IS DISSIPATION	ST	759
	READ (NTP1) PP,P	ST	760
710	IF (INV,NE,LVFU0X) GO TO 714	ST	761
C	---- HERE PP IS KF, P IS DISS	ST	762
	WRITE (NTP2) PP,P	ST	763
C	---- HERE PP IS PH, P IS MFU, DU IS MCD	ST	764
	READ (NTP1) PP,P,DU	ST	765
714	IF (INV,NE,LVH) GO TO 720	ST	766
C	---- HERE DV IS ENTHALPY, DW IS FAV	ST	767
	RFAO (NTP1) DV,DW	ST	768
	NCPS=3	NOX	209
	NS1=ID02	NOX	210
	NS2=ION2	NOX	211
	S2(ID02)=RATIO2/SMW(ID02)	NOX	212
	S2(ION2)=(1.0-RATIO2)/SMW(ION2)	NOX	213
C	---- BOUNDARY VALUES OF ENTHALPY.	COMMENT	149
	DO 716 K=1,NP1	ST	769
	DO 717 I=1,LP1	ST	770
	IF (IKIN(I,K).EQ.2.0R.IKIN(I,K).EQ.3) GO TO 712	ST	771
	LP=KM(K)+JM(JWL(I,4))+I	ST	772
	LPH=L P+NVH(NVH)	ST	773
	TK=TEMP(LP)	NOX	214
	TKINV=1.000/TK	NOX	215
	CALL MCPS	NOX	216
	F(LPH)=HSUM+UNICON+TK	NOX	217
712	IF (IKIN(I,K).EQ.1.0R.IKIN(I,K).EQ.3) GO TO 717	ST	775
	LP=KM(K)+JM(JWL(I,4))+I	ST	776
	LPH=L P+NVH(NVH)	ST	777
	TK=TEMP(LP)	NOX	218
	TKINV=1.000/TK	NOX	219
	CALL MCPS	NOX	220
	F(LPH)=HSUM+UNICON+TK	NOX	221
717	CONTINUE	ST	779
	DO 716 J=1,NP3	ST	780
	IF (JWLN(J,K).EQ.1) GO TO 760	ST	781
	LP=KM(K)+JM(J)+IWLD(J,4)-1	ST	782
	LPH=L P+NVH(NVH)	ST	783
	TK=TEMP(LP)	NOX	222
	TKINV=1.000/TK	NOX	223
	CALL MCPS	NOX	224
	F(LPH)=HSUM+UNICON+TK	NOX	225
760	IF (J,GT,JW01.AND.J.LT.JW00) GO TO 716	ST	785
	LP=KM(K)+JM(J)+IWLD(J,4)+1	ST	786
	LPH=L P+NVH(NVH)	ST	787
	TK=TEMP(LP)	NOX	226
	TKINV=1.000/TK	NOX	227
	CALL MCPS	NOX	228
	F(LPH)=HSUM+UNICON+TK	NOX	229
716	CONTINUE	ST	789
720	IF (ISOLVE(NV)) 703,702,703	ST	790
703	IF (MODITSTEP,ISOLVE(NV))) 702,704,702	ST	791
704	CONTINUE	ST	792
	ISTR=2	ST	793
	JSTR=2	ST	794
	KSTR=2	ST	795
C	---- OBTAIN DIFFUSION COEFFICIENTS.	COMMENT	190
	CALL GAMMA	ST	796
	DO 70 J=2,M	ST	797
	IS=IWLD(J,NGOTO)	ST	798
	TF=IWLD(J,NGOTO)	ST	799
	T7FAC=R(J)/(R(M)+DFAC*(R(J)-R(M)))	ST	800
	DO 70 I=IS,IE	ST	801
	LP=JM(J)+I	ST	802
	L7P=LP+NIJ	ST	803

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AREA=XS(I)*YS(J)	ST	004
ALZ=RHO(LP)*V(LZP)*AREA	ST	005
ALZ=ALZ/2.	ST	006
TZ=GAM(LP)*AREA*TZFAC/(2SW(NP1)*R(J))	ST	007
T7=AMAX1(TZ,ABS(ALZ))	ST	008
CZU(LP)=2.*ALZ	ST	009
70 C7(LP)=TZ+ALZ	ST	010
DO 701 K=2,N	ST	011
C----OBTAIN SOURCE TERMS AND EVAPORATION RATES.		
CALL SOURCE	COMMENT	151
CALL SOMAS	ST	012
DO 71 I=2,L	ST	013
J=JWL(I,I,NGOT0)+1	ST	014
LP=KM(K)+JM(J-1)+I	ST	015
LYP=LP+NI	ST	016
AREA=ZS(K)*XS(I)*RM(J)	ST	017
ALY=RHO(LP)*V(LYP)*AREA	ST	018
DIST=.20VDIF(J)	ST	019
IF (J,EO,21) DIST=VDIF(2)	ST	020
TY=GAM(LP)*AREA/DIST	ST	021
TY=AMAX1(TY,-ALY)	ST	022
CYU(I)=ALY	ST	023
71 CY(I)=TY+ALY	ST	024
DO 72 J=2,M	ST	025
KJM=KM(K)+JM(J)	ST	026
IS=IWLT(J,NGOT0)	ST	027
IE=IWLO(J,NGOT0)	ST	028
LXP=KJM+IS	ST	029
LP=LXP-1	ST	030
AREA=YSR(J)*ZS(K)	ST	031
ALY=RHO(LP)*U(LXP)*AREA	ST	032
DIST=.20XDIF(IS)	ST	033
IF (IS,EO,2) DIST=XDIF(2)	ST	034
TX=GAM(LP)*AREA/DIST	ST	035
TX=AMAX1(TX,-ALX)	ST	036
CXU=ALX	ST	037
CX=TX+ALX	ST	038
TZFAC=R(J)/(R(M)+DFAC*(R(J)-R(M)))	ST	039
DO 72 I=IS,IE	ST	040
MAT=JUL0(I,NGOT0)-1	ST	041
LTJ=JM(J)+I	ST	042
LP=KJM+I	ST	043
LYP=LP+NI	ST	044
LZP=LP+NI+NINJ	ST	045
AXM(LTJ)=CX	ST	046
AYM(LIJ)=CY(I)	ST	047
ATM(LIJ)=CZ(LIJ)	ST	048
AREA=YSR(J)*ZS(K)	ST	049
TF (I,EO,IFI) GO TO 73	ST	050
ALX=.25*(RHO(LP)+RHO(LXP))+U(LXP)*AREA	ST	051
TX=.2*(GAM(LP)+GAM(LXP))*AREA/XDIF(I+1)	ST	052
TX=AMAX1(TX,ABS(ALX))	ST	053
CXUP=2.*ALX	ST	054
GO TO 74	ST	055
73 ALX=RHO(LXP)*U(LXP)*AREA	ST	056
DIST=.20XDIF(I+1)	ST	057
IF (I,EO,L) DIST=XDIF(LP1)	ST	058
TX=GAM(LXP)*AREA/DIST	ST	059
TY=AMAX1(TX,ALX)	ST	060
CXUP=ALX	ST	061
74 AXP(LIJ)=TX-ALX	ST	062
CX=TX+ALX	ST	063
DIVG(LIJ)=DIVG(LIJ)+CXUP-CXU	ST	064
	ST	065
	ST	066

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CXU=CXUP
AREA=7S(K)*XS(I)*RM(J+1)
IF (J,EO,MAX) GO TO 79
ALY=.25*(RHO(LP)+RHO(LYP))*V(LYP)*AREA
TY=.5*(GAM(LP)+GAM(LYP))*AREA/YDIF(J+1)
TY=AMAX1(TY,ABS(ALY))
CYUP=2.*ALY
GO TO 76
75 ALY=RHO(LYP)*V(LYP)*AREA
DIST=.5*YDIF(J+1)
IF (J,EO,M) DIST=YDIF(MP1)
TY=GAM(LYP)*AREA/DIST
TY=AMAX1(TY,ALY)
CYUP=ALY
76 AYP(LIJ)=TY-ALY
CY(I)=TY+ALY
DIVG(LIJ)=DIVG(LIJ)+CYUP-CYU(I)
CYU(I)=CYUP
AREA=XS(I)*YS(J)
IF(K,EO,N) GO TO 77
ALZ=.25*(RHO(LP)+RHO(LZP))*W(LZP)*AREA
TZ=.5*(GAM(LP)+GAM(LZP))*AREA+TZFAC/(ZDIF(K+1)*R(J))
TZ=AMAX1(TZ,ABS(ALZ))
CZUP=2.*ALZ
GO TO 78
77 ALZ=RHO(LZP)*W(LZP)*AREA
ALZ=ALZ/2.
TZ=GAM(LZP)*AREA+TZFAC/(ZSW(NP1)*R(J))
TZ=AMAX1(TZ,ABS(ALZ))
CZUP=2.*ALZ
78 AZP(LIJ)=TZ-ALZ
C7(LIJ)=TZ+ALZ
DIVG(LIJ)=DIVG(LIJ)+CZUP-CZU(LIJ)
CZU(LIJ)=CZUP
VOL=XS(I)*YSR(J)*ZS(K)
79 RDT=0.
792 DIVG(LIJ)=AMAX1(RDT,DIVG(LIJ))
LPF=LP+NVM(NVF(NV))
SU(LIJ)=SU(LIJ)+VOL+DIVG(LIJ)*F(LPF)
SP(LIJ)=SP(LIJ)+VOL-DIVG(LIJ)
72 CONTINUE
C-----SOURCE TERM MODIFICATIONS - BOUNDARY CONDITIONS.
CALL SOMOD
C-----CHEMICAL KINETICS CALCULATIONS.
C
IF(NV,NE,LVH1)GO TO 722
PA=PRESS
DO 723 J=2,M
TS=IWL1(I,J,NGOTO1)
TF=IWL0(I,J,NGOTO1)
DO 723 I=IS,IE
LIJ=I+J*M(J)
LP=LIJ+NM(K)
TK=TEMP(LP)
EMV=AKP(LIJ)+AKM(LIJ)+AYP(LIJ)+AZP(LIJ)+AZM(LIJ)
C-----NODE IN BLOCKAGE - SKIP CALCULATION - GO TO 723
IF(EMV,LT,1.0E-1G)GO TO 723
EMV=EMV-SP(LIJ)
TF(EMV,GT,1.0E20)GO TO 723
LPF=LP+1
LPW=LP-1
LPN=LP+NI
LPB=LP-NI
LPT=LP+NMJ

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	ST	067
CXU=CXUP	ST	068
AREA=7S(K)*XS(I)*RM(J+1)	ST	069
IF (J,EO,MAX) GO TO 79	ST	070
ALY=.25*(RHO(LP)+RHO(LYP))*V(LYP)*AREA	ST	071
TY=.5*(GAM(LP)+GAM(LYP))*AREA/YDIF(J+1)	ST	072
TY=AMAX1(TY,ABS(ALY))	ST	073
CYUP=2.*ALY	ST	074
GO TO 76	ST	075
75 ALY=RHO(LYP)*V(LYP)*AREA	ST	076
DIST=.5*YDIF(J+1)	ST	077
IF (J,EO,M) DIST=YDIF(MP1)	ST	078
TY=GAM(LYP)*AREA/DIST	ST	079
TY=AMAX1(TY,ALY)	ST	080
CYUP=ALY	ST	081
76 AYP(LIJ)=TY-ALY	ST	082
CY(I)=TY+ALY	ST	083
DIVG(LIJ)=DIVG(LIJ)+CYUP-CYU(I)	ST	084
CYU(I)=CYUP	ST	085
AREA=XS(I)*YS(J)	ST	086
IF(K,EO,N) GO TO 77	ST	087
ALZ=.25*(RHO(LP)+RHO(LZP))*W(LZP)*AREA	ST	088
TZ=.5*(GAM(LP)+GAM(LZP))*AREA+TZFAC/(ZDIF(K+1)*R(J))	ST	089
TZ=AMAX1(TZ,ABS(ALZ))	ST	090
CZUP=2.*ALZ	ST	091
GO TO 78	ST	092
77 ALZ=RHO(LZP)*W(LZP)*AREA	ST	093
ALZ=ALZ/2.	ST	094
TZ=GAM(LZP)*AREA+TZFAC/(ZSW(NP1)*R(J))	ST	095
TZ=AMAX1(TZ,ABS(ALZ))	ST	096
CZUP=2.*ALZ	ST	097
78 AZP(LIJ)=TZ-ALZ	ST	098
C7(LIJ)=TZ+ALZ	ST	099
DIVG(LIJ)=DIVG(LIJ)+CZUP-CZU(LIJ)	ST	900
CZU(LIJ)=CZUP	ST	901
VOL=XS(I)*YSR(J)*ZS(K)	ST	902
79 RDT=0.	ST	903
792 DIVG(LIJ)=AMAX1(RDT,DIVG(LIJ))	ST	904
LPF=LP+NVM(NVF(NV))	ST	905
SU(LIJ)=SU(LIJ)+VOL+DIVG(LIJ)*F(LPF)	ST	906
SP(LIJ)=SP(LIJ)+VOL-DIVG(LIJ)	ST	907
72 CONTINUE	COMMENT	152
C-----SOURCE TERM MODIFICATIONS - BOUNDARY CONDITIONS.	ST	908
CALL SOMOD	COMMENT	153
C-----CHEMICAL KINETICS CALCULATIONS.	COMMENT	154
C	NOX	230
IF(NV,NE,LVH1)GO TO 722	NOX	231
PA=PRESS	NOX	232
DO 723 J=2,M	NOX	233
TS=IWL1(I,J,NGOTO1)	NOX	234
TF=IWL0(I,J,NGOTO1)	NOX	235
DO 723 I=IS,IE	NOX	236
LIJ=I+J*M(J)	NOX	237
LP=LIJ+NM(K)	NOX	238
TK=TEMP(LP)	NOX	239
EMV=AKP(LIJ)+AKM(LIJ)+AYP(LIJ)+AZP(LIJ)+AZM(LIJ)	COMMENT	155
C-----NODE IN BLOCKAGE - SKIP CALCULATION - GO TO 723	NOX	240
IF(EMV,LT,1.0E-1G)GO TO 723	NOX	241
EMV=EMV-SP(LIJ)	NOX	242
TF(EMV,GT,1.0E20)GO TO 723	NOX	243
LPF=LP+1	NOX	244
LPW=LP-1	NOX	245
LPN=LP+NI	NOX	246
LPB=LP-NI	NOX	247
LPT=LP+NMJ	NOX	

LPA=LP-NINJ
 LIJ2=LID+NM(2)
 LPFHDX=LP+NM(NVFUDX)
 IF(IITR,NE,1)GO TO 741
 IF(ISTEP,NE,INOX)GO TO 741
 C-----FIRST ITERATION - SET SPECIES CONCENTRATIONS EQUAL TO THOSE
 C AT NEIGHBORING NODE WHICH HAS ALREADY BEEN SOLVED.
 IF(IRES,NE,0)GO TO 741
 IF(I,EQ,ISIGN)TO 743
 DO 742 II=9,NS
 FS(LP,II)=FS(LPN,II)
 IF(I,NE,IE)FS(LPE,II)=FS(LPN,II)
 TF(J,NE,JWLO(I,NGOTO)-1)FS(LPN,II)=FS(LPN,II)
 FS(LPT,II)=FS(LPN,II)
 742 IF(K,FQ,N)FS(LPT,II)=FS(LIJ2,II)
 GO TO 741
 743 TF(J,EC,JWLI(I,NGOTO)+1)GO TO 741
 DO 744 II=9,NS
 FS(LP,II)=FS(LPS,II)
 IF(I,NE,IE)FS(LPE,II)=FS(LPS,II)
 IF(J,NE,JWLO(I,NGOTO)-1)FS(LPN,II)=FS(LPS,II)
 FS(LPT,II)=FS(LPS,II)
 744 IF(K,FQ,N)FS(LPT,II)=FS(LIJ2,II)
 741 CONTINUE
 C-----PREPARE INPUTS TO CHEMICAL KINETICS PROGRAM CREK.
 DO 724 II=1,NS
 S2(II)=FS(LP,II)/SMW(II)
 724 S1(II)=(AKP(LIJ)+FS(LPE,II)+AKM(LIJ)+FS(LPN,II)+AYP(LTJ))
 1*FS(LPN,II)+AYM(LIJ)*FS(LPS,II)+AZP(LIJ)*FS(LPT,II)+APM(LIJ))
 2*FS(LPB,II))/(EMV*SMW(II))
 HSURO=F(LP+NVP(NVH))
 LPC=I-1+(J-2)*(NI-2)+(K-KSTR)*(NI-2)*(NJ-2)
 EDKIJ=EDK(LPC)
 C-----MODER=1, LAMINAR RATES USED.
 IF(MODER,EQ,1)EDKIJ=1.0E30
 FUT=F(LPFUDX)
 IF(NFNZ,NE,0)S1(IDFU)=S1(IDFU)+EVAP(LPC)/(EMV*SMW(IDFU))
 FMV=EMV/(XS(I)*YS(J)*ZS(K))
 IF(TK,LT,TNOX)GO TO 735
 C-----BYPASS CALCULATION IF TEMPERATURE.LT.TNOX (TNOX INPUT
 C BY USR1).
 CALL CREK
 C-----OUTPTS FROM CREK.
 RHO(LP)=RHOPP
 TEMP(LP)=TK
 C-----STORE SPECIES CONCENTRATIONS IN RESPECTIVE ARRAYS.
 DO 725 II=1,NS
 FSLP=S2(II)*SMW(II)
 IF(FSLP,LT,1.0E-20)GO TO 729
 C-----CHECK CONVERGENCE.
 IF(ABS(FSLP-FS(LP,II))/FSLP,GT,0.01)ICONVG=1
 725 FS(LP,II)=FSLP
 GO TO 738
 738 CONTINUE
 DO 736 II=9,NS
 FSLP=S1(II)*SMW(II)
 TF(FSLP,LT,1.0E-20)GO TO 736
 IF(ABS(FSLP-FS(LP,II))/FSLP,GT,0.01)ICONVG=1
 736 FS(LP,II)=FSLP
 738 CONTINUE
 LPD2=(LP+NVM(LV02))
 LPFDU=(LP+NVM(NVFU))
 LPFU1=(LP+NVM(LVFU))
 LPOD=(LP+NVM(NVCD))
 NOX 248
 NOX 249
 NOX 250
 NOX 251
 NOX 252
 COMMENT 196
 COMMENT 197
 JAN10 1
 NOX 254
 4STEP 329
 NOX 256
 NOX 257
 NOX 258
 NOX 259
 NOX 260
 NOX 261
 NOX 262
 4STEP 330
 NOX 264
 NOX 265
 NOX 266
 NOX 267
 NOX 268
 NOX 269
 COMMENT 158
 NOX 270
 NOX 271
 NOX 272
 NOX 273
 NOX 274
 NOX 275
 NOX 276
 NOX 277
 COMMENT 159
 NOX 278
 4STEP 331
 FEB2 3
 NOX 280
 NOX 281
 COMMENT 160
 COMMENT 161
 NOX 282
 COMMENT 162
 NOX 283
 NOX 284
 COMMENT 163
 NOX 285
 NOX 286
 NOX 287
 COMMENT 164
 NOX 288
 NOX 289
 NOX 290
 NOX 291
 4STEP 332
 NOX 292
 NOX 294
 NOX 295
 NOX 296
 NOX 297
 NOX 298
 NOX 299
 NOX 300
 NOX 301

**ORIGINAL PAGE IS
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NOX	302
NOX	303
NOX	304
NOX	305
NOX	306
4STEP	333
4STEP	334
4STEP	335
4STEP	336
4STEP	337
4STEP	338
NOX	307
NOX	308
COMMENT	165
NOX	309
ST	910
NOX	310
ST	912
ST	913
NOX	311
NOX	312
ST	914
COMMENT	166
NOX	313
NOX	314
NOX	315
NOX	316
NOX	317
NOX	318
NOX	319
NOX	320
NOX	321
NOX	322
NOX	323
4STEP	339
4STEP	340
4STEP	341
4STEP	342
NOX	324
COMMENT	167
NOX	325
NOX	326
NOX	327
NOX	328
NOX	329
COMMENT	168
NOX	330
NOX	331
NOX	332
NOX	333
NOX	334
COMMENT	169
NOX	335
NOX	336
NOX	337
NOX	338
NOX	339
NOX	340
NOX	341
NOX	342
ST	915
ST	916
ST	917
ST	918

$$\text{EQUATIONS} \quad A = A + A - A + A - A + A - A + A - A + A - A$$

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DO 730 NV=LVRX,LVRZ
IF (ISCLVE(NV)) 733,730,733
733 IF (MD(ISTEP,ISOLVE(NV))) 730,734,730
734 IF (IND,F0,0) CALL GAMRAD
    XF (IPMAX,F0,1) TNO=1
    CALL STRAD
    CALL FMOD
730 CONTINUE
C ----- COMPUTE AVG RADIATION FLUX -----
DO 740 K=1,NP1
DO 740 J=1,NP1
KJM=KM(K)+JM(J)
DO 740 I=1,LP1
    LP=KJM+I
    LPRX=LP+NVM(NVRX)
    LPRY=LP+NVM(NVRY)
    LPRZ=LP+NVM(NVRZ)
    LPFAV=LP+NVM(NVFAV)
    740 FIL(LPFAV)=(F(LPRX)+F(LPRY)+F(LPRZ))/3.
C ----- HERE PP IS PHI, P IS NFM, DU IS NCO
    WRITE (NTP2) PP,P,DU
C ----- HERE DV IS ENTHALPY, DW IS FAV
    WRITE (NTP2) DV,DW
C ----- HERE U IS FX, V IS FY, W IS FZ
    WRITE (NTP2) U,V,W
    WRITE (NTP2) TEMP,RHO
    WRITE (NTP2) FCH,FH2
    WRITE (NTP2) ANUC,SOOT1,SOOT2
    WRITE (NTP2) FS
799 NTPT=NTP1+NTP2
NTP1=NTPT-NTP1
NTP2=NTPT-NTP2
200 ISTEP=ISTEP+1
IXY= 3-IXY
RETURN
END
SUBROUTINE STRAD
COMMON/Coeff/A(40),B(40),EP(30),DP(30),APP(30),BPP(30)
COMMON F(3500),OU(500),DV(500),DW(500),
1 ANUC(500),SOOT1(500),SOOT2(500),FCH(500),FH2(500),FS(500,14),
1 RHO(500),VIS(500),AHSR(500),SCTR(500),SU(100),SP(100),
1 DRHOOP(500),
1 AXP(100),AYX(100),AYP(100),AYM(100),AZP(100),
2 APM(100),C7(100),CY(10),C2U(100),CYU(10),
3 C2P(100),CYF(10),DIVG(100),NTP1,NTP2
1,AYMK(192),AXPK(192),AYMK(192),AYPK(192),AZMK(192),AZPK(192),
2 SUK(192),SPK(192)
DIMENSION U(500),V(500),W(500),PP(500),P(500),TEMP(500)
DIMENSION GAM(500)
EQUIVALENCE (F(1),U(1)),(F(501),V(1)),(F(1001),W(1))
EQUIVALENCE (F(1901),PP(1)),(F(2001),P(1)),(F(2501),TEMP(1))
EQUIVALENCE (F(3001),GAM(1))
COMMON/CYL/R(30),RM(30),RMV(30),YSR(30),YSVR(30),IPMAX
COMMON/GRID/X(40),Y(30),Z(30),XS(40),YS(30),ZS(30),XSU(40),
1 YSV(30),ZSW(30),XDIF(40),YDIF(30),ZDIF(30),FXP(40),FXM(40),
2 FYP(30),FYM(30),FZP(30),FZN(30),DT,TIME
COMMON
1/CINDEX/IDCO,IDFU,IDO2,IDM2,IDH20,IDCO2,IDM1,IDH2,IDN1,IDNO,IDNO2
1,IND,IOOM,IMCPS,ILC,ILH,IMAT,ITER,JJJ,M1,M2,M3,MA,MGL08,MGL09P,
2 MLM,NO,NSP,NS1,NS2,IOCH
3/CCHEMI/CPSUM,HSUM,FQ,PPLN,RGAS,RGASTM,SMINV,TRINV,TLM,LNG
4/CPARAP/ASUB(30,31),EMV,ER,HSUB0,MDERUG,MS,PA,QQ,Q1,Q2,Q3,Q4,RHOFP,
4 SM,SMV(30),SMO,S1(30),S2(30),TK,LADIA,R,DEBUG,LEQUIL,LREACT,
4 LENFR,EDK1J,LCNVGA
ST      919
ST      920
ST      921
ST      922
ST      923
ST      924
ST      925
ST      926
ST      927
ST      928
ST      929
ST      930
ST      931
ST      932
ST      933
ST      934
ST      935
ST      936
ST      937
ST      938
ST      939
ST      940
ST      941
ST      942
ST      943
ST      944
ST      945
ST      946
ST      947
ST      948
ST      949
ST      950
ST      951
STR      2
MASAK   44
COMFB   2
4STEP   18
SOOT    403
NOX     343
4STEP   343
SOOT    403
NOX     343
ST      945
ST      946
ST      947
ST      948
ST      949
ST      950
ST      951
CTDMA   2
CTDMA   44
CTDMA   2
CTDMA   18
RAD     3
RAD     4
RAD     4
RAD     5
RAD     6
RAD     7
RAD     8
RAD     9
RAD     10
RAD     11
CTDMA   3
CTDMA   4
CTDMA   4
CTDMA   5
CTDMA   6
CTDMA   7
CTDMA   8
CTDMA   9
CTDMA   10
CTDMA   11
COMMON   2
COMMON   3
COMMON   4
COMMON   5
NOX     2
NOX     3
NOX     4
NOX     5
NOX     6
NOX     7
NOX     8
NOX     9
NOX     10
NOX     11
COMMON   2
COMMON   3
COMMON   4
COMMON   5
NOX     2
NOX     3
NOX     4
NOX     5
NOX     6
NOX     7
NOX     8
NOX     9

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      DOUBLE PRECISION CPSUM,ENV,ER,FQ,HSUBD,HSUM,PA,PPLN,Q0,Q1,Q2,Q3,
1  Q4,RGAS,RGASIN,RHOPP,SM,SMINV,SMW,S1,S2,TK,TKINV,TLN,SMO
2,FIUT,FST
      COMMON/STEP4/PEXP1,PEXP2,PEXP3,PEXP4,ER1,ER2,ER3,ER4,CE8U1,CE8U2,
1  CE8U3,CE8U4,AEXP1,AEXP2,AEXP3,AEXP4,BEXP1,BEXP2,BEXP3,BEXP4,
2  CEXP1,CEXP2,CEXP3,CEXP4,FIUT,FST
      LOGICAL LADTAR,LCONVG,LDEBUG,LEQUIL,I,NRG,LREACT,LENER
      COMMON/INT/L,M,N,LCV,NCV,LP1,MP1,MP1,NI,NJ,NK,NINJ,NINJHK,NV,
1  NVV,NGOTO,K,ISTP,JSTR,KSTR,NVM(32),NM(30),JM(30),ISTEP,
2  ISOLVE(32),IPRINT(32),TITLE(10,32),IXY,ISWP,JSWP,RELAX(32),NP,
3  NRHO,NGAM,IWLI(30,5),IWLO(30,5),JWL0(40,5),JWL1(40,5),IVEI,
4  TWD0,PM1,JWIT,JWTO,JWPO,IMD,JKIN(30,30),IKEIM(40,30)
      COMMON/INDEX/IPAR,LPREF,LISTM,INCIMP,ITRAD,NVRX,NVRV,NVRZ,JPLANE
1  PLAXM1,LVK,LVD,LVFUOX,LVFU1,LVCO,LVM,LVRX,LVRT,LVRZ,NVF(32),
2  TJJHP,IPFS,TITLEF2(20),IMAX,JMAX,KMAX,NVCO,FUNCC,NVH20,NVC02,
3  NVN2,NVCH,NVH2
      COMMON/CNOX/LVH1,LVH2,LVN1,LVNO,LVNQ2,LVD,LVNH,LVH20,LVN2,LVQ2,
1  LVC02,LVFU1,LVC01,MNOX,INOX,ITNOX,SMOX,TNOX
      COMMON/THERM/NVH,NVFU,NVDX,NVFUOX,NVTE,NODEN,IKS,FSTOIC,HFU,CP,
1  G45CON,RHCON,UNICON,PRESS,NVFAV,TCYLW,TINLW,TLIP,ACDEF(4),
2  T4,DFAC,WFU,WCO2,WCO,WDX,WH20,WN2,MYY,CXX,RATIO1,RATIO2,
3  RATIO3,RATIO4,HCD,TAN,ITWALL
      COMMON/CTDMA/KEND,ICTDMA(32)
C-----SUBROUTINE STRAD IS USED FOR CALCULATING THE FINITE-
C DIFFERENCE COEFFICIENTS IN THE RADIATION FLUX EQUATIONS
C AND FOR SOLVING THESE EQUATIONS BY USING THE
C TRI-DIAGONAL-MATRIX-ALGORITHM(TDMA).
C
      KONTRO=NV=LVRX+1
      GO TO (100,200,300),KONTRO
C ----- X-DIRECTION FLUX -----
100 CONTINUE
      DO 101 K=2,N
      NVKM=NVM(NVRX)+KM(K)
C-----ORTAIN SOURCE TERMS (SORAD) AND BOUNDARY CONDITIONS (SOMOD).
      CALL SORAD
      CALL SOMOD
      DO 102 J=2,M
      TX=0.
      IS=IWLI(J,NGOTO)
      IE=IWLC(J,NGOTO)
      DO 103 T=IS,IF
      LIJ=JM(JT+I)
      LP=LIJ+KPK(K)
      LXP=LP+1
      AXM(LIJ)=TX
      TX=.5*(GAM(LP)+GAM(LXP))/XDIF(I+1)
      AXP(LIJ)=TX
      SH(LIJ)=SU(LIJ)*XS(I)
      SP(LIJ)=SP(LIJ)*XS(I)
103 CONTINUE
      AXP(LIJ)=0.
102 CONTINUE
C-----TOMA SOLUTION.
      DO 104 J=2,M
      LPF=NVKM+JM(J)
      IS=IWLI(J,NGOTO)
      IF=IWLC(J,NGOTO)
      ISTR1=IS-1
      A(IFSTP)=0.
      B(IFSTP)=0.
      DO 105 I=IS,IF
      LIJ=JM(I)+I
      SP(LIJ)=SP(LIJ)-AXM(LIJ)+A(I-1)
      A(I)=SP(LIJ)
      B(I)=SP(LIJ)-SP(LIJ)
      105 CONTINUE
      104 CONTINUE
      CALL SORAD
      CALL SOMOD
      DO 106 I=1,M
      TX=0.
      DO 107 J=1,M
      LIJ=JM(I)+J
      SP(LIJ)=SP(LIJ)+A(J)*B(I-J)
      107 CONTINUE
      TX=SP(LIJ)/B(I)
      SP(LIJ)=TX
      106 CONTINUE
      CALL SORAD
      CALL SOMOD
      DO 108 I=1,M
      TX=0.
      DO 109 J=1,M
      LIJ=JM(I)+J
      SP(LIJ)=SP(LIJ)+A(J)*B(I-J)
      109 CONTINUE
      TX=SP(LIJ)/B(I)
      SP(LIJ)=TX
      108 CONTINUE
      CALL SORAD
      CALL SOMOD
      DO 110 I=1,M
      TX=0.
      DO 111 J=1,M
      LIJ=JM(I)+J
      SP(LIJ)=SP(LIJ)+A(J)*B(I-J)
      111 CONTINUE
      TX=SP(LIJ)/B(I)
      SP(LIJ)=TX
      110 CONTINUE
      CALL SORAD
      CALL SOMOD
      DO 112 I=1,M
      TX=0.
      DO 113 J=1,M
      LIJ=JM(I)+J
      SP(LIJ)=SP(LIJ)+A(J)*B(I-J)
      113 CONTINUE
      TX=SP(LIJ)/B(I)
      SP(LIJ)=TX
      112 CONTINUE
      CALL SORAD
      CALL SOMOD
      DO 114 I=1,M
      TX=0.
      DO 115 J=1,M
      LIJ=JM(I)+J
      SP(LIJ)=SP(LIJ)+A(J)*B(I-J)
      115 CONTINUE
      TX=SP(LIJ)/B(I)
      SP(LIJ)=TX
      114 CONTINUE
      CALL SORAD
      CALL SOMOD
      DO 116 I=1,M
      TX=0.
      DO 117 J=1,M
      LIJ=JM(I)+J
      SP(LIJ)=SP(LIJ)+A(J)*B(I-J)
      117 CONTINUE
      TX=SP(LIJ)/B(I)
      SP(LIJ)=TX
      116 CONTINUE
      CALL SORAD
      CALL SOMOD
      DO 118 I=1,M
      TX=0.
      DO 119 J=1,M
      LIJ=JM(I)+J
      SP(LIJ)=SP(LIJ)+A(J)*B(I-J)
      119 CONTINUE
      TX=SP(LIJ)/B(I)
      SP(LIJ)=TX
      118 CONTINUE
      CALL SORAD
      CALL SOMOD
      DO 120 I=1,M
      TX=0.
      DO 121 J=1,M
      LIJ=JM(I)+J
      SP(LIJ)=SP(LIJ)+A(J)*B(I-J)
      121 CONTINUE
      TX=SP(LIJ)/B(I)
      SP(LIJ)=TX
      120 CONTINUE
      CALL SORAD
      CALL SOMOD
      DO 122 I=1,M
      TX=0.
      DO 123 J=1,M
      LIJ=JM(I)+J
      SP(LIJ)=SP(LIJ)+A(J)*B(I-J)
      123 CONTINUE
      TX=SP(LIJ)/B(I)
      SP(LIJ)=TX
      122 CONTINUE
      CALL SORAD
      CALL SOMOD
      DO 124 I=1,M
      TX=0.
      DO 125 J=1,M
      LIJ=JM(I)+J
      SP(LIJ)=SP(LIJ)+A(J)*B(I-J)
      125 CONTINUE
      TX=SP(LIJ)/B(I)
      SP(LIJ)=TX
      124 CONTINUE
      CALL SORAD
      CALL SOMOD
      DO 126 I=1,M
      TX=0.
      DO 127 J=1,M
      LIJ=JM(I)+J
      SP(LIJ)=SP(LIJ)+A(J)*B(I-J)
      127 CONTINUE
      TX=SP(LIJ)/B(I)
      SP(LIJ)=TX
      126 CONTINUE
      CALL SORAD
      CALL SOMOD
      DO 128 I=1,M
      TX=0.
      DO 129 J=1,M
      LIJ=JM(I)+J
      SP(LIJ)=SP(LIJ)+A(J)*B(I-J)
      129 CONTINUE
      TX=SP(LIJ)/B(I)
      SP(LIJ)=TX
      128 CONTINUE
      CALL SORAD
      CALL SOMOD
      DO 130 I=1,M
      TX=0.
      DO 131 J=1,M
      LIJ=JM(I)+J
      SP(LIJ)=SP(LIJ)+A(J)*B(I-J)
      131 CONTINUE
      TX=SP(LIJ)/B(I)
      SP(LIJ)=TX
      130 CONTINUE
      CALL SORAD
      CALL SOMOD
      DO 132 I=1,M
      TX=0.
      DO 133 J=1,M
      LIJ=JM(I)+J
      SP(LIJ)=SP(LIJ)+A(J)*B(I-J)
      133 CONTINUE
      TX=SP(LIJ)/B(I)
      SP(LIJ)=TX
      132 CONTINUE
      CALL SORAD
      CALL SOMOD
      DO 134 I=1,M
      TX=0.
      DO 135 J=1,M
      LIJ=JM(I)+J
      SP(LIJ)=SP(LIJ)+A(J)*B(I-J)
      135 CONTINUE
      TX=SP(LIJ)/B(I)
      SP(LIJ)=TX
      134 CONTINUE
      CALL SORAD
      CALL SOMOD
      DO 136 I=1,M
      TX=0.
      DO 137 J=1,M
      LIJ=JM(I)+J
      SP(LIJ)=SP(LIJ)+A(J)*B(I-J)
      137 CONTINUE
      TX=SP(LIJ)/B(I)
      SP(LIJ)=TX
      136 CONTINUE
      CALL SORAD
      CALL SOMOD
      DO 138 I=1,M
      TX=0.
      DO 139 J=1,M
      LIJ=JM(I)+J
      SP(LIJ)=SP(LIJ)+A(J)*B(I-J)
      139 CONTINUE
      TX=SP(LIJ)/B(I)
      SP(LIJ)=TX
      138 CONTINUE
      CALL SORAD
      CALL SOMOD
      DO 140 I=1,M
      TX=0.
      DO 141 J=1,M
      LIJ=JM(I)+J
      SP(LIJ)=SP(LIJ)+A(J)*B(I-J)
      141 CONTINUE
      TX=SP(LIJ)/B(I)
      SP(LIJ)=TX
      140 CONTINUE
      CALL SORAD
      CALL SOMOD
      DO 142 I=1,M
      TX=0.
      DO 143 J=1,M
      LIJ=JM(I)+J
      SP(LIJ)=SP(LIJ)+A(J)*B(I-J)
      143 CONTINUE
      TX=SP(LIJ)/B(I)
      SP(LIJ)=TX
      142 CONTINUE
      CALL SORAD
      CALL SOMOD
      DO 144 I=1,M
      TX=0.
      DO 145 J=1,M
      LIJ=JM(I)+J
      SP(LIJ)=SP(LIJ)+A(J)*B(I-J)
      145 CONTINUE
      TX=SP(LIJ)/B(I)
      SP(LIJ)=TX
      144 CONTINUE
      CALL SORAD
      CALL SOMOD
      DO 146 I=1,M
      TX=0.
      DO 147 J=1,M
      LIJ=JM(I)+J
      SP(LIJ)=SP(LIJ)+A(J)*B(I-J)
      147 CONTINUE
      TX=SP(LIJ)/B(I)
      SP(LIJ)=TX
      146 CONTINUE
      CALL SORAD
      CALL SOMOD
      DO 148 I=1,M
      TX=0.
      DO 149 J=1,M
      LIJ=JM(I)+J
      SP(LIJ)=SP(LIJ)+A(J)*B(I-J)
      149 CONTINUE
      TX=SP(LIJ)/B(I)
      SP(LIJ)=TX
      148 CONTINUE
      CALL SORAD
      CALL SOMOD
      DO 150 I=1,M
      TX=0.
      DO 151 J=1,M
      LIJ=JM(I)+J
      SP(LIJ)=SP(LIJ)+A(J)*B(I-J)
      151 CONTINUE
      TX=SP(LIJ)/B(I)
      SP(LIJ)=TX
      150 CONTINUE
      CALL SORAD
      CALL SOMOD
      DO 152 I=1,M
      TX=0.
      DO 153 J=1,M
      LIJ=JM(I)+J
      SP(LIJ)=SP(LIJ)+A(J)*B(I-J)
      153 CONTINUE
      TX=SP(LIJ)/B(I)
      SP(LIJ)=TX
      152 CONTINUE
      CALL SORAD
      CALL SOMOD
      DO 154 I=1,M
      TX=0.
      DO 155 J=1,M
      LIJ=JM(I)+J
      SP(LIJ)=SP(LIJ)+A(J)*B(I-J)
      155 CONTINUE
      TX=SP(LIJ)/B(I)
      SP(LIJ)=TX
      154 CONTINUE
      CALL SORAD
      CALL SOMOD
      DO 156 I=1,M
      TX=0.
      DO 157 J=1,M
      LIJ=JM(I)+J
      SP(LIJ)=SP(LIJ)+A(J)*B(I-J)
      157 CONTINUE
      TX=SP(LIJ)/B(I)
      SP(LIJ)=TX
      156 CONTINUE
      CALL SORAD
      CALL SOMOD
      DO 158 I=1,M
      TX=0.
      DO 159 J=1,M
      LIJ=JM(I)+J
      SP(LIJ)=SP(LIJ)+A(J)*B(I-J)
      159 CONTINUE
      TX=SP(LIJ)/B(I)
      SP(LIJ)=TX
      158 CONTINUE
      CALL SORAD
      CALL SOMOD
      DO 160 I=1,M
      TX=0.
      DO 161 J=1,M
      LIJ=JM(I)+J
      SP(LIJ)=SP(LIJ)+A(J)*B(I-J)
      161 CONTINUE
      TX=SP(LIJ)/B(I)
      SP(LIJ)=TX
      160 CONTINUE
      CALL SORAD
      CALL SOMOD
      DO 162 I=1,M
      TX=0.
      DO 163 J=1,M
      LIJ=JM(I)+J
      SP(LIJ)=SP(LIJ)+A(J)*B(I-J)
      163 CONTINUE
      TX=SP(LIJ)/B(I)
      SP(LIJ)=TX
      162 CONTINUE
      CALL SORAD
      CALL SOMOD
      DO 164 I=1,M
      TX=0.
      DO 165 J=1,M
      LIJ=JM(I)+J
      SP(LIJ)=SP(LIJ)+A(J)*B(I-J)
      165 CONTINUE
      TX=SP(LIJ)/B(I)
      SP(LIJ)=TX
      164 CONTINUE
      CALL SORAD
      CALL SOMOD
      DO 166 I=1,M
      TX=0.
      DO 167 J=1,M
      LIJ=JM(I)+J
      SP(LIJ)=SP(LIJ)+A(J)*B(I-J)
      167 CONTINUE
      TX=SP(LIJ)/B(I)
      SP(LIJ)=TX
      166 CONTINUE
      CALL SORAD
      CALL SOMOD
      DO 168 I=1,M
      TX=0.
      DO 169 J=1,M
      LIJ=JM(I)+J
      SP(LIJ)=SP(LIJ)+A(J)*B(I-J)
      169 CONTINUE
      TX=SP(LIJ)/B(I)
      SP(LIJ)=TX
      168 CONTINUE
      CALL SORAD
      CALL SOMOD
      DO 170 I=1,M
      TX=0.
      DO 171 J=1,M
      LIJ=JM(I)+J
      SP(LIJ)=SP(LIJ)+A(J)*B(I-J)
      171 CONTINUE
      TX=SP(LIJ)/B(I)
      SP(LIJ)=TX
      170 CONTINUE
      CALL SORAD
      CALL SOMOD
      DO 172 I=1,M
      TX=0.
      DO 173 J=1,M
      LIJ=JM(I)+J
      SP(LIJ)=SP(LIJ)+A(J)*B(I-J)
      173 CONTINUE
      TX=SP(LIJ)/B(I)
      SP(LIJ)=TX
      172 CONTINUE
      CALL SORAD
      CALL SOMOD
      DO 174 I=1,M
      TX=0.
      DO 175 J=1,M
      LIJ=JM(I)+J
      SP(LIJ)=SP(LIJ)+A(J)*B(I-J)
      175 CONTINUE
      TX=SP(LIJ)/B(I)
      SP(LIJ)=TX
      174 CONTINUE

```

```

A(IJ)=AP(LIJ)/STORE
105 R(IJ)=(SU(LIJ)+AP(LIJ)*R(I-1))/STORE
JSUM=IS+TF
DO 106 II=IS,IE
I=ISUM-II
LP=LPF+I
106 F(LP)=A(IJ)*F(LP+1)+B(IJ)
104 CONTINUE
101 CONTINUE
RETURN
C ----- Y-DIRECTION FLUX -----
200 CONTINUE
DO 201 K=2,M
NVKN=NVM(NVRY)+KM(K)
(-----) ORTATN SOURCE TERMS (SORAD) AND BOUNDARY CONDITIONS (SOMOD).
CALL SORAD
CALL SOMOD
DO 202 I=2,L
TY=0.
JS=JUL(I,I,NGCTO)+1
JE=JWL(I,I,NGCTO)-1
DO 203 J=JS,JE
LIJ=JM(J)+I
LP=LIJ+KM(K)
LYP=LP+NI
AYM(LIJ)=TY
TY=.5*(GAM(LP)+GAM(LYP))/YDIF(J+1)*RN(J+1)
AYP(LIJ)=TY
SU(LIJ)=SU(LIJ)*YS(J)*R(J)
SP(LIJ)=SP(LIJ)*YS(J)*R(J)
203 CONTINUE
AYP(LIJ)=0.
202 CONTINUE
C----- TDMA SOLUTION.
DO 204 I=2,L
LPF=MVKM+I
JS=JUL(I,I,NGOTO)+1
JE=JWL(I,I,NGOTO)-1
JSTR1=JS-1
A(JSTR1)=0.
R(JSTR1)=0.
DO 205 J=JS,JE
LID=JM(J)+I
STORE=AYP(LIJ)+AYM(LIJ)-SP(LIJ)-AYN(LIJ)*A(J-1)
A(J)=AYP(LIJ)/STORE
205 R(J)=(SU(LIJ)+AYM(LIJ)+R(J-1))/STORE
JSUM=JS+JE
DO 206 JJ=JS,JE
J=JSUM-JJ
LP=LPF+JR(J)
LYP=LP+NI
206 FILP)=A(J)*F(LYP)+R(J)
204 CONTINUE
201 CONTINUE
RETURN
C ----- Z-DIRECTION FLUX -----
300 KSUM=2+N
DO 301 J=2,M
JPLAHF=J
NVJR=NVM(NVRZ)+JME(J)
C-----) ORTATN SOURCE TERMS (SORAD) AND BOUNDARY CONDITIONS (SOMODZ).
CALL SORAD
CALL SOMODZ
IS=JWL(I,I,NGOTZ)

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	COMMENT	177
STR		94
STR		95
STR		96
STR		97
STR		98
STR		99
STR		100

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IF=IWLOC(J,NGOTO)
DO 302 I=IS,IF
  LIJ=JM(J)+I
  T7=0.
  DO 303 K=2,N
    LTK=JM(K)+I
    LP=LJ+NM(K)
    LTP=LP+NMJ
    AZM(ILIK)=T7
    T2=(GAM(LP)+GAM(LTP))/(2DIF(K+1)*R(J))
    AZP(ILIK)=T2
    SU(LIK)=SU(LIK)+ZS(K)*R(J)
    SP(LIK)=SP(LIK)+ZS(K)*R(J)
  303 CONTINUE
  A7P(ILIK)=0.
  302 CONTINUE
C-----TOMA SOLUTION.
  DO 304 I=IS,IE
    A(I)=0.
    R(I)=0.
    LPF=NVJM+I
    DO 305 K=2,N
      LIK=JM(K)+I
      STORE=AZP(ILIK)+AZM(ILIK)-SP(ILIK)-AZR(ILIK)*A(K-1)
      A(K)=AZP(ILIK)/STORE
      305 R(K)=(SU(LIK)+AZM(ILIK)*B(K-1))/STORE
    DO 306 KK=2,N
      K=KSUM-KK
      LD=LPF+NM(K)
      LZD=LP+NMJ
      306 F(LP)=A(K)+F(LZP)+B(K)
    304 CONTINUE
    301 CONTINUE
    RETURN
    END
    FUNCTION TSOLVE(TWN,TGAS,RAD,HTCI,STG,ENI,ITRA0)
C-----SOLVE FOR WALL TEMPERATURES.
    ITR=MIND(ITRA0,2)
    KOUNT=0
    10 TW=TWN
    KOUNT=KOUNT+1
    IF(KOUNT.GT.10)GO TO 30
    TW2=TW+TW
    C-----RADIATION.
    ORH=2.0*EMI*(STG+TW2+TW2-RAD)*FLOAT(ITR-1)
    C-----CONVECTION.
    QCH=HTCI*(TW-TGAS)
    NORM=8.0*EMI*STG+TW+TW2*FLOAT(ITR-1)
    DOCH=HTCI
    FTH=ORH+QCH
    DFTW=NORM+DOCH
    TWN=TW-FTH/(DFTW+1.E-30)
    IF(ABS(TWN/TW-1.).GT..001)GO TO 10
    30 TSOLVE=TWN
    RETURN
    END
    SUBROUTINE ABSORBITS,T,PATH,SOOTK,PCO2,PH2O,ALPHA1
    
```

SUBROUTINE ABSROB COMPUTES THE ABSORPTIVITIES (WITH RESPECT TO A BLACKBODY SOURCE) OF ISOTHERMAL, HOMOGENEOUS MIXTURES OF SOO CO₂ AND H₂O AT A TOTAL PRESSURE OF 1 ATMOSPHERE. ABSORPTIVITIES CALCULATED BY SUBROUTINE ABSROB ARE IN GOOD AGREEMENT WITH ABSORPTIVITIES COMPUTED BY THE ABSORBTION CODE.

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EXPERIMENTAL MEASUREMENTS.

FOR A BLACKBODY SOURCE TEMPERATURE EQUAL TO THE MIXTURE TEMPERATURE, ABSORPTIVITY EQUALS EMISSIVITY. EMISSIVITIES SO CALCULATED ARE IN GOOD AGREEMENT WITH SPECTRAL CALCULATIONS AND WITH EXPERIMENTAL MEASUREMENTS.

EACH CALL ON SUBROUTINE ABSORR REQUIRES LESS THAN 12 MILLISECOND OF CPU TIME ON AN IBM 370/190.

INPUTS

1. TS (IN DEGREES KELVIN) IS BLACKBODY SOURCE TEMPERATURE. TS MUST BE GREATER THAN OR EQUAL TO 300.K AND LESS THAN OR EQUAL TO 2000.K.

2. T (IN DEGREES KELVIN) IS MIXTURE TEMPERATURE. T MUST BE GREAT THAN OR EQUAL TO 300.K AND LESS THAN OR EQUAL TO 2000.K.

3. PATH (IN METRES) IS MIXTURE PATHLENGTH. PATH MUST BE GREATER THAN OR EQUAL TO 0.0 METRES.

4. SOOTK (IN INVERSE METRES) IS ABSORPTION COEFFICIENT OF SOOT AT A WAVELENGTH OF 0.94 MICRONESTERS. SOOTK IS (APPROXIMATELY) RELATED TO THE SOOT VOLUME FRACTION, FV, BY ESOOTK=7FV/0.94E-6. SOOTK MUST BE GREATER THAN OR EQUAL TO 0.0 INVERSE METRES.

5. PCO2 (IN ATMOSPHERES) IS PARTIAL PRESSURE OF CO2 IN A MIXTURE WHOSE TOTAL PRESSURE IS 1 ATMOSPHERE. PCO2 MUST BE GREATER THAN OR EQUAL TO 0.0 ATMOSPHERES AND LESS THAN OR EQUAL TO 1.0 ATMOSPHERES. FOR PCO2 LESS THAN 0.0011 ATMOSPHERES, THE CONTRIBUTION OF CO2 TO THE MIXTURE ABSORPTIVITY IS ASSUMED TO BE ZERO. FOR (PATH*TS/T*PCO2) LESS THAN 0.0011 ATM-METRE, THE CONTRIBUTION OF CO2 TO THE MIXTURE ABSORPTIVITY IS ASSUMED TO BE ZERO. IF (PATH*TS/T*PCO2) EXCEEDS 9.98 ATM-METRE, SUBROUTINE ABSORR ABORTS AND RETURNS A VALUE OF ABSORPTIVITY SET AT -1.E30. A DIAGNOSTIC MESSAGE IS PROVIDED.

6. PH2O (IN ATMOSPHERES) IS PARTIAL PRESSURE OF H2O IN A MIXTURE WHOSE TOTAL PRESSURE IS 1 ATMOSPHERE. PH2O MUST BE GREATER THAN OR EQUAL TO 0.0 ATM AND LESS THAN OR EQUAL TO (1.0-PCO2). FOR PH2O LESS THAN 0.0011 ATM, THE CONTRIBUTION OF H2O TO THE MIXTURE ABSORPTIVITY IS ASSUMED TO BE ZERO. FOR (PATH*TS/T*PH2O) LESS THAN 0.0011 ATM-METRE, THE CONTRIBUTION OF H2O TO THE MIXTURE ABSORPTIVITY IS ASSUMED TO BE ZERO. IF (PATH*TS/T*PH2O) EXCEEDS 9.98 ATM-METRE, SUBROUTINE ABSORR ABORTS AND RETURNS A VALUE OF ABSORPTIVITY SET AT -1.E30. A DIAGNOSTIC MESSAGE IS PROVIDED.

OUTPUTS

ABSOR	10
ABSOR	11
ABSOR	12
ABSOR	13
ABSOR	14
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ABSOR	73

SUBROUTINE ABSOR RETURNS ALPHA, THE (DIMENSIONLESS)
ABSORPTIVITY OF A MIXTURE OF S_{CO2}, CO₂ AND H₂O AT A TOTAL
PRESSURE OF 1 ATMOSPHERE.

THE FOLLOWING SUBROUTINES MUST BE USED WITH

1. ASYMP
2. CHFRY
3. DLECK
4. FGAS
5. PENTA
6. SCOT
7. SCRTCH

QUESTIONS ABOUT SUBROUTINE ABSOR MAY BE ADDRESSED TO:
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WORCESTER, MASS. 01801
USA
TEL. NO. (617) 935-9050 EXT 264.

```

IF(TS.LT.300. .OR. TS.GT.2000.)GOTO 1
IF(T .LT.300. .OR. T .GT.2000.)GOTO 2
PSUM=PCO2+PH20
IF(PSUM.GT.1.0) GOTO 3
COMPUTE RATIO OF MIXTURE AND SOURCE TEMPERATURES.
RATIO=T/TS
COMPUTE EFFECTIVE PATHLENGTH,PATHL
PATHL=PATH/RATIO
PCL=PCO2*PATHL
PWL=PH20*PATHL
IF(PCL.GT.5.98 .OR. PWL.GT.5.98) GOTO 4
COMPUTE SOOT ABSORPTIVITY,AS
AS=0.0
IF(SOOTK.LE.0.01) GOTO 51
CALL SCOT(SOOTK,PATH,TS,TAUS)
AS=1.-TAUS
C
C
51 CONTINUE
COMPUTE GAS ABSORPTIVITY,AG
AG=0.0
IF(PCO2.LT.0.0011 .AND. PH20.LT.0.0011)GOTO 52
IF(PCL .LT.0.0011 .AND. PWL .LT.0.0011)GOTO 52
AG=FGAS(PATHL,PCO2,PH20,TS)
COMPUTE WATER VAPOR FRACTION,ZETA
ZETA=PH20/PSUM
POWER=0.63-0.2*ZETA
AG=AG*POWER
AG=AG*RATIO**POWER
52 CONTINUE
ALPHA=AS+AG-AS*AG
RETURN
4 CONTINUE
WRITE(6,*)
3 FORMAT(* IF THE PRODUCT,PATH,TS/T,PCO2,OR PATH,TS/T,PH20 EXCEEDS
105.5, OR AT P=1E-5)
WRITE(6,*)

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ABSOR	74
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ABSOR	136
ABSOR	137

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6 FORMAT( THIS CALCULATION LIES OUTSIDE THE RANGE OF SUBROUTINE ABS ABSOR 138
10PR, SUBROUTINE ABSOR ABORTS AND RETURNS A VALUE OF+1
  WRITE(6,7) ABSOR 139
7 FORMAT( ALPHA SET EQUAL TO -1.E300) ABSOR 140
  GOTO 8 ABSOR 141
3 CONTINUE ABSOR 142
  WRITE(6,9) ABSOR 143
9 FORMAT( SUM OF GAS PARTIAL PRESSURES, PCO2+PH2O, EXCEEDS 1 ATM) ABSOR 144
  WRITE(6,6) ABSOR 145
  WRITE(6,7) ABSOR 146
  GOTO 8 ABSOR 147
2 CONTINUE ABSOR 148
  WRITE(6,11) ABSOR 149
11 FORMAT( MIXTURE TEMPERATURE , T, LIES OUTSIDE THE TEMPERATURE RANG ABSOR 150
  IE 300 TO 2000 DEGREES KELVIN) ABSOR 151
  WRITE(6,6) ABSOR 152
  WRITE(6,7) ABSOR 153
  GOTO 8 ABSOR 154
1 CONTINUE ABSOR 155
  WRITE(6,10) ABSOR 156
10 FORMAT( BLACKBODY SOURCE TEMPERATURE, TS, LIES OUTSIDE THE TEMPERAT ABSOR 157
  URE RANGE 300 TO 2000 DEGREES KELVIN) ABSOR 158
  WRITE(6,6) ABSOR 159
  WRITE(6,7) ABSOR 160
9 CONTINUE ABSOR 161
  ALPHA=-1.E30 ABSOR 162
  RETURN ABSOR 163
  END ABSOR 164
  SUBROUTINE ASYMP(Z,ZV) ABSOR 165
    SURROUNTR ASYMP COMPUTES THE ASYMPTOTIC EXPANSION FOR THE ABSOR 166
    PENTAGAMMA FUNCTION. ABSOR 167
C C
C C
    Z11=1./Z ABSOR 168
    Z12=Z11*Z11 ABSOR 169
    Z13=Z11*Z12 ABSOR 170
    ZV=Z13*(Z.+3.+Z11)+Z12*(Z.+Z12*(-1.+Z12*(1.3333333333
    +Z12*(-3.+10.*Z12)))) ABSOR 171
    RETURN ABSOR 172
    END ABSOR 173
    SUBROUTINE CHERY(N,X,V) ABSOR 174
      V REPRESENTS VALUE OF CHEBYSHEV POLYNOMIAL OF ORDER N ABSOR 175
      AND ARGUMENT X. ABSOR 176
      V=1. ABSOR 177
      IF(N) 1,1,2 ABSOR 178
      1 RETURN ABSOR 179
C C
C C
      2 V=Y ABSOR 180
      IF(N=1) 1,1,3 ABSOR 181
      3 F=N*X ABSOR 182
      VM1=X ABSOR 183
      VM2=1. ABSOR 184
      DO 4 I=2,N ABSOR 185
      Y=F*VM1-VM2 ABSOR 186
      VM2=VM1 ABSOR 187
      VM1=Y ABSOR 188
      4 CONTINUE ABSOR 189
      RETURN ABSOR 190
      END ABSOR 191
      FUNCTION DLECK(X,PL,T)
        SURROUNTR DLECK COMPUTES THE 2,7 AND 15 MICROMETRE OVERLAP ABSOR 192
        CORRECTION FOR MIXTURES OF CO2 AND H2O. THE OVERLAP CORRECTION ABSOR 193
        IS COMPUTED BY USING A TEMPERATURE-ADJUSTED VERSION OF THE ABSOR 194
        OVERLAP CORRECTION FACTOR SUGGESTED BY R. LECKNFT ABSOR 195
        (COMBUSTION AND FLAME VOLUME 19 PAGES 33-48, 1972) ABSOR 196
C C
C C
C C
        ABSOR 197
        ABSOR 198
        ABSOR 199
        ABSOR 200
        ABSOR 201

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IF(IPL,LT.0.1) GOTO 1
TERM=X/(10.7+101.0K) -X**10.4/111.7
TERM2=ALOG10(101.325*PL)
TERM2=TERM2**2.76
TT=T/1000.
TT2=TT*TT
A=-1.0204082
B=2.244979
C=-0.23449386
TERM3=A+TT2+B*TT+C
TERMC REPRESENTS THE TEMPERATURE ADJUSTMENT
DLECK=TERM +TERM2+TERM3
RETURN
1 DLFCK=0.0
RETURN
END
FUNCTION EGAS(PATHL,PC,PH,T)
FUNCTION EGAS COMPUTES THE EMISSIVITY OF A GIVEN PATH (PATHL)
OF A MIXTURE OF CO2 AND H2O AT TEMPERATURE T.
PC = PARTIAL PRESSURE OF CO2
PH = PARTIAL PRESSURE OF H2O
EGAS=0.0
IF(T,LT,300. .OR. T.GT,2000.) RETURN
FC=0.0
IF(PC,LT,0.0011 .OR. PC.GT,1.0) GOTO 1
PCL=PC+PATHL
IF(PCL,LT,0.0011 .OR. PCL.GT,5.98) GOTO 1
CALL SCRTCH(PC,PCL,T,1,EC)
1 CONTINUE
IF(PH,LT,0.0011 .OR. PH.GT,1.0) GOTO 2
PWL=PH+PATHL
IF(PWL,LT,0.0011 .OR. PWL.GT,5.98) GOTO 2
CALL SCRTCH(PW,PWL,T,2,EW)
EGAS=FC+FW
IF(EC,LF,C.0) RETURN
PCPH=PC+PH
V1=PW/PCPH
IF(XI,LT,0.01) RETURN
PCWL=PCPH+PATHL
IF(PCWL,LT,0.1 ) RETURN
DELE=DLECK(XI,PCWL,T)
EGAS=EGAS-DELE
RETURN
2 CONTINUE
EGAS=FC
RETURN
END
SUBROUTINE PENTA(X,V)
SUBROUTINE PENTA RETURNS THE VALUE V OF THE PENTAGAMMA FUNCTION
OF ARGUMENT X. RECURRENCE FORMULA 6.4.6, AND ASYMPTOTIC FORMUL
6.4.14 (PAGE 260) OF ABRAMOWITZ AND STEGUN ARE USED IN
THIS CALCULATION.
IF(X,GF,4.1) GOTO 1
IF(X,GE,3.1) GOTO 2
IF(X,GF,2.1) GOTO 3
S=(1. / (X+2.1004+1. / (X+1.1004+1. / X004))**6.
Z=X+3.
CALL ASYMP(Z,ZV)
GOTO 4
3 CONTINUE
S=(1. / (X+1.1004+1. / X004))**6.

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T=X+2.
CALL ASYMP(Z,ZV)
GOTO 4
2 CONTINUE
S=6./X**6
T=X+1.
CALL ASYMP(Z,ZV)
GOTO 4
1 CONTINUE
S=0.0
CALL ASYMP(X,ZV)
4 CONTINUE
V=ZV+S
RETURN
END

SUBROUTINE SOOT(ZKLED,PATHL,TBLACK,TAUS)
SUBROUTINE SOOT COMPUTES THE TRANSMISSIVITY (TAUS) OF PATH (PATHL)
OF SOOT TO A BLACKBODY RADIATION SOURCE AT A GIVEN
TEMPERATURE (TBBLACK).

IF(ZKLED.LE. 0.) GOTO 1
ARG=1.+ZKLED*PATHL*TBLACK*6.5337E-5
TBBLACK - SOURCE TEMPERATURE OR GAS TEMPERATURE
CALL PENTA(ARG,V)
SUBROUTINE PENTA COMPUTES THE PENTAGAMMA FUNCTION
ARG - ARGUMENT OF THE PENTAGAMMA FUNCTION
TAUS=V*1539897336
TAUS = SOOT TRANSMISSIVITY
RETURN
1 TAUS=1.
RETURN
END

SUBROUTINE SCRTCH(P,PL,T,INDEX,V)
DIMENSION CC(3,4,4),CW(3,4,4),           SC(3,4,4)
IF(INDEX.EQ.2) GOTO 2
CC REPRESENTS AN ARRAY OF 40 COEFFICIENTS FOR CO2

CC(1,1,1)=0.2754568E+01
CC(1,1,2)=0.2997857E+00
CC(1,1,3)=0.1232494E+00
CC(1,1,4)=0.1279287E-01
CC(1,2,1)=0.1503051E+01
CC(1,2,2)=0.3156449E+00
CC(1,2,3)=0.1098126E-01
CC(1,2,4)=0.3729629E-01
CC(1,3,1)=0.2474119E+00
CC(1,3,2)=0.3323046E-01
CC(1,3,3)=0.1019471E-01
CC(1,3,4)=0.2269709E-01
CC(1,4,1)=0.4994029E-01
CC(1,4,2)=0.1986766E-02
CC(1,4,3)=0.3007698E-02
CC(1,4,4)=0.1179598E-02
CC(2,1,1)=0.5737722E-02
CC(2,1,2)=0.9328498E-02
CC(2,1,3)=0.2906266E-02
CC(2,1,4)=0.4227520E-03
CC(2,2,1)=0.3121784E-02
CC(2,2,2)=0.5632821E-02
CC(2,2,3)=0.3260295E-02
CC(2,2,4)=0.7067884E-03
CC(2,3,1)=0.1666731E-03

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CC(2,3,2)=-0.7326533E-03	ABSOR	330
CC(2,3,3)=0.3639835E-03	ABSOR	331
CC(2,3,4)=0.3226318E-03	ABSOR	332
CC(2,4,1)=0.7386638E-03	ABSOR	333
CC(2,4,2)=-0.7277073E-03	ABSOR	334
CC(2,4,3)=0.3925968E-03	ABSOR	335
CC(2,4,4)=-0.2021413E-03	ABSOR	336
CC(3,1,1)=0.3385611E-02	ABSOR	337
CC(3,1,2)=-0.5439185E-02	ABSOR	338
CC(3,1,3)=0.1764560E-02	ABSOR	339
CC(3,1,4)=0.3035031E-03	ABSOR	340
CC(3,2,1)=-0.1862700E-02	ABSOR	341
CC(3,2,2)=0.3236275E-02	ABSOR	342
CC(3,2,3)=-0.1992250E-02	ABSOR	343
CC(3,2,4)=0.3474022E-03	ABSOR	344
CC(3,3,1)=0.1204807E-03	ABSOR	345
CC(3,3,2)=-0.4479927E-03	ABSOR	346
CC(3,3,3)=0.2497521E-03	ABSOR	347
CC(3,3,4)=0.1812996E-03	ABSOR	348
CC(3,4,1)=0.4218169E-03	ABSOR	349
CC(3,4,2)=-0.4046608E-03	A. R.	350
CC(3,4,3)=0.3256061E-03	ABSOR	351
CC(3,4,4)=-0.9514981E-04	ABSOR	352
GOTO4	ABSOR	353
2 CONTINUE	ABSOR	354
C C C CW REPRESENTS AN ARRAY OF 48 COEFFICIENTS FOR H2O	ABSOR	355
CW(1,1,1)=-0.2594279E+01	ABSOR	356
CW(1,1,2)=-0.7118472E+00	ABSOR	357
CW(1,1,3)=-0.9956839E-03	ABSOR	358
CW(1,1,4)=0.12226560E-01	ABSOR	359
CW(1,2,1)=0.2510331E+01	ABSOR	360
CW(1,2,2)=0.6481808E+00	ABSOR	361
CW(1,2,3)=-0.3390597E-01	ABSOR	362
CW(1,2,4)=-0.5524345E-02	ABSOR	363
CW(1,3,1)=-0.4191636E+00	ABSOR	364
CW(1,3,2)=-0.1379180E+00	ABSOR	365
CW(1,3,3)=0.3077930E-01	ABSOR	366
CW(1,3,4)=0.8862328E-03	ABSOR	367
CW(1,4,1)=-0.3223912E-01	ABSOR	368
CW(1,4,2)=-0.1820241E-01	ABSOR	369
CW(1,4,3)=-0.2223143E-01	ABSOR	370
CW(1,4,4)=-0.5940781E-03	ABSOR	371
CW(2,1,1)=0.1126569E+00	ABSOR	372
CW(2,1,2)=-C.0133829E-01	ABSOR	373
CW(2,1,3)=0.1514940E-01	ABSOR	374
CW(2,1,4)=0.1993880E-02	ABSOR	375
CW(2,2,1)=-C.4298803E-02	ABSOR	376
CW(2,2,2)=0.4530660E-01	ABSOR	377
CW(2,2,3)=-C.2082004E-01	ABSOR	378
CW(2,2,4)=0.2013361E-02	ABSOR	379
CW(2,3,1)=-0.4375032E-01	ABSOR	380
CW(2,3,2)=0.1924597E-01	ABSOR	381
CW(2,3,3)=0.8859877E-02	ABSOR	382
CW(2,3,4)=-0.4618414E-02	ABSOR	383
CW(2,4,1)=0.7077876E-02	ABSOR	384
CW(2,4,2)=-C.2096168E-01	ABSOR	385
CW(2,4,3)=0.1458262E-02	ABSOR	386
CW(2,4,4)=0.3851421E-02	ABSOR	387
CW(3,1,1)=0.9341917E-01	ABSOR	388
CW(3,1,2)=-0.9407693E-01	ABSOR	389
CW(3,1,3)=0.4394611E-02	ABSOR	390
CW(3,1,4)=C.149203E-02	ABSOR	391


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4/CPARAM/ASUR(30,3),ENV,ER,HSUB0,NOEBUG,NS,PA,00,01,02,03,04,RHOFP, NOX    7
4 SM,SMW(30),SP0,S1(30),S2(30),TK,LADIAR,LDEBUG,LEQUIL,LREACT, NOX    8
4 LENER,ER0IJ,LCONVG
  DOUBLE PRECISION CPSUM,ENV,ER,FQ,HSUB0,HSUM,PA,PPLN,00,01,02,03,
1 Q4,RGAS,RGASIN,RHOFP,SM,SINV,SMW,S1,S2,TK,TKINV,TLN,SMO NOX    9
2 FUT,FST
  COMMON/STEP4/PEXP1,PEXP2,PEXP3,PEXP4,ER1,ER2,ER3,ER4,CEBU1,CEBU2,
1 CFRU3,CFRU4,AEXP1,AEXP2,AEXP3,AEXP4,BEXP1,BEXP2,BEXP3,BEXP4, 4STEP   4
2 CEXP1,CEXP2,CEXP3,CEXP4,FUT,FST
  LOGICAL LADIAR,LCONVG,LDEBUG,LEQUIL,LNRG,LREACT,LENER
  COMMON/INT/L,M,N,LCV,MCV,NCV,LP1,MP1,NP1,NI,NJ,NK,NINJ,NINJK,NV,
1 NNV,NGOTO,K,ISTR,JSTR,KSTR,NVM(35),KM(30),JM(30),ISTEP, 4STEP   5
2 ISOLVE(32),IPRINT(33),TITLE(10,33),IXY,ISWP,JSWP,RELAX(35),NP,
3 NRHO,NGAM,IWLI(30,5),IWLD(30,5),JWLI(40,5),JWLW(40,5),IWEI,
4 IWEN,MM1,JWID,JWID,JWDD,INW,JKIN(30,30),IKIN(40,30)
  COMMON/INDEX/IPAR,LPREF,ISTUM,INCMP,ITRAD,NVRX,NVRY,NVRZ,JPLANE
1 PLAXW1,LVH,LVD,LVFUOX,LVFU,LVC0,LVH,LVRY,LVZ,NVF(32),
2 IJUMP,IRES,TITLE2(20),IMAX,JMAX,KMAX,NVCO,FUMCO,NVH20,NVCD2,
3 NVN2,NVCH,NVH2
  COMMON/CNOX/LVH1,LVH2,LVN1,LVN02,LVO,LVOH,LVH20,LVN2,LVO2,
1 LVC02,LVFU1,LVC01,NNOX,INOX,ITNOX,SNOK,TNOX
  COMMON/THERP/NVM,NVFU,NVOX,NVFUOX,NVTE,NGDEN,IKR,FSTOIC,HFU,CP,
1 GASCON,RHOCON,UNICON,PRESS,NVFAV,TCYLW,TINLW,TLIP,ACOEF(4),
2 T4,DFAC,WFU,WCO2,WCO,WDX,WH20,WN2,HYY,CXX,RATIO1,RATIO2,
3 RATIO3,RATIO4,HCO,TAN,ITWALL
  COMMON/CTDMA/KEND,ICTDMA(32)
C-----SUBROUTINE SOLVE IS USED TO SOLVE THE FINITE-DIFFERENCE
C EQUATIONS BY THE TRI-DIAGONAL-MATRIX-ALGORITHM(TDMA).
C
C ENTRY SOLVE1
  RELAXM=1,-RELAX(NV)
  DO 10 J=JSTR,M
  KJM=KM(K)+JME(J)
  IS=TWL(I(J),NGETO)
  IF=IWLD(I(J),NGOTO)
  DO 10 I=IS,IE
  LIJ=JM(J)+I
  LP=KJM+I
  LPF=LP+NVMINV(NV)
  L7P=LPF+MINJ
  L7N=LPF-MINJ
  FL7P=F(L7P)
  IF (INV.EQ.3.AND.K.EQ.NP1) FL7P=W(LIJ+2*MINJ)
10 CONTINUE
  SP(LIJ)=(AXM(LIJ)+AXP(LIJ)+AYM(LIJ)+AYP(LIJ)+AZM(LIJ)+AZP(LIJ)-
  1SP(LIJ))/RELAX(NV)
C-----STORE COEFFICIENTS FOR CYCLIC TDMA.
  LPC=T-1+(J-2)*(NI-2)+(K-KSTR)*(NI-2)*(NJ-2)
  AYMK(LPC)=AYM(LIJ)
  AXPK(LPC)=AXP(LIJ)
  AYNK(LPC)=AYM(LIJ)
  AYPK(LPC)=AYP(LIJ)
  AZMK(LPC)=AZM(LIJ)
  AZPK(LPC)=AZP(LIJ)
  SU(LPC)=SU(LIJ)+SP(LIJ)*RELAXN*F(LPF)
  SPK(LPC)=SP(LIJ)+1.0E-30
  SU(LIJ)=SU(LIJ)+SP(LIJ)*RELAXN*F(LPF)+AZM(LIJ)*F(LZM)+AZP(LIJ)*
1  FL7P
  GO TO (11,12,13,10),NGOTO
11 DU(LP)=DU(LP)/SP(LIJ)
  GO TO 10
12 DV(LP)=DV(LP)/SP(LIJ)
  GO TO 10
13 DW(LP)=DW(LP)/SP(LIJ)

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10	CONTINUE	\$0	32
	NVKM=NM(K)+NVP(NVF(NV))	\$0	33
	ISUM=ISTP+L	\$0	34
	JSUM=JSTR+N	\$0	35
	INOMAX=ICTDMA(NV)	\$0	36
	DO 45 INO=1,INOMAX	\$0	37
	GO TO (20,30),IXY	\$0	38
20	CONTINUE	\$0	39
	C----TOMA TRAVERSE IN X-DIRECTION.	COMMENT	100
	DO 21 JJ=JSTR,N	\$0	40
	GO TO (24,29),JSWP	\$0	41
24	J=JJ	\$0	42
	GO TO 26	\$0	43
25	J=JSUM-JJ	\$0	44
26	CONTINUE	\$0	45
	LPF=NVKM+JM(J)	\$0	46
	IS=IWLI(J,NGOTO)	\$0	47
	IF=IWLO(J,NGOTO)	\$0	48
	ISTR1=IS-1	\$0	49
	LPFI=LPF+ISTR1	\$0	50
	AP(ISTR1)=0.	\$0	51
	RP(ISTR1)=F(LPFI)	\$0	52
	DO 22 I=IS,IE	\$0	53
	LIJ=JM(J)+I	\$0	54
	LYP=LPF+NI+I	\$0	55
	LYM=LPF-NI+I	\$0	56
	STORE=SP(LIJ)-AXH(LIJ)*AP(I-1)+1.E-30	\$0	57
	AP(I)=AYP(LIJ)/STORE	\$0	58
22	RP(I)=(SUI(LIJ)+AYP(LIJ)*F(LYP)+AYH(LIJ)*F(LYN)+AXH(LIJ)*BP(I-1))/	\$0	59
	1STORE	\$0	60
	ISUM1=IS+IE	\$0	61
	DO 23 II=IS,IE	\$0	62
	I=ISUM1-II	\$0	63
	LP=LPF+I	\$0	64
23	F(LP)=AP(I)*F(LP+1)+BP(I)	\$0	65
21	CONTINUE	\$0	66
	JSWP=3-JSWP	\$0	67
	GO TO (20,20),JSWP	\$0	68
28	CONTINUE	\$0	69
	GO TO (30,40),IXY	\$0	70
	C----TOMA TRAVERSE IN Y-DIRECTION.	COMMENT	189
30	DO 31 II=ISTR,L	\$0	71
	GO TO (34,35),TSWP	\$0	72
34	I=II	\$0	73
	GO TO 36	\$0	74
35	I=ISUM-II	\$0	75
36	CONTINUE	\$0	76
	LPF=NVKM+I	\$0	77
	JS=JWL(I,NGOTO)+1	\$0	78
	JE=JWL(I,NGOTO)-1	\$0	79
	JSTR1=JS-1	\$0	80
	LPFI=LPF+JM(JSTR1)	\$0	81
	AP(JSTR1)=0.	\$0	82
	RP(JSTR1)=F(LPFI)	\$0	83
	DO 32 J=JS,JE	\$0	84
	LIJ=JM(J)+I	\$0	85
	LXP=NVKM+IJ+1	\$0	86
	LXM=LXP-2	\$0	87
	STORE=SP(LIJ)-AYH(LIJ)*AP(J-1)+1.E-30	\$0	88
	AP(J)=AYP(LIJ)/STORE	\$0	89
32	RP(J)=(SUI(LIJ)+AYP(LIJ)*F(LXP)+AXH(LIJ)*F(LXM)+AYH(LIJ)*BP(J-1))/	\$0	90
	1STORE	\$0	91
	JSUM1=JS+JE	\$0	92
	DO 33 JJ=JS,JE	\$0	93

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J=JSUM1-JJ
LP=LPP+JM(J)
LYP=LP+NI
F(LP)=AP(J)*F(LYP)+BP(J)
CONTINUF
ISWP=3-ISWP
GO TO (30,30),ISWP
30 CONTINUE
GO TO 140,20),IXY
40 CONTINUF
45 CONTINUE
RETURN
C ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** ** * SO 105
ENTRY SOLVE2
C-----CYCLIC T0MA IN Z-DIRECTION.
KEND=N
IF(INV.EQ.3)KFND=NP1
IF(CTDMA(NV).EQ.0)GO TO 606
INOMAX=CTDMA(NV)
DO 605 INO=1,INOMAX
DO 600 J=JSTR,M
IS=IWLI(J,NGOTO)
IE=IWLO(J,NGOTO)
DO 600 I=IS,IE
LIJ=I+JM(J)
LIJNV=LIJ+NVN(NVF(NV))
LPSTR=LIJNV+KM(KSTR)
LPCSTR=I-1+(J-2)*(NI-2)
AP(KSTR)=A7PK(LPCSTR)
BP(KSTR)=A7MK(LPCSTR)
FP(KSTR)=SUH(LPCSTR)+AXMK(LPCSTR)*F(LPSTR-1)+AXPK(LPCSTR)*F(LPSTR+
21)+AYMK(LPCSTR)*F(LPSTR-NI)+AYPK(LPCSTR)*F(LPSTR+NI)
DP(KSTR)=SPK(LPCSTR)
TF(DPK(KSTR)).LT.1.E-30)DP(KSTR)=1.E30
KMTN=KSTR+1
DO 601 K=KMIN,KEND
LPC=I-1+(J-2)*(NI-2)+(K-KSTR)*(NI-2)*(NJ-2)
LP=LTJNV+KM(K)
AP(K)=A7PK(LPC)
BK=A7MK(LPC)
CK=SUH(LPC)+AXMK(LPC)*F(LP-1)+AXPK(LPC)*F(LP+1)+AYMK(LPC)*F(LP-NI)
2 +AYPK(LPC)*F(LP+NI)
DK=SPK(LPC)
RP(K)=BK+BP(K-1)/DP(K-1)
EP(K)=EP(K-1)+BK/DP(K-1)+CK
DP(K)=DK-BK+AP(K-1)/DP(K-1)
IF(DPK(K).LT.1.E-30)DP(K)=1.E30
501 CONTINUF
KSUM=KEND-2+KSTR
APP(KEND-1)=(AP(KEND-1)+BP(KEND-1))/DP(KEND-1)
BP(KEND-1)=FP(KEND-1)/DP(KEND-1)
KENDM2=KEND-2
DO 602 KK=KSTR,KENDM2
KKSUM=KK
APP(K)=(AP(K)+APP(K+1)+BP(K))/(DP(K)+1.0E-30)
BP(K)=(AP(K)+APP(K+1)+EP(K))/(DP(K)+1.0E-30)
502 CONTINUF
DENOM=DP(KEND)-BP(KEND)-APP(KSTR)+AP(KEND)
IF((ABS(CENOM)).LT.1.E-30)DENOM=1.E30
FEND=(APP(KSTR)+AP(KEND)+EP(KEND))/DENOM
KENDM1=KEND-1
DO 603 K=KSTR,KENDM1
LP=LTJNV+KM(K)
F(LP)=APP(K)*FEND+APP(K)

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603	CONTINUE	CTDMA	61
	LPCF=LJNV+KM(KEND)	CTDMA	62
	F(LPCE)=FEND	CTDMA	63
600	CONTINUE	CTDMA	64
601	CONTINUE	CTDMA	65
602	CONTINUE	CTDMA	66
	RETURN	SD	108
	FND	SD	109
	SURROUNITE FPRINT (ISTRAT,ISTOP,NVVV)	FP	2
	COMMON F(3500),DU(500),OV(500),DW(500),	COMFA	2
1	AMUC(500),SNOT1(500),SNOT2(500),FCN(500),FH2(500),FS(500,14),	4STEP	10
1	RHO(500),VIS(500),ABSR(500),SCTR(500),SU(100),SP(100),	RAD	3
1	DRHOOP(500),	RAD	4
1	AXPK(100),AKM(100),AYM(100),AZP(100),	COMFB	4
2	AZM(100),C7(100),CY(100),CZU(100),CYU(100),	COMFB	5
3	CZP(100),CYP(100),DIVG(100),NTP1,NTP2	COMFB	6
1	AXMK(192),AYPK(192),AYM(192),AZPK(192),AZMK(192),	CTDMA	3
2	SUK(192),SPK(192)	CTDMA	4
	DIMENSION U(500),V(500),W(500),PP(500),P(500),TEMP(500)	COMFB	7
	DIMENSION GAM(500)	COMFB	8
	EQUIVALENCE (F(1),U(1)),(F(901),V(1)),(F(1001),W(1))	COMFB	9
	EQUIVALENCE (F(1501),PP(1)),(F(2001),P(1)),(F(2501),TEMP(1))	COMFB	10
	EQUIVALENCE (F(3001),GAM(1))	COMMON	11
	COMMON/CYL/R(30),RM(30),RMV(30),YSR(30),YSVR(30),IPLAK	COMMON	2
	COMMON/GRID/X(40),Y(30),Z(30),XS(40),YS(30),ZS(30),XSU(40),	COMMON	3
1	YSV(30),ZSW(30),XOIF(40),YOIF(30),ZDIF(30),FXP(40),FXM(40),	COMMON	4
2	FYP(30),FYM(30),FZP(30),FZN(30),DT,TIME	COMMON	5
	COMMON	NOX	2
1	/CTNOFX/IDCF, IDFU, IDO2, IDN2, IDH20, IDC02, IDH1, IDH2, IDN1, IDNO, IDNO2	NOX	3
1	,IDH, IDOH, IMCPS, ILC, ILH, IMAT, ITER, JJJ, N1, N2, N3, NA, NGLO8, NGLO8P,	NOX	4
2	NLM, NO, NSM, NS1, NS2, IDCH	4STEP	3
3	/CCHE=I/CPSUM,HSUM,FO,PPLN,RGAS,RGASIN,SINV,TKINV,TLN,LNRG	NOX	6
4	/CPARAM/ASUB(30,3),ENV,ER,HSURO,NOEBUG,NS,PA,00,01,02,03,04,RHOOPP,	NOX	7
4	SM,SMW(30),SMW,S1(30),S2(30),TK,LADIA8,LDEBUG,LEQUIL,LREACT,	NOX	8
4	LENER,EDKIJ,LCONVG	NOX	9
	DOUBLE PRECISION CPSUM,ENV,ER,FQ,HSUB0,HSUM,PA,PPLN,00,01,02,03,	NOX	10
1	04,RGAS,RGASIN,RHOOPP,SM,SMINV,SMW,S1,S2,TK,TKINV,TLN,SMW	NOX	11
2	,FUT,FST	4STEP	4
	COMMON/STEP4/PEXP1,PEXP2,PEXP3,PEXP4,ER1,ER2,ER3,ER4,CB8U1,CB8U2,	4STEP	9
1	CB8U3,CB8U4,AEXP1,AEXP2,AEXP3,AEXP4,BEXP1,BEXP2,BEXP3,BEXP4,	4STEP	6
2	CEXP1,CEXP2,CEXP3,CEXP4,FUT,FST	4STEP	7
	LOGICAL LADIA8,LCONVG,LDEBUG,LEQUIL,LNRG,LREACT,LENER	NOX	12
	COMMON/INT/L,M,N,LCV,MCV,NCV,LP1,MP1,NP1,NT,NJ,MM,MINJ,MINJNK,NV,	COMMON	6
1	NNV,NGCT0,K,ISTR,JSTR,KSTR,NVM(35),KM(30),JM(30),ISTEP,	4STEP	8
2	TSOLVE(32),IPRINT(33),TITLE(10,33),IXY,ISWP,JSWP,RELAX(35),NP,	4STEP	9
3	NRHO,NCAP,ILHI(30,9),IWLO(30,5),JWL0(40,5),JWL1(40,5),TWFI,	COMMON	9
4	IWN,PM1,JWI1,JWI0,JW01,JW00,INW,JKIN(30,30),IKIN(40,30)	COMMON	10
	COMMON/INDEX/IPAP,LPRF,ISTUM,INCNP,ITRAD,NVRX,NVRY,NVRZ,JPLANE	COMMON	11
1	PLAKM1,LVK,LVD,LVFU0X,LVFU,LVCO,LVH,LVRX,LVRY,LVRZ,NVF(32),	4STEP	10
2	IJUMP,IRFS,TITLE2(20),IMAX,JMAX,KMAX,NVC0,FUNCD,NVH20,NVC02,	COMMON	13
3	NVM2,NVC1,NVH2	4STEP	11
	COMMON/CNOX/LVH1,LVH2,LVN1,LVN0,LVN02,LVO,LVOH,LVH20,LVN2,LV02,	NOX	14
!	LVC02,LVFU1,LVCD1,NNOX,INOX,ITNOX,SNOK,TNOX	NOX	17
	COMMON/THERM/NVH,NVFU,NVOK,NVFUOX,NVTE,MODEN,IK,FSTOIC,MFU,CP,	COMMON	19
1	GASCON,RHOCCN,UNICON,PRESS,NVFAV,TCYLW,TINLW,TLIP,ACDEF(4),	COMMON	16
2	T4,DFAC,MFU,WCD2,WCN,WOK,WH20,MM2,MVY,CXX,RATIO1,RATIO2,	COMMON	17
3	RATIO3,RATIC4,HCD,TAM,ITWALL	COMMON	18
	COMMON/CTDMA/KEND,ICTDMA(192)	4STEP	12
C	-----SURROUNITE FPRINT IS USED TO PRINT THE FIELD VALUES OF	COMMENT	191
C	ALL THE DEPENDENT VARIABLES.	COMMENT	192
C	NVV=NVVV-1	COMMENT	193
00	108 NV=ISTRAT,ISTOP	FP	7
	NVV=NVV+	FP	8
		FP	9

```

IF (IPRINT(NVV),EQ,0) GO TO 108
WRITE (6,101) (TITLE(I,NVV),I=1,10)
101 FORMAT (1H0,20(2H*-),10A4,3X,20(2H-*))
KONE=1
IF (NVV.EQ.3) KONE=2
NSKIP=IPRINT(NVV)
DO 100 K=KONE,NP1,NSKIP
WRITE(6,102) K
102 FORMAT(1H0,5BX,4HK = ,I2)
NVKM=NVM(NV)+KM(K)
JONE=1
IF (NVV.EQ.2) JONE=2
IONE=1
IF (NVV.EQ.1) IONE=2
ISTART=IONE-12
103 CONTINUE
ISTART=ISTART+12
IEND=ISTART+11
IEND=MIND(IEND,LP1)
WRITE(6,103) (I,I=ISTART,IEND)
103 FORMAT(1H0,6H I = ,I3,11I10)
WRITE(6,104)
104 FORMAT(2H JJ)
JSUM=JONE+MP1
DO 106 JJ=JONE,MP1
J=JSUM-JJ
LPF=NVKM+JM(J)
LPL=LPF+IEND
LPF=LPF+ISTART
106 WRITE(6,107) J,(F(LP),LP=LPF,LPL)
107 FORMAT(1I9,1P12E10.2)
IF (TFND.LT.LP1) GO TO 105
100 CONTINUE
108 CONTINUE
RETURN
END
SUBROUTINE CREK
C
C A COMPUTER PROGRAM FOR CALCULATION OF
C CHEMICAL REACTION EQUILIBRIUM AND KINETICS
C IN LAMINAR OR TURBULENT FLOWS
C
C CALLING PROGRAM MUST FIRST EXPRESS SPECIES AND ENERGY CONSERVATION
C FINITE-DIFFERENCE EQUATIONS IN THE STANDARD FORMS
C
C AP0$2(I),P = AE0$2(I),E + AH0$2(I),H + AN0$2(I),N + AS0$2(I),S
C           +AH0$2(I),H + AL0$2(I),L + SD(S2(I)) ,   I=1,NS
C DEPT M.E.    WASHINGTON STATE UNIVERSITY
C PULLMAN, WASHINGTON 99163
C MARCH 1976
C DAVID T. PRATT AND JOHN S. WORRECK
C
C ***SUMMARY***
C CREK CONSISTS OF 3 FORTRAN-IV SUBROUTINES: CREK, CREK0, SPECE, CALC, MCPS
C WHICH ENABLES THE EXTENSION OF ANY EXISTING HYDRODYNAMIC COMPUTER
C CODE TO THE CALCULATION OF COMPLEX FLOW WITH CHEMICALLY COMPLEX
C EQUILIBRIUM OR KINETIC STATIONARY STATES
C THIS VERSION OF CREK IS LIMITED TO IDEAL HOMOGENEOUS GAS-PHASE
C CHEMICAL EQUILIBRIUM AND NON-EQUILIBRIUM (KINETIC) STATES
C
C ***CALLING CREK ***
C CALLING PROGRAM SEEKS SOLUTION FOR VALUES AT A POINT P OF MOLE

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FP	34
FP	35
FP	36
FP	37
FP	38
FP	39
FP	40
FP	41
FP	42
FP	43
FP	44
FP	45
NOXXX	1
CREK	3
CREK	4
CREK	5
CREK	6
CREK	7
CREK	8
CREK	9
CREK	10
CREK	11
CREK	12
CREK	13
CREK	14
CREK	15
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CREK	20
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CREK	22
CREK	23
CREK	24
CREK	25
CREK	26
CREK	27
CREK	28
CREK	29

C NUMBERS OF CHEMICAL SPECIES, (S2(I),I=1,NS) AND THE TEMPERATURE TK,
 C GIVEN THE VALUES OF SAME VARIABLES AT NEIGHBORING NODES, AND VALUES
 C AT P AT A PREVIOUS TIME STEP OR ESTIMATES FROM PREVIOUS ITERATION
 C WHERE
 C $AP = AE + AM + AN + AS + AH + AL + APP$
 C AD DENOTES CONVECTIVE AND DIFFUSIVE FLUX COEFFICIENTS
 C AT NEIGHBORING NODES D=E,W,N,S,H AND L, KG/CU M-SEC
 C APP IS INFLUENCE TERM FROM P AT PREVIOUS TIME STEP
 C S2(I) IS THE MOLE NO. OF SPECIES I AT THE POINT P, KG-MOLE/KG
 C S2(I),D IS THE MOLE NO. OF SPECIES I AT NEAR-NODE D,
 C KG-MOLE I/KG
 C SO(S2(I)) IS RATE OF APPEARANCE OF SPECIES I DUE TO
 C CHEMICAL REACTION, KG-MOLES I/CU M-SEC
 C
 C AND
 C $APP_H,P = AEH_E + AHM_W + ANH_N + ASH_S + AHG_H + ALH_L$
 C $+ SO(H)$
 C WHERE
 C H_P IS THE MIXTURE ENTHALPY AT POINT P, J/KG
 C H_D IS THE MIXTURE ENTHALPY AT NEIGHBOR NODES D,
 C SO(H) IS RATE OF HEAT ADDITION TO CONTROL VOLUME BY
 C RADIATIVE AND KINETIC HEATING, J/CU M-SEC
 C
 C CALLING PROGRAM MUST SUPPLY FOLLOWING VARIABLES THROUGH LABLELED
 C COMMON BLOCK /CPARAM/
 C
 C $TK =$ TEMPERATURE AT NODE P, DEGREES KELVIN (ESTIMATE)
 C $PA =$ PRESSURE AT POINT P, PASCALS (INT/SQ M)
 C $FMV = AP$, KG/CU M-SEC
 C $S1(I) = (AE+S2(I),E+AN+S2(I),W...+AL+S2(I),L) / AP$
 C * $S2(I) =$ PREVIOUS SOLUTIONS OR ESTIMATES FOR S2(I)...
 C ** IF TEMP TK IS SET TO ZERO, PROGRAM CONSTRUCTS
 C *** OWN ESTIMATES
 C * $HSUB0 = (AE^4,E+ANH,W...+ALH,L) / AP$, J/KG
 C ** COEFFICIENTS IN EXPRESSION FOLLOWING...
 C $SO(H) = -(00+01*T+02*T^2+03*T^3+04*T^4)$, J/CU M-SEC
 C
 C LADIAN = T --- IGNORES ABOVE EXPRESSION FOR SO(H), TAKES
 C SOURCE(H)=0,C
 C LEQUIL = T --- EQUILIBRIUM SOLUTION SOUGHT
 C * F --- KINETIC SOLUTION SOUGHT
 C LREACT = T --- CHEMICAL REACTION (FAL OR KIN)
 C * F --- ADIABATIC NON-REACTING MIXING
 C LOERUG = T --- INTERMEDIATE DEBUG PRINTING
 C * F --- NO INTERMEDIATE DEBUG PRINTING
 C
 C #RETURN#
 C S2(I),I=1,NS IS THE MOLE NUMBER OF CHEMICAL SPECIES I (KG-MOLE I/KG)
 C TK IS THE TEMPERATURE (DEGREES K) FROM THERMAL ENERGY EQUATION
 C HSUB0 IS STATIC ENTHALPY AT NODE POINT P (J/KG)
 C RHOP IS THE MASS DENSITY AT NODE POINT P (KG/CU M)
 C SM IS RECIPROCAL OF MIXTURE MOLECULAR WEIGHT (KG-MOLE/KG)
 C ASUR(I,3) IS THE SPECIES NAME (HOLLERITH FIELD)
 C
 C #DIMENSIONS#
 C NE = NUMBER OF ELEMENTS (7)
 C NS = NUMBER OF CHEMICAL SPECIES (20)
 C JJ = NUMBER OF CHEMICAL REACTIONS (36)
 C
 C THESE DIMENSIONS MAY BE ADJUSTED BY SIMPLY CHANGING THE
 C FOLLOWING LABLELED COMMON BLOCKS#
 C
 CREK 20
 CPEK 31
 CREK 32
 CREK 33
 CREK 34
 CREK 35
 CREK 36
 CPEK 37
 CREK 38
 CREK 39
 CPEK 40
 CREK 41
 CREK 42
 CPEK 43
 CREK 44
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 CPEK 90
 CPEK 91
 CPEK 92
 CPEK 93

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C C EQUIL...NLM,NS          CPEK    94
C C INDEX...             CPEK    95
C C KINET...             CPEK    96
C C MATRI...NS+2          CPEK    97
C C PARAM...NS            CPEK    98
C C FACT...NS              CPEK    99
C C SPECFC...NS           CPEK   100
C C AND THE FOLLOWING DIMENSION STATEMENT IN ROUTINE CALC WHICH
C SHOULD BE DOUBLE DIMENSIONED FOR IBM MACHINES
C C A(NS+2,NS+3)          CPEK   101
C C
C C DOUBLE PRECISION AL,RO,CPSUM,EMV,ER,FO,HSURO,HSUM,HQ,PA,PI,PPLN,
C 1 Q0,Q1,Q2,Q3,Q4,RGAS,RGASIN,RHOP,SM,SMINV,SMW,SSAVE,SA,S1,S2,TK,
C 2 TKINV,TLN,T,SMO
C C DOUBLE PRECISION EMVSAY,FACTOR,SMALL,TSAVE,KHI,XLD
C C LOGICAL LADTAB,LCONVG,LODEBUG,LEQUIL,LHRCG,LREACT,LEMER
C C
C C COMMON
C 3/CCHEMI/CPSUM,HSUM,FO,PPLN,RGAS,RGASIN,SMINV,TKINV,TLN,LHRCG
C 1/CFOUTL/AL(7,30),ATOM(3,7),HO(7),PI(7)
C 1/CTINDEX/IDCO,IDFU,IDOH,IDON2,IDH20,IDCO2,IDH1,IDH2,IDN1,IDNO,IDNO2
C 1,TD0,TD0H,IHCPS,ILC,ILH,IMAT,ITER,JJ,N1,N2,N3,NA,MGLOB,MGLOBP,
C 2,NI,NO,NSM,NS1,NS2,IOCH
C 1/CPARAM/ASUR(30,3),EMV,ER,HSURO,MDEBUG,NS,PA,Q0,Q1,Q2,Q3,Q4,RHOP,
C 1,SM,SMW(30),SMO,S1(30),S2(30),TK,LADTAB,LDEBUG,LEQUIL,LREACT,LEMER
C 2,FDTIJ,LCONVG
C 1/CSPECFC/HO(30),SO(30),SSAVE(30),Z(7,2,30)
C
C *****
C THIS SUBROUTINE IS THE MAIN EQUILIBRIUM AND KINETIC SOLUTION ROUTINE.
C THE CALLING PROGRAM MUST SUPPLY ALL THE VARIABLES EXCEPT RHOP AND SM
C THROUGH THE LABELLED COMMON BLOCK CPARAM IN SI UNITS. BOTH EQUIL
C SOLUTIONS (LEQUIL=1) -- BY MINIMIZATION OF THE GIBBS FUNCTION --
C AND KINETIC (LEQUIL=2) SOLUTIONS ARE CALCULATED BY A MF7 .-RAPHSON
C TECHNIQUE. CPEK ALSO CONTROLS THE LOGIC FOR PROBLEM CELLS
C REFERENCE CPEK (WASHINGTON STATE UNIVERSITY) MARCH 1976
C *****
C
C DATA FACTOR/5.000/,SMALL/1.0D-6/
C
C C #NORMAL SOLUTION#00
C
C DETERMINE EQUIVALENCE RATIO AND IF OUTSIDE INTERVAL (0,1,10) ASSUME
C NO REACTION AND RETURN ADIABATIC NON-REFACTED MIXTURE PROPERTIES
C SAVE GIVEN ESTIMATES OR PROGRAM GENERATED ESTIMATES IF TK IS SMALL
C IF SOLUTION IS SUCCESSFUL, RETURN TO CALLING ROUTINE OTHERWISE.
C ENTER PROBLEM CELL LOGIC BELOW
C LCONVG=.TRUE.
C
C CALL EPATC
C IF (1,NOT,LODEBUG) GO TO 30
C WRITE(6,10) LFACT,LEQUIL,LADTAB,EMV,ER,HSURO,Q0,Q1,Q2,Q3,Q4,PA,TK
C 10 FORMAT(3X,3L3,1P10D12.3)
C IF (NDEBUG,ER,1) GO TO 30
C WRITE(6,20) (S1(I),I=1,NS)
C WRITE(6,20) (S2(I),I=1,NS)
C 20 FORMAT(1X,1P10D12.3)
C 30 IF (1,NET,LREACT) GO TO 400
C EMVSAY=EMV

```

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C      11.52609 IS E-LOG OF STD PATH=101325.0 N/M442          CREK    155
C      PPLM=DLOG(PA)=11.5260 .00          CREK    156
C      TSAVE=TK          CREK    157
C      DO 40 I=1,NS          CREK    158
C      40 SSAVE(I)=S2(I)          CREK    159
C      IF (TK.LT.SMALL) GO TO 100          CREK    160
C
C      CALL SPEC
C
C      IF (LCNVG) GO TO 900          CREK    161
C      DO 101 I=1,NS          CREK    162
C      IF(S2(I).LT.2.00-20)S2(I)=S1(I)          CREK    163
C      101 CONTINUE          NOXX    12
C      IF(.NOT.LCNVG)GO TO 900          NOXX    13
C
C      ****PROBLEM CEIL000          NOXX    14
C
C      SOLUTION LOGIC IS DIFFERENT FOR FOUR TYPES OF PROBLEMS AS FOLLOWS          NOXX    15
C      MODE 1 ... LEQUIL = T, LADIAR = T          CREK    165
C      MODE 2 ... LEQUIL = T, LADIAB = F          CREK    166
C      MODE 3 ... LEQUIL = F, LADIAR = T          CREK    167
C      MODE 4 ... LEQUIL = F, LADIAB = F          CREK    168
C
C      ALWAYS TRY RT=0.0 (LNRC=F) AFTER SOLUTION FAILURE WHEN LEQUIL=F.          CREK    169
C      LOGIC TO FIND SOLUTION IS CONTROLLED IN CHAPTERS 1 AND 2 BELOW          CREK    170
C      WHEREIN EACH SECTION, NEW ESTIMATES ARE DETERMINED EITHER BY          CREK    171
C      SAVED GIVEN ONES, NEW ASSIGNED ONES, OR SOLUTION FOUND NOT AT          CREK    172
C      REQUIRED CONDITIONS. THE VARIABLES NEXTOK AND NEXTNG ARE ASSIGNED          CREK    173
C      THE STATEMENT NUMBERS OF WHERE TO GO IF THE SOLUTION ATTEMPT IS          CREK    174
C      SUCCESSFUL OR NOT, RESPECTIVELY.          CREK    175
C
C      ASSIGN 900 TO NEXTOK          CREK    176
C      ASSIGN 100 TO NEXTNG          CREK    177
C      GO TO 520          CREK    178
C
C      ****EQUILIBRIUM***          CREK    179
C      THIS CHAPTER MAKES EQUILIBRIUM ESTIMATES AND INITIATES STRATEGY FOR          CREK    180
C      CASES IN WHICH CONVERGENCE WAS NOT ACHIEVED ON FIRST CALL TO SPEC          CREK    181
C
C      100 MODE=4          CREK    182
C      IF (LEQUIL) MODE=MODE-2          CREK    183
C      IF (LADIAR) MODE=MODE-1          CREK    184
C      LEQUIL=.TRUE.          CREK    185
C      LADIAR=.TRUE.          CREK    186
C      IF (MODE.LT.3.0R.TK.LT.SMALL) GO TO 170          CREK    187
C
C      -----FIRST USE GIVEN ESTIMATES FOR EQUIL SOLN IN MODE 3 AND 4 PROBLEMS          CREK    188
C
C      TK=TSAVE          CREK    189
C      DO 120 I=1,NS          CREK    190
C      120 S2(I)=SSAVE(I)          CREK    191
C      ASSIGN 200 TO NEXTOK          CREK    192
C      ASSIGN 170 TO NEXTNG          CREK    193
C      GO TO 500          CREK    194
C
C      -----GARBAGE ESTIMATES (GORDON AND MCARDELL)          CREK    195
C
C      170 TK=3800.000          CREK    196
C      SM=0.100/FLOAT(NS)          CREK    197
C      DO 171 I=1,NS          NOXXX    6
C

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171 S2(I)=SM
SM=0.1NC
IF (IMODE.EQ.1) ASSIGN 900 TO NEXTOK
IF (IMODE.EQ.2) ASSIGN 300 TO NEXTOK
IF (IMODE.EQ.3) ASSIGN 200 TO NEXTOK
ASSIGN 600 TO NXXTNG
GO TO 300
C
C   00  00  00  00  00  00  00  00  00  00  00  00  CHAPTER 2  00  00  00
C   00  00  00  00  00  00  00  00  00  00  00  00  CHAPTER 2  00  00  00
C
C   ***KINETIC****
C   SECTION FOR KINETIC SOLUTION FROM ADIABATIC EQUILIBRIUM ESTIMATES
C   (IMODE 3 AND 4 ONLY)
C
C-----NEAR-EQUILIBRIUM SOLUTION (KINETIC WITH EMV=1.00E-3 KG/CU M-SEC)
C
200 LFAULT=.FALSE.
IX=0
EMV=1.00E-3
XL0=FMV
C-----INCREASE MINOR SPECIES FROM EQUILIBRIUM ESTIMATES
DO 201 I=1,NS
IF (S2(I).LT.SMALL) S2(I)=SMALL
201 CONTINUE
ASSIGN 230 TO NEXTOK
ASSIGN 210 TO NXXTNG
GO TO 500
C
C
C-----FAILURE ON NEAR-EQUIL WITH EMV=XL0, DECREASE EMV BY AN ORDER OF
C-----MAGNITUDE AND ATTEMPT AGAIN, ITERATING THIS WAY UP TO 12 TIMES
C
210 EMV=EMV*0.100
XL0=FMV
IX=IX+1
IF (IX.EQ.12) GO TO 610
TK=TSAVE
DO 211 I=1,NS
211 S2(I)=SSAVE(I)
ASSIGN 230 TO NEXTOK
ASSIGN 210 TO NXXTNG
GO TO 500
C
C
C-----HAVE NEAR-EQUIL SOLUTION, SO FIRST TRY DIRECTLY TO OBTAIN
C-----REQUIRED SOLUTION AT GIVEN EMV
C
230 EMV=EMVSAY
IF (IMODE.EQ.3) ASSIGN 900 TO NEXTOK
IF (IMODE.EQ.4) ASSIGN 300 TO NEXTOK
ASSIGN 230 TO NXXTNG
GO TO 500
C
C   ***UPPER BRANCH MARCHING***
C   HAVE A KINETIC SOLUTION BUT AT EMV .LT. EMVSAY. START AT
C   KNOWN SOLUTION AND INCREASE EMV BY FACTOR TO MOVE TOWARDS
C   A SOLN THERE, IF SUCCESSFUL, REPEAT UNTIL EMVSAY IS REACHED. IF
C   NOT SUCCESSFUL START HALF INTERVAL SEARCHING DESCRIBED BELOW
C
250 FMV=XL0*FACTOR
IF (EMV.GT.EMVSAY) EMV=EMVSAY
XHT=FMV
IT=0

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250

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ORIGINAL PAGE IS
OF POOR QUALITY

ORIGINAL PAGE IS
OF POOR QUALITY

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TK=TSAVE
DO 251 I=1,NS
251 S2(I)=SSAVE(I)
ASSIGN 250 TO NEXTOK
IF (EMV.GE.FMVSAV.AND.MODE.EQ.3) ASSIGN 900 TO NEXTOK
IF (EMV.GE.FMVSAV.AND.MODE.EQ.4) ASSIGN 900 TO NEXTOK
ASSIGN 270 TO NEXTNG
GO TO 300

C
C ***HALF-INTERVAL SEARCHING*** 
C HAVE SOLUTION AT XLC BUT NOT AT XHI. HENCE START INTERVAL
C SEARCHING BY SETTING EMV TO THE LOGARITHMIC AVERAGE
C IF ITERATING MORE THAN TEN TIMES, TERMINATE.
C

270 IX=IX+1
TK=TSAVE
DO 271 I=1,NS
271 S2(I)=SSAVF(I)
IF (IX.GT.10) GO TO 620
EMV=DSORT(XLO*XHI)
XHT=EMV
ASSIGN 250 TO NEXTOK
ASSIGN 270 TO NEXTNG
GO TO 300

C
C***NON-ADIABATIC*** 
C SECTION FOR NON-ADIABATIC SOLUTIONS FROM ADIABATIC ESTIMATES
C (MODE 2 AND 4 ONLY)
C TRY DIRECTLY TO OBTAIN NON-ADIABATIC SOLUTION IF NOT SUCCESSFUL,
C START HALF-INTERVAL SCALING FROM THE ADIABATIC SOLUTION BY
C DEFINING A SCALING FACTOR FO (0.0-1.0) TO MULTIPLY THE NON-ADIABATIC
C TERM (O) IN THE ENERGY EQUATION IN SPEC
C

300 LADTAB=.FALSE.
XLO=0.000
XHI=1.000
FO=1.000
IX=0
310 ASSIGN 320 TO NEXTOK
ASSIGN 330 TO NEXTNG
GO TO 900

C
320 IF (FO.EC.1.000) GO TO 900
XLO=FO
FO=1.000
XHI=1.000
IX=0
GO TO 310

C
330 IX=IX+1
IF (IX.GT.10) GO TO 340
TK=TSAVE
DO 331 I=1,NS
331 S2(I)=SSAVF(I)
FO=0.500*(XLO+XHI)
XHT=FO
GO TO 310

C
340 FO=1.000
GO TO 630
C

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CREK	279
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CREK	342

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C*****      *****      *****      *****      *****      *****      CHAPTER 4      *****
C*****      *****      *****      *****      *****      *****      CHAPTER 4      *****
C
C ***FAILURE EXITS***  

C FAILED EQUIL OR KINETIC SOLN OR EQUIV RATIO OUTSIDE (0.1,10)  

C RETURN ADIABATIC, NON-REACTED MIXTURE PROPERTIES  

400 SM=0.000  

    DO 401 I=1,NS  

    S2(I)=S1(I)  

    SM=SM+S2(I)  

401 CONTINUE  

    TK=1000.000  

    XLO=TK  

    IMCPS=1  

    NS1=1  

    NS2=NS  

    TKINV=1.0D-3  

    DO 403 I=1,30  

    CALL HCPS  

    HSUM=0.000  

    DO 402 K=1,NS  

    HSUM=HSUM+H0(K)*S2(K)  

402 CONTINUE  

    IF(.NOT.LADIAB)HSUM=HSUM+((Q4*TK+Q3)*TK+Q2)*TK+Q1+Q0*TKINV)/  

    (RGAS*EMV)  

    TK=TK*(1.0D+0.500*(HSUB0*RGASIN*TKINV-HSUM)/CPSUM)  

    TKINV=1.0D/TK  

    XHI=DARS(TK-XLO)  

    XLO=TK  

    IF (XHI.LT.1.000) GO TO 404  

403 CONTINUE  

404 CONTINUE  

    IF(.NOT.LADIAB)HSUB0=HSUM*RGAS/TK  

C  

    GO TO 900  

C
C*****      *****      *****      *****      *****      *****      CHAPTER 5      *****
C*****      *****      *****      *****      *****      *****      CHAPTER 5      *****
C
C ***PROBLEM CELL CALL TO SPECIE***  

C TAKE THE ESTIMATES GENERATED IN CHAPTERS 1,2 AND ATTEMPT A SOLUTION  

C WITH FULL EQUATIONS. IF SUCCESSFUL, UPDATE THE SAVE ANSWERS WITH THE  

C SOLUTION AND RETURN TO STATEMENT NUMBER NEXTNG. IF NOT, THE ACTION  

C DEPENDS ON WHETHER AN EQUILIBR OR KINETIC SOLN IS SOUGHT. FAILED  

C EQUIL SOLN, RETURN TO STATEMENT NUMBER NEXTNG, WHILE FAILURE IN A  

C KINETIC SOLN WILL BE FOLLOWED BY AN ATTEMPT WITH LNRCG=F --- RT=0.0  

C AND SAME ESTIMATES. SETTING RT=0.0 IMPLIES THAT A CHANGE IN TEMP  

C FIELD HAS NO EFFECT ON SPECIES DISTRIBUTION FOR THAT PARTICULAR  

C ITERATION, BUT DOES ALLOW THE SPECIES CHANGES TO INFLUENCE THE TEMP  

C CHANGE --- PARTIAL DECOUPLING OF THE ENERGY EQUATION.  

C IF STILL NO GOOD, RETURN TO STATEMENT NUMBER NEXTNG.  

C  

500 CALL SPECF  

    IF (LCONVG) GO TO 540  

C  

    SOLUTION FAILED TRY RT=0.0  

    IF (LNRCG) GO TO 520  

    LNRCG=.TRUE.  

510 GO TO NEXTNG, (100,170,210,250,270,330,600)  

520 IF (LFCUTL) GO TO 510  

530 LNRCG=.FALSE.  

    GO TO 500  

540 IF (LNRCG) GE TO 550  

    LNRCG=.TRUE.  

C

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C      GO TO 500      *REMOVED PER D.T.PRATT 7/19/7800
C*****IF COMPLEX CASES DO NOT CONVERGE, IT MAY BE NECESSARY TO*****
C*****RETURN THIS STATEMENT TO THE PROGRAM.      ****
C
C
C-----SOLUTION IS SUCCESSFUL, UPDATE SAVE ANSWERS AND CONTINUE.
C
C      550 TSAVE=TK
C         00 560 I=1,NS
C      560 SSAVE(I)=S2(I)
C
C      GO TO NEXTOK, (200,230,250,300,320,900)
C
C*****      000000      000000      000000      CHAPTER 6      000000      CREK      408
C*****      000000      000000      000000      CHAPTER 6      000000      CREK      409
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C
C-----RESTORE FAILED PROBLEM MODE PRIOR TO RETURN
C
C      650 IF (MODE.EQ.2) LADIAB=.FALSE.
C         IF (MODE.EQ.3) LEQUIL=.FALSE.
C         IF (MODE.EQ.4) LADIAB=.FALSE.
C         GO TO 400
C
C-----FAILED NON-ADIAHATIC SOLUTION...RETURN ADIAHATIC
C-----EQUIL OR KINETIC SOLUTION
C
C      670 TK=TSAVE
C         SM=0.000
C         DO 671 I=1,NS
C            S2(I)=SSAVE(I)
C 671   SM=SM+S2(I)
C 900   RHOP=PA/(RGAS*TK*SM)
C         RETURN
C         END
C         SUBROUTINE CALC
C
C         DOUBLE PRECISION AL,BQ,CPSUM,EMV,ER,FQ,HSUB0,HSUM,HQ,PA,PI,PPLN,
C 1  OO,Q1,Q2,Q3,Q4,RGAS,RGASIN,RHOP,SM,SMINV,SM,SSAVE,S0,S1,S2,TK,
C 2  TKINV,TLN,Z,SM
C         DOUBLE PRECISION RK,RX2,TACT,TACT2,TEM,TEM2,T1,X2,CERU
C         DOUBLE PRECISION XCYH,FUT,FST,SSS
C         DOUBLE PRECISION X,Y
C         DOUBLE PRECISION ANG,BIG,RXX,DSUM,EN,HH,HEH,Q,QDRV,RHSM,RHSQ,
C 1  RM,RT,R1,R2,SS,SUM,S2,T1,T2,TM1,TM2,TM3,TN2,XC,YH
C         LOGICAL LADTAB,LCCNVG,DEBUG,LEQUIL,LNRG,LREACT,LENER
C
C

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      DOUBLE PRECISION RLAM,RTURA,PHT
      THE FOLLOWING DOUBLE PRECISION REQUIRED ONLY FOR IBM MACHINES
      DOUBLE PRECISION A,DTM1

      COMMON
      3/CCHEMI/CPSUM,HSUM,FQ,PPLN,RGAS,RGASIM,SHINV,TKINV,TLM,LMRG
      1/CEQUIL/AL(7,30),ATOM(3,7),R0(7),PI(7)
      1/CINDFX/IDCO,INFO1,IO02,IDH2,IDH20,IDCO2,IDH1,IDH2,IDM1,IDM2,IDN02
      1,ID00,ID0H,IHCPS,ILC,ILH,IMAT,ITER,JJ,N1,N2,N3,NA,NGL08,NGL0P,
      2,MLM,NQ,NSM,NS1,NS2,IDCH
      1/CMATR/X(32),Y(32)
      1/CPARAM/ASUB(30,31),ENV,ER,HSUB0,NDEBUG,NS,PA,OO,O1,O2,O3,O4,RHOP,
      1,SM,SNW(30),SM0,S1(30),S2(30),TK,LADIAB,LDEBUG,LREACT,LENER
      2,ENKIJ,LCNVG
      1/CREACT/RX(36),BX2(36),ID(6,36),MDR(36),TACT(36),TACT2(36),
      2,TEN(36),TEN2(36),X1(36),X2(36),CEBU(36)
      1/CSPEC/EQ(30),SO(30),SSAVE(30),Z(7,2,30)
      COMMON/STEP4/PEXP1,PEXP2,PEXP3,PEXP4,ER1,ER2,ER3,ER4,CEBU1,CEBU2,
      1,CEBU3,CEBU4,AEXP1,AEXP2,AEXP3,AEXP4,BEXP1,BEXP2,BEXP3,BEXP4,
      2,CEXP1,CEXP2,CEXP3,CEXP4,FUT,FST

C
C ***** THIS SUBROUTINE CONSTRUCTS THE NEWTON-RAPHSON DERIVATIVE MATRIX FOR
C ***** BOTH KINETIC AND EQUILIBRIUM SOLUTIONS AND SOLVES IT BY PIVOTAL
C ***** GAUSSIAN REDUCTION. WHENEVER TEMP IS LESS THAN 1500K, THE REVERSE
C ***** RATE IS CALCULATED FROM THE FORWARD RATE AND EQUILIBRIUM CONSTANT.
C ***** PROVISION IS MADE FOR GLOBAL REACTIONS
C ***** REFERENCE CREK (WASHINGTON STATE UNIVERSITY) MARCH 1976
C
      DIMENSION A(32,33)
      DATA RIG/46.05100/
      DO 10 I=1,NO
      X(I)=0.0
      DO 10 K=1,NA
      10 A(I,K)=0.000
      THCPS=1
      IF (LFOUIL) IMCPS=2
      IF (TK.LT.1500.0001) IMCPS=2
      NS1=1
      NS2=NS
      CALL HCPS
      WIN=HSUB0*RGASIN*TKINV
      O=0.000
      ORRV=0.000
      IF (LADIAB) GO TO 20
      C-----0 AND ORRV ARE NON-DIMENSIONAL
      TM1=FQ/(ENV*RGAS)
      O=((((O4+TK+Q3)*TK+Q2)*TK+Q1+OO*TKINV)*TM1
      ORRV=((((4.000*O4+TK+3.000*Q3)*TK+2.000*Q2)*TK+Q1)*TM1
      20 CONTINUE
      IF (LFOUIL) GO TO 300
      RHSM=PAB*RGASIN*TKINV
      RHOP=RHSM+SHINV
      RHCO=RHOP*OO2
      **** CHAPTER 1 ****
      **** CHAPTER 1 ****

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ORIGINAL EDITION
OF POOR GRAMMAR

GLOBAL REACTIONS
OF POOR QUALITY

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C
C ***GLOBAL REACTION***          CALC    61
C GLOBAL RATE EQUATIONS FOR HYDROCARBON PYROLYSIS...  CALC    62
C GLOBAL RATE EXPRESSIONS DUE TO KOLLRACK...   CALC    63
C (1) C12H23 + O2 --- 5 C2H4 + C2H3 + O2  CALC    64
C (2) C12H23 + OH --- 6 C2H4 + O  CALC    65
C
C IF (NGLOR,EQ,0) GO TO 110  CALC    66
C IF (TK,LT,500,00) GO TO 110  CALC    67
C DO 100 J=1,NGLOR  CALC    68
C I=ID(1,J)  CALC    69
C K=ID(2,J)  CALC    70
C M=ID(4,J)  CALC    71
C N=ID(5,J)  CALC    72
C IF (I,FQ,1DFU,AND,M,EQ,1DH,AND,N,EQ,1DH2) GO TO 190  4STEP  350
C IF (I,FQ,1DCO,AND,K,EQ,1D02) GO TO 160  4STEP  351
C IF (I,EQ,1DCO,AND,K,EQ,1D02) GO TO 170  4STEP  352
C IF (I,EQ,1DH2,AND,K,EQ,1D02) GO TO 180  4STEP  353
C IF (M,EQ,1DCO,AND,N,EQ,1DH2) GO TO 105  CALC    73
C IF (M,EQ,1DCO,AND,N,EQ,1DH2) GO TO 111  NOXX   35
C IF (I,EQ,1DCO,AND,K,EQ,1D02) GO TO 121  NOXX   36
C TK1=TACT(J)*TKINV  CALC    74
C TM2=TK1-TEM(J)*TLM-BX(J)  CALC    75
C IF (DABS(TM2).GT.RIG) GO TO 100  CALC    76
C R1=DEXP(-TM2)  CALC    77
C
C -----PROVISION FOR CONTACT INDEX  CALC    78
C R1=X1(J)*R1  CALC    79
C R1=R1*S2(J)*RHS0*S2(K)  CALC    80
C RT=R1*(TEM(J)+TK1-2.00)  CALC    81
C RN=R1*2.00  CALC    82
C -----A(ANY,M)=A(ANY,N)=0 BECAUSE NO REVERSE REACTION ASSUMED  CALC    83
C A(I,I)=A(I,I)+R1  CALC    84
C A(T,K)=A(T,K)+R1  CALC    85
C A(I,NA)=A(I,NA)-R1  CALC    86
C A(T,NSM)=A(T,NSM)-RN  CALC    87
C A(I,NO)=A(I,NO)+RT  CALC    88
C A(N,I)=A(N,I)-R1  CALC    89
C A(N,K)=A(N,K)-R1  CALC    90
C A(N,NA)=A(N,NA)+R1  CALC    91
C A(N,NSM)=A(N,NSM)+RN  CALC    92
C A(N,NO)=A(N,NO)-RT  CALC    93
C AND=5.00  CALC    94
C IF (J,FQ,1) GO TO 101  CALC    95
C A(K,I)=A(K,I)+R1  CALC    96
C A(K,K)=A(K,K)+R1  CALC    97
C A(K,NA)=A(K,NA)-R1  CALC    98
C A(K,NSM)=A(K,NSM)-RN  CALC    99
C A(K,NO)=A(K,NO)+RT  CALC    100
C AND=6.00  CALC    101
C 101 CONTINUE  CALC    102
C R1=R1+AND  CALC    103
C RN=RN+ANC  CALC    104
C RT=RT+AND  CALC    105
C A(M,I)=A(M,I)-R1  CALC    106
C A(M,K)=A(M,K)-R1  CALC    107
C A(M,NA)=A(M,NA)+R1  CALC    108
C A(M,NSM)=A(M,NSM)+RN  CALC    109
C A(M,NO)=A(M,NO)-RT  CALC    110
C GO TO 200  CALC    111
C 105 CONTINUE
C ***GLOBAL REACTION***          CALC    112
C GLOBAL RATE EQUATIONS FOR HYDROCARBON PYROLYSIS...  CALC    113
C GLOBAL RATE EXPRESSION DUE TO ROELMAN AND FORTUNE  CALC    114
C
C

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C      CHXY + (X/2) O2 ---- X CO + (Y/2) H2          CALC    119
C
C      XC=AL(ILC,I)
C      YH=AL(ILH,I)
C      TK1=TACT(J)*TKINV
C      TM2=TK1-BX(J)-(0.3*PPLN)
C      IF(TEM(J).NE.0.C.1TM2=TM2-TEM(J)*TLN
C      IF(DARS(TM2).GT.BIG)GO TO 100
C      R1=DEXP(-TM2)
C
C      -----PROVISION FOR CONTACT INDEX
C      R1=Y1(J)*R1
C      R1=R1*(RHOP*S2(K))*DSORT(RHOP*S2(I))
C      TM1=R1*0.5
C      A(I,I)=A(I,I)+TM1
C      A(I,K)=A(I,K)+R1
C      A(K,I)=A(K,I)+R1*XC*0.25
C      A(K,K)=A(K,K)+TM1*XC
C      A(M,I)=A(M,I)-TM1*YC
C      A(M,K)=A(M,K)-R1*YC
C      A(N,I)=A(N,I)-R1*YH*0.25
C      A(N,K)=A(N,K)-TM1*YH
C      -----A(NY,M)=A(NY,N)=0 BECAUSE NO REVERSE REACTION ASSUMED
C      RN=R1*1.5
C      A(I,NSM)=A(I,NSM)-RN
C      A(K,NSM)=A(K,NSM)-RN*XC*0.5
C      A(M,NSM)=A(M,NSM)+RN*XC
C      A(N,NSM)=A(N,NSM)+RN*YH*0.5
C      A(I,NA)=A(I,NA)-R1
C      A(K,NA)=A(K,NA)-R1*XC*0.5
C      A(M,NA)=A(M,NA)+R1*XC
C      A(N,NA)=A(N,NA)+R1*YH*0.5
C      IF (.NOT.LNRG) GO TO 100
C      RT=R1*(TK1+TFN(J)-1.5)
C      A(I,NO)=A(I,NO)+RT
C      A(K,NO)=A(K,NO)+RT*XC*0.5
C      A(M,NO)=A(M,NO)-RT*XC
C      A(N,NO)=A(N,NO)-RT*YH*0.5
C      GO TO 100
111 CONTINUE
C      ***GLOBAL REACTIONS***
C      FLORAL RATE EQUATIONS FOR 2-STEP REACTION.
C      FIRST STEP   CHXY+(X/2+Y/4)O2 ---- XCO+(Y/2)H2O
C
C      XC=AL(ILC,I)
C      YH=AL(ILH,I)
C      TK1=TACT(J)*TKINV
C      TM2=TK1-BX(J)-TFN(J)*TLN
C      IF(DARS(TM2).GT.BIG)GO TO 100
C      R1=DEXP(-TM2)
C
C      -----PROVISION FOR CONTACT INDEX.
C      R1=Y1(J)*R1
C      R1=R1*(RHOP*S2(K))*DSORT(RHOP*S2(I))
C      RLAM=R1
C      PHI=DMIN1(S2(I),S2(K)/(XC+0.25*YH))
C      RTURR=(CFLU(J)*RHOP*PHI*EOKIJ
C      TFIRLAM,LT,RTURR)GO TO 130
C      P1=RTURR
C      FN=1.000
C      TFIS2K/(XC+0.25*YH),LT,S2(I))GO TO 131
C      R1T=RTURR
C      R1K=0.0
C      GO TO 132

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131 R1T=0.0
 R1K=RTURN
 GO TO 132
 130 R1I=0.500*RLAM
 R1K=RLAM
 R1=RLAM
 EN=1.302
 132 CONTINUE
 $A(I,I)=A(I,I)+R1I$
 $A(I,K)=A(I,K)+R1K$
 $A(K,I)=A(K,I)+R1I+0.5*(XC+0.5*YH)$
 $A(K,K)=A(K,K)+0.5*R1K*(XC+0.5*YH)$
 $A(M,I)=A(M,I)-R1I*XC$
 $A(M,K)=A(M,K)-R1K*XC$
 $A(N,I)=A(N,I)-R1I*YH+0.5$
 $A(N,K)=A(N,K)-0.5*R1K*YH$
 C-----A(ANY,N)=A(ANY,N)=0 BECAUSE NO REVERSE REACTION ASSUMED.
 RN=R1*EN
 $A(I,NSM)=A(I,NSM)-RN$
 $A(K,NSM)=A(K,NSM)-RN+0.5*(XC+0.5*YH)$
 $A(M,NSM)=A(M,NSM)+RN*XC$
 $A(N,NSM)=A(N,NSM)+RN*YH+0.5$
 $A(I,NA)=A(I,NA)-R1$
 $A(K,NA)=A(K,NA)-R1+0.5*(XC+0.5*YH)$
 $A(M,NA)=A(M,NA)+R1*XC$
 $A(N,NA)=A(N,NA)+R1*YH+0.5$
 IF(.NOT.LNRG)GO TO 100
 IF(RTURN.LT.RLAM)GO TO 100
 RT=R1*(TK1+TEN(J)-1.5)
 $A(I,NO)=A(I,NO)+RT$
 $A(K,NO)=A(K,NO)+RT+0.5*(XC+0.5*YH)$
 $A(M,NO)=A(M,NO)-RT*XC$
 $A(N,NO)=A(N,NO)-RT*YH+0.5$
 GO TO 100
 121 CONTINUE
 C ***GLOBAL REACTION***
 C GLOBAL RATE EQUATIONS FOR 2-STEP REACTION.
 C SECOND STEP CO+(1/2)O2 --- CO2
 C
 $TK1=TACT(J)*TK1INV$
 $TM2=TK1-BX(J)-TEH(J)*TLN$
 IF(DABS(TM2).GT.0.016)GO TO 100
 R1=DEXP(-TM2)
 C-----PROVISION FOR CONTACT INDEX.
 $R1=X1(J)*R1$
 $R1=R1*RHSQ*S2(K)*S2(I)$
 RLAM=R1
 $PHI=DMIN1(2.0*S2(K),S2(I))$
 RTURA=CEPU(J)*RHDP*PHI*ENDKIJ
 TF(RLAM,LT,RTURA)GO TO 140
 R1=RTURN
 EN=1.000
 TF(2.0*S2(K),LT,S2(I))GO TO 141
 R1I=RTURA
 $R1K=0.0$
 GO TO 142
 141 R1I=0.0
 R1K=RTURN
 GO TO 142
 140 R1I=RLAM
 R1K=RLAM
 R1=RLAM
 EN=2.000

ORIGINAL PAGE IS
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NOXX	63
NOXX	64
NOXX	65
NOXF	66
NOXX	67
NOXX	68
NOXX	69
NOXX	70
NOXX	71
NOXX	72
NOXX	73
NOXX	74
NOXX	75
NOXX	76
NOXX	77
NOXX	78
NOXX	79
NOXX	80
NOXX	81
NOXX	82
NOXX	83
NOXY	84
NOXX	85
NOXX	86
NOXX	87
NOXX	88
NOXX	89
NOXX	90
NOXX	91
NOXX	92
NOXX	93
NOXX	94
NOXX	95
NOXX	96
NOXX	97
NOXX	98
NOXX	99
NOXX	100
NOXF	101
NOXX	102
NOXX	103
NOXX	104
NOXX	105
NOXX	106
NOXY	107
NOXX	108
NOXX	109
NOXX	110
NOXX	111
NOXX	112
NOXX	113
NOXX	114
NOXX	115
NOXX	116
NOXX	117
NOXX	118
NOXY	119
NOXX	120
NOXX	121
NOXX	122
NOXX	123
NOXX	124
NOXX	125
NOXX	126

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142 CONTINUE
A(I,I)=A(I,I)+R1I
A(I,K)=A(I,K)+R1K
A(K,I)=A(K,I)+0.5*R1I
A(K,K)=A(K,K)+0.5*R1K
A(M,I)=A(M,I)-R1I
A(M,K)=A(M,K)-R1K
C=====A(NY,M)=A(ANY,N)=0 BECAUSE NO REVERSE REACTION ASSUMED.
RN=R1+EN
A(I,NSM)=A(I,NSM)-RN
A(K,NSM)=A(K,NSM)-RN*0.5
A(M,NSM)=A(M,NSM)+RN
A(I,NA)=A(I,NA)-R1
A(K,NA)=A(K,NA)-R1*0.5
A(M,NA)=A(M,NA)+R1
IF(NDNT,LNRG)GO TO 100
IF(RTURB,LT,RLAM)GO TO 100
RT=R1*(TK1+TEM(J)*2.0)
A(I,NO)=A(I,NO)+RT
A(K,NO)=A(K,NO)+RT*0.5
A(M,NO)=A(M,NO)-RT
GO TO 100
150 CONTINUE
C ***GLOBAL REACTION***
C GLOBAL RATE EQUATIONS FOR 4-STEP REACTION.
C FIRST STEP CXHY --- CXHY-2+H2
C
XC=AL(ILC,I)
YH=AL(ILH,I)
TACT(J)=ER1
TEM(J)=0.000
CERU(J)=CEBU1
RX(J)=PEXP1
TK1=TACT(J)*TKINV
TM2=TK1-RX(J)-TEM(J)+TLN
IF(DARS(TM2),GT,0.01)GO TO 100
R1=DEXP(-TM2)

C-----PROVISION FOR CONTACT INDEX.
R1=X1(J)*R1
R1=R1*((RHCP*S2(IDFU))**AEXP1)*((RHOP*S2(IDO2))**BEXP1)
1=((RHOP*S2(IDCH))**CEXP1)
PLAM=R1
PHT=S2(I)
RTURR=CERU(J)*RHOP*PHI*EDKIJ
IF(RLAM,LT,RTURR)GO TO 151
R1=RTURR
EN=1.000
R1I=RTURR
R1M=0.0
R1O2=0.0
GO TO 152
151 R1I=AEXP1*RLAM
R1O2=BEXP1*RLAM
R1M=CEXP1*RLAM
R1=RLAM
FH=AEXP1+BEXP1+CEXP1
152 A(I,I)=A(I,I)+R2I
A(T,M)=A(T,M)+R3M
A(I,IDO2)=A(I,IDO2)+R1O2
A(M,I)=A(M,I)-R1I
A(M,M)=A(M,M)-R1M
A(M,IDO2)=A(M,IDO2)-R1O2
A(M,I)=A(M,I)-R1I

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	NOXX	127
	NOXX	128
	NOXX	129
	NOXX	130
	NOXX	131
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	NOXX	133
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	NOXX	137
	NOXX	138
	NOXX	139
	NOXX	140
	NOXX	141
	NOXX	142
	NOXX	143
	NOXX	144
	NOXX	145
	NOXX	146
	NOXX	147
	4STEP	354
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	4STEP	387
	4STEP	388
	4STEP	389
	4STFP	390
	4STFP	391
	4STFP	392
	4STFP	393
	4STFP	394
	4STFP	395
	4STFP	396

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A(N,M)=A(N,M)-R1M          4STEP    397
A(N,1002)=A(N,1002)-R102   4STEP    398
RN=R1+FN                    4STEP    399
A(I,NSM)=A(I,NSM)-RN      4STEP    400
A(M,NSM)=A(M,NSM)+RN      4STEP    401
A(N,NSM)=A(N,NSM)+RN      4STEP    402
A(I,NA)=A(I,NA)-R1        4STEP    403
A(M,NA)=A(M,NA)+R1        4STEP    404
A(N,NA)=A(N,NA)+R1        4STEP    405
IF(.NOT.LNRCG)GO TO 100    4STEP    406
IF(RTURA.LT.RLAM)GO TO 100 4STEP    407
RT=R1*(TH1+TEN(J)-EN)      4STEP    408
A(I,NQ)=A(I,NQ)+RT        4STEP    409
A(M,NQ)=A(M,NQ)-RT        4STEP    410
A(N,NQ)=A(N,NQ)-RT        4STEP    411
GO TO 100                  4STEP    412
160 CONTINUE                4STEP    413
C ***GLOBAL REACTION***     4STEP    414
C GLOBAL RATE EQUATIONS FOR 4-STEP REACTION.  4STEP    415
C SECOND STEP CXHY=2+(X/2)O2 === XCO+(Y-2)/2)H2 4STEP    416
C                                         4STEP    417
XC=AL(ILC,1DFU)             4STEP    418
YH=AL(ILH,1DFU)             4STEP    419
XCYH=XC+C.2500*(YH-2.000)   4STEP    420
TACT(J)=FR2                 4STEP    421
TEN(J)=0.000                 4STEP    422
CEBU(J)=CEBU2               4STEP    423
RX(J)=PEXP2                 4STEP    424
TK1=TACT(J)*TKINV           4STEP    425
TM2=TK1-RX(J)-TEN(J)*TLN   4STEP    426
IF(DARS(TM2),GT,R1)GO TO 100 4STEP    427
R1=DEXP(-TM2)               4STEP    428
                                         4STEP    429
C-----PROVISION FOR CONTACT INDEX.  4STEP    430
R1=X1(J)*R1                 4STEP    431
R1=R1*((RHOP*S2(10CH))**AEXP2)*(RHOP*S2(1002))**BEXP2) 4STEP    432
1*((RHOP*S2(1DFU)+1.0-30)**CEXP2) 4STEP    433
RLAM=R1                      4STEP    434
PHI=0*M1(S2(10CH),S2(1002)/XCYH) 4STEP    435
RTURB=(CEBU(J)*RHOP*PHI*EDKIJ 4STEP    436
IF(RLAM.LT.RTURB)GO TO 161 4STEP    437
R1=RTURA                     4STEP    438
R1FU=0.0                      4STEP    439
EN=1.000                      4STEP    440
IF(S2(1002)/XCYH.LT.S2(10CH))GO TO 162 4STEP    441
R1I=RTURA                     4STEP    442
R1K=0.0                        4STEP    443
GO TO 163                     4STEP    444
162 R1I=0.0                     4STEP    445
R1K=RTURB                     4STEP    446
GO TO 163                     4STEP    447
161 R1T=1FXP2*RLAM            4STEP    448
R1K=REXP2*RLAM               4STEP    449
R1FU=CEXP2*RLAM              4STEP    450
R1=RLAM                       4STEP    451
EN=AEXP2+REXP2+CEXP2          4STEP    452
163 A(I,I)=A(I,I)+R1T        4STEP    453
A(I,K)=A(I,K)+R1K            4STEP    454
A(I,1DFU)=A(I,1DFU)+R1FU    4STEP    455
A(K,I)=A(K,I)+R1I+0.500*XC 4STEP    456
A(K,K)=A(K,K)+R1K+0.500*XC 4STEP    457
A(M,1DFU)=A(M,1DFU)+R1FU+0.500*XC 4STEP    458
A(M,I)=A(M,I)+R1I*XC        4STEP    459
A(M,K)=A(M,K)+R1K*XC        4STEP    460

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A(M,INFU)=A(M,INFU)-P1FU*XC
A(N,I)=A(N,I)-R2I*(YH-2.000)*0.500
A(N,K)=A(N,K)-R1K*(YH-2.000)*0.500
A(N,TDFU)=A(N,TDFU)-R1FU*(YH-2.000)*0.500
RN=R1*EN
A(I,NSP)=A(I,NSM)-RN
A(K,NSM)=A(K,NSM)-RN*0.500*XC
A(M,NSM)=A(P,NSM)+RN*XC
A(N,NSM)=A(N,NSM)+RN*(YH-2.000)*0.500
A(I,NA)=A(I,NA)-R1
A(K,NA)=A(K,NA)-R1*0.500*XC
A(M,NA)=A(M,NA)+R1*XC
A(N,NA)=A(N,NA)+R1*(YH-2.000)*0.500
IF(I,NOT,LNR6)GO TO 100
IF(RTURR,LT,RLAM)GO TO 100
RT=R1*(TK1+TEN(J)-EN)
A(I,NO)=A(I,NO)+RT
A(K,NO)=A(K,NO)+RT*0.500*XC
A(M,NO)=A(M,NO)-RT*XC
A(N,NO)=A(N,NO)-RT*(YH-2.000)*0.500
GO TO 100
170 CONTINUE
C ***GLOBAL REACTIONS**
C GLOBAL RATE EQUATIONS FOR 4-STEP REACTION.
C THIRD STEP CO+(1/2)O2 --- CO2
C
        TACT(J)=ER3
        TEN(J)=0.000
        CERU(J)=CERU3
        RX(J)=PEXP3
        TK1=TACT(J)*TRINV
        TM2=TK1-RX(J)-TEN(J)*TLN
        IF(DARS(TM2),GT,RIG)GO TO 100
        R1=DEXP1-TM2
C-----PROVISION FOR CONTACT INDEX.
        R1=Y1(J)*R1
        SSS=7.9300*DEXP1*(-2.4800*FUT*(1.000-FST)/(FST*(1.000-FUT)))
        SSS=DMIN1(1.000,SSS)
        R1=R1*((RHOP+S2(IDCO))**AEXP3)*((RHOP+S2(IDO2))**BEXP3)
        1*((RHOP+S2(IDH2O1))**CEXP3)+SSS
        RLAM=R1
        PHI=DMIN1(2.000*S2(K),S2(I))
        RTURR=CERU(J)*RHOP**PHI*ENKIJ
        TF(PLAM,I,T,RTURR)GO TO 171
        R1=RTURR
        R1H2O=C.O
        FN=1.000
        TF(2.000*S2(K),LT,S2(I))GO TO 172
        RII=RTURR
        R1K=0.C
        GO TO 173
172 RII=0.O
        RIK=RTURR
        GO TO 173
171 R1I=AEXP3*RLAM
        R1K=REXP3*RLAM
        R1H2O=CEXP3*RLAM
        R1=RLAM
        FN=AEXP3+REXP3+CEXP3
173 A(I,I)=A(I,I)+R1I
        A(I,K)=A(I,K)+R1K
        A(I,IDO2)=A(I,IDO2)+R1H2O
        A(K,I)=A(K,I)+R1I*0.500

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A(K,K)=A(K,K)+R1K*0.500	4STEP	525
A(K,1DH2D)=A(K,1DH2D)+R1H2D*0.500	4STEP	526
A(M,I)=A(M,I)-R1I	4STEP	527
A(M,K)=A(M,K)-R1K	4STEP	528
A(M,1DH2C)=A(M,1DH2C)-R1H2D	4STEP	529
RN=R1+EN	4STEP	530
A(I,NSM)=A(I,NSM)-RN	4STEP	531
A(K,NSM)=A(K,NSM)-RN*0.500	4STEP	532
A(M,NSM)=A(M,NSM)+RN	4STEP	533
A(T,NA)=A(T,NA)-R1	4STEP	534
A(K,NA)=A(K,NA)-R1*0.500	4STEP	535
A(M,NA)=A(M,NA)+R1	4STEP	536
IF(I,NOT,LMPG)GO TO 100	4STEP	537
IF(URTRG,LT,RLAM)GO TO 100	4STEP	538
RT=R1*(TK1+TEN(J)-EN)	4STEP	539
A(T,NO)=A(T,NO)+RT	4STEP	540
A(K,NO)=A(K,NO)+RT*0.500	4STEP	541
A(M,NO)=A(M,NO)-RT	4STEP	542
GO TO 100	4STEP	543
180 CONTINUE	4STEP	544
C ***GLOBAL REACTION***	4STEP	545
C GLOBAL RATE EQUATIONS FOR 4-STEP REACTION.	4STEP	546
C FOURTH STEP H2+(1/2)O2 --- H2O	4STEP	547
C	4STEP	548
TAUT(J)=ERA4	4STEP	549
TEN(J)=0.0DC	4STEP	550
CEMU(J)=CEBU4	4STEP	551
RX(J)=PEXP4	4STEP	552
TKJ=TAUT(J)*TKINV	4STEP	553
TM2=TK1-RX(J)-TEN(J)*TLN	4STEP	554
IF(DARS(TM2),GT,RIG6)GO TO 100	4STEP	555
R1=DEXP(-TM2)	4STEP	556
C	4STEP	557
-----PROVISION FOR CONTACT INDEX.	4STEP	558
R1=Y1(J)+R1	4STEP	559
R1=R1*((RHOP*S2(IDH2))**AEXP4)*((RHOP*S2(IDO2))**BEXP4)	4STEP	560
1*((RHOP*S2(IDCH)+1.0-30)**CEXP4)	4STEP	561
RLAM=R1	4STEP	562
PHT=DMIN1(2.000*S2(K),S2(I))	4STEP	563
RTURR=CF8U(J)*RHLR*PHI*EDKIJ	4STEP	564
IF(RLAM,LT,RTURR)GO TO 181	4STEP	565
R1=RTURR	4STEP	566
R1CH=0.0	4STEP	567
EN=1.000	4STEP	568
IF(2.000*S2(K),LT,S2(I))GO TO 182	4STEP	569
R1I=RTURR	4STEP	570
R1K=0.0	4STEP	571
GO TO 183	4STEP	572
182 R1I=0.0	4STEP	573
R1K=RTURR	4STEP	574
GO TO 183	4STEP	575
181 R1I=AEXP4*RLAM	4STEP	576
R1K=REXP4*RLAM	4STEP	577
R1CH=CEXP4*RLAM	4STEP	578
EN=AEXP4+BEXP4+CEXP4	4STEP	579
183 A(I,I)=A(I,I)+R1I	4STEP	580
A(I,K)=A(I,K)+R1K	4STEP	581
A(I,1DCH)=A(I,1DCH)+R1CH	4STEP	582
A(K,I)=A(K,I)+R1I*0.500	4STEP	583
A(K,K)=A(K,K)+R1K*0.500	4STEP	584
A(K,1DCH)=A(K,1DCH)+R1CH*0.500	4STEP	585
A(M,I)=A(M,I)-R1I	4STEP	586
A(M,K)=A(M,K)-R1K	4STEP	587
A(M,1DCH)=A(M,1DCH)-R1CH	4STEP	588

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RN=R1*FN
A(I,NRM)=A(I,NRM)-RN
A(K,NRM)=A(K,NRM)-RN*0.500
A(M,NRM)=A(M,NRM)+RN
A(I,NA)=A(I,NA)-R1
A(K,NA)=A(K,NA)-R1*0.500
A(M,NA)=A(M,NA)+R1
IF(I,MRT,LNRG) GO TO 100
IF(IRTURR,LT,RLAM) GO TO 100
RT=R1*(TK1+TEN(J)-EN)
A(I,NQ)=A(I,NQ)+RT
A(K,NQ)=A(K,NQ)+RT*0.500
A(M,NQ)=A(M,NQ)-RT
100 CONTINUE
C 110 CONTINUE
IF(NRLOOP.GT.JJ) GO TO 271
C 200 270 J=NRLOOP,JJ
C
C   **REACTION RATES**+
C   CALCULATE FORWARD AND REVERSE RATES R1 AND R2
C   THREE TYPES OF REACTIONS
C
C   MDR 1 ... A + B (+C) --- D + E (+F)
C   MDR 2 ... AB + M --- A + B + M
C   MDR 3 ... A + B + M --- AB + M
C
C   ID(I,J)
C   ID(2,J)
C   ID(3,J)
C   ID(4,J)
C   ID(5,J)
C   ID(6,J)
C   MDR=MDR(J)
C
C   R1=0.000
C   R2=0.000
C   TM1=0.000
C   TM2=0.000
C   RN=0.000
C   RT=0.000
C   R1T=0.0
C   R1K=0.0
C   R1KK=0.0
C   R2M=0.0
C   R2MN=0.0
C   R2NN=0.0
C
C   TK1=TAUT(J)*TKINV
C   TM2=TK1-RX(J)
C   IF (TEN(J),NE,0.001) TM2=TM2-TEN(J)*TLN
C   IF (DARS(TM2),GT,RIG) GO TO 205
C   R1=DEXP(-TM2)
C
C-----PROVISION FOR CONTACT INDEX
C   PI=R1*X1(J)
C   IF (MDRF-2) 200,201,202
C   200 R1=R1*S2(J)*RHSQ*S2(K)
C   RLAM=R1
C   PHT=DMIN1(S2(K),S2(J))
C   RTURB=CERUL(J)*RHUP*PHI*EDK(J)

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	4STEP	589
	4STEP	590
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	4STEP	597
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	4STEP	599
	4STEP	600
	4STEP	601
	CALC	157
	CALC	158
	CALC	159
	4STFP	602
	CALC	160
	CALC	161
	CALC	162
	CALC	163
CSE	CALC	164
CSE	CALC	165
	CALC	166
	CALC	167
	CALC	168
	CALC	169
	CALC	170
	CALC	171
	CALC	172
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	CALC	179
	CALC	180
	CALC	181
	CALC	182
	CALC	183
	CALC	184
	CALC	185
	CALC	186
	CALC	187
	NOXX	148
	NOXX	149
	NOXX	150
	NOXX	151
	NOXX	152
	NOXX	153
	CALC	188
	CALC	189
	CALC	190
	CALC	191
	CALC	192
	CALC	193
	CALC	194
	CALC	195
	CALC	196
	CALC	197
	NOXX	154
	NOXX	155
	NOXX	156

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IF(RLAH,LT,RTURB)GO TO 291
R1=RTUPR
EN=1.000
IF(S2(K),LT,S2(I))GO TO 292
RII=RTURB
R1K=0.0
GO TO 293
292 RII=0.0
R1K=RTURB
GO TO 293
291 R1T=RLAH
R1K=RLAM
R1=RLAM
FN=2.000
293 CONTINUE
IF(KK,EO.O) GO TO 290
RLAM=R(AM)*RHOP*S2(KK)
PHI=DMIN1(PHI,S2(KN))
RTURB=CEBU(J)*RHOP+PHI*EDKIJ
IF(RLAH,LT,RTURB)GO TO 294
EN=1.000
R1=RTUPR
IF(S2(K),LT,S2(I))GO TO 295
IF(S2(I),LT,S2(KK))GO TO 296
GO TO 298
295 IF(S2(K),LT,S2(KK))GO TO 297
298 RIKK=RTURB
R1K=0.0
R1T=0.0
GO TO 299
297 RIK=RTURB
R1KK=0.0
R1=0.0
GO TO 299
296 R1T=RTURB
R1K=0.0
R1KK=0.0
GO TO 299
294 RII=RLAH
R1K=RLAM
R1KK=RLAM
R1=RLAM
EN=3.000
299 CONTINUE
290 RN=R1*EN
IF(.NOT.LNRG)GO TO 205
IF(RTURB,LT,RLAM)GO TO 205
R=R1*(TEN(J)+TK1-EN)
GO TO 205
C
201 R1=R1*RHSM*RHOP*S2(I)
RLAM=R1
PHI=S2(I)
RTURB=CEBU(J)*RHOP+PHI*EDKIJ
R1T=DMIN1(RLAM,RTURB)
R1=R1T
RN=R1
IF(.NOT.LNRG)GO TO 205
IF(RTURB,LT,RLAM)GO TO 205
RT=R1*(TEN(J)+TK1-2.000)
GO TO 205
C
202 R1=R1*RHSM*S2(I)*RHSQ*S2(K)
RLAM=R1

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NOXX	157
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NOXX	161
NOXX	162
NOXX	164
NOXX	165
NOXX	166
NOXX	167
NOXX	168
NOXX	169
CALC	170
NOXY	170
CALC	170
NOXX	171
NOXX	172
NOXX	173
NOXX	174
NOXX	175
NOXX	176
NOXX	177
NOXX	178
NOXX	179
NOXX	180
NOXX	191
NOXX	192
NOXX	193
NOXX	194
NOXX	195
NOXX	196
NOXX	197
NOXX	198
CALC	199
NOXX	199
NOXX	200
NOXX	201
CALC	204
CALC	205
CALC	206
NOXX	202
NOXX	203
NOXX	204
NOXX	205
NOXX	206
CALC	207
NOXX	207
NOXX	208
NOXX	209
CALC	209
CALC	210
CALC	211
NOXX	210

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PHI=DMIN1(S2(K),S2(I))
RTURR=CEAU(J)*PHOP*PHI*EDKIJ
IF(PLAP,LT,RTURR) GO TO 301
R1=RTURR
FN=1.000
IF(S2(K),LT,S2(I)) GO TO 302
R1T=RTURR
R1K=0.0
GO TO 303
302 R1I=0.0
R1K=RTURR
GO TO 303
301 R1I=R1AM
R1K=R1AM
R1=R1AM
FN=2.000
303 CONTINUE
RN=R10EN
IF(.NOT.LNPG) GO TO 205
IF(RTURR,LT,R1AM) GO TO 205
RT=R1*(TEN(J)+TK1-3.000)
C
205 TM1=R1
C
C-----CALCULATE REVERSE RATE CONST FROM FWD RATE CONST AND EQUIL CONST
C-----WHENEVER TEMP IS LESS THAN 1500 K
C
IF (TK,GT,1500.000) GO TO 220
C
HH=HO(I)-HO(M)
SS=S0(I)-S0(M)
IF (M0DF-2) 210,211,212
C
210 HH=HH+HO(K)-HO(N)
SS=SS+S0(K)-S0(N)
IF(KK,F0,0) GO TO 218
HH=HH+HO(KK)
SS=SS+S0(KK)
218 IF(NN,F0,0) GO TO 219
HH=HH-HO(NN)
SS=SS-S0(NN)
219 CONTINUE
RXX=RX(J)+SS
TK2=TK1+HH
TN2=TFN(J)
GO TO 230
C
211 HH=HH-HO(N)
SS=SS-S0(N)
C -2.500304 IS E-LG OF GAS CONST 0.00206 NOF3-ATM/KGMOL-DEG K.
RXX=RX(J)+SS-2.50030400
TK2=TK1+HH
TN2=TFN(J)+1.000
GO TO 230
C
212 HH=HH+HO(K)
SS=SS+S0(K)
RXX=RX(J)+SS+2.50030400
TK2=TK1+HH
TN2=TEN(J)-1.000
GO TO 230
C
220 RXX=RX2(J)

```

ADDITIONAL PAGE IS
OF POOR QUALITY

NOXX	211
NOXX	212
NOXX	213
NOXX	214
NOXX	215
NOXX	216
NOXX	217
NOXX	218
NOXX	219
NOXX	220
NOXX	221
NOXX	222
NOXX	223
NOXX	224
NOXX	225
NOXX	226
NOXX	227
NOXX	228
NOXX	229
NOXX	230
NOXX	231
CALC	214
CALC	215
CALC	216
CALC	217
CALC	218
CALC	219
CALC	220
CALC	221
CALC	222
CALC	223
CALC	224
CALC	225
CALC	226
CALC	227
CALC	228
CALC	229
CALC	230
CALC	231
CALC	232
CALC	233
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CALC	245
CALC	246
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CALC	248
CALC	249
CALC	250
CALC	251
CALC	252
CALC	253
CALC	254
CALC	255
CALC	256

ORIGINAL FROM GS
OF POOR QUALITY

```

TK2=TACT2(J)*TKINV
TN2=TFN2(J)

C
230 TN2=TK2-RXX
IF (TN2,NE,0.00) TN2=TN2-TN2*TLN
IF (DABS(TN2),GT,BIG) GO TO 250
R2=DEXP(-TN2)
C----MULTIPLY HOMOGENEOUS RATE CONSTANT BY CONTACT INDEX
R2=R2*X?(J)
C
IF (MODE=2) 240,241,242
C
240 R2=R2*S2(M)*RH50*S2(N)
RLAM=R2
PHI=DMIN1(S2(M),S2(N))
RTURB=CERU(J)*RHOP*PHI*EDKIJ
IF(RLAM,LT,RTURB)GO TO 311
R2=RTURB
EN=1.000
IF(S2(M),LT,S2(N))GO TO 312
R2M=RTURB
P2M=0.0
GO TO 313
312 R2N=0.0
R2M=RTURB
GO TO 313
311 R2N=RLAM
R2M=RLAM
R2=RLAM
EN=2.000
313 CONTINUE
IF(NN,EQ,0) GO TO 249
RLAM=RLAM+RHOP*S2(NN)
PHI=DMIN1(PHI,S2(NN))
RTURB=CERU(J)*RHOP*PHI*EDKIJ
IF(PLAM,LT,RTURB)GO TO 314
R2=RTURB
EN=1.000
IF(S2(M),LT,S2(N))GO TO 315
IF(S2(N),LT,S2(NN))GO TO 316
GO TO 318
315 IF(S2(M),LT,S2(NN))GO TO 317
316 R2NN=RTURB
R2M=0.0
R2N=0.0
GO TO 319
317 R2M=RTURB
R2NN=0.0
R2N=0.0
GO TO 319
316 R2N=RTURB
R2NN=0.0
R2M=0.0
GO TO 319
314 R2N=RLAM
R2M=RLAM
R2NN=RLAM
R2=RLAM
EN=3.000
319 CONTINUE
249 RH=RN=R2*EN
IFI,NOT,LNRG1GO TO 250
IFI RTURB,LT,RLAM1GO TO 250
PT=PT-R2*(TN2+TK2-EN)

```

	CALC	257
	CALC	258
	CALC	259
	CALC	260
	CALC	261
	CALC	262
	CALC	263
	CALC	264
	CALC	265
	CALC	266
	CALC	267
	CALC	268
	CALC	269
	NOXX	232
	NOXX	233
	NOXX	234
	NOXX	235
	NOXX	236
	NOXX	237
	NOXX	238
	NOXX	239
	NOXX	240
	NOXX	241
	NOXX	242
	NOXX	243
	NOXX	244
	NOXX	245
	NOXX	246
	NOXX	247
	CALC	270
	NOXX	248
	CALC	271
	NOXX	249
	NOXX	250
	NOXX	251
	NOXX	252
	NOXX	253
	NOXX	254
	NOXX	255
	NOXX	256
	NOXX	257
	NOXX	258
	NOXX	259
	NOXX	260
	NOXX	261
	NOXX	262
	NOXX	263
	NOXX	264
	NOXX	265
	NOXX	266
	NOXX	267
	NOXX	268
	NOXX	269
	NOXX	270
	NOXX	271
	NOXX	272
	NOXX	273
	NOXX	274
	NOXX	275
	NOXX	276
	CALC	274
	NOXX	277
	NOXX	278
	NOXX	279

ORIGINAL PAGE IS
OF POOR QUALITY

```

GO TO 250                                CALC    276
C
241 R2=R2+RHSM*S2(M)+RHSD*S2(N)          CALC    277
      RLAM=R2
      PHI=DMIN1(S2(M),S2(N))
      RTURB=CEAU(J)*RHOP*PHI*EDKIJ
      IF(RLAM.LT.RTURB)GO TO 321
      R2=RTURB
      FN=1.000
      IF(S2(M).LT.S2(N))GO TO 322
      R2N=RTURB
      R2M=0.0
      GO TO 323
322 R2M=0.0
      R2M=RTURB
      GO TO 323
321 R2H=RLAM
      R2M=RLAM
      R2=RLAM
      FN=2.000
323 CONTINUE
      RN=RN-R2*FN
      TF(.NOT.,LNRG)GO TO 250
      TF(,RTURB,LT,RLAM)GO TO 250
      RT=RT-R2*(TN2+TK2-3.000)
      GO TO 250                                NOXX   280
                                                NOXY   281
                                                NOXX   282
                                                NOXX   283
                                                NOXX   284
                                                NOXX   285
                                                NOXX   286
                                                NOXX   287
                                                NOXX   288
                                                NOXX   289
                                                NOXX   290
                                                NOXX   291
                                                NOXX   292
                                                NOXY   293
                                                NOXX   294
                                                NOXX   295
                                                NOXX   296
                                                NOXX   297
                                                NOXX   298
                                                NOXX   299
                                                NOXX   300
                                                NOXX   301
                                                CALC   281
                                                CALC   282
                                                CALC   283
                                                NOXX   302
                                                NOXX   303
                                                NOXX   304
                                                NOXX   305
                                                NOXX   306
                                                CALC   284
                                                NOXX   307
                                                NOXY   308
                                                NOXX   309
                                                CALC   286
                                                CALC   287
                                                CALC   288
                                                CALC   289
                                                CALC   290
                                                CALC   291
                                                CALC   292
                                                NOXX   310
                                                NOXX   311
                                                NOXX   312
                                                NOXX   313
                                                CALC   297
                                                CALC   298
                                                CALC   299
                                                CALC   300
                                                CALC   301
                                                CALC   302
                                                CALC   303
                                                CALC   304
                                                NOXX   314
                                                NOXX   315
                                                NOXX   316
                                                NOXX   317
                                                NOXX   318
                                                CALC   310
                                                CALC   311
                                                CALC   312
A(I,I)=A(I,I)+R1I                         CALC   304
A(M,I)=A(M,I)-R1I                         NOXX   314
A(T,M)=A(T,M)-R2M                         NOXX   315
A(M,M)=A(M,M)+R2M                         NOXX   316
A(I,NSM)=A(I,NSM)-RN                      CALC   297
A(M,NSM)=A(M,NSM)+RN                      CALC   298
A(I,NQ)=A(I,NQ)+RT                        CALC   299
A(M,NQ)=A(M,NQ)-RT                        CALC   300
A(I,NA)=A(I,NA)-TM1                        CALC   301
A(M,NA)=A(M,NA)+TM1                        CALC   302
IF (MODE,EO,3) GO TO 260                  CALC   303
C
A(N,I)=A(N,I)-R1I                         CALC   304
A(M,N)=A(M,N)+R2M                         NOXX   314
A(T,N)=A(T,N)-R2M                         NOXX   315
A(M,N)=A(M,N)+R2M                         NOXX   316
A(N,N)=A(N,N)+R2N                         NOXX   317
A(N,NSM)=A(N,NSM)+RN                      CALC   310
A(M,NQ)=A(M,NQ)-RT                        CALC   311
A(M,NA)=A(M,NA)+TM1                        CALC   312
                                                CALC   313

```

CHAPTER 1
OF POOR QUALITY

IF (MODE.EQ.2) GO TO 270

260 CONTINUE

```

A(K,I)=A(K,I)+R1K
A(I,K)=A(I,K)+R1K
A(K,K)=A(K,K)+R1K
A(M,K)=A(M,K)+R1K
A(K,M)=A(K,M)+R2M
A(K,NSM)=A(K,NSM)+RN
A(K,NQ)=A(K,NQ)+RT
A(K,NA)=A(K,NA)+TM1
IF (MODE.EQ.3) GO TO 270

```

A(N,K)=A(N,K)+R1K

A(K,N)=A(K,N)+R2N

IF (KK.EQ.0) GO TO 268

A(I,KK)=A(I,KK)+R1KK

A(K,KK)=A(K,KK)+R1KK

A(KK,I)=A(KK,I)+R1I

A(KK,K)=A(KK,K)+R1K

A(KK,KK)=A(KK,KK)+R1KK

A(M,KK)=A(M,KK)+R1KK

A(N,KK)=A(N,KK)+R1KK

A(KK,M)=A(KK,M)+R2M

A(KK,N)=A(KK,N)+R2N

A(KK,NSM)=A(KK,NSM)+RN

A(KK,NQ)=A(KK,NQ)+RT

A(KK,NA)=A(KK,NA)+TM1

268 IF (NN.EQ.0) GO TO 269

A(I,NN)=A(I,NN)+R2NN

A(K,NN)=A(K,NN)+R2NN

A(NN,I)=A(NN,I)+R1I

A(NN,K)=A(NN,K)+R1K

A(M,NN)=A(M,NN)+R2NN

A(N,NN)=A(N,NN)+R2NN

A(NH,NN)=A(NH,NN)+R2NN

A(NH,HN)=A(NH,HN)+R2N

A(NH,HN)=A(NH,HN)+R2NN

A(NH,NSM)=A(NH,NSM)+RN

A(NH,NQ)=A(NH,NQ)+RT

A(NH,NA)=A(NH,NA)+TM1

269 CONTINUE

270 CONTINUE

271 CONTINUE

HSUM=0.000

DO 280 I=1,NS

S2I=S2(I)

A(I,I)=A(I,I)+EMV*S2I

A(I,NA)=A(I,NA)+EMV*(S1(I)-S2I)

A(NSM,I)=S2I

A(NSM,NA)=A(NSM,NA)-S2I

A(NO,I)=HC(I)*S2I

HSUM=HSUM+A(NO,I)

280 CONTINUE

281 CONTINUE

A(NSM,NSP)=SP

C-----A(NSM,NQ) AND A(NO,NSM) ARE EQUAL TO ZERO.

A(NSM,NA)=A(NSM,NA)+SP

A(NO,NO)=CPSUM+QDRV

A(NO,NA)=HTN-Q-HSUM

THAT AND

THE ENERGY GO TO 282

CALC	313
CALC	314
CALC	315
NOXX	319
NOXX	320
NOXX	321
NOXX	322
NOXX	323
CALC	321
CALC	322
CALC	323
CALC	324
CALC	325
NOXX	324
NOXX	325
CALC	326
NOXY	326
NOXX	327
NOXX	328
NOXX	329
NOXX	330
NOXX	331
NOXX	332
NOXX	333
NOXX	334
CALC	336
CALC	339
CALC	340
CALC	341
NOXX	335
NOXX	336
NOXX	337
NOXX	338
NOXX	339
NOXX	340
NOXX	341
NOXX	342
NOXX	343
CALC	351
CALC	352
CALC	353
CALC	354
CALC	355
CALC	356
CALC	357
4STEP	603
CALC	358
CALC	359
CALC	360
CALC	361
CALC	362
CALC	363
CALC	364
CALC	365
CALC	366
CALC	367
CALC	368
CALC	369
CALC	370
CALC	371
CALC	372
CALC	373
CALC	374
NOXY	344

ORIGINAL PAGE 13
OF POOR QUALITY

```

IMAT=NS
DO 281 I=1,NS
281 A(I,NSM)=A(I,NM)
282 CONTINUE
GO TO 400

C
C***EQUILIBRIUM***  

C DERIVATIVE AND FUNCTION MATRIX FOR EQUILIBRIUM SOLUTION
C
300 DO 310 L=1,NLM
310 R0(L)=0.000
C
HSUM=0.000
SUM=0.000
DO 340 I=1,NS
SUM=SUM+S2(I)
TM1=H0(I)*S2(I)
HSUM=HSUM+TM1
TM2=(H0(I)-S0(I)+Y(I)-Y(NSM)+PPLN)*S2(I)
A(N1,N3)=A(N1,N3)+TM1
A(N2,N2)=A(N2,N2)+H0(I)*TM2
A(N2,N3)=A(N2,N3)+H0(I)*TM2
C
DO 330 L=1,NLM
IF (AL(L,I).EQ.0.000) GO TO 390
TM3=AL(L,I)*S2(I)
C----CROSS-DERIVATIVES OF ELEMENT EQUATIONS, D F(L)/D PI(K)
DO 320 K=L,NLM
IF (AL(K,I).EQ.0.000) GO TO 320
AL(L,K)=AL(K,L)+AL(K,I)*TM3
320 CONTINUE
C----DERIVATIVES OF L-ELEMENT EQN W.R.T. LN SM AND LN T
A(L,N1)=A(L,N1)+TM3
A(L,N2)=A(L,N2)+AL(L,I)*TM1
C----NEGATIVE OF L-ELEMENT EQN, F(L)
A(L,N3)=A(L,N3)+AL(L,I)*TM2
R0(L)=R0(L)+AL(L,I)*S1(I)
330 CONTINUE
340 CONTINUE
C
A(N1,N1)=SUM-SM
A(N1,N3)=A(N1,N3)-(SUM-SM)
A(N1,N2)=HSUM
A(N2,N2)=A(N2,N2)+CPSUM+ODRV
A(N2,N3)=A(N2,N3)+HIN=HSUM=0
C
C----NEGATIVE OF L-ELEMENT EQNS, F(L)
DO 350 L=1,NLM
A(L,N3)=A(L,N3)+R0(L)-A(L,N1)
350 CONTINUE
C
C----STORE SYMMETRIC ELEMENTS OF MATRIX
C
DO 360 I=1,N2
DO 360 J=I,N2
A(I,J)=A(I,J)
360 CONTINUE
C
C----INTERCHANGE SM-EQN WITH ELEMENT ROW L WITH LARGEST A(L,N1) TO
C----AVOID POTENTIAL ZERO IN DIAGONAL ELEMENT A(N1,N1)
C
NOX 345
NOXX 346
NOXX 347
NOXX 348
CALC 375
CALC 376
CALC 377
CALC 378
CALC 379
CALC 380
CALC 381
CALC 382
CALC 383
CALC 384
CALC 385
CALC 386
CALC 387
CALC 388
CALC 389
CALC 390
CALC 391
CALC 392
CALC 393
CALC 394
CALC 395
CALC 396
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CALC 415
CALC 416
CALC 417
CALC 418
CALC 419
CALC 420
CALC 421
CALC 422
CALC 423
CALC 424
CALC 425
CALC 426
CALC 427
CALC 428
CALC 429
CALC 430
CALC 431
CALC 432
CALC 433
CALC 434

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OPTIONAL OUTPUT
OF PEEK QUALITY

```

TM1=0.000          CALC  435
DO 370 L=1,NLM    CALC  436
IF (A(L,N1).LT.TM1) GO TO 370  CALC  437
TM1=A(L,N1)        CALC  438
LL=L               CALC  439
170 CONTINUE       CALC  440
C                   CALC  441
      DO 380 J=1,N3  CALC  442
      TM1=A(N1,J)    CALC  443
      A(N1,J)=A(LL,J)  CALC  444
      A(LL,J)=TM1    CALC  445
180 CONTINUE       CALC  446
      IMAT=N2         CALC  447
C                   CALC  448
      CCCCC   0000   0000   0000   0000   0000   CHAPTER 4   0000  000  CALC  449
      CCCCC   0000   0000   0000   0000   0000   CHAPTER 4   0000  000  CALC  450
C                   CALC  451
C ***MATRIX SOLUTION***  CALC  452
C SOLVE FOR CORRECTIONS BY STANDARD PIVOTAL GAUSSIAN ELIMINATION  CALC  453
C                   CALC  454
400 KMAT=IMAT+1    CALC  455
C-----OPTIONAL OUTPUT OF INTERMEDIATE VALUES FOR DEBUGGING  CALC  456
      IF (.NOT.LOERUG) GO TO 410  CALC  457
      IF (INERUG.LT.5) GO TO 410  CALC  458
      WRITE(6,4C1)            CALC  459
401 FORMAT(1H0,10X,36HELEMENTS A(I,K) OF CORRECTION MATRIX)  CALC  460
      DO 402 K=1,IMAT  CALC  461
      WRITE(6,402) (A(K,I),I=1,KMAT)  CALC  462
402 FORMAT(1X,1P16.0,0)  CALC  463
403 CONTINUE       CALC  464
410 CONTINUE       CALC  465
      DO 450 NN=1,IMAT  CALC  466
      IF (A(NN,NN).EQ.0.000) GO TO 900  CALC  467
C-----CHANGE 1.000 TO 1.0 FOR NON-IBM MACHINES NOT REQUIRING DOUBLE PRE  CALC  468
C      DTN1=1.000/A(NN,NN)  CALC  469
C      DTN1=1.000/A(NN,NN)  CALC  470
      K=NN+1             CALC  471
      DO 420 J=K,KMAT  CALC  472
      A(NN,J)=A(NN,J)*DTN1  CALC  473
420 CONTINUE       CALC  474
      IF (K.EQ.KMAT) GO TO 450  CALC  475
      DO 440 I=K,IMAT  CALC  476
      IF (A(I,NN).EQ.0.000) GO TO 440  CALC  477
      DO 430 J=K,KMAT  CALC  478
      A(I,J)=A(I,J)-A(I,NN)*A(NN,J)  CALC  479
430 CONTINUE       CALC  480
440 CONTINUE       CALC  481
450 CONTINUE       CALC  482
C-----BACK SOLVE FOR CORRECTION VECTOR  CALC  483
C
      K=IMAT  CALC  484
460 J=K+1           CALC  485
      DSUM=0.000  CALC  486
      X(K)=0.000  CALC  487
      IF (IMAT.LT.J) GO TO 480  CALC  488
      DO 470 I=J,IMAT  CALC  489
      DSUM=DSUM+A(I,K)*X(I)  CALC  490
470 CONTINUE       CALC  491
480 CONTINUE       CALC  492
      X(K)=A(K,KMAT)-DSUM  CALC  493
      K=K-1             CALC  494
      IF (K.NE.0) GO TO 460  CALC  495
      CALC  496
      CALC  497
      CALC  498

```

```

      RETURN
C
C*****SINGULAR MATRIX***  

C
      500 WRITE(6,501)
      501 FORMAT(1HO,10X,3(4H****),16HSINGULAR MATRIX//)
C----SET LCONVG=.TRUE. TO NOTIFY SPECIE OF SINGULAR MATRIX
      LCONVG=.TRUE.
      RETURN
      END
      SUBROUTINE SPECIE
C
      DOUBLE PRECISION AL,BO,CPSUM,EMV,ER,FQ,HSUB0,HSUM,H0,PA,PI,PPLN,
      1 00,01,02,03,04,RGAS,RGASIN,RHOP,SM,SHINV,SMW,SSAVE,S0,S1,S2,TK,
      2 TKINV,TLN,2,SM0
      DOUBLE PRECISION X,Y
      DOUBLE PRECISION ETA,ETA0,ETA1,SUM,TINY,TH1,TNY,TST1,VM,VP
      LOGICAL LADIAB,LCONVG,LDEBUG,LEQUIL,LNRG,LREACT,LENER
      COMMON
      3/CCHEM/CPSUP,HSUM,F0,PPLN,RGAS,RGASIN,SHINV,TKINV,TLN,LNRG
      1/CEQUIL/AL(17,301),ATOM(3,7),R0(7),PI(7)
      1/CINDEF/IDCO,INFOU,10D2,1DN2,1D420,1DCO2,1DH1,1DH2,1DN1,1DN0,1DN02
      1,1D0,1D0H,1HCPS,1LC,1LH,IMAT,ITER,JJ,N1,N2,N3,NA,NGLOR,NGLORP,
      2 NLM,NQ,NSM,NS1,NS2,1DCH
      1/CMATRIX/X(32),Y(32)
      1/CARAM/ASUB(30,3),EMV,ER,HSUB0,NDEBUG,NS,PA,00,01,02,03,04,RHOP,
      1 SM,SMW(301),SM0,S1(301),S2(301),TK,LADIAB,LDEBUG,LEQUIL,LREACT,LENER
      2,FOKIJ,LCONVG
      1/CSPECIE/H0(301),S0(301),SSAVE(301),Z(7,2,301)
C
***** THIS SUBROUTINE CALLS CALC TO COMPUTE THE CORRECTIONS TO THE
C CHEMICAL SPECIES AND TEMP AND DETERMINES THE UNDERRELAXATION
C PARAMETER PRIOR TO THE APPLICATION OF THESE CORRECTIONS TO THE
C ESTIMATES FOR BOTH EQUILIBRIUM AND KINETIC STATIONARY STATES
C FOR EACH ITERATION. SPECIE ALSO CONTROLS THE CONVERGENCE TESTS
C PREFERENCE CRELK (WASHINGTON STATE UNIVERSITY) MARCH 1976
*****  

C
      DATA ITMAX/50/,TINY/1.0D-20/,TNY/-46.051700/
      LCONVG=.FALSE.
      SM=0.0D0
      DO 20 I=1,NS
      TF (S2(I).GT.TINY) GO TO 10
      S2(I)=TINY
      Y(I)=TNY
      GO TO 20
10   SM=SM+S2(I)
      Y(I)=DLNG(S2(I))
20   CONTINUE
      TKINV=1.000/TK
      TLN=DLNG(TK)
      Y(NSM)=DLNG(NSM)
      SHINV=1.000/SM
      Y(1NO)=TLN
      
```

```

C ***SOLVE FOR CORRECTIONS***          SPEC    47
C INITIATE THE ITER LOOP AND CALL CALC TO SET UP AND CALCULATE THE SPEC    48
C CORRECTIONS FOR EITHER EQUILIBRIUM OR KINETIC SOLUTION      SPEC    49
C
C      ETA=1.000          SPEC    50
C      ETA0=ETA          SPEC    51
C      NDEC=0            SPEC    52
C      NRlx=0            SPEC    53
C      DO 550 ITER=1,ITMAX      SPEC    54
C
C      CALL CALC          SPEC    55
C
C      IF (IMAT.EQ.NQ) GO TO 300      SPEC    56
C      IF (IMAT.EQ.NS) GO TO 300      SPEC    57
C
C
C*** 00 00 00 00 00 00 00 00 00 00 00 00 CHAPTER 2 00 00 00      SPEC    58
C*** 00 00 00 00 00 00 00 00 00 00 00 00 CHAPTER 2 00 00 00      SPEC    59
C
C      SPEC    60
C      SPEC    61
C      ***CONSTRUCT CORRECTIONS FOR EQUILIBRIUM SPECIES***      SPEC    62
C      CHECK FOR SINGULAR MATRIX (LCONVG SET TO TRUE AT END OF CALC)      SPEC    63
C      IF (NMT.LCONVG) GO TO 200      SPEC    64
C      LCONVG=.FALSE.
C      RETURN      SPEC    65
C
C      200 DO 210 L=1,NLM      SPEC    66
C      210 PI(L)=X(L)          SPEC    67
C          X(NSM)=X(N1)          SPEC    68
C          X(ND)=X(N2)          SPEC    69
C      DO 230 I=1,NS          SPEC    70
C          Y(I)=HO(I)*X(NQ)-(HO(I)-SO(I)+Y(I)+PPLN-Y(NSM))+X(NSM)      SPEC    71
C      DO 220 L=1,NLM          SPEC    72
C          X(I)=Y(I)+AL(L,I)*PI(L)          SPEC    73
C      220 CONTINUE          SPEC    74
C      230 CONTINUE          SPEC    75
C
C
C*** 000 000 000 000 000 000 000 000 000 000 000 000 CHAPTER 3 000 000      SPEC    76
C*** 000 000 000 000 000 000 000 000 000 000 000 000 CHAPTER 3 000 000      SPEC    77
C
C      SPEC    78
C      ***CALCULATE UNDERRELAXATION PARAMETER ETA***      SPEC    79
C      UNDERRELAXATION TESTS ARE DIFFERENT FOR MAJOR AND MINOR SPECIES WITH      SPEC    80
C      ETA = MIN(ETA1,ETA2,1) WHERE      SPEC    81
C      MAJOR SPECIES --- S2(I)/SM 1.00-B      SPEC    82
C      MINOR SPECIES --- S2(I)/SM 1.00-B      SPEC    83
C      AND ONLY POSITIVE CORRECTION CHANGES FOR MOLE NUMBERS ARE MONITORED      SPEC    84
C      ETA1 = MAJOR SPECIES CONTROL      SPEC    85
C      ETA2 = MINOR SPECIES CONTROL      SPEC    86
C
C      300 ETA0=ETA          SPEC    87
C          ETA=1.000          SPEC    88
C          ETA1=1.000          SPEC    89
C          SUM=DAOS(X(NSP))          SPEC    90
C          TM1=DARS(X(NO))          SPEC    91
C          IF (TM1.GT.SUM) SUM=TM1          SPEC    92
C          DO 320 I=1,NS          SPEC    93
C              IF (X(I).LE.0.000) GO TO 320          SPEC    94
C              IF (S2(I)*SPINV.LE.1.00-B) GO TO 320          SPEC    95
C-----MAJOR SPECIES          SPEC    96
C              IF (X(I).GT.SUM) SUM=K(I)          SPEC    97
C              GO TO 320          SPEC    98
C-----MINOR SPECIES          SPEC    99
C              320 TST1=DAOS((Y(NSM)-Y(I)-11.91292900)/(((X(I)-X(NSM))+TINY))      SPEC    100
C                  IF (TST1.LT.ETA1) ETA1=TST1          SPEC    101
C              320 CONTINUE          SPEC    102
C
C
C      NOXX 363
C      SPEC 103
C      SPEC 104
C      SPEC 105
C      SPEC 106
C      NOXX 363
C      SPEC 107
C      SPEC 108
C      SPEC 109

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CHART 1
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IF(SUM.GT.0.200)ETA=0.200/SUM
IF (ETA1.LT.ETA) ETA=ETA1
IF(LEQUILGE TD 400

C
C ***CONVERGENCE MONITORING***  

C AFTER TEN SUCCESSIVE UNDERRELAXED ITERATIONS, IN WHICH ETA DOES NOT  

C INCREASE BY 1.1 OR MORE, OR AFTER SIX ITERATIONS IN WHICH ETA  

C DECREASES, DIVergENCE IS ASSUMED AND THE SOLUTION TERMINATED
C
C LNRG=.TRUE. ---- FULL EQUATIONS
  IF (ETA.EQ.1.000) NRLX=-1
  IF((ETA/FTAO).GE.1.1D0)NRLX= 2
  NRLX=NRLX+1
  IF (NRLX.GT.10) GO TO 900
  IF (FTA.LT.ETA0) NDEC=NDEC+1
  IF (.NOT.LNPG) NDEC=1
  IF (NDEC.GT.6) GO TO 900

C
C     0000      0000      0000      0000      0000      CHAPTER 4      0000      0000      SPEC      120
C     0000      0000      0000      0000      0000      CHAPTER 4      0000      0000      SPEC      129
C
C APPLY CORRECTIONS TO ESTIMATES
C
C
C 400 CONTINUE
  SUM=0.000
  DO 420 I=1,NS
    Y(I)=Y(I)+ETA*X(I)
    IF (Y(I).LT.TNY) GO TO 410
    S2(I)=DEXP(Y(I))
    SUM=SUM+S2(I)*SMW(I)
    GO TO 420

C
C 410 Y(T)=TNy
  S2(I)=TINY
C-----INSURE CONVERGENCE TEST PASSED WHENEVER Y(I)=TNy
  Y(I)=0.000
  420 CONTINUE
  DO 450 I=1,NS
    S2(I)=S2(I)/SUM
  450 Y(T)=DLOG(S2(I))
  Y(NSM)=Y(NSM)+ETA*X(NSM)
  SM=DEXP(Y(NSM))
  SMINV=1.000/SM
  Y(NQ)=Y(NQ)+ETA*X(NQ)
  TLN=Y(NQ)
  TK=DEXP(TLN)
  TKINV=1.000/TK

C
  IF (.NOT.LDEBUG) GO TO 500
  IF (NDEBUG.GE.3) WRITE(6,430) ITER,ETA,LREACT,LEQUIL,LADTAB,
  1                           LNRG,HSUB0,SM,EMV,TK
  1   IF (NDEBUG.GE.4) WRITE(6,440) (I,ASUB(I,1),S1(I),S2(I),Y(I),
  1                               X(I),HO(I),SO(I),I=1,NS)
  630 FORMAT(2X,I3,1P012.3,4L8,1P4012.3)
  440 FORMAT(20X,7HSPECIFS,4X,9HS1(I),7X,9HS2(I),7X,4HY(I),8X,
  84HK(I),8X,9HHO(I),7X,9HSO(I)/(10X,I2,3X,A4,2X,1P6012.3))
C
C     00000      00000      00000      00000      00000      CHAPTER 5      00000  0      SPEC      162
C     00000      00000      00000      00000      00000      CHAPTER 5      00000  0      SPEC      163
C
C CONVERGENCE CHECK...ALL MOLE NUMBER CORRECTIONS MUST BE .LT. 1.0 PCT
C
  500 IF (ETA.LT.1.000) GO TO 550

```

```

      DO 510 I=1,NS
      IF (DABS(X(I)),GT.0.0100) GO TO 550
510 CONTINUE
      LCONVG=.TRUE.
      HSUB0=HSUM*RGAS*TK
      RETURN
C
550 CONTINUE
C
C      RETURN
C
      F000000      000000      000000      000000      CHAPTER 6      000000      SPEC   169
      C000000      000000      000000      000000      CHAPTER 6      000000      SPEC   170
C
      ENTRY ERATIC
C
C      CALCULATES FUEL/AIR EQUIV RATIO, GIVEN MOLE NUMBERS IN S1 ARRAY,
C      USING POSITIVE AND NEGATIVE OXIDATION STATES (VALENCES)
C
      VP=0.000
      VM=0.000
      DO 610 I=1,NS
      IF (S1(I),LE,TINY) GO TO 610
      DO 600 L=1,NLP
      IF (AL(L,I),EQ.0.00) GO TO 600
      IF (ATOM(3,L),GT.0.000) VP=VP+AL(L,I)*ATOM(3,L)*S1(I)
      IF (ATOM(3,L),LT.0.000) VM=VM+AL(L,I)*ATOM(3,L)*S1(I)
600 CONTINUE
610 CONTINUE
C
      VM=-VM
      IF (VM,LT,TINY) GO TO 620
      IF (VP,LT,TINY) GO TO 630
      ER=VP/VM
      RETURN
C
620 ER=1000000.000
      RETURN
C
630 ER=0.000
C
900 RETURN
END
      SUBROUTINE CREKO
C
      DOUBLE PRECISION AL,B0,CPSUM,EMV,ER,FQ,HSUB0,HSUM,H0,P0,PI,PPLN,
1 00,01,02,03,04,RGAS,RGASIM,RHOP,SM,SMINV,SMW,SSAVE,S0,S1,S2,TK,
2 TKINV,TLN,Z,SM0
      DOUBLE PRECISION RX,RX2,TACT,TACT2,TEN,TEN2,X1,X2,CERU
      DOUBLE PRECISION X,Y
      DOUBLE PRECISION AMOLE,B0,DX,GF,PECHT,RTLN,SUM,SUMX,SUMY,SUM1,
1 TENLN,TM1,TM2,T1,T2,XBAR,XMAX,XMIN,YBAR
      LOGICAL LADAR,LCONVG,LDEBUG,LEQUIL,LMOLES,LNRG,LFACT,LSI,LENER
C
      COMMON
3/CCHEM1/CPSUM,HSUM,F0,PPLN,RGAS,RGASIM,SMINV,TKINV,TLN,LNRG
1/CEQUIL/AL(7,30),ATOM(3,7),B0(7),PI(7)
1/CTNDEX/IDCO,IFNU,ION2,ION2,IDC02,IDH1,IDH2,IDM1,IDM0,IDM02
1,ION,IDOM,THCP,ILC,ILH,IMAT,ITER,JD,N1,N2,N3,N4,NGL00,NGL0P,
2 NLH,NQ,NSM,NS1,NS2,IDCM
1/CMATR/N(32),Y(32)
1/CPARAM/ASUR(30,2),EMV,FR,HSUB0,NDEBUG,NS,PA,QQ,Q1,Q2,Q3,Q4,RHOP,
1 SM,SMW(30),SM0,S1(30),S2(30),TK,LADAR,LDEBUG,LEQUIL,LREACT,LENER
      NOXX 372
      NOXXX 22
      NOXXX 23
      NOXX 373
      NOXXX 25
      NOXXX 26
      NOXXX 27
      NOXX 374
      CRKO   2
      CRKO   3
      NOXX 372
      NOXXX 22
      NOXXX 23
      NOXX 373
      NOXXX 25
      NOXXX 26
      NOXXX 27
      NOXX 374
      CRKO   6
      CRKO   7
      NOXX 375
      CRKO   9
      NOXX 376
      NOXX 377
      4STEP 605
      NOXX 378
      CRKO  13
      NOXX 380

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C
      NLM=1
110 READ(5,120) (ATOM(K,NLM),K=1,3)
120 FORMAT(1A2,7X,2F10.6)
      IF (ATOM(1,NLM).EQ.BLANK) GO TO 140
      WRITE(6,130) (ATOM(K,NLM),K=1,3)
130 FORMAT(1X,A2,5X,2F10.6/)
      IF (ATOM(1,NLM).EQ.CARB) ILC=NLM
      IF (ATOM(1,NLM).EQ.MYDR) ILH=NLM
      NLM=NLM+1
      GO TO 110
C
140 CONTINUE
      NLM=NLM-1
      N1=NLM+1
      N2=NLM+2
      N3=NLM+3
      GO TO 10
C
C     00 00 00 00 00 00 00 00 00 00 00 CHAPTER 2 00 00 00
C     00 00 00 00 00 00 00 00 00 00 00 CHAPTER 2 00 00 00
C
C   ***THERMO***  

C   READ THERMODYNAMIC DATA CARDS
C
200 NS=1
201 READ(5,210) (CDATA(I),I=1,3),DT1,DT2,(AT(J),B(J),J=1,4),PHAZ,
      1T1,T2,NCD
210 FORMAT(3A4,6X,2A3,4(A2,F3.0),A1,2F10.3,I19)
      IF (CDATA(1).EQ.BLANK) GO TO 260
      WRITE(6,211)(CDATA(I),I=1,3),DT1,DT2,(AT(J),B(J),J=1,4),PHAZ,
      1T1,T2,NCD
211 FORMAT(10X,3A4,6X,2A3,2X,4(A2,2X,F3.0),2K,A1,2X,2F10.3,I19)
      IF (PHAZ.NE.GAZ) WRITE(6,212) (CDATA(I),I=1,3),PHAZ
212 FORMAT(1H0,10X,26HWARNING...DATA FOR SPECIES,2X,3A4,3X,
      A1HNOT GAS BUT,2X,A1//)
C-----READ Z WITH FIRST AND SECOND SUBSCRIPTS REVERSED
      READ(5,213) (Z(J,1,NS),J=1,5),NCD
213 FORMAT(5D15.8,I5)
      WRITE(6,214) (Z(J,1,NS),J=1,5),NCD
214 FORMAT(10X,5D15.8,I5)
      READ(5,215) (Z(J,1,NS),J=6,7),(Z(K,2,NS),K=1,3),NCD
      WRITE(6,216) (Z(J,1,NS),J=6,7),(Z(K,2,NS),K=1,3),NCD
      READ(5,217) (Z(J,2,NS),J=4,7),NCD
215 FORMAT(4D15.8,I20)
      WRITE(6,218) (Z(J,2,NS),J=4,7),NCD
216 FORMAT(10X,4D15.8,I20//)
C
C-----ESTABLISH ATOM STOICHIOMETRY...AL(L,NS) = (KG-ATOMS ELEMENT L
C-----PER KG-MOLECULE OF SPECIES NS)
C
      DO 220 L=1,NLM
220 AL(L,NS)=0.0DC
C
      SUM=0.0DC
      DO 240 K=1,4
      IF (R(K).EQ.0.0001) GO TO 240
      DO 230 L=1,NLM
      IF (ATOM(1,L).NE.AT(K)) GO TO 230
      AL(L,NS)=AL(L,NS)+R(K)
230
C-----ESTABLISH MOLECULAR WEIGHT OF SPECIES
C
      SUM=SUM+ATOM(2,L)*R(K)

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230 CONTINUE
240 CONTINUE
  SMW(NS)=SUM
  S2(NS)=1.0D-6
C
C-----STORE MOLLERITH NAME OF SPECIES
C
  DO 250 I=1,3
  250 ASUR(NS,I)=CDATA(I)
C
C-----STORE INDEX NUMBER OF SPECIES
C
  IF (ASUR(NS,1).EQ.AC0) 10C0=NS
  TF (ASUR(NS,1).EQ.AC02) 10C02=NS
  IF (ASUR(NS,1).EQ.AH2) 10H2=NS
  IF (ASUR(NS,1).EQ.AH20) 10H20=NS
  IF (ASUR(NS,1).EQ.AN2) 10N2=NS
  IF (ASUR(NS,1).EQ.AO2) 10O2=NS
  IF (NS.NE.10CH) GO TO 292
  DO 251 I=1,2
  DO 251 J=1,7
  251 7(J,I,10CH)=Z(J,I,10CH)*(SMW(10FU)-2.0D0)/28.0D0
  252 CONTINUE
C
  NS=NS+1
  GO TO 201
C
  260 NS=NS-1
  NSM=NS+1
  NQ=NS+2
  NA=NS+3
  GO TO 10
C
  **** 000 MECHANISM ****
C  READ MECHANISM/RATE DATA CARDS
C  THE VARIABLE DT1 (COLUMNS 73/76) IS USED AS A FLAG,
C  CGS --- CGS UNITS, RATE CONSTANTS IN GM-MOLEs, CM, SEC
C  AND EACH IN (KCAL/GM-MOLE)
C  COMM --- COMMENT CARD, FIRST 48 CHARACTERS PRINTED OUT
C  REVF --- REVERSE RATE DATA, IN SAME UNITS AS FORWARD DATA
C  GLOB --- GLOBAL RATE EXPRESSION DATA IN SI UNITS
C  OTHERWISE THE SI UNITS (KG-MOLEs, M, SEC) ARE ASSUMED
C  DT1 AND DT2 (COL 73/80) CAN HAVE ANYTHING (COMMENTS) IF ABOVE FOUR
C  WORDS ARE NOT REQUIRED
C  TACT IS ACTIVATION TEMPERATURE, = EACT/GASCON, DEG K
C
  300 JJ=1
  NGLOR=0
C
  310 READ(5,3111)(CDATA(I),I=1,12),8X(JJ),TEN(JJ),TACT(JJ),
  1 CFRU(JJ),DT1,DT2
  311 FORMAT(12A4,F7.3,F5.3,F7.3,F5.3,2A4)
  IF (CDATA(1).EQ.BLANK.AND.DT1.NE.COMM) GO TO 356
C-----CHECK FOR COMMENT CARD
  IF (DT1.NE.COMM) GO TO 313
  WRITE(6,3121)(CDATA(I),I=1,12)
  312 FORMAT(1H0,9X,3H#00,12A4,3H#00)
  GO TO 310
C-----CHECK FOR REVERSE RATE DATA...ORDER OF CARDS MUST BE CORRECT
C-----UNITS OF REVERSE DATA ASSUMED SAME AS FORWARD DATA
  313 IF (DT1.NE.REVF) GO TO 315

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CRKO	141
CRKO	142
CRKO	143
CRKO	144
CRKO	145
CRKO	146
CRKO	147
CRKO	148
CRKO	149
CRKO	150
CRKO	151
CRKO	152
CRKO	153
CRKO	154
CRKO	155
CRKO	156
CRKO	157
CRKO	158
4STEP	606
4STEP	607
4STEP	608
4STEP	609
4STEP	610
CRKO	159
CRKO	160
CRKO	161
CRKO	162
CRKO	163
CRKO	164
CRKO	165
CRKO	166
CRKO	167
CRKO	168
CRKO	169
CRKO	170
CRKO	171
CRKO	172
CRKO	173
CRKO	174
CRKO	175
CRKO	176
CRKO	177
CRKO	178
CRKO	179
CRKO	180
CRKO	181
CRKO	182
CRKO	183
CRKO	184
CRKO	185
CRKO	186
CRKO	187
NOXX	387
NOXX	388
NOXX	389
CRKO	190
CRKO	191
CRKO	192
CRKO	193
CRKO	194
CRKO	195
CRKO	196
CRKO	197
CRKO	198

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J=JJ-1
RX2(J)=RX(JJ)
TEM2(J)=TEM(JJ)
TACT2(J)=TALT(JJ)
WRITE(6,314) RX2(J),TEM2(J),TACT2(J),DT1,DT2
314 FORMAT(14X,17HREVERSE RATE DATA,20X,3F15.3,2A4)
C-----CONVERT RX2 FOR INTERNAL CALCULATIONS
BX2(J)=BX2(J)*TEMLN
IF (LSI) GO TO 310
RX2(J)=RX2(J)-TEMLN*3.000
TACT2(J)=TACT2(J)+1000.000/1.96700
IF (MDR(J),EQ.2) BX2(J)=BX2(J)-TEMLN*3.000
GO TO 310
C-----CHECK FOR UNITS
315 LST=.TRUE.
IF (DT1,EQ.CGS) LSI=.FALSE.
C
WRITE(6,316) JJ,(CDATA(I),I=1,12),BX(JJ),TEM(JJ),TACT(JJ),DT1,DT2
316 FORMAT(1HO,5X,I5,4H, ,12A4,3F15.3,5X,2A4)
F (.NOT. LSI) TACT(JJ)=TACT(JJ)+1000.00/1.96700
IF (DT1,EQ.GLOB) MGLOR=MGLOR+1
C-----CONVERT RX FOR INTERNAL CALCULATIONS
BX(JJ)=BX(JJ)*TEMLN
C
C-----ID(I,J) IS THE INDEX NUMBER OF THE I-TH DISTINCT SPECIES IN
C-----REACTION J ... I=1,4 AS NO DISTINCT THIRD BODIES ARE CONSIDERED
C
DO 320 I=1,6
320 ID(I,JJ)=0
C
DO 325 N=1,6
K=N*2-1
IF (CDATA(K),EQ.BLANK) GO TO 325
IF (CDATA(K),NE.THIRD) GO TO 321
CDATA(K)=BLANK
GO TO 325
321 CONTINUE
DO 322 I=1,NS
IF (CDATA(K),NE.ASUR(I,2)) GO TO 322
IF (CDATA(K+1),NE.ASUB(I,2)) GO TO 322
II=I
GO TO 323
322 CONTINUE
323 CONTINUE
ID(N,JJ)=II
325 CONTINUE
C
C-----STORE THE TYPE OF REACTION...THREE TYPES
C
MDR 1 ... A + B (+C) --- D + E (+F)
C
MDR 2 ... AB + M --- A + B + M
C
MDR 3 ... A + B + M --- AB + M
C
MDR(JJ)=1
IF (ID(2,JJ),EQ.0) MDR(JJ)=2
IF (ID(5,JJ),EQ.0) MDR(JJ)=3
C
C-----THE FOLLOWING SECTION, UP TO STATEMENT 395 INCLUSIVE, MAY BE
C-----ELIMINATED IF REVERSE (AS WELL AS FORWARD) RATE DATA IS SUPPLIED
C-----FOR ** ALL ** REACTIONS.
C
C-----CALCULATES REVERSE RATE CONSTANTS FROM EQUILIBRIUM CONSTANTS
C-----AND FORWARD RATE CONSTANTS FOR FIFTEEN POINTS

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CRKO	199
CRKO	200
CRKO	201
CRKO	202
CRKO	203
CRKO	204
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CRKO	206
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CRKO	211
CRKO	212
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CRKO	251
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CRKO	254
CRKO	255
CRKO	256
CRKO	257
CRKO	258
CRKO	259
CRKO	260
CRKO	261
CRKO	262

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C   OVER THE TEMPERATURE RANGE 1000 TO 3000 DEG K          CRKO    263
C   INSERTED 1 STEP IN D,HODVEN, 7/22/79)                  CRKO    264
C   IF (DT1.EQ.GLOK) GO TO 357                            CRKO    265
C   IF (DT1.EQ.GLOR) GO TO 355                            CRKO    266
C   DX=(XMAX-XMIN)/14.000                                  CRKO    267
C   SUMX=0.000                                              CRKO    268
C   SUMY=0.000                                              CRKO    269
C   HCPS=2                                                 CRKO    270
C   DO 351 N=1,15                                         LRKO    271
C   X(N)=XMIN+DX*FLOAT(N-1)                               CRKO    272
C   SUMX=SUMX+X(N)                                         NOXXX   28
C   TINV=X(N)                                              CRKO    274
C   TV=1.000/TINV                                         CRKO    275
C   TLN=DLGG(TV)                                         CRKO    276
C   NS1=1                                                 CRKO    277
C   NS2=NS                                               NOXX    390
C   CALL HCPS                                           CRKO    391
C   SUM1=0.000                                              CRKO    278
C   DO 350 ND=1,6                                         CRKO    279
C   K=ID(ND,JJ)                                         CRKO    280
C   IF (K.EQ.0) GO TO 350                                CRKO    281
C   GF=HA(K)-SO(K)                                       CRKO    282
C   IF (ND.LT.4) SUM1=SUM1+GF                           CRKO    283
C   IF (ND.GE.4) SUM1=SUM1-GF                           CRKO    284
C   350 CONTINUE                                         CRKO    285
C   TM1=0.000                                              CRKO    286
C   NATURAL LOGS OF GAS CONSTANTS...R=82.057 CN3=ATH/GMOL,K (CGS) CRKO    287
C   AND R=C.002057 M3=ATM/KGMOL,K (SI)                   CRKO    288
C   RTLN=TLN+4.4074DC                                     CRKO    289
C   TF (LSI) RTLN=TLN-2.50034D0                          CRKO    290
C   IF (MDP(JJ).GT.1) GO TO 3501                         CRKO    291
C   IF (ID(3,JJ).EQ.0) TM1=TM1+RTLN                      CRKO    292
C   IF (ID(6,JJ).EQ.0) TM1=TM1-RTLN                      CRKO    293
C   GO TO 3502                                         CRKO    294
C   3501 CONTINUE                                         CRKO    295
C   IF (ID(2,JJ).EQ.0) TM1=RTLN                         CRKO    296
C   IF (ID(5,JJ).EQ.0) TM1=-RTLN                        CRKO    297
C   3502 CONTINUE                                         CRKO    298
C   Y(N)=TM1-SUM1+TEN(JJ)*TLN-TACT(JJ)*TINV+BX(JJ)      CRKO    299
C   SUMY=SUMY+Y(N)                                         CRKO    300
C   351 CONTINUE                                         CRKO    301
C   XRAR=SUMX/15.000                                     CRKO    302
C   YRAR=SUMY/15.000                                     CRKO    303
C   SUMX=0.000                                              CRKO    304
C   SUM1=0.000                                              CRKO    305
C   SUMY=0.000                                              CRKO    306
C   DO 352 N=1,15                                         CRKO    307
C   SUMX=SUMX+Y(N)*(X(N)-XRAR)                           CRKO    308
C   SUM1=SUM1+(X(N)-XRAR)**2                            CRKO    309
C   SUMY=SUMY+(Y(N)-YRAR)**2                            CRKO    310
C   352 CONTINUE                                         CRKO    311
C   TEN2(JJ)=0.000                                         CRKO    312
C   TACT2(JJ)=SUMX/SUM1                                    CRKO    313
C   BX2(JJ)=(YRAR+TACT2(JJ)*XRAR)/TENLN                 CRKO    314
C   SUMX=0.000                                              CRKO    315
C   DO 353 N=1,15                                         CRKO    316
C   SUMY=SUMX+(Y(N)+TACT2(JJ)*X(N)-TENLN*BX2(JJ))**2   CRKO    317
C   353 CONTINUE                                         CRKO    318
C   SUMY=DSORT(1.000-SUMX/SUMY)                           CRKO    319
C   SUMX=DSORT(SUMX/14.000)                             CRKO    320
C   CDATA(1)=TACT2(JJ)                                    CRKO    321
C   IF (.NOT.ISI) CDATA(1)=TACT2(JJ)*1.98700*0.00100     CRKO    322
C   WRITE(*,354) BX2(JJ),TEN2(JJ),CDATA(1),SUMX,SUMY      CRKO    323
C   354

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DO NOT USE THIS
FOR SCIENTIFIC QUALITY

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354 FORMAT(6X,57H CALCULATED REVERSE RATE DATA, STD DEV AND CORR COEF CRKO 325
      1 = ,3F15.3,4K,1P2010,3) CRKO 326
C-----CONVERT RX2 FOR INTERNAL CALCULATIONS CRKO 327
      RX2(JJ)=RX2(JJ)*TFMLN CRKO 328
C CRKO 329
C-----SET REVERSE REACTION RATE VARIABLES=0 FOR GLOBAL REACTIONS CRKO 330
C-----SO THAT THESE VARIABLES ARE DEFINED FOR THE KINETIC RATE CRKO 331
C-----PRINTOUT (M,D,MQIVEN 7/22/79)
      357 IF (DT1,NE,GLCR) GO TO 395 CRKO 332
      TACT2(JJ)=C CRKO 333
      TFM2(JJ)=0 CRKO 334
      RX2(JJ)=0 CRKO 335
      355 JJ=JJ+1 CRKO 336
C-----CONVERT ALL RATE DATA TO SI UNITS CRKO 337
      TF (LS1) GO TO 310 CRKO 338
      J=JJ-1 CRKO 339
      RX(J)=BX(J)-TENLN#3.000 CRKO 340
      BX2(J)=BX2(J)-TENLN#3.000 CRKO 341
      IF (MODR(J),EQ.2) RX2(J)=RX2(J)-TENLN#3.000 CRKO 342
      IF (MODR(J),EQ.3) BX(J)=BX(J)-TENLN#3.000 CRKO 343
      IF (MODR(J),NE.1) GO TO 310 CRKO 344
      IF (ID(3,J),NE.0) BX(J)=BX(J)-TENLN#3.000 CRKO 345
      IF (ID(6,J),NE.0) BX2(J)=BX2(J)-TENLN#3.000 CRKO 346
      GO TO 310 CRKO 347
      CRKO 348
C 356 JJ=JJ-1 CRKO 349
      NGLORP=NGLOR+1 CRKO 350
C CRKO 351
C-----PRINT OUT ARRAY OF STOICHIOMETRIC COEFFICIENTS CRKO 352
C CRKO 353
      DO 372 J=1,JJ CRKO 354
      DO 370 N=1,6 CRKO 355
      K=N#2-2 CRKO 356
      L=N CRKO 357
      CDATA(K)=BLANK CRKO 358
      CDATA(K+1)=BLANK CRKO 359
      IDLJ=ID(L,J) CRKO 360
      IF (IDLJ,EQ.0) GO TO 370 CRKO 361
      CDATA(K)=ASUR(IDLJ,1) CRKO 362
      CDATA(K+1)=ASUR(IDLJ,2) CRKO 363
      370 CONTINUE CRKO 364
      IF (ID(2,J),EQ.0) CDATA(5)=THIRD CRKO 365
      IF (ID(5,J),EQ.0) CDATA(9)=THIRD CRKO 366
      IF (MODR(J),GT.1) CDATA(11)=THIRD CRKO 367
      WRITE(6,371) J,(CDATA(K),K=1,12) CRKO 368
      371 FORMAT(5X,15,1H,,5X,6A4,,H---- ,6X,6A4/) CRKO 369
      372 CONTINUE CRKO 370
      CRKO 371
C-----PRINT OUT ALL RATE DATA IN SI UNITS CRKO 372
C CRKO 373
      WRITE(6,380) CRKO 374
      380 FORMAT(//1H0,40X,29HKINETIC RATE DATA IN SI UNITS/
      41H0,6X,1HJ,2X,4HMDR,16X,2HID,19X,2HAX,10X,3HTEN,9X,4HTACT,
      413X,3HBX2,4X,4HTEN2,9X,5HTACT2/) CRKO 375
      DO 382 J=1,JJ CRKO 376
      TM1=BX(J)/TENLN CRKO 377
      TM2=BX2(J)/TENLN CRKO 378
      WRITE(6,381) J,MDR(J),(ID(I,J),I=1,6),TM1,TEN(J),TACT(J),
      1TM2,TEN2(J),TACT2(J) CRKO 379
      382 CONTINUE CRKO 380
      381 FORMAT(5X, 2,1H,,14,3K,6I4,2(3X,3F13.9)) CRKO 381
      CRKO 382
C-----SET CONTACT INDEXES TO UNITY CRKO 383
      DO 390 J=1,JJ CRKO 384
      CRKO 385
      CRKO 386
      CRKO 387
      CRKO 388

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      X1(J)=1.000          CRKO 389
      X2(J)=1.000          CRKO 390
  390 CONTINUE
C
      RETURN
C
      0000    0000    0000    0000    0000    0000    CHAPTER 4    0000  000
      0000    0000    0000    0000    0000    0000    CHAPTER 4    0000  000
C
C 0000 REACTANTS000
C  READ REACTANTS DATA CARDS FOR EACH INLET STREAM
C
      400 NSTRM=NSTR'+1
      LMOLES=.FALSE.
C-----SCRUB SPECIES MOLE NUMBER ARRAY
      DO 405 I=1,NS
      405 S2(I)=0.000
      SUM1=0.000
C
      410 READ(5,411) (AT(I),B(I),I=1,4), (CDATA(I),I=1,21),PECWHT,MOLE,PHAZ
      411 FORMAT(4(A2,FT,5),2A4,1X,F7.5,A1,9X,A1)
      IF (AT(1).EQ.RLMK) GO TO 450
      WRITE(6,412) (AT(I),B(I),I=1,4), (CDATA(I),I=1,21),PECWHT,MOLE,
      1PHAZ,NSTRM
      412 FORMAT(1X,4(2X,A2,F9.5),2X,2A4,2X,F9.5,2X,A1,2X,A1,2X,I5)
      IF (MOLE.EQ.MOL) LMOLES=.TRUE.
C
C-----ESTABLISH MOLE NUMBERS (KG-MOL / KG M MIXTURE) IN INLET STREAM
C
      TKINV=1.000/TR
      SCREEN FOR CONDENSED SPECIES
      DO 430 I=1,NS
C-----SCREEN FOR SPECIES NAME
      IF (CDATA(1).NE.ASUB(1,1)) GO TO 430
      IF (CDATA(2).NE.ASUB(1,2)) GO TO 430
      DO 422 L=1,NM
C-----SCREEN FOR ATOMIC COMPOSITION
      DO 420 K=1,4
      IF (ATOM(1,L).NE.AT(K)) GO TO 420
      IF (AL(1,L).NE.R(K)) GO TO 430
      420 CONTINUE
C-----IF PECWT IS RELATIVE MASS, CONVERT TO RELATIVE MOLE NUMBERS
      AMOLE=PECWHT/SMW(I)
      IF (.NOT.LMOLES) AMOLE=PECWHT
      S2(I)=S2(I)+AMOLE
      SUM1=SUM1+AMOLE*SMW(I)
      GO TO 410
      430 CONTINUE
C
      WRITE(6,440)
      440 FORMAT(1HC,10X,4SH REACTANT ABOVE NOT FOUND IN THERMO LIBRARY/ )
      GO TO 410
C
      450 CONTINUE
C-----ESTABLISH MIXTURE ENTHALPY
C
      IMCAS=1
      CALL HCPS
C
      WRITE(6,460) NSTRM
      460 FORMAT(1HO,10H000 REACTANT STREAM,13,4H 000/
      A1HO,5X,2HI,4X,7HSPECIES,14X,16HMOLECULAR WEIGHT,2X,
      A12HMOLE NUMBERS,8X,144MASS FRACTIONS/32X,17H(MOLE %)/KG %)

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END

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C 6X,17H(KGMOLE I)/(KG X),9X,13H(KG I)/(KG X)//
HSUM=0.000 CRKO 453
SM=0.000 CRKO 454
DO 480 I=1,NS CRKO 455
S2(I)=S2(I)/SUM1 CRKO 456
C-----S2(I) IN MOLE NUMBERS, KG-MOLES I/KG MIXTURE CRKO 457
HSUM=HSUM+HO(I)*S2(I) CRKO 458
SM=SM+S2(I) CRKO 459
DT1=S2(I)*SMW(I) CRKO 460
WRITE(6,470) I,(ASHR(I,J),J=1,3),SMW(I),S2(I),DT1 CRKO 461
470 FORMAT(9F,1H.,4X,3A4,1P3D20.3) CRKO 462
480 CONTINUE CRKO 463
C-----HSUB0 IN JOULES/KG REACTANT MIXTURE CRKO 464
HSUB0=HSUM*RGAS*TK CRKO 465
C-----RHOP IS MASS DENSITY, KG/CU M CRKO 466
RHOP=PA/(RGAS*TK*SM) CRKO 467
C CRKO 468
SMINV=1.000/SM CRKO 469
WRITE(6,490) TK,HSUB0,PA,RHOP,SMINV CRKO 470
490 FORMAT(1HC/,12X,13HTMPFRATIURE ,1PD12.3,3X,9HDEG K/
A12X,10HENHALPY ,3X,1PD12.3,3X,9HJOULES/KG/ CRKO 471
R12X,10HPRESSURE ,3X,1PD12.3,3X,6HN/M**2/ CRKO 472
C12X,9HDFNSITY ,4X,1PD12.3,3X,7HKG/M**3/ CRKO 473
D12X,19HMEN MOL WT ,1PD12.3,3X,9HKG/KGMOLE//) CRKO 474
C CRKO 475
C-----ON RETURN, CALLING PROGRAM MUST STORE MOLE NUMBERS S2(I).
C-----PRESSURE, TEMPERATURE, ENTHALPY AND DENSITY AT APPROPRIATE INLET CRKO 476
C-----INLET #10 NODE CRKO 477
C
      RETURN
END
SURROUNTE HCPS
C *** MODIFIED FOR CONDENSED SPECIES 7-79 D.T.PRATT HCPS 2
C
      DNIMALE PRECISION CPSUM,FMV,ER,FQ,HSUB0,HSUM,HO,PA,PPLN,
1  QO,O1,O2,O3,O4,RGAS,RGASIN,RHOP,SM,SMINV,SMW,SSAVE,SQ,S1,S2,TK, NOXX 392
2  TKINV,TLN,7,SMO NOXXX 30
      DOURLF PRFCISION CP1,CP2,CP3,CP4,CP5,P2,P25,P333,P5,TKCU,TKSQ,TK4 NOXXX 31
      LOGICAL LADIAF,LCONVG,LOFRUG,LEQUIL,LNRG,LREACT,LENER NOXX 372
      NOXX 393
C
      COMMON
9/CCHEMI/CPSUM,HSUM,FQ,PPLN,RGAS,RGASEN,SMINV,TKINV,TLN,LNRG HCPS 7
1/CMINDEX/IDCD,IDFU,IDO2,ION2,IDM20,IDCO2,IDH1,IDH2,IDH1,IDM1,IDN02 NOXX 394
1,IND,TOCH,THCPS,ILC,ILM,IMAT,ITER,JD,N1,N2,N3,NA,NGLOR,NGLDRP, NOXX 395
2,NLM,NO,NSM,NS1,NS2,IDCH NOXX 396
1/CPARAM/ASHR(30,3),EMV,ER,HSUB0,MDERUG,NS,PA,QO,O1,O2,O3,O4,RHOP, 4STEP 611
1,SM,SMW(30),SP0,S1(30),S2(30),TY,LADIAF,LOFRUG,LFOUTL,LREACT,LENER NOXX 397
2,EDKIJ,LCONVG NOXX 398
1/CSPECE/HG(30),SO(30),SSAVE(30),Z(420) NOXX 400
C
ooooooooooooooooooooooooooooooooooooooooooooooooooooooooooooo HCPS 15
C THIS SURROUNTE CALCULATES THE NON-DIMENSIONAL, 1-ATM VALUFS OF HCPS 16
C ENTHALPY, SPECIFIC HEAT, AND ENTROPY FOR A GIVEN VALUE OF TEMPERATURE HCPS 17
C (DEG K). THE Z ARRAY IS REFERENCED AS HAVING ONLY ONE SUBSCRIPT HCPS 18
C TO SAVE INTERNAL SUPERSCRIPT CALCULATIONS. HCPS 19
C Z(IC,IT,IS) --- Z(IC+7*(IT-1)+7*(IS-1)) FOR Z(7,2,20) HCPS 20
C WHERE IC=1,7, COEF FOR TEMP RANGE IT=1 OR 2, FOR SPECIES IS=1,NS. HCPS 21
C NOTE THAT THE FIRST 2 SUBSCRIPTS ARE REVERSED FROM THE HCPS 22
C GORDON AND MCRRIDGE PRACTICE HCPS 23
C REFERENCE GORDON AND MCRRIDGE (NASA SP-279, 1971) HCPS 24
ooooooooooooooooooooooooooooooooooooooooooooooooooooooooooooo HCPS 25
C
      DATA ICIT/14/ HCPS 26
      DATA P2,P25,P333,P5/0.200,0.2500,0.3333333D0,0.700/ HCPS 27
      DATA P25/0.2500/ HCPS 28
      DATA P333/0.3333333D0/ HCPS 29

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C
 IT=0
 IF (TK.LT.1000,000) IT=7
 C
 TKSQ=TK#2
 TKCU=TK\$00TK
 TK4=TKCU#TK
 CPSUM=0,000
 GO TO 11,21,31,41,11,1HCPS
 C
 C-----1HCPS=1 --- JUST CPSUM AND HO(I) REQUIRED
 C
 11 DO 10 I=NS1,NS2
 K=IT+ICIT*(I-1)
 CP1=7(K+1)
 CP2=TK#2(K+2)
 CP3=TKSQ#2(K+3)
 CP4=TKCU#2(K+4)
 CP5=TK4#2(K+5)
 CPSUM=CPSUM+(CP1+CP2+CP3+CP4+CP5)*S2(I)
 HO(I)=P2*CP5+P25*CP4+P333*CP3+P5
 X *CP2+CP1+TKINV#2(K+6)
 10 CONTINUE
 RETURN
 C
 C-----1HCPS=2 --- CPSUM, HO(I) AND SO(I) REQUIRED
 C
 21 DO 30 I=NS1,NS2
 K=IT+ICIT*(I-1)
 CP1=7(K+1)
 CP2=TK#2(K+2)
 CP3=TKSQ#2(K+3)
 CP4=TKCU#2(K+4)
 CP5=TK4#2(K+5)
 CPSUM=CPSUM+(CP1+CP2+CP3+CP4+CP5)*S2(I)
 HO(I)=P2*CP5+P25*CP4+P333*CP3+P5
 X *CP2+CP1+TKINV#2(K+6)
 SO(I)=P25*CP5+P333*CP4+P5*CP3
 X *CP2+TLN#CP1#7(K+7)
 30 CONTINUE
 RETURN
 C-----1HCPS=3 --- HSUM REQUIRED
 31 HSUM=0,000
 DO 40 I=NS1,NS2
 K=IT+ICIT*(I-1)
 CP1=7(K+1)
 CP2=TK#2(K+2)
 CP3=TKSQ#2(K+3)
 CP4=TKCU#2(K+4)
 CP5=TK4#2(K+5)
 HO(I)=P2*CP5+P25*CP4+P333*CP3+P5*CP2+CP1+TKINV#2(K+6)
 HSUM=HSUM+HO(I)*S2(I)
 40 CONTINUE
 RETURN
 C-----1HCPS=4 --- HSUM AND CPSUM REQUIRED
 41 HSUM=0,000
 DO 50 I=NS1,NS2
 K=IT+ICIT*(I-1)
 CP1=7(K+1)
 CP2=TK#2(K+2)
 CP3=TKSQ#2(K+3)
 CP4=TKCU#2(K+4)
 CP5=TK4#2(K+5)
 CPSUM=CPSUM+(CP1+CP2+CP3+CP4+CP5)*S2(I)

```
H0(I)=P2*CP5+P25*CP4+P333*CP3+P5*CP2+CP1+TKINV02(K+6)  
HSUM=HSUM+H0(I)*S2(I)  
50 CONTINUE  
RETURN  
END
```

NOXX	427
NOXX	428
NOXX	429
NOXX	430
MCPS	72

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APPENDIX E
LIST OF DEPENDENT VARIABLES
AND SOURCE TERMS

APPENDIX E

LIST OF DEPENDENT VARIABLES AND SOURCE TERMS

TABLE E-1

Dependent Variable	Source Term
u (axial velocity)	$\frac{\partial}{\partial x} (\mu_{eff} \frac{\partial u}{\partial x}) + \frac{1}{r} \frac{\partial}{\partial r} (\mu_{eff} r \frac{\partial v}{\partial x}) + \frac{1}{r} \frac{\partial}{\partial \theta}$ $(\mu_{eff} \frac{\partial w}{\partial x}) + s_u^u_{spray} - \frac{\partial p}{\partial x}$
v (radial velocity)	$\frac{\partial}{\partial x} (\mu_{eff} \frac{\partial u}{\partial r}) + \frac{1}{r} \frac{\partial}{\partial r} (\mu_{eff} r \frac{\partial v}{\partial r}) + \frac{1}{r} \frac{\partial}{\partial \theta}$ $[\mu_{eff} (\frac{\partial w}{\partial r} - \frac{w}{r})] - 2 \frac{\mu_{eff}}{r} (\frac{1}{r} \frac{\partial w}{\partial \theta} + \frac{v}{r}) + \frac{\rho w^2}{r}$ $+ s_v^v_{spray} - \frac{\partial p}{\partial r}$
w (tangential velocity)	$\frac{\partial}{\partial x} (\frac{\mu_{eff}}{r} \frac{\partial u}{\partial \theta}) + \frac{1}{r} \frac{\partial}{\partial r} [\mu_{eff} r (\frac{1}{r} \frac{\partial v}{\partial \theta} - \frac{w}{r})]$ $+ \frac{1}{r} \frac{\partial}{\partial \theta} [\frac{\mu_{eff}}{r} (\frac{\partial w}{\partial \theta} + 2v)] - \frac{\rho v w}{r} + \frac{\mu_{eff}}{r} (\frac{\partial w}{\partial r} +$ $\frac{\partial v}{\partial \theta} - \frac{w}{r}) + s_w^w_{spray} - \frac{1}{r} \frac{\partial p}{\partial \theta}$
k (Turbulent kinetic energy)	$G_k \sim \rho \epsilon$ $(C_1 G_k - C_2 \rho \epsilon) \frac{1}{k}$
ϵ (Dissipation rate)	

TABLE E-1 (Contd)

Dependent Variable	Source Term
ϕ (Mixture fraction)	m_{evap}
m_{fu} (Unburnt fuel mass fraction)	As per four-step mechanism, (Chapter VI) and modified by the eddy-break-up model as in Ref. 1, Page 23.
m_{CH} (Intermediate hydrocarbon mass fraction)	m_{evap} added on to m_{fu} source.
m_{CO} (CO mass fraction)	
m_{H_2} (H ₂ mass fraction)	
Soot nuclei and particle concentrations	As given in Chapter III, equations (28) and (29).
\tilde{h} (Stagnation enthalpy)	$2a [(R^x - E) + (R^r - E) + (R^z - E)]$ + $m_{evap} H_{fuel}$

In the above table, the symbols have the meanings:

x, r, θ = axial, radial, tangential directions;

μ_{eff} = effective viscosity;

p = pressure;

ρ = density;

$$G_k = \mu_{\text{eff}} [2 \{ (\frac{\partial u}{\partial x})^2 + (\frac{\partial v}{\partial r})^2 + (\frac{\partial w}{\partial \theta} + \frac{v}{r})^2 \} \\ + (\frac{\partial w}{\partial x} + \frac{u}{r \partial \theta})^2 + (\frac{\partial u}{\partial r} + \frac{\partial v}{\partial x})^2 + (\frac{\partial w}{\partial r} + \frac{\partial v}{r \partial \theta} - \frac{w}{r})^2];$$

c_1, c_2 = Turbulence model constants;

$s_{\text{spray}}^u, s_{\text{spray}}^v, s_{\text{spray}}^w \}$ = Momentum transfer from spray to the gas phase $u, v,$ and w - momentum equations;

\dot{m}_{evap} = rate of spray evaporation per unit volume;

a = Absorption coefficient defined as radiation absorbed per unit length;

E = Blackbody emissive power;

R^x, R^r, R^z = Composite radiation fluxes (See equations 37, 38, and 39);

H_{fuel} = Heat of formation of fuel.

**APPENDIX F
INPUT DATA FOR JT8D-17 COMBUSTOR TEST CASE**

APPENDIX F

INPUT DATA FOR JT8D-17 COMBUSTOR TEST CASE

In this Appendix, a listing of the input data used for the JT8D-17 Combustor computations is provided. The data shown is for the takeoff case using the four-step hydrocarbon oxidation mechanism. The specificaiton of the x , r , and θ grids is contained in lines 630-670. Other inputs may be easily interpreted with reference to the input description provided in Appendix B.

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	OPERATING POINT OF POOR QUALITY							
U-VELOCITY								10
V-VELOCITY								20
W-VELOCITY								30
PRESSURE								40
TURBULENT KIN. ENERGY								50
TURBULENCE LENGTH SCALE								60
PHI (INITIAL FUEL)								70
FUEL MASS FRACTION								80
TEMPERATURE								90
SPECIFIC ENTHALPY								100
AVG. RAD.								110
RX								120
RY								130
RZ								140
CC								150
H2O								160
C2								170
CO2								180
N2								190
RHO								200
FFF. VISCOSITY								210
EVAPORATION RATE								220
NUCLEI CONCENTRATION								230
SOOT CONCENTRATION - SIZE 1								240
SOOT CONCENTRATION - SIZE 2								250
H								260
K								270
NO								280
NO2								290
O								300
CH								310
CKH7-2								320
H2								330
JT8D-LGARSE GRID-TAKEOFF-JETA-4 STEP								340
10	10	0.5	0.2	0.2	0.2	0.2	0.3	350
0.1	0.2	0.1	0.0	0.0				360
0.1	0.1	0.1	0.1	0.1	0.1	0.1	0.1	370
0.1	0.0	0.1	0.1	0.1	0.1	0.1	0.1	380
								390
0.1	0.1	0.1	0.3	0.1	0.1	0.1	0.1	410
0.1	0.1	0.1	0.1	0.1	0.1	0.1	0.1	420
0.1	0.1	0.1	0.1	0.1	0.1	0.1	0.1	430
0.1	0.1	0.1	0.1	0.1	0.1	0.1	0.1	440
0.1	0.1	0.1	0.0	0.0	0.0	0.1	0.1	450
0.1	0.0	0.0	0.0	0.0	0.0	0.1	0.0	460
0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	470
0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.1	480
0.1								490
0.2	0.2	0.2	1.0	0.5	0.5	0.5	0.5	500
0.5	0.2	0.2	0.5	0.5	0.5	0.2	0.5	510
0.5	0.2	0.5	0.5	0.5	0.5	0.5	0.5	520
0.5	0.2	0.5	0.5	0.5	1.0	1.0	1.0	530
0.2	0.3	0.3						540
1.0	1.0	1.0	1.0	0.7	0.7	0.7	0.7	550
0.7	0.7	0.7	0.7	0.7	0.7	0.7	0.7	560
0.7	0.7	0.7	0.7	0.7	0.7	0.7	0.7	570
0.7	0.7	0.7	0.7	0.7	1.0	1.0	1.0	580
1.0	1.0	1.0	1.0	0.9	0.9	0.9	0.9	590
0.9	0.9	0.9	0.9	0.9	0.9	0.9	0.9	600
0.9	0.9	0.9	0.9	0.9	0.9	0.9	0.9	610
0.9	0.9	0.9	0.9	0.9	1.0	1.0	1.0	620
0.0	0.250	0.007	0.012	0.017	0.022	0.021	0.016	630
0.0	0.0181							640
0.0								

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0.0	0.005	0.015	0.025	0.035	0.045	0.057	0.07	650
0.001	0.0064							660
0.0	0.1496	0.4484	0.7480	0.8376				670
02	10	64	10					680
1.7650E+16	1.0	0.1	0.01	0.003	0.002			690
10.	19.00	-49317.	.001					700
2.0893E+17	76000.	1.0	5.0117E+19	25000.	3.0			710
3.9811E+17	20000.	3.0	3.3113E+18	20500.	3.0			720
0.5	1.07	0.5	0.3	1.18	-0.37			730
1.0	1.15	0.5	0.85	1.42	-0.50			740
1.42	1.92	0.07	1.7100E-05	0.00001	713.0	713.0	713.0	750
075	100	04	04	00	02			760
46.418	0.3	1.10	0.081	0.0	713.0			770
01	02	300.0						780
.0001	0.0001	0.6488	1.570795	-1.570795	0.0	5.8343E	0.6488	790
5.00	0.01916	46.0	40.00	0.0				800
03	07							810
10	10							820
03	63							830
-80.6	-80.0							840
95.	95.							850
0.0001	0.0001							860
0.2626	0.7114							870
713.6	713.6							880
01	30	02						890
0.05	1.1000E+31	40000.	1.0000E+038	0.0000E-16	100.0	1.0000E-15	2000.0	900
1.5626E+13	16000.0	-1.94	1.81	-0.5	4.5000E+070.1	400.0		910
0.025	1.0							920
96.0	100.0							930
3C	0.301							940
01	49	02	0.0005	500.0				950
ELEMENTS								960
C	12.01115	+0.600000						970
H	1.007470	1.000000						980
N	14.006700	0.0						990
O	15.999400	-2.000000						1000
								1010
								1020
THERMO								
C10H14	J 3/01C	10.0 19.00	0.00 0.6	300.000	5000.000			1030
	L.26845936E+02	0.46476050E-01	-0.22957813E-04	0.48494616E-06	-0.37080214E-12			1040
	-L.24819829E+05	0.10767143E+02	0.57799475E+01	0.50561468E-01	0.51144225E-04			1050
	-L.94968140E-07	0.39004875E-10	-0.24819829E+05	0.86690068E+01				1060
	02	J 9/05D	2.0 0.0 0.0 0.6	300.000	5000.000			1070
	C.36219521E	J 1 0.73018256E-03	-0.19652219E-05	0.36201556E-10	-0.26945023E-14			1080
	-0.12014922E	04	0.36150492E	01	0.36255980E	01-0.18782103E-02	0.76254943E-05	1090
	-L.67635537E-08	0.21555477E-11	-0.10475225E	04	0.43052764E	01		1100
	N2	J 9/05N	2.0 0.0 0.0 0.6	300.000	5000.000			1110
	C.28943144E	J 1 0.15154863E-02	-0.57235275E-06	0.99807385E-10	-0.65223530E-14			1120
	-C.90586182E	03	0.01015143E	01	0.36748257E	01-0.12081496E-02	0.23240100E-05	1130
	-L.63217570E-04	-0.22577253E-12	-0.10011587E	04	0.23580418E	01		1140
	CL	J 9/05C	1.0 1.00 0.00 0.6	300.000	5000.000			1150
	C.29840099E	J 1 0.14941387E-02	-0.573998678E-06	0.10364576E-04	-0.69353494E-14			1160
	-L.14245227E	05	0.63479147E	01	0.37100914E	01-0.16190964E-02	0.30423584E-05	1170
	-C.20314073E-08	0.23453346E-12	-0.14355309E	05	0.24555334E	01		1180
	C2H4	J 3/01C	2.01 4.000 0.00 0.6	300.000	5000.000			1190
	C.23312489E+04	1.32141704E-02	-0.11224078E-04	0.83920416E-16	-0.3043019E-14			1200
	5.10531973E+03	9.38961110E+00	2.41624020E+00	1.27921279E-04	-2.46080270E-06			1210
	2.13882527E-06	-1.44524497E-12	5.05491829E+03	0.02623346E+00				1220
	02	J 3/01H	2.0 0.0 0.0 0.6	300.000	5000.000			1230
	C.310015d4	J 1 0.51114453E-01	0.52044204E-07	-0.354909964E-16	0.36465341E-14			1240
	-C.97726413E	03	-L.195154412E	01	C.30574444E	01-0.26765148E-02	-0.580499144E-05	1250
	C.55210443E-08	-0.18122776E-11	-0.98390430E	03	-0.22997046E	01		1260
	020	J 3/01C	2.0 1.00 0.00 0.6	300.000	5000.000			1270
	C.27117616E	J 1 0.24451370E-02	-0.80224368E-06	0.10226641E-16	-0.46672134E-14			1280

-0.269001770 05 0.663056666 01 0.407012750 01-0.410844998-02 0.41221x001-05
 -0.276374141-06 0.367621031-17-0.30797191 05-0.322700101 06
 C12 3.97650 1.0 2.00 0.00 0.0 300.000 500.00000
 0.446080401 01 0.331817171-02-0.123075661-05 0.22741323-06-0.155277581-13
 -0.489614301 05-0.4966354781 00 0.2400777841 01 0.873569038-02-0.600700611-05
 0.200214601-06 0.631740321-15-0.483775201 05 0.969514471 0.
 H 3.97650 1.00 2.00 0.00 0.0 300.000 500.00000
 0.250000000 01 0.0 0.0 0.0 0.0 0.0 0.0
 0.254716270 05-0.460117591 00 0.250000001 01 0.0 0.0 0.0
 C10 0.0 0.0 0.0 0.0 0.0 0.0 0.0
 N 3.3761N 1.00 2.00 0.00 0.0 300.000 500.00000
 C.255026781 01 0.106614501-04-C.746533151-07 0.167455201-10-0.167558371-14
 0.561160351 05 0.464175721 01 0.29030699F 01-0.210001811-06 0.952052841-07
 -0.564755621-10 0.209990381-13 0.560098898F 05 0.416757491 01
 NP 3.6764N 1.0 2.00 0.00 0.0 300.000 500.00000
 C.318897721 01 0.133822771-02-C.521993161-05 0.959173161-11-0.640579201-16
 0.482032421 04 0.674581151 01 0.604695091 01-0.341617531-02 0.790191761-05
 -0.611392561-03 0.159190721-11 0.974538A7F 04 0.299764761 01
 NL2 3.9765N 1.0 2.00 0.00 0.0 300.000 500.00000
 0.462407591 01 0.252601301-07-0.10609483F-05 0.198772391-09-0.137794461-13
 C.228977601 04 0.133261371 01 0.34389224F 01 0.206470031-07 0.666666601-05
 -0.955566661-06 0.361969731-11 0.781522610 06 0.831104801 01
 H 3.6762D 1.00 2.00 0.00 0.0 300.000 500.00000
 0.254702601 01-0.275000031-04-0.31028029F-08 0.45510670F-14-0.438346441-15
 C.292306012 05 0.49203072E 01 0.29464283F 01-0.163816661-02 0.242113303F-05
 -0.16026932L-08 0.309069641-12 0.29147641F 05 0.296399311 01
 at 3.3766D 1.0 2.00 0.00 0.0 300.000 500.00000
 C.29100417. 01 0.959316271-03-0.19441700F-05 0.137506461-10 0.142245421-12
 0.393518111 04 0.346134201 01 0.33375931F 01-0.107730591-02 0.908303241-05
 C.18713471L-09-0.229713891-12 0.36412420F 04 0.493700091 00

MECHANISM

	C10H19	C2H4	H2					
C2H4	12	C3	H2				51.04	-51.0
CO	1e	C32					10.30	
O2	02	C2D					0.108	124.0
O	0	H2		12.3	-1.0 0 0.0	0.0		165.0
O	0	D2		11.0	-1.0 0 0.0	0.0		138.0
O	0F	H2D		13.05	-1.0 0 0.0	0.0		167.0
O	1e	D1	0	11.30	0.0 0 0.0	0.0		164.0
O	02	D1	0	10.24	0.0 0 0.0	0.0		164.0
H	H2D	D1	H2	10.92	0.0 0 0.0	0.0		170.0
O	02D	D1	DH	10.70	0.0 0 0.0	0.0		171.0
N2	0	ND	N	9.0	0.0 0 0.0	0.0		172.0
N	12	ND	0	2.0000	1.0 0 0.0	0.0		173.0
N	11	ND	0	4.0000	0.0 0 0.0	0.0		174.0
N2	1C	R	ND2	11.531	-1.0 0 0.0	0.0		175.0
NE	ND	R	ND2	7.00	0.0 0 0.0	0.0		176.0
NI	12	ND2	0	8.0	0.0 0 0.0	0.0		177.0
H	9.02	ND	01t	10.477	0.0 0 0.0	0.0		178.0
								179.0

DRUGMA 7.0
OF POOR QUALITY

APPENDIX G
DIMENSIONS OF VARIABLE ARRAYS

APPENDIX G

DIMENSIONS OF VARIABLE ARRAYS

The program listing shown in Appendix D is for a 10 x 10 x 5 (axial x radial x tangential) grid. In order to change the number of nodes to any NX, NY, NZ, the dimensions of various variable arrays have to be changed as indicated on the following page. Some of the variables are dimensioned as (NX, NY, NZ) in some subroutines and as (NXYZ) in others. Both forms are indicated below. In addition, in BLOCK DATA, NI, NJ, and NK have to be set to NX, NY, and NZ, respectively.

$$\begin{aligned} \text{NXYZ} &= \text{NX} * \text{NY} * \text{NZ} \\ \text{NXY} &= \text{NX} * \text{NY} \end{aligned}$$

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Variable	Dimensions
F	(NXYZ, 7) or (7* NXYZ)
DU, DV, DW, ANUC, SOOT1, SOOT2, FCH, FH2, RHO, VIS, ABSR, SCTR, DRHODP, U, V, W, PP, P, TEMP, GAM	(NX, NY, NZ) or (NXYZ)
FS	(NXYZ, 14)
GENR, SUFU, SPFU	(NXYZ)
SU, SP, AXP, AXM, AYP, AYM, AZP, AZM, CZ, CZU, CZP, DIVG	(NX, NY) or (NXY)
AXMK, AXPK, AYMK, AYPK, AZMK, AZPK, SUK, SPK, EVAP, EVAPU, EVAPV, EVAPW, EDK, EDK 2	(NX-2) * (NY-2) * (NZ-2)
EVSU	(NX-2) * (NY-2)
CY, CYU, CYP, X, XS, XSU, XDIF, FXP, FXM, FLO, TEMTM, H, FUEL, FUOX, UIN, TIN, FUELS	GE . (NX)
R, RM, RMV, YSR, YSVR, Y, YS, YSV YDIF, FYP, FYM, JM	GE . (NY)
Z, ZS, ZSW, ZDIF, FZP, FZM, KM	GE . (NZ)
IWLI, IWLO	GE . (NY, 5)
JWLO, JWLI	GE . (NX, 5)
JKIN	GE . (NY, NZ)
IKIN	GE . (NX, NZ)